#### Smith, Claudia

From: Brad Rogers <bradr@samson.com>
Sent: Thursday, January 08, 2015 9:10 AM

**To:** Smith, Claudia

Subject: RE: Spring Creek Compressor Station SMNSR Permit Questions

Follow Up Flag: Follow up Flag Status: Flagged

#### Hi Claudia,

I have reviewed this with our operations and we have no intentions at this time or near future of setting the 10<sup>th</sup> engine. Let's proceed with permitting of 9 engines.

#### Thanks,

Brad M. Rogers Sr. Environmental Specialist Samson Resources 370 17th Street, Suite 3000 Denver, CO 80202 (o) 720.239.4406 (c) 303.229.1228 bradr@samson.com



**From:** Smith, Claudia [mailto:Smith.Claudia@epa.gov]

Sent: Thursday, December 11, 2014 4:07 PM

To: Brad Rogers

Subject: RE: Spring Creek Compressor Station SMNSR Permit Questions

#### Thanks for the quick reply.

Do you still want the permit to cover a tenth engine, as contemplated in the Consent Agreement and the application? If so, we probably need to include some kind of qualitative air quality impact assessment in the least before proposing to approve what would technically be an emissions increase for an additional engine. Alternatively, we can permit the 9 engines now, and you could apply for a new permit for a minor modification at the time plans are made to install it, if at all. However, if you plan to terminate the Consent Agreement upon issuance of the SMNSR permit, the new permit would be required prior to installing the engine. Another thing to consider if we did end up permitting the tenth engine, you would need to commence construction within 18 months of permit issuance; otherwise the permit conditions for that engine would become invalid and a new permit would be required anyway.

I'm happy to set up a call if you'd like to discuss.

Thanks,

#### Claudia

From: Brad Rogers [mailto:bradr@samson.com]
Sent: Thursday, December 11, 2014 3:42 PM

To: Smith, Claudia

Subject: RE: Spring Creek Compressor Station SMNSR Permit Questions

Hi Claudia,

No the 10<sup>th</sup> engine has not been installed and currently there are no plans to do so at this time.

#### Thanks,

Brad M. Rogers Sr. Environmental Specialist Samson Resources 370 17th Street, Suite 3000 Denver, CO 80202 (o) 720.239.4406 (c) 303.229.1228 bradr@samson.com



From: Smith, Claudia [mailto:Smith.Claudia@epa.gov]

Sent: Thursday, December 11, 2014 3:39 PM

To: Brad Rogers

Subject: Spring Creek Compressor Station SMNSR Permit Questions

Importance: High

Hi, Brad,

We are getting close to putting the Proposed SMNSR permit for the Spring Creek Compressor Station out to public comment and I wanted to check first to see if the tenth engine has been installed/started up yet, so I can update language in the permit and technical support document if it has.

Thanks for your assistance,

Claudia

Claudia Young Smith Environmental Scientist US EPA Region 8 Air Program Phone: (303) 312-6520 Fax: (303) 312-6064

http://www2.epa.gov/region8/air-permitting

\*

US EPA Region 8 1595 Wynkoop Street Mail Code 8P-AR Denver, Colorado 80202

This transmission may contain deliberative, attorney-client, attorney work product or otherwise privileged material. Do not release under FOIA without appropriate review. If this message has been received by you in error, you are instructed to delete this message from your machine and all storage media whether electronic or hard copy.

#### **MEMO TO FILE**

DATE: September 8, 2014

SUBJECT: Southern Ute Indian Reservation Natural Gas Production Facilities

**Environmental Justice** 

FROM: Victoria Parker-Christensen, EPA Region 8 Air Program

TO: Source Files:

205c AirTribal SU Samson Spring Creek Compressor Station

SMNSR-SU-000053-2013.001

FRED # 105462

On February 11, 1994, the President issued Executive Order 12898, entitled "Federal Actions to Address Environmental Justice in Minority Populations and Low-Income Populations." The Executive Order calls on each federal agency to make environmental justice a part of its mission by "identifying and addressing, as appropriate, disproportionately high and adverse human health or environmental effects of its programs, policies and activities on minority populations and low-income populations."

EPA defines "Environmental Justice" to include meaningful involvement of all people regardless of race, color, national origin, or income with respect to the development, implementation, and enforcement of environmental laws, regulations, and polices.

On June 10, 2011, the EPA promulgated a final Clean Air Act (CAA) Federal Implementation Plan (FIP) that implements New Source Review (NSR) preconstruction air pollution control requirements in Indian country. The FIP includes two NSR rules for the protection of air quality in Indian country. One of those rules, known as the minor NSR Rule, applies to new industrial facilities or modifications at existing industrial facilities with the potential to emit (PTE) certain pollutants equal to or more than the minor NSR thresholds but less than the major NSR thresholds, generally 100 to 250 tons per year. The EPA permit issuance process includes public notice of a draft permit, opportunity for public comment, as well as administrative and judicial review provisions.

This memorandum describes EPA's efforts to identify environmental justice communities and assess potential effects in connection with issuing a CAA synthetic minor NSR permit in La Plata County within the exterior boundaries of the Southern Ute Indian Reservation.

#### **Permit Request**

On December 24, 2013, the EPA received an application from Samson Resources Company (Samson) requesting a synthetic minor permit for the Spring Creek Compressor Station in accordance the requirements of the MNSR Permit Program. This permit action applies to an existing facility operating on the Southern Ute Indian Reservation in Colorado. The Spring Creek Compressor Station is located at:

#### S23, T33N, R7W Latitude 37.09241, Longitude -107.57601.

Spring Creek Compressor Station currently operates nine (9) natural gas-fired reciprocating internal combustion engines used for natural gas compression, with future planned expansion to 10 engines. The engines are operating under enforceable nitrogen oxide (NO<sub>X</sub>) emission limits required by a May 1, 2014 Consent Agreement Final Order (CAFO) #CAA-08-2013-0015 between Samson and the EPA. These emission limits provide enforceable recognition of the air fuel ratio control (AFRC) systems installed on each of the engines reducing the emission of NO<sub>X</sub> pollutants to synthetically minor levels.

This MNSR permit action does not authorize the construction of any new emission sources, or emission increases from existing units, nor does it otherwise authorize any other physical modifications to the facility or its operations. This permit is intended only to incorporate required and requested emission limits and provisions from the CAFO. Additionally, the CAFO requires testing, monitoring, recordkeeping, and reporting requirements to verify compliance with the emission limitations. The emissions, approved at present, from the existing facility will not increase due to the associated permit action and the emissions will continue to be well controlled at all times. This is an administrative action with no physical changes to the existing facility or surrounding area.

This permit reflects the incorporation of the requirements established in the CAFO. Samson requested these requirements in order to maintain the Spring Creek Compressor Station's status as a synthetic minor source of  $NO_X$  emissions with respect to the Prevention of Significant Deterioration (PSD) Permit Program at 40 CFR Part 52. Section 49.153(a)(3)(iv) of the MNSR rule provides the EPA with the authority to transfer such limits to a MNSR permit. The MNSR regulations at \$\$49.158(c)(2)(ii) and (iii) also provide the EPA with the discretion to require any additional requirements, including control technology requirements, based on the specific circumstances of the source.

#### **Environmental Impacts to Potential Environmental Justice Communities**

#### **Air Emissions**

This proposed permit action does not authorize the construction of any new emission sources, or emission increases from existing units, nor does it otherwise authorize any other physical modifications to the facility or its operations. This permit is intended only to incorporate required and requested emission limits and provisions from the CAFO. The emissions, approved at present, from the existing facility will not increase due to the associated permit action and the emissions will continue to be well controlled at all times. This is an administrative action with no physical changes to the existing facility or surrounding area.

#### **Air Quality Review**

The Federal Minor New Source Review Regulations at 40 CFR 49.154(d) require that an Air Quality Impact Assessment (AQIA) modeling analysis be performed if there is reason to be concerned that new construction would cause or contribute to a National Ambient Air Quality Standard (NAAQS) or PSD increment violation. If an AQIA reveals that the proposed construction could cause or contribute to a

NAAQS or PSD increment violation, such impacts must be addressed before a pre-construction permit can be issued.

The emissions, approved at present, from the existing facility will not be increasing due to this permit action and the emissions will continue to be well controlled at all times. This permit action will have no air quality impacts; therefore, the EPA has determined that an AQIA modeling analysis is not required for the proposed permit.

Furthermore, the permit contains a provision stating, "The permitted source shall not cause or contribute to a National Ambient Air Quality Standard violation or a PSD increment violation." Noncompliance with this permit provision is a violation of the permit and is grounds for enforcement action and for permit termination or revocation. As a result, the EPA concludes that issuance of the aforementioned synthetic minor NSR permit will not have disproportionately high and adverse human health effects on communities in the vicinity of the SUIR.

#### **Tribal Consultation and Public Participation**

The EPA offers the Tribal Government Leaders an opportunity to consult on each proposed permit action. The Tribal Government Leaders are asked to respond to the EPA's offer to consult within 30 days and if no response is received within that time, the EPA notifies the Tribal Government Leaders that the consultation period has closed. The Chairman of the Southern Ute Tribe has been offered an opportunity to consult on this permit action via letter dated February 28, 2014. To date, the EPA has not received a response to our offer to consult on this permit action and the Chairman was notified when the consultation period closed.

All minor source applications (synthetic minor, modification to an existing facility, new true minor or general permit) are submitted to both the EPA and the Tribal Environmental Director per the application instructions (see <a href="http://epa.gov/region8/air/permitting/tmnsr.html">http://epa.gov/region8/air/permitting/tmnsr.html</a>). The Tribal Environmental Office has 10 business days to respond to the EPA with questions and comments on the application. In the event an Air Quality Impact Assessment (AQIA) is triggered, a copy of that document is emailed to the tribe within 5 business days of receipt by the EPA.

Given the presence of potential environmental justice communities in the vicinity of the facilities, the EPA is providing an enhanced public participation process for this permit. Interested parties can subscribe to an EPA listserve that notifies them of public comment opportunities on the Southern Ute Indian Reservation for draft air pollution control permits via email at <a href="http://epa.gov/region8/air/permitting/pubcomment.html">http://epa.gov/region8/air/permitting/pubcomment.html</a>.

Additionally, the Tribe's Environmental Director is notified of the public comment period for the proposed permit and provided copies of the notice of public comment opportunity to post in various locations on the Reservation that they deem fit. The Tribe is also notified of the issuance of the final permit.

#### **MEMO TO FILE**

DATE: September 8, 2014

SUBJECT: Southern Ute Indian Reservation Natural Gas Production Facilities

**Endangered Species Act** 

FROM: Victoria Parker-Christensen, EPA Region 8 Air Program

TO: Source Files:

205c AirTribal SU Samson Spring Creek Compressor Stations

SMNSR-SU-000053-2013.001

FRED #105462

Pursuant to Section 7 of the Endangered Species Act (ESA), 16 U.S.C. §1536, and its implementing regulations at 50 CFR, part 402, the EPA is required to ensure that any action authorized, funded, or carried out by the Agency is not likely to jeopardize the continued existence of any Federally-listed endangered or threatened species or result in the destruction or adverse modification of such species' designated critical habitat. Under ESA, those agencies that authorize, fund, or carry out the federal action are commonly known as "action agencies." If an action agency determines that its federal action "may affect" listed species or critical habitat, it must consult with the U.S. Fish and Wildlife Service (FWS). If an action agency determines that the federal action will have no effect on listed species or critical habitat, the agency will make a "no effect" determination. In that case, the action agency does not initiate consultation with the FWS and its obligations under Section 7 are complete.

In complying with its duty under ESA, the EPA, as the action agency, examined the potential effects on listed species and designated critical habitat relating to issuing this Clean Air Act (CAA) synthetic minor New Source Review (NSR) permit.

#### **Region 8 Air Program Determination**

The EPA has concluded that the proposed synthetic minor NSR permit action will have "*No effect*" on listed species or critical habitat. These proposed permit action does not authorize the construction of any new emission sources, or emission increases from existing units, nor does it otherwise authorize any other physical modifications to the associated facility or its operations. This is an administrative action with no physical changes to the existing facility or surrounding area. Because the EPA has determined that the federal action will have no effect, the agency made a "*No effect*" determination, did not initiate consultation with the FWS and its obligations under Section 7 are complete.

#### **Permit Request**

On December 24, 2013, the EPA received an application from Samson Resources Company (Samson) requesting a synthetic minor permit for the Spring Creek Compressor Station in accordance the requirements of the MNSR Permit Program. This permit action applies to an existing facility operating on the Southern Ute Indian Reservation in Colorado. The Spring Creek Compressor Station is located at:

S23, T33N, R7W Latitude 37.09241, Longitude -107.57601. Spring Creek Compressor Station currently operates nine (9) natural gas-fired reciprocating internal combustion engines used for natural gas compression, with future planned expansion to 10 engines. The engines are operating under enforceable nitrogen oxide (NO<sub>X</sub>) emission limits required by a May 1, 2014 Consent Agreement Final Order (CAFO) #CAA-08-2013-0015 between Samson and the EPA. These emission limits provide enforceable recognition of the air fuel ratio control (AFRC) systems installed on each of the engines reducing the emission of NO<sub>X</sub> pollutants to synthetically minor levels.

This MNSR permit action does not authorize the construction of any new emission sources, or emission increases from existing units, nor does it otherwise authorize any other physical modifications to the facility or its operations. This permit is intended only to incorporate required and requested emission limits and provisions from the CAFO. Additionally, the CAFO requires testing, monitoring, recordkeeping, and reporting requirements to verify compliance with the emission limitations. The emissions, approved at present, from the existing facility will not increase due to the associated permit action and the emissions will continue to be well controlled at all times. This is an administrative action with no physical changes to the existing facility or surrounding area.

This permit reflects the incorporation of the requirements established in the CAFO. Samson requested these requirements in order to maintain the Spring Creek Compressor Station's status as a synthetic minor source of  $NO_X$  emissions with respect to the Prevention of Significant Deterioration (PSD) Permit Program at 40 CFR Part 52. Section 49.153(a)(3)(iv) of the MNSR rule provides the EPA with the authority to transfer such limits to a MNSR permit. The MNSR regulations at \$49.158(c)(2)(ii) and (iii) also provide the EPA with the discretion to require any additional requirements, including control technology requirements, based on the specific circumstances of the source.

#### **Threatened and Endangered Species**

The U.S. Fish and Wildlife Service (FWS) maintains an internet resource, *Environmental Conservation Online System* (ECOS, <a href="http://ecos.fws.gov/ecos/indexPublic.do">http://ecos.fws.gov/ecos/indexPublic.do</a>), that provides access to databases for threatened and endangered species that may be present within the proposed project area and designated critical habitat. A search of the databases was not undertaken because this is an administrative action with no physical changes to the existing facility or surrounding area.

#### **Conclusion**

The EPA has concluded that the proposed synthetic minor NSR permit action will have "No effect" on listed species or critical habitat. This proposed permit action does not authorize the construction of any new emission sources, or emission increases from existing units, nor does it otherwise authorize any other physical modifications to the associated facility or its operations. The emissions, approved at present, from the existing facility will not increase due to the associated permit action and the emissions will continue to be well controlled at all times. This is an administrative action with no physical changes to the existing facility or surrounding area. Because the EPA has determined that the federal action will have no effect, the agency will make a "No effect" determination. In that case, the EPA does not initiate consultation with the FWS and its obligations under Section 7 are complete.

#### **MEMO TO FILE**

DATE: September 8, 2014

SUBJECT: Southern Ute Indian Reservation Natural Gas Production Facilities

National Historic Preservation Act

FROM: Victoria Parker-Christensen, EPA Region 8 Air Program

TO: Source Files:

205c AirTribal SU Samson Spring Creek Compressor Station

SMNSR-SU-000053-2013.001

FRED #105462

Section 106 of the National Historic Preservation Act (NHPA) requires federal agencies to take into account the effects of their undertakings on historic properties and afford the Advisory Council on Historic Preservation (ACHP) a reasonable opportunity to comment with regard to such undertakings. Under the ACHP's implementing regulations at 36 C.F.R. Part 800, Section 106 consultation is generally with state and tribal historic preservation officials in the first instance, with opportunities for the ACHP to become directly involved in certain cases. An "undertaking" is "a project, activity, or program funded in whole or in part under the direct or indirect jurisdiction of a Federal agency, including those carried out by or on behalf of a Federal agency; those carried out with Federal financial assistance; and those requiring a Federal permit, license or approval." 36 C.F.R. § 800.16(y).

Under the NHPA Section 106 implementing regulations, federal agencies consult with relevant historic preservation partners to determine the area of potential effect (APE) of the undertaking, to identify historic properties that may exist in that area, and to assess and address any adverse effects that may be caused on such properties by the undertaking. Specifically, 36 C.F.R. § 800.4(b)(1) of the regulations states that federal agency officials shall make a "reasonable and good faith effort" to identify historic properties.

If an undertaking is a type of activity that does not have the potential to cause effects on historic properties, assuming such historic properties were present, the federal agency has no further obligations under 36 C.F.R. § 800.3(a)(1). Because this permit will not authorize new construction or modification or related activities at an existing site, this undertaking does not have the potential to cause effects on historic properties.

This memorandum describes EPA's efforts to assess potential effects in connection with issuing a draft synthetic minor New Source Review (NSR) permit for an existing oil and gas production facility located within the exterior boundaries of the Southern Ute Indian Reservation in La Plata County, Colorado.

#### **Region 8, Air Program Determination**

The EPA has reviewed the proposed action for potential impacts on historic properties in the APE. The proposed permit action does not authorize the construction of any new emission sources, or emission increases from existing units, nor does it otherwise authorize any other physical modifications to the associated facility or its operations. The emissions, approved at present, from the existing facility will not increase due to the associated permit action and the emissions will continue to be well controlled at all times. Because the EPA has determined that the federal action will have no effect, the agency is making the finding of "No historic properties affected" for the APE.

#### **Area of Potential Effects (APE)**

The APE for the existing facility is the location within the areas currently occupied by the facility.

Regulation 36 C.F.R. 800.16(d) defines "area of potential effects" - as:

"... the geographic area or areas within which an undertaking may directly or indirectly cause alterations in the character or use of historic properties, if any such properties exist. The area of potential effects is influenced by the scale and nature of an undertaking and may be different for different kinds of effects caused by the undertaking."

#### **Permit Request**

On December 24, 2013, the EPA received an application from Samson Resources Company (Samson) requesting a synthetic minor permit for the Spring Creek Compressor Station in accordance the requirements of the MNSR Permit Program. This permit action applies to an existing facility operating on the Southern Ute Indian Reservation in Colorado. The Spring Creek Compressor Station is located at:

S23, T33N, R7W Latitude 37.09241, Longitude -107.57601.

Spring Creek Compressor Station currently operates nine (9) natural gas-fired reciprocating internal combustion engines used for natural gas compression, with future planned expansion to 10 engines. The engines are operating under enforceable nitrogen oxide (NO<sub>X</sub>) emission limits required by a May 1, 2014 Consent Agreement Final Order (CAFO) #CAA-08-2013-0015 between Samson and the EPA. These emission limits provide enforceable recognition of the air fuel ratio control (AFRC) systems installed on each of the engines reducing the emission of NO<sub>X</sub> pollutants to synthetically minor levels.

This MNSR permit action does not authorize the construction of any new emission sources, or emission increases from existing units, nor does it otherwise authorize any other physical modifications to the facility or its operations. This permit is intended only to incorporate required and requested emission limits and provisions from the CAFO. Additionally, the CAFO requires testing, monitoring, recordkeeping, and reporting requirements to verify compliance with the emission limitations. The emissions, approved at present, from the existing facility will not increase due to the associated permit

action and the emissions will continue to be well controlled at all times. This is an administrative action with no physical changes to the existing facility or surrounding area.

This permit reflects the incorporation of the requirements established in the CAFO. Samson requested these requirements in order to maintain the Spring Creek Compressor Station's status as a synthetic minor source of NO<sub>X</sub> emissions with respect to the Prevention of Significant Deterioration (PSD) Permit Program at 40 CFR Part 52. Section 49.153(a)(3)(iv) of the MNSR rule provides the EPA with the authority to transfer such limits to a MNSR permit. The MNSR regulations at §\$49.158(c)(2)(ii) and (iii) also provide the EPA with the discretion to require any additional requirements, including control technology requirements, based on the specific circumstances of the source.

#### **Registered Historic Places**

The National Park Service maintains an internet resource that can be used to determine whether any registered historic places are within the area of potential effect. The resource is:

1. National Register of Historic Places database, http://www.nps.gov/history/nr/research/index.htm

An additional site is available to provide additional information on these historic places. The resource is:

- 2. National Register of Historic Places, <a href="http://www.nationalregisterofhistoricplaces.com/">http://www.nationalregisterofhistoricplaces.com/</a>
  - a. County information, http://www.nationalregisterofhistoricplaces.com/ut/Uintah/state.html
  - b. Historic Districts within a county, <a href="http://www.nationalregisterofhistoricplaces.com/ut/Uintah/districts.html">http://www.nationalregisterofhistoricplaces.com/ut/Uintah/districts.html</a>

A search of registered historic places or districts was not undertaken because this is an administrative action with no physical changes to the existing facility or surrounding area.

#### **State and Tribal Consultation**

Because this undertaking does not have the potential to cause effects on historic properties, assuming such historic properties were present, the EPA has no further obligations under 36 C.F.R. § 800.3(a)(1).

Remit # SmNSR-SU-000053-2013.001

## SYNTHETIC MINOR PERMIT APPLICATION

## **SPRING CREEK COMPRESSOR STATION**



Prepared for:



Samson Plaza Two West Second Street Tulsa, Oklahoma 74103

Prepared by:



4038 Timberline Road, Suite 100 Fort Collins, CO 80525

**DECEMBER 2013** 

### SYNTHETIC MINOR PERMIT APPLICATION SPRING CREEK COMPRESSOR STATION SAMSON RESOURCES

#### **CONTENTS**

#### **Administrative and Plant-Wide Information**

Form NEW – Application for New Construction
Form SYNMIN – New Source Review Synthetic Minor Limit Request Form
Description of Operations
Potential to Emit Summary
Directions to the Facility
Regulatory Applicability Assessment
Endangered Species Act (ESA) Report
National Historic Preservation Act (NHPA) Report

#### **Figures**

Figure 1 - General Location Map

Figure 2 - Simplified Plot Plan

Figure 3 - Simplified Process Flow Diagram

#### **Insignificant Emissions**

Insignificant Emissions Justification

Tanks 4.0.9d Output – Lubricating Oil Storage Tanks

Tanks 4.0.9d Output - Skid Drains Tanks

Tanks 4.0.9d Output – Ethylene Glycol Storage Tanks

Tanks 4.0.9d Output - Waste Oil/Slop Tanks

Tanks 4.0.9d Output - Slop Tank

Facility Water Analysis

#### **Emission Units**

#### Caterpillar G3516LE Compressor Engines

**Emissions Unit Descriptions** 

Manufacturer's Specification Sheets

Emissions Unit E1 Emission Estimates

**Emissions Unit E2 Emission Estimates** 

**Emissions Unit E3 Emission Estimates** 

**Emissions Unit E4 Emission Estimates** 

**Emissions Unit E5 Emission Estimates** 

**Emissions Unit E6 Emission Estimates** 

**Emissions Unit E7 Emission Estimates** 

Emissions Unit E8 Emission Estimates

**Emissions Unit E9 Emission Estimates** 

**Emissions Unit E10 Emission Estimates** 

# SYNTHETIC MINOR PERMIT APPLICATION SPRING CREEK COMPRESSOR STATION SAMSON RESOURCES

#### **CONTENTS CONTINUED**

#### **TEG Dehydration Unit**

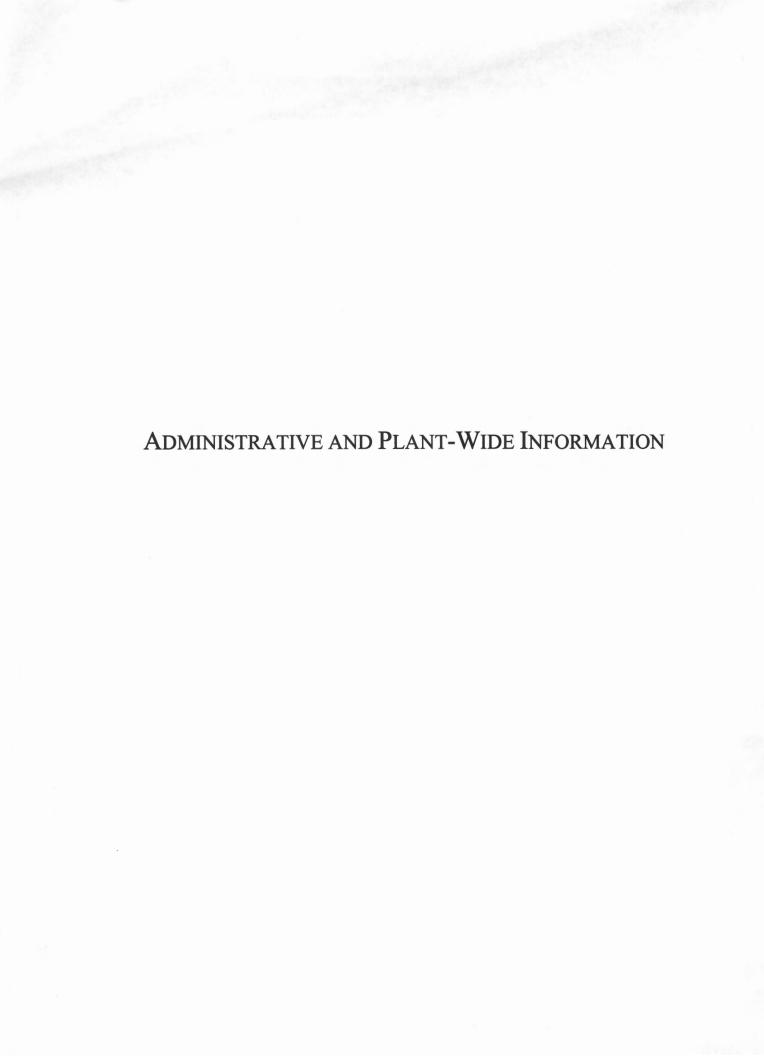
Emissions Unit D1 Emission Estimates Gas Sample Analysis GRI GLYCalc Model Output

#### **Fugitive Emissions**

**Emissions Unit FUG Emission Estimates** 

#### **Greenhouse Gas Emissions**

Facility Greenhouse Gas PTE Emission Estimates Example Calculations





## UNITED STATES ENVIRONMENTAL PROTECTION AGENCY FEDERAL MINOR NEW SOURCE REVIEW PROGRAM IN INDIAN COUNTRY

40 CFR 49.151

Application for New Construction (Form NEW)									
Please check all that apply to show how you are using this form:  Proposed Construction of a New Source Proposed Construction of New Equipment at an Existing Source Proposed Modification of an Existing Source Other - Please Explain - Synthetic Minor Permit Application									
The following is a check list of t project. While submittal of this requested approval and providin	the type of information that form is not required, it do g the information requesto be of Management and Bu	not yet approved by the Office of at Region 8 will use to process info bes offer details on the information ed may help expedite the process. Undget review and these information	ormation on your proposed we will use to complete your Use of application forms for this						
Please submit information t	o following two entitie	<b>25:</b>							
Federal Minor NSR Permit C U.S. EPA, Region 8 1595 Wynkoop Street, 8P-AR Denver, CO 80202-1129 R8airpermitting@epa.gov  For more information, visit: http://www2.epa.gov/regiominor-new-source-review-  A. GENERAL SOURCE  1. (a) Company Name Samson Resources (b) Operator Name Samson Resources (c)	n8/tribal- permitting  INFORMATION  Company	reservation:  If you need assistance in							
3. Type of Operation Natural Gas Production		5. Temporary Source?	5. Temporary Source? □ Yes ⊠ No						
6. NAICS Code <b>211111</b>		7. SIC Code <b>1311</b>	7. SIC Code 1311						
8. Physical Address (home b 1000 County Road 324, I About 5 miles southeast	gnacio, CO	3)							
9. Reservation* Southern Ute	10. County* La Plata	11a. Latitude* 37° 5' 32.6" N	11b. Longitude* -107° 34' 33.7" W						
12a. Quarter Quarter Section* SWNE	12b. Section* 23	12c. Township* 33 North	12d. Range* 7 West						

<sup>\*</sup>Provide all proposed locations of operation for portable sources

B. PREVIOUS PERMIT ACTIONS (Provide information in this format for each permit that has
been issued to this source. Provide as an attachment if additional space is necessary)  Source Name on the Permit
Permit Number (xx-xxx-xxxxx-xxxxxxxxxxxxxxxxxxxxxxxx
Date of the Permit Action
Source Name on the Permit
Permit Number (xx-xxx-xxxxxxxxxxxxxxxxxxxxxxxxxxxxxx
remit Number (XX-XXX-XXXXXXX)
Date of the Permit Action
Date of the Lemma rection
Source Name on the Permit
Permit Number (xx-xxx-xxxxxxxxxxxxxxxxxxxxxxxxxxxxxx
Date of the Permit Action
Source Name on the Permit
Permit Number (xx-xxx-xxxx-xxxx)
Date of the Permit Action
Source Name on the Permit
Permit Number (xx-xxx-xxxxx.xx)
,

#### C. CONTACT INFORMATION

Company Contact		Title			
Brad Rogers		Senior Environmental Specialist			
Mailing Address 370 17 <sup>th</sup> Street, Suite 3000		Specialise			
Email Address bradr@samson.com					
Telephone Number (720) 239-4406					
Operator Contact (if different from company contact)		Title			
Mailing Address					
Email Address					
Telephone Number Facsimile Number					
Source Contact Lynn Davis		Title Superintendent			
Mailing Address PO Box 9 Bayfield, CO 8112					
Email Address ldavis@samson.com					
Telephone Number (970) 884-5085	Facsimile Number				
Compliance Contact Brad Rogers	Title Senior Environmental Specialist				
Mailing Address 370 17 <sup>th</sup> Street, Suite 3000					
Email Address bradr@samson.com					
Telephone Number (720) 239-4406	Facsimile Number				

#### D. ATTACHMENTS

#### Include all of the following information (see the attached instructions)

- ☑ **FORM SYNMIN** New Source Review Synthetic Minor Limit Request Form, if synthetic minor limits are being requested.
- ☑ Narrative description of the proposed production processes. This description should follow the flow of the process flow diagram to be submitted with this application.
- ☑ Process flow chart identifying all proposed processing, combustion, handling, storage, and emission control equipment.
- ☑ A list and descriptions of all proposed emission units and air pollution-generating activities.
- ☑ Type and quantity of fuels, including sulfur content of fuels, proposed to be used on a daily, annual and maximum hourly basis.
- ☑ Type and quantity of raw materials used or final product produced proposed to be used on a daily, annual and maximum hourly basis.
- ☑ Proposed operating schedule, including number of hours per day, number of days per week and number of weeks per year.
- A list and description of all proposed emission controls, control efficiencies, emission limits, and monitoring for each emission unit and air pollution generating activity.
- $\boxtimes$  Criteria Pollutant Emissions Estimates of Current Actual Emissions, Current Allowable Emissions, Post-Change Uncontrolled Emissions, and Post-Change Allowable Emissions for the following air pollutants: particulate matter, PM<sub>10</sub>, PM<sub>2.5</sub>, sulfur oxides (SOx), nitrogen oxides (NOx), carbon monoxide (CO), volatile organic compound (VOC), lead (Pb) and lead compounds, fluorides (gaseous and particulate), sulfuric acid mist (H<sub>2</sub>SO<sub>4</sub>), hydrogen sulfide (H<sub>2</sub>S), total reduced sulfur (TRS) and reduced sulfur compounds, including all calculations for the estimates.

These estimates are to be made for each emission unit, emission generating activity, and the project/source in total.

- ☑ Air Quality Review
- **⊠** ESA (Endangered Species Act)
- **⋈** NHPA (National Historic Preservation Act)

#### E. TABLE OF ESTIMATED EMISSIONS

The following tables provide the total emissions in tons/year for all pollutants from the calculations required in Section D of this form, as appropriate for the use specified at the top of the form.

E(i) - Proposed New Source

Pollutant	Potential Emissions (tpy)	Proposed Allowable Emissions (tpy)	
PM	0	0	PM - Particulate Matter PM <sub>10</sub> - Particulate Matter less
PM <sub>10</sub>	0	0	than 10 microns in size
PM <sub>2.5</sub>	0	0	PM <sub>2.5</sub> - Particulate Matter less than 2.5 microns in size
SO <sub>2</sub>	0	0	SO2 - Sulfur Oxides NOx - Nitrogen Oxides
NO <sub>x</sub>	211.3	211.3	CO - Carbon Monoxide
СО	196.3	196.3	VOC - Volatile Organic Compound
VOC	60.5	60.5	Pb - Lead and lead compounds Fluorides - Gaseous and
Pb	0	0	particulates
Fluorides	0	0	H <sub>2</sub> SO <sub>4</sub> - Sulfuric Acid Mist H <sub>2</sub> S - Hydrogen Sulfide
H <sub>2</sub> SO <sub>4</sub>	0	0	TRS - Total Reduced Sulfur
H <sub>2</sub> S	0	0	RSC - Reduced Sulfur Compounds
TRS	0	0	
RSC	0	0	

Emissions calculations must include fugitive emissions if the source is one the following listed sources, pursuant to CAA Section 302(j):

- (a) Coal cleaning plants (with thermal dryers);
- (b) Kraft pulp mills;
- (c) Portland cement plants;
- (d) Primary zinc smelters;
- (e) Iron and steel mills;
- (f) Primary aluminum ore reduction plants;
- (g) Primary copper smelters;
- (h) Municipal incinerators capable of charging more than 250 tons of refuse per day;
- (i) Hydrofluoric, sulfuric, or nitric acid plants;
- (j) Petroleum refineries;
- (k) Lime plants;
- (1) Phosphate rock processing plants;
- (m) Coke oven batteries;
- (n) Sulfur recovery plants;
- (o) Carbon black plants (furnace process);
- (p) Primary lead smelters;
- (q) Fuel conversion plants;

- (r) Sintering plants;
- (s) Secondary metal production plants;
- (t) Chemical process plants
- (u) Fossil-fuel boilers (or combination thereof) totaling more than 250 million British thermal units per hour heat input;
- (v) Petroleum storage and transfer units with a total storage capacity exceeding 300,000 barrels;
- (w) Taconite ore processing plants;
- (x) Glass fiber processing plants;
- (y) Charcoal production plants;
- (z) Fossil fuel-fired steam electric plants of more that 250 million British thermal units per hour heat input, and
- (aa) Any other stationary source category which, as of August 7, 1980, is being regulated under section 111 or 112 of the Act.

E(ii) – Proposed New Construction at an Existing Source or Modification of an Existing Source

Pollutant	Current Actual Emissions (tpy)	Current Allowable Emissions (tpy)	Post-Change Potential Emissions (tpy)	Post-Change Allowable Emissions (tpy)
PM	0	0	0	0
PM <sub>10</sub>	0	0	0	0
PM <sub>2.5</sub>	0	0	0	0
SO <sub>2</sub>	0	0	0	0
NO <sub>x</sub>	211.3	211.3	211.3	211.3
СО	196.3	196.3	196.3	196.3
VOC	60.5	60.5	60.5	60.5
Pb	0	0	0	0
Fluorides	0	0	0	0
H <sub>2</sub> SO <sub>4</sub>	0	0	0	0
H <sub>2</sub> S	0	0	0	0
TRS	0	0	0	0
RSC	0	0	0	0

PM - Particulate Matter

PM<sub>10</sub> - Particulate Matter less than 10 microns in size

PM<sub>2.5</sub> - Particulate Matter less than 2.5 microns in size

SO<sub>2</sub> - Sulfur Oxides

NOx - Nitrogen Oxides

CO - Carbon Monoxide

VOC - Volatile Organic Compound

Pb - Lead and lead compounds

Fluorides - Gaseous and particulates

H<sub>2</sub>SO<sub>4</sub> - Sulfuric Acid Mist

H<sub>2</sub>S - Hydrogen Sulfide

TRS - Total Reduced Sulfur

RSC - Reduced Sulfur Compounds

The public reporting and recordkeeping burden for this collection of information is estimated to average 20 hours per response, unless a modeling analysis is required. If a modeling analysis is required, the public reporting and recordkeeping burden for this collection of information is estimated to average 60 hours per response .Send comments on the Agency's need for this information, the accuracy of the provided burden estimates, and any suggested methods for minimizing respondent burden, including through the use of automated collection techniques to the Director, Collection Strategies Division, U.S. Environmental Protection Agency (2822T), 1200 Pennsylvania Ave., NW, Washington, D.C. 20460. Include the OMB control number in any correspondence. Do not send the completed form to this address.



#### UNITED STATES ENVIRONMENTAL PROTECTION AGENCY FEDERAL MINOR NEW SOURCE REVIEW PROGRAM IN INDIAN COUNTRY 40 CFR 49.151

#### **Application For Synthetic Minor Limit**

(Form SYNMIN)

Use of this information request form is voluntary and not yet approved by the Office of Management and Budget. The following is a check list of the type of information that Region 8 will use to process information on your proposed project. While submittal of this form is not required, it does offer details on the information we will use to complete your requested approval and providing the information requested may help expedite the process. Use of application forms for this program is currently under Office of Management and Budget review and these information request forms will be replaced/updated after that review is completed.

#### Please submit information to following two entities:

Federal Minor NSR Permit Coordinator U.S. EPA, Region 8 1595 Wynkoop Street, 8P-AR Denver, CO 80202-1129 R8airpermitting@epa.gov

For more information, visit:

http://www2.epa.gov/region8/tribal-minor-new-source-review-permitting

reservation:

If you need assistance in identifying the appropriate Tribal Environmental Contact and address, please contact:

The Tribal Environmental Contact for the specific

R8airpermitting@epa.gov

#### A. GENERAL INFORMATION

Company Name Samson Resources Company	Source Name Spring Creek Compressor Station				
Company Contact or Owner Name Brad Rogers		Title Senior Environmental Specialist			
Mailing Address 370 17 <sup>th</sup> Street, Suite 3000					
Email Address bradr@samson.com					
Telephone Number (720) 239-4406	Facsimile Number	r			

#### **B. ATTACHMENTS**

For each criteria air pollutant, hazardous air pollutant and for all emission units and air pollutant-generating activities to be covered by a limitation, include the following:

- ☑ Item 1 The proposed limitation and a description of its effect on current actual, allowable and the potential to emit.
- ☑ Item 2 The proposed testing, monitoring, recordkeeping, and reporting requirements to be used to demonstrate and assure compliance with the proposed limitation.
- ☑ Item 3 A description of estimated efficiency of air pollution control equipment under present or anticipated operating conditions, including documentation of the manufacturer specifications and guarantees.
- ☑ Item 4 Estimates of the Post-Change Allowable Emissions that would result from compliance with the proposed limitation, including all calculations for the estimates.
- ☑ Item 5 Estimates of the potential emissions of Greenhouse Gas (GHG) pollutants:

#### Description of Operations Spring Creek Compressor Station Section 23, Township 33N, Range 7W La Plata County, Colorado

The Spring Creek Compressor Station is owned and operated by Samson Resources. The facility is located within the exterior boundaries of the Southern Ute Indian Reservation in the NE ¼ of Section 23, Township 33 North, Range 7 West in La Plata County, Colorado. A facility location map is included as Figure 1. Figure 2 contains a simplified facility plot plan. A process flow diagram is attached as Figure 3.

The Spring Creek Compressor Station receives coal-bed methane gas gathered from nearby sources and compresses the natural gas to transmission pipeline specifications. Gas entering the facility from the field is first fed to an inlet separator that gravimetrically removes water that may have condensed during transportation from the supplying gas wells. Separator overhead gas is fed to one of up to ten compressor engines from a common suction header. The compressors discharge gas to a common discharge header that feeds to scrubbers. The scrubbers separate and collect liquids that may have formed during compression. The compressed gas is then fed to a dehydration unit. Tri-ethylene glycol is circulated counter-currently and absorbs water in the wet gas. Rich glycol is circulated to a reboiler, where moisture is driven to the atmosphere by heating the glycol. Dry gas exits the contactors and is directed to the sales line, where it is metered and exits the facility. The gas processing capacity of the facility is approximately 60 MMscfd with ten compressor engines operating.

There are currently nine, with future expansion to ten, natural gas-fired 4-stroke lean burn 1340 horsepower Caterpillar G3516LE compressor engines operating at the facility. These units have a site rating of 1092 horsepower. The facility also contains one triethylene-glycol (TEG) dehydration unit with two 30 MMscfd contact towers and one 0.75 MMBtu/hr reboiler burner. The facility emission units are listed in Table 1. There are several insignificant emission units at this facility; these units are listed in Table 2. The facility potential to emit is contained in Table 3.

Table 1: Spring Creek Compressor Station Emission Units

Emission Unit ID	Description	Control Equipment
E1	1092 hp Caterpillar G3516LE Compressor Engine	Oxidation Catalyst
E2	1092 hp Caterpillar G3516LE Compressor Engine	Oxidation Catalyst
E3	1092 hp Caterpillar G3516LE Compressor Engine	Oxidation Catalyst
E4	1092 hp Caterpillar G3516LE Compressor Engine	Oxidation Catalyst
E5	1092 hp Caterpillar G3516LE Compressor Engine	Oxidation Catalyst
E6	1092 hp Caterpillar G3516LE Compressor Engine	Oxidation Catalyst
E7	1092 hp Caterpillar G3516LE Compressor Engine	Oxidation Catalyst
E8	1092 hp Caterpillar G3516LE Compressor Engine	Oxidation Catalyst
E9	1092 hp Caterpillar G3516LE Compressor Engine	Oxidation Catalyst
E10	1092 hp Caterpillar G3516LE Compressor Engine	Oxidation Catalyst
D1	60 MMscfd PESCO Dehydration Unit Glycol Regenerator	None
FUG	Facility Fugitive Emissions	None

Table 2: Spring Creek Compressor Station Insignificant Emission Units

Emission Unit ID	Description			
IEU1	10 – 500 gallon lubricating oil storage tanks			
IEU2	10 – 500 gallon skid drain tanks			
IEU3	2 – 500 gallon ethylene glycol storage tanks			
IEU4	10 – 500 gallon waste oil/slop tanks			
IEU5	1 – 750 bbl produced water storage tank			
IEU6	5 – 1000 bbl produced water storage tanks			
IEU7	1 – 500 bbl slop tank			
IEU8	10 - Compressor blowdown emissions			
IEU9	10 – Compressor starter emissions			
IEU10	10 - Compressor cylinder rod packing vent emissions			

This facility is subject to the National Emission Standard for Hazardous Air Pollutants (NESHAP) for reciprocating internal combustion engines (RICE) regulation 40 CFR 63, Subpart ZZZZ because it emits or has the potential to emit a single Hazardous Air Pollutant (HAP) at a rate greater than 10 tons per year. Per 40 CFR 63, Subpart ZZZZ §63.6640, an affected facility is required to develop a Startup, Shutdown and Malfunction Plan (SSMP). The Spring Creek Compressor Station operates in accordance with the current facility SSMP that was last revised in January 2009.

Unit E3 is subject to the requirements of 40 CFR Part 60, Subpart JJJJ. Performance test are conducted on Unit E3 in accordance with 40 CFR 60.4244 every 8760 hours of operating or every three years, whichever comes first.

Each of the Caterpillar G3516LE compressor engines is equipped with either a NO<sub>X</sub> sensor or O<sub>2</sub> sensor as part of the air fuel ration controller system (AFRC) and an oxidation catalytic converter to reduce emissions in the exhaust stream. A continuous parameter monitoring system (CPMS) is used to record the catalyst inlet temperature of each engine to ensure that the inlet temperature remains between 450 °F and 1350 °F. The CPMS continuously monitors the catalyst inlet temperature and reduces the data to a 4-hour rolling average. The CPMS also logs the shutdown times and events and displays the unit process and fuel flows for each engine. The pressure drop across the catalyst is manually recorded at least once a month. Facility data is recorded in accordance with applicable parts of Section §63.6640.

The Spring Creek Compressor Station is an existing, constructed, and operating facility. There are no increases in emission rates or facility potential to emit with this application so an ambient impact analysis has not been included. In addition the facility will have no adverse effects with respect to the ESA or NHPA. ESA and NHPA reports are attached.

Table 3: Spring Creek Compressor Station Potential to Emit

Unit	Model	hn		NO <sub>X</sub>			CO			VOC		Fo	ormaldehyd	е	Total HA
Ollit	t Model hp	пр	g/hphr	lb/hr	tpy	g/hphr	lb/hr	tpy	g/hphr	lb/hr	tpy	g/hphr	lb/hr	tpy	tpy
E1	Caterpillar G3516LE	1092	2.00	4.8	21.1	1.86	4.5	19.6	0.35	0.8	3.7	0.14	0.3	1.5	1.5
E2	Caterpillar G3516LE	1092	2.00	4.8	21.1	1.86	4.5	19.6	0.35	0.8	3.7	0.14	0.3	1.5	1.5
E3	Caterpillar G3516LE	1092	2.00	4.8	21.1	1.86	4.5	19.6	1.00	2.4	10.5	0.14	0.3	1.5	1.5
E4	Caterpillar G3516LE	1092	2.00	4.8	21.1	1.86	4.5	19.6	0.35	0.8	3.7	0.14	0.3	1.5	1.5
E5	Caterpillar G3516LE	1092	2.00	4.8	21.1	1.86	4.5	19.6	0.35	0.8	3.7	0.14	0.3	1.5	1.5
E6	Caterpillar G3516LE	1092	2.00	4.8	21.1	1.86	4.5	19.6	0.35	0.8	3.7	0.14	0.3	1.5	1.5
E7	Caterpillar G3516LE	1092	2.00	4.8	21.1	1.86	4.5	19.6	0.35	0.8	3.7	0.14	0.3	1.5	1.5
E8	Caterpillar G3516LE	1092	2.00	4.8	21.1	1.86	4.5	19.6	0.35	0.8	3.7	0.14	0.3	1.5	1.5
E9	Caterpillar G3516LE	1092	2.00	4.8	21.1	1.86	4.5	19.6	0.35	0.8	3.7	0.14	0.3	1.5	1.5
E10	Caterpillar G3516LE	1092	2.00	4.8	21.1	1.86	4.5	19.6	0.35	0.8	3.7	0.14	0.3	1.5	1.5
D1	TEG Dehydration Unit	60 MMscfd		0.07	0.3		0.06	0.3			13.1			0.0	9.9
FUG	Facility Fugitive Emissio	ns			0.0			0.0			3.2			0.0	0.0
IEUs	Insignificant Emission U	nits			0.0			0.0			0.4			0.0	0.0
Total					211.3			196.3			60.5			15.0	24.9

#### Directions to the Facility Spring Creek Compressor Station Section 23, Township 33N, Range 7W La Plata County, Colorado

The Spring Creek Compressor Station is located southeast of Ignacio, Colorado. To get to the Spring Creek Compressor Station from Ignacio at the intersection of Highway 172 and County Road 151 go east on County Road 151. Follow County Road 151 east for 3.3 miles and turn south onto County Road 324. Follow County Road 324 for approximately 0.9 miles. The facility is located on the east side of the road at 1000 County Road 324.

## Regulatory Applicability Assessment Spring Creek Compressor Station

40 CFR Part	Description	Applicable Requirement	Reason
Part 50	National Primary and Secondary Ambient Air Quality Standards	N	Ambient standards set forth by theses provisions are not directly enforceable upon a facility. The demonstration of the maintenance of an air quality standard is the responsibility of the Administrator and not that of a specific facility. It is recognized that the Administrator may incorporate requirements into a State or Federal Implementation Plan designed to mitigate an air quality violation which can apply to specific facilities, but the specific air quality standards are not direct applicable requirements to this facility.
Part 51	Requirements for Preparation, Adoption and submittal of Implementation Plans	N	Provisions of this part are administrative in nature and implement mandates of the Clean Air Act.
Part 52	Approval of Promulgation of Implementation Plans	ET BURNEY	是一个一个一个一个一个一个一个一个一个一个一个一个一个一个一个一个一个一个一个
52.21	Prevention of Significant Deterioration	N	The facility is not a major stationary source as defined at 40 CFR 52.21(b). The facility has a potential to emit criteria pollutants below the 250 tpy PSD threshold.
52.24	New Source Review	N	The facility is not located in a nonattainment area
Part 53	Ambient Air Monitoring Reference and Equivalent Methods	N	This part sets forth requirements for the monitoring of ambient air. The facility is not required and does not perform ambient air monitoring.
Part 54	Prior Notice of Citizen Suits	N	Provisions of this part are administrative in nature and implement mandates of the Clean Air Act.
Part 55	Outer Continental Shelf Air Regulations	N	The facility is not located on the Outer Continental Shelf
Part 56	Regional Consistency	N	Provisions of this part are administrative in nature and implement mandates of the Clean Air Act.
Part 57	Primary Nonferrous Smelter Orders	N	The facility is not a Nonferrous Smelter
Part 58	Ambient Air Quality Surveillance	N	This part sets forth requirements for the monitoring of ambient air. The facility is not required and does not perform ambient air monitoring.
Part 59	Not PromulgatedReserved		
Part 60	Standards of Performance for New Stationary Sources	N	Most of the standards set forth by these regulations do not apply to the facility because no applicable units exist at the facility. Specific standards which may apply at the facility and may apply in general to natural gas transmission and/or processing facilities include:
Subpart K	VOL Storage Tanks	N	There are no storage tanks at this facility which were constructed prior to March 8, 1978
Subpart Ka	VOL Storage Tanks	N	There are no storage tanks at this facility which were constructed between May18, 1978 and July 23, 1984
	VOL Storage Tanks	N	All tanks which contain VOL and which were constructed after July 23, 1984 either have capacities less than the applicability threshold of 40 m <sup>3</sup> (251.6 bbl) or have vapor pressures below the 15 kPa applicability threshold.
	Stationary Gas Turbines	N	There are no gas turbines located at this facility.
Subpart KKK	On-Shore Natural Gas Processing Facilities	N	This facility does not process natural gas to extract natural gas liquids.

## Regulatory Applicability Assessment Spring Creek Compressor Station

40 CFR Part	Description	Applicable Requirement	Reason
Subpart LLL	On-Shore Natural Gas Sweetening Plants	N	This facility does not process natural gas to remove sulfur compounds.
	JJJJ National Emision Standrads for Hazardous Air Pollutants for Recipricating Internal Combustion Engines		Unit E3 is subject to this Subpart. Future Internal Combustion Engines installed at this facility may be subject to this Subpart and will be in compliance.
Subpart KKKK	Standards of Performance for Stationary Gas Turbines	N	There are no gas turbines located at this facility.
Subpart OOOO	Standards of Performance for Crude Oil and Natural Gas Production, Transmission, and Distribution	Currently N/Possible Future Applicability	All equipment at this facility potentially subject to this Subpart was installed prior to the August 23, 2011 applicability date and is not subject to this regulation. Future compressor installed at this facility may be subject to this Subpart and will be in compliance.
Part 61	National Emission Standards for Hazardous Air Pollutants	N	This facility is not part of any source category for which provisions set forth by these regulations apply.
Part 62	Approval and Promulgation of State Plans for Designated Facilities and Pollutants	N	Provisions of this part are administrative in nature and implement mandates of the Clean Air Act. They do not directly apply to this facility.
Part 63	National Emission Standards for Hazardous Air Pollutants for Source Categories	Y	Most of the standards set forth by these regulations do not apply to the facility because no applicable units exist at the facility. Specific standards which apply at the facility and may apply in general to natural gas transmission and/or processing facilities include:
Subpart HH	National Emission Standards for Hazardous Air Pollutants from Oil and Natural Gas Production Facilities	Y	This facility is an area source of HAP with respect to this subpart. The dehydration unit operates under the optimum glycol circulation rate.
Subpart HHH	National Emission Standards for Hazardous Air Pollutants from Natural Gas Transmission and Storage Facilities	N	Facility is not a natural gas transmission or storage facility.
Subpart ZZZZ	National Emission Standards for Hazardous Air Pollutants for Recipricating Internal Combustion Engines	Y	This facility is subject to this subpart because potential emissions are above major source thresholds.
Part 64	Compliance Assurance Monitoring	N	No emission units at the facility are equipped with emission control technology or are limited by an applicable emission limitation.
Part 65	Not PromulgatedReserved	The state of	
Part 66	Assessment and Collection of Noncompliance Penalties by EPA	N	Provisions of this part are administrative in nature and implement mandates of the Clean Air Act. They do not directly apply to this facility.
Part 67	EPA Approval of State Noncompliance Penalty Program	N	Provisions of this part are administrative in nature and implement mandates of the Clean Air Act. They do not directly apply to this facility.
Part 68	Chemical Accident Prevention Provisions	N	No substance listed by this regulations is stored on-site at the facility in quantities above applicable threshold values set forth by the regulation.
Part 69	Special Exemptions from the Requirements of the Clean Air Act	N	The facility is not located in an area covered by this regulation.
Part 70	State Operating Permit Programs	N	The facility is not located in an area under the jurisdiction of a regulatory authority which has an EPA-approved part 70 program.
Part 71	Federal Operating Permit Programs	Y	The facility is a major source subject to the provisions of this regulation.
Part 72	Permits Regulation	N	The facility is not an affected facility under the Acid Rain Program.
Part 73	Sulfur Dioxide Allowance System	N	The facility is not an affected facility under the Acid Rain Program.
Part 74	Sulfur Dioxide Opt-Ins	N	The facility has not elected to opt-in to the Acid Rain Program.
Part 75	Continuous Emissions Monitoring	N	The facility is not an affected facility under the Acid Rain Program.

## Regulatory Applicability Assessment Spring Creek Compressor Station

40 CFR Part	Description	Applicable Requirement	Reason
Part 76	Acid Rain Nitrogen Oxides Emission Reduction Program	N	The facility is not an affected facility under the Acid Rain Program.
Part 77	Excess Emissions	N	The facility is not an affected facility under the Acid Rain Program.
Part 78	Appeal Procedures for Acid Rain Program	N	The facility is not an affected facility under the Acid Rain Program.
Part 79	Registration of Fuels and Fuel Additives	N	The facility does not sell fuels or additives which are designated by this provision.
Part 80	Regulation of Fuels and Fuel Additives	N	The facility does not sell fuels or additives which are designated by this provision.
Part 81	Designation of Areas for Air Quality Planning Purposes	N	Provision of this part are administrative in nature and implement mandates of the Clean Air Act. They do not directly apply to his facility.
Part 82	Protection of Stratospheric Ozone	N	The Facility does not engage in the distribution or sale of controlled substances, and it does not produce, transform, destroy, import, or export products containing controlled substances.
Part 85	Control of Air Pollution from Mobile Sources	N	The facility does not engage in vehicle manufacturing activities.
Part 86	Control of Air Pollution from New and In-Use Motor Vehicles and New and In-use Motor Vehicle Engines: Certification and Test Procedures	N	The facility does not engage in the certification or testing of motor vehicle engines.
Part 87	Control of Air Pollution from Aircraft and Aircraft Engines	N	The facility does not engage in the use of aircraft or aircraft engines.
Part 88	Clean-fuel Vehicles	N	These provisions apply to vehicle fleets and not to stationary sources.
Part 89	Control of Emissions from new and in-use Nonroad Engines	N	The facility does not engage in the use of nonraod engines as define by these provisions.
Part 90	Control of Emissions from Nonroad Spark-ignition Engines	N	The facility does not engage in the use of nonroad spark-ignition engines as defined by these provisions.
Part 91	Control of Emissions from Marine Spark-ignition Engines	N	The facility does not engage in the use of marine spark-ignition engines.
Part 92	Control of Emissions from Locomotives and Locomotive Engine	N	The facility does not engage in the use of locomotives or locomotive engines.
Part 93	Determining Conformity of Federal Actions to State or Federal Implementation Plans	N	The facility operations are not federal actions.
Part 94	Not PromulgatedReserved		MATERIAL TO THE STATE OF THE S
Part 95	Mandatory Patent Licenses	N	Provisions of this part are administrative in nature and implement mandates of the Clean Air Act. They do not directly apply to his facility.
Parts 96-99	Not PromulgatedReserved		

Group	Name	Population	Status	Lead Office	Recovery Plan Name	Recovery Plan Stage
Birds	Yellow-billed Cuckoo (Coccyzus	Western U.S. DPS	Proposed Threatened	Sacramento Fish And Wildlife		
Birds	Mexican spotted owl (Strix	Entire	Threatened	Arizona Ecological Services	Final Recovery Plan for the	Final Revision 1
Birds	Southwestern willow flycatcher	Entire	Endangered	Arizona Ecological Services	Final Recovery Plan for the	Final
Flowering Plants	Knowlton's cactus (Pediocactus		Endangered	New Mexico Ecological Services	Knowlton's (=Hedgehog) Cactus	Final
Insects	Uncompangre fritillary butterfly	Entire	Endangered	Western Colorado Ecological	Uncompangre Fritillary Butterfly	Final
Mammals	Black-footed ferret (Mustela	U.S.A. (specific portions of AZ,	Experimental Population, Non-	Office Of The Regional Director		
Mammals	New Mexico meadow jumping		Proposed Endangered	New Mexico Ecological Services		
Mammals	North American wolverine (Gulo		Proposed Threatened	Montana Ecological Services		



Prev#;#1#;#Next

Freedom of Information Act

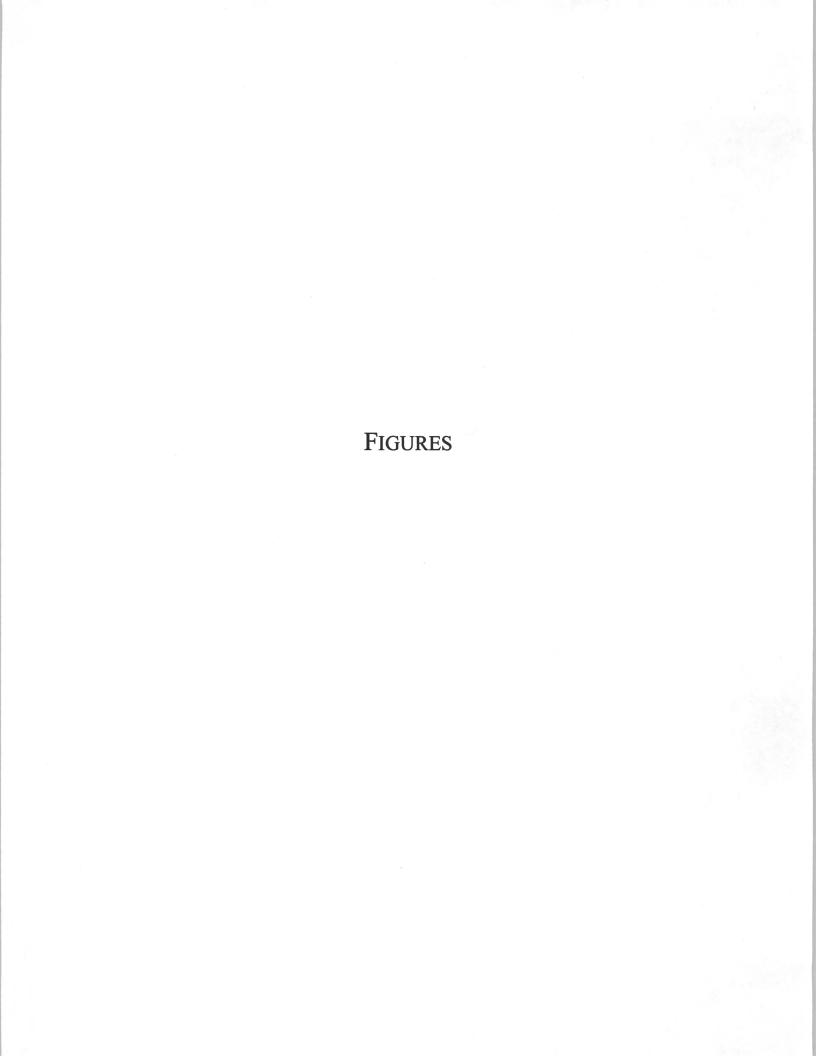
**Privacy Policy** 

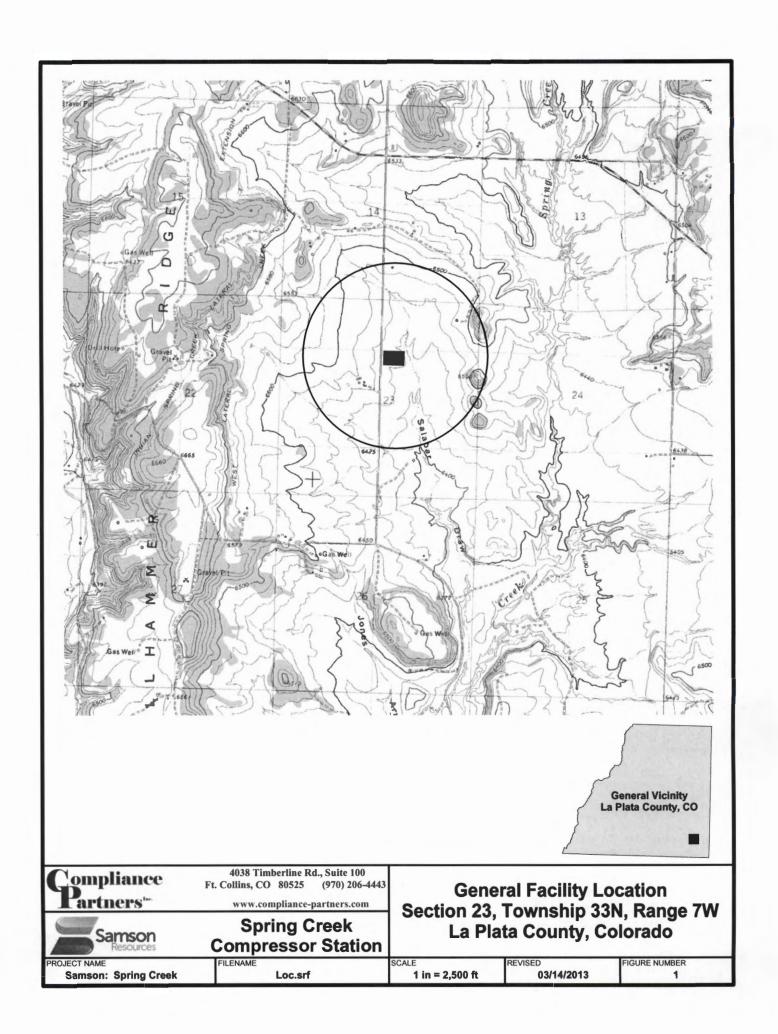
Disclaimer

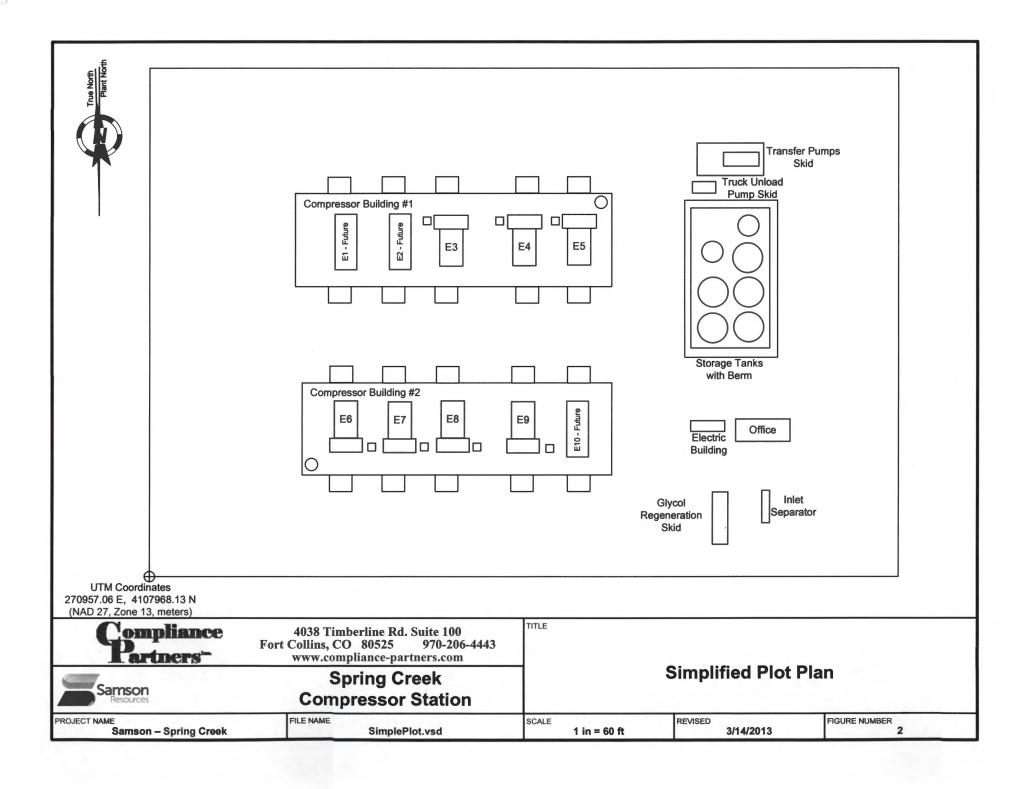
Accessibility

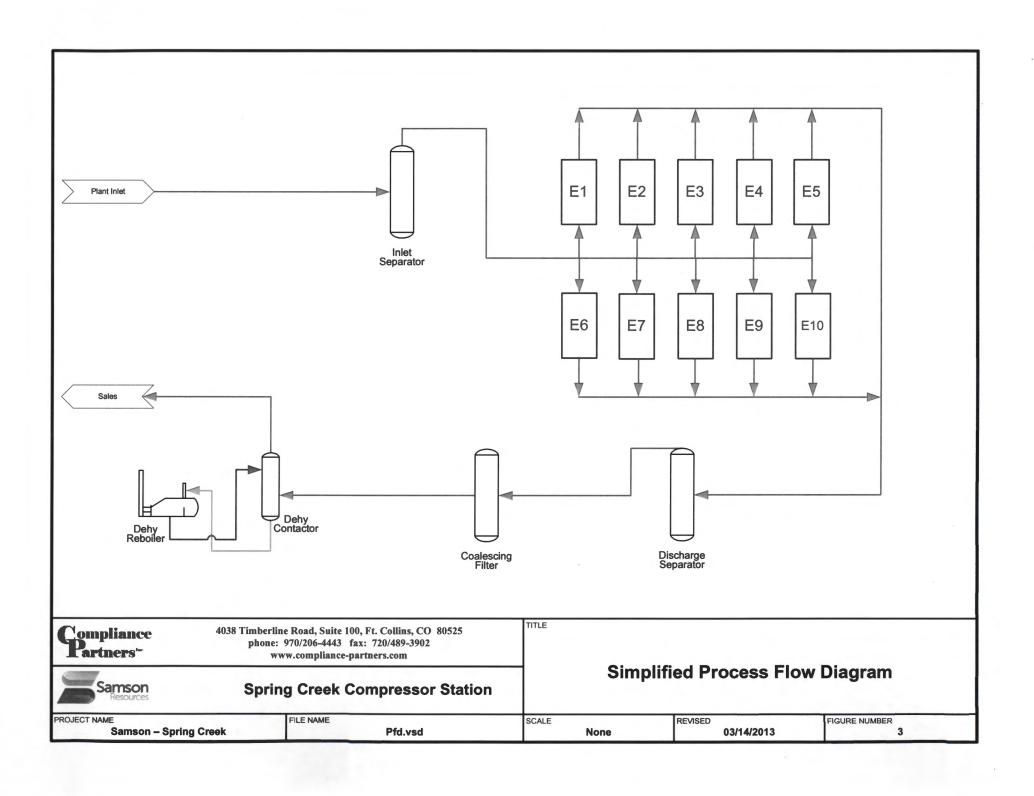
##Ddvw#ksgdwhg=#45245246#

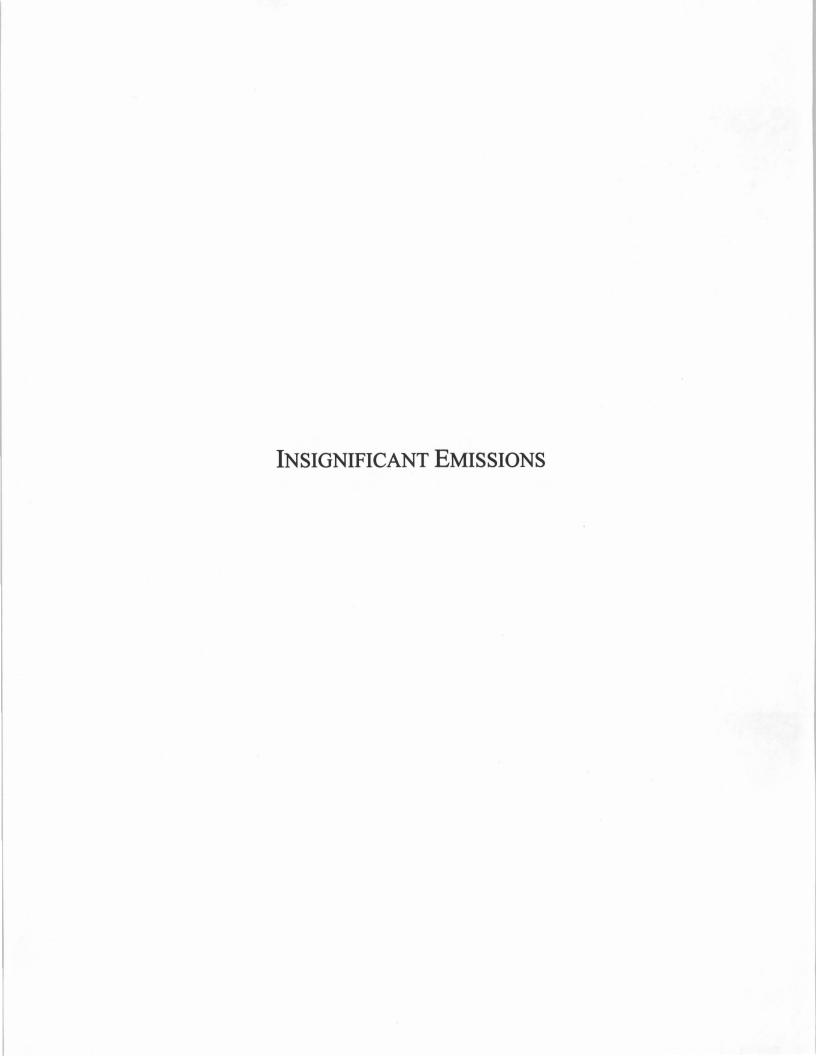
:6#











## **Insignificant Emission Justification Spring Creek Compressor Station**

#### **Tanks**

Emissions for the facility storage tanks were estimated using EPA Tanks 4.0.9d. Table 1 illustrates the emission units, the numbers of turnovers per year assumed when estimating emissions from the unit and the emissions from each unit. The Tanks output for each unit is attached. The produced water storage tanks are used to store produced water with very low VOC content, so emissions from these tanks are negligible. An analysis of this water is attached. The tanks at this facility are all insignificant emission units.

**Table 1: Facility Tank Emissions** 

Unit ID	Description	Turnovers per Year	VOC Emissions per Tank lb/yr	VOC Emissions per Unit lb/yr
IEU1 <sup>1</sup>	10 - 500 gal lubricating oil storage tanks	18	0.12	1.20
IEU2 <sup>1</sup>	10 - 500 gal used oil/waste oil storage tanks	6	0.10	0.6
IEU3 <sup>1</sup>	2-500 gal ethylene glycol storage tanks	18	1.44	2.88
IEU4 <sup>2</sup>	5 – 1000 gal produced water storage tanks 1 – 750 bbl produced water storage tank	6	<0.1	<0.1
IEU5 <sup>3</sup>	1 – 500 bbl slop tank	12	3.77	3.77
IEU6 <sup>1</sup>	10 - 500 gal skid drains tanks	12	0.12	1.20

<sup>&</sup>lt;sup>1</sup>Low vapor pressure.

### **Reciprocating Compressors**

Reciprocating compressors are sources of VOC emissions from compressor blowdown, cylinder rod packing leaks and starter gas. Compressor blowdown, starter gas, and cylinder rod packing vent emissions for the compressors at this facility are insignificant.

#### **Compressor Blowdown**

Gas remaining in the compressor when shutdown will either remain pressurized in the compressor or it will be vented, usually to atmosphere. The total volume vented when the unit is blown down is a function of the compressor size and the size and pressure of the piping and vessels between the compressor suction and discharge isolation valves. The blowdown volume was based on equipment type and typical operating conditions, as well as the estimation of the VOC emissions from blowdown activities given the typical number of events per year. The facility's representative gas composition was used for these estimations. It should be noted that the number of blowdown events during a given year can change and Samson cannot commit to a limitation on the number of events that may occur. The blowdown emission calculation is illustrated below:

<sup>&</sup>lt;sup>2</sup>Low VOC content.

<sup>&</sup>lt;sup>3</sup> Low vapor pressure, mostly water with some lubricating oil.

$$CBD = \left(40,927scf\right) \left(\frac{mole}{385scf}\right) \left(\frac{0.0172moles_{voc}}{100moles}\right) \left(\frac{57.895lb_{voc}}{mole_{voc}}\right) \left(\frac{20events}{yr}\right) \left(\frac{ton}{2000lb}\right) = 0.01 \frac{ton_{voc}}{yr}$$

Compressor blowdown VOC emissions are estimated to be 0.01 tpy for each compressor and 0.1 tpy VOC for all ten compressors at the facility.

#### Starter Gas

Compressor starter emissions were estimated using the starter's fuel usage at 110 psi and facility's representative gas composition. The example calculation for short term VOC emissions is presented below.

$$\frac{lb_{voc}}{hr} = \left(1,100 \frac{scf}{min}\right) \left(\frac{mole}{385 scf}\right) \left(\frac{0.0172 moles_{voc}}{100 moles}\right) \left(\frac{57.895 lb_{voc}}{mole_{voc}}\right) \left(\frac{60 min}{hr}\right) = 1.7 \frac{lb_{voc}}{hr}$$

The starter was assumed to operate for 30 seconds per starting event resulting in 0.01 lbs of VOC emitted per starting event. It is estimated that there are 52 starting events per year for each engine. The VOC emissions are estimated at 0.0004 tpy for each compressor and 0.004 tpy VOC for all ten compressors.

#### **Cylinder Rod Packing Vents**

Compressor cylinder rod packing gas leakage is a continuous source of compressor emissions. Gas will leak from the packing and within the distance piece, and a vent is typically provided either at both the packing flange and distance piece, or just at the distance piece to direct this gas outside of any building the compressor may be housed within. EPA GasStar reports indicated vent rates of about 12 scfh for new state of the art best performing seals, and these rates can be as high as 900 scfh depending upon seal wear. Canadian/GRI research reports typical rod packing vent rates for standard seals of between 60 and 120 scfh. Vent rates are typically 30 percent higher when the compressor is idle and pressurized. The 60 scfh leakage rate along with a typical facility gas analysis was applied to determine VOC emissions from the facility gas compressor packing.

#### Assumptions:

Gas VOC MW	57.895	lb/mole
Gas Molar Volume	385	scf/mole
Gas VOC Mole %	0.0172	%
Number of Cylinders	4	
Vent Volume	60	scf/cylinde
Vent Rate	240	scf/hr
Total Vent Volume	2102.4	Mscf/yr

Compressor Packing Vent Emissions 
$$= \frac{\left(60 \frac{scf}{hr - cyl}\right) \left(4 \frac{cyl}{comp}\right) \left(\frac{0.0172 \, mole_{voc}}{100 \, mole}\right) \left(57.895 \frac{lb_{voc}}{mole_{voc}}\right) \left(8,760 \frac{hr}{yr}\right)}{\left(\frac{385 \, scf}{mole}\right) \left(2,000 \frac{lb}{ton}\right)} = 0.03 \frac{ton}{yr - comp}$$

Annual VOC Emissions

0.03 ton VOC/year per compressor

0.3 ton VOC/year for all compressors

## TANKS 4.0.9D OUTPUT LUBRICATING OIL STORAGE TANKS

#### **TANKS 4.0.9d Emissions Report - Detail Format Tank Indentification and Physical Characteristics**

Lubricating Oil Storage Tanks

Identification
User Identification:
City:
State:
Company:
Type of Tank:
Description:

Libricating Oil Storage Tariks Ignacio Colorado Samson Resources Horizontal Tank Spring Creek 500 gallon lubricating oil tanks

Tank Dimensions
Shell Length (ft):
Diameter (ft):
Volume (gallons):
Turnovers:

5.00 4.00 500.00 18.00 9,000.00

Net Throughput(gal/yr): Is Tank Heated (y/n): Is Tank Underground (y/n):

Paint Characteristics Shell Color/Shade: Shell Condition

Gray/Medium Good

Breather Vent Settings Vacuum Settings (psig): Pressure Settings (psig) -0.03 0.03

Meterological Data used in Emissions Calculations: Alamosa, Colorado (Avg Atmospheric Pressure = 11.19 psia)

#### TANKS 4.0.9d Emissions Report - Detail Format Liquid Contents of Storage Tank

Lubricating Oil Storage Tanks - Horizontal Tank Ignacio, Colorado

Mixture/Component	Month		ily Liquid Su perature (de Min.		Liquid Bulk Temp (deg F)	Vapo Avg.	r Pressure Min.	(pala) Max.	Vapor Mol. Weight.	Liquid Mass Fract.	Vapor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calculations
Lube Oil	All	51.76	37.44	66.07	44.16	0.0004	0.0002	0.0008	700.0000			0.01	

#### TANKS 4.0.9d Emissions Report - Detail Format Detail Calculations (AP-42)

## Lubricating Oil Storage Tanks - Horizontal Tank Ignacio, Colorado

Annual Emission Calcaulations	
Standing Losses (lb):	0.0795
Vapor Space Volume (cu ft):	40.0203
Vapor Density (lb/cu ft):	0.0001
Vapor Space Expansion Factor:	0.1066
Vented Vapor Saturation Factor:	1.0000
Tank Vapor Space Volume:	
Vapor Space Volume (cu ft):	40.0203
Tank Diameter (ft):	4.0000
Effective Diameter (ft):	5.0475
Vapor Space Outage (ft):	2.0000
Tank Shell Length (ft):	5.0000
Vapor Density	
Vapor Density (lb/cu ft):	0.0001
Vapor Molecular Weight (lb/lb-mole):	700.0000
Vapor Pressure at Daily Average Liquid	
Surface Temperature (psia):	0.0004
Daily Avg. Liquid Surface Temp. (deg. R):	511.4276
Daily Average Ambient Temp. (deg. F):	41.0750
Ideal Gas Constant R	10.731
(psia cuft / (lb-mol-deg R)):	503.8250
Liquid Bulk Temperature (deg. R):	0.6800
Tank Paint Solar Absorptance (Shell): Daily Total Solar Insulation	0.0000
Factor (Btu/sqft day):	1,667.4918
Vapor Space Expansion Factor	
Vapor Space Expansion Factor:	0.1086
Daily Vapor Temperature Range (deg. R):	57.2610
Daily Vapor Pressure Range (pala):	0.0004
Breather Vent Press. Setting Range(pala):	0.0800
Vapor Pressure at Daily Average Liquid	
Surface Temperature (psia):	0.0004
Vapor Pressure at Daily Minimum Liquid	
Surface Temperature (psia):	0.0002
Vapor Pressure at Daily Maximum Liquid	
Surface Temperature (psia):	0.0000
Daily Avg. Liquid Surface Temp. (deg R):	511.4270
Daily Min. Liquid Surface Temp. (deg R):	497.1123
Daily Max. Liquid Surface Temp. (deg R):	525.7428
Daily Ambient Temp. Range (deg. R):	35.433
Vented Vapor Saturation Factor	
Vented Vapor Saturation Factor:	1.0000
Vapor Pressure at Daily Average Liquid:	
Surface Temperature (psia):	0.0004
Vapor Space Outage (ft):	2.0000
Morking Losses (fb):	0.0456
Working Losses (lb): Vapor Molecular Weight (lb/lb-mole):	700.000
Vapor Pressure at Daily Average Liquid	700.000
	0.000
Surface Temperature (pala): Annual Net Throughput (gal/yr.):	9,000,000
Annual Turnovers:	18.000
	1.0000
Turnover Factor:	4.000
Tank Diameter (ft):	0.750
Working Loss Product Factor:	0.750

#### TANKS 4.0.9d Emissions Report - Detail Format Individual Tank Emission Totals

**Emissions Report for: Annual** 

Lubricating Oil Storage Tanks - Horizontal Tank Ignacio, Colorado

	Losses(lbs)									
Components	Working Loss	Breathing Loss	Total Emissions							
Lube Oil	0.05	0.08	0.12							

TANKS 4.0.9D OUTPUT SKID DRAINS TANKS

#### **TANKS 4.0.9d Emissions Report - Detail Format Tank Indentification and Physical Characteristics**

Identification
User Identification:
City:
State:
Company:
Type of Tank:
Description: Skid Drains Tanks Ignacio Colorado Samson Resources Horizontal Tank Spring Creek 500 gallon skid drains tanks

Tank Dimensions Shell Length (ft): Diameter (ft): Volume (gallons): 5.00 4.00 500.00 12.00 6,000.00 Turnovers:
Net Throughput(gal/yr):
Is Tank Heated (y/n):
Is Tank Underground (y/n):

Paint Characteristics Shell Color/Shade: Shell Condition Gray/Medium Good

Breather Vent Settings Vacuum Settings (psig): Pressure Settings (psig)

Meterological Data used in Emissions Calculations: Alamosa, Colorado (Avg Atmospheric Pressure = 11.19 psia)

#### TANKS 4.0.9d Emissions Report - Detail Format Liquid Contents of Storage Tank

Skid Drains Tanks - Horizontal Tank Ignacio, Colorado

Mbture/Component	Month		illy Liquid So perature (de Min.		Liquid Bulk Temp (deg F)	Vapo Avg.	or Pressure Min.	(pala) Max.	Vapor Mol. Weight.	Liquid Mass Fract.	Vapor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calculations
Skid Drains	All	51.78	37.44	66.07	44.16	0.0004	0.0002	0.0006	700.0000			0.00	

#### TANKS 4.0.9d Emissions Report - Detail Format Detail Calculations (AP-42)

### Skid Drains Tanks - Horizontal Tank Ignacio, Colorado

Standing Losses (lb):	0.0798
Vapor Space Volume (cu ft):	40.0203
Vapor Density (lb/cu ft):	0.000
Vapor Space Expansion Factor:	0.1086
Vented Vapor Saturation Factor:	1.0000
Tank Vapor Space Volume:	
Vapor Space Volume (cu ft):	40.0203
Tank Diameter (ft):	4.0000
Effective Diameter (ft):	5.0475
Vapor Space Outage (ft):	2.0000
Tank Shell Length (ft):	5.0000
Vapor Density	
Vapor Density (lb/cu ft):	0.000
Vapor Molecular Weight (lb/lb-mole):	700.0000
Vapor Pressure at Daily Average Liquid	
Surface Temperature (psia):	0.0004
Daily Avg. Liquid Surface Temp. (deg. R):	511.4270
Daily Average Ambient Temp. (deg. F):	41.0750
Ideal Gas Constant R	
(psia cuft / (lb-mol-deg R)):	10.73
Liquid Bulk Temperature (deg. R):	503.8250
Tank Paint Solar Absorptance (Shell):	0.6800
Daily Total Solar Insulation	
Factor (Btu/sqft day):	1,087.491
Vapor Space Expansion Factor	
Vapor Space Expansion Factor:	0.106
Daily Vapor Temperature Range (deg. R):	57.261
Daily Vapor Pressure Range (pala):	0.000
Breather Vent Press. Setting Range(pala): Vapor Pressure at Daily Average Liquid	0.080
Surface Temperature (psia):	0.000
Vapor Pressure at Daily Minimum Liquid	
Surface Temperature (psia):	0.000
Vapor Pressure at Dally Maximum Liquid	
Surface Temperature (pala):	0.000
Daily Avg. Liquid Surface Temp. (deg R): Daily Min. Liquid Surface Temp. (deg R):	511.427
Daily Min. Liquid Surface Temp. (deg R):	497.112
Daily Max. Liquid Surface Temp. (deg R):	525.742
Daily Ambient Temp. Range (deg. R):	35.433
Vented Vapor Saturation Factor	
Vented Vapor Saturation Factor:	1.000
Vapor Pressure at Daily Average Liquid:	
Surface Temperature (paia):	0.000
Vapor Space Outage (ft):	2.000
Marking Laces (B)	0.040
Working Losess (lb): Vapor Molecular Weight (lb/lb-mole):	700.000
Vapor Molecular Vieigni (iono-mole).	700.000
Vapor Pressure at Dally Average Liquid	0.000
Surface Temperature (pala): Annual Net Throughput (gal/yr.):	6.000.000
Annual Turnovers:	12.000
Turnover Factor:	1,000
Tank Diameter (ft):	4.000
Working Loss Product Factor:	1.000
Working Loss Floduce Factor:	1.000

#### TANKS 4.0.9d Emissions Report - Detail Format Individual Tank Emission Totals

#### **Emissions Report for: Annual**

Skid Drains Tanks - Horizontal Tank Ignacio, Colorado

		Losses(lbs)	
Components	Working Loss	Breathing Loss	Total Emissions
Skid Drains	0.04	0.08	0.12

## TANKS 4.0.9D OUTPUT ETHYLENE GLYCOL STORAGE TANKS

#### **TANKS 4.0.9d Emissions Report - Detail Format Tank Indentification and Physical Characteristics**

Identification
User Identification:
City:
State:
Company:
Type of Tank:
Description: Ethylene Glycol Tanks Ignacio Colorado Samson Resources Horizontal Tank Spring Creek 500 gallon Ethylene Glycol Tanks

Tank Dimensions
Shell Length (ft):
Diameter (ft):
Volume (gallons):
Turnovers:
Net Throughput(gal/yr):
Is Tank Heated (y/n):
Is Tank Underground (y/n): 5.00 4.00 500.00 18.00 9,000.00

Paint Characteristics Shell Color/Shade: Shell Condition Gray/Medium Good

Breather Vent Settings Vacuum Settings (psig): Pressure Settings (psig) -0.03 0.03

Meterological Data used in Emissions Calculations: Alamosa, Colorado (Avg Atmospheric Pressure = 11.19 psia)

#### TANKS 4.0.9d Emissions Report - Detail Format Liquid Contents of Storage Tank

Ethylene Glycol Tanks - Horizontal Tank Ignacio, Colorado

Mbdure/Component	Month		ily Liquid Soperature (de Min.		Liquid Bulk Temp (deg F)	Vapo Avg.	r Pressure	(pala) Max.	Vapor Mol. Weight.	Liquid Mass Fract	Vapor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calculations
Triethylene Glycol	All	51.78	37.44	66.07	44.16	0.0193	0.0193	0.0193	150.2000			0.00	

#### TANKS 4.0.9d Emissions Report - Detail Format Detail Calculations (AP-42)

## Ethylene Glycol Tanks - Horizontal Tank Ignacio, Colorado

Annual Emission Calcaulations	
Standing Losses (ib):	0.820
Vapor Space Volume (cu ft):	40.0203
Vapor Density (lb/cu ft):	0.0008
Vapor Space Expansion Factor:	0.108
Vented Vapor Saturation Factor:	0.998
Tank Vapor Space Volume:	
Vapor Space Volume (cu ft):	40.020
Tank Diameter (ft):	4.000
Effective Diameter (ft):	5.047
Vapor Space Outage (ft):	2.000
Tank Shell Length (ft):	5.000
Vapor Density	
Vapor Density (lb/cu ft):	0.000
Vapor Molecular Weight (lb/lb-mole):	150.200
Vapor Pressure at Daily Average Liquid	
Surface Temperature (psia):	0.019
Daily Avg. Liquid Surface Temp. (deg. R):	511.427
Daily Average Ambient Temp. (deg. F): Ideal Gas Constant R	41.075
(pala cuft / (lb-mol-deg R)):	10.73
Liquid Bulk Temperature (deg. R):	503.825
Tank Paint Solar Absorptance (Shell):	0.680
Daily Total Solar Insulation Factor (Btu/sqft day):	1,667.491
Vapor Space Expansion Factor	
Vapor Space Expansion Factor:	0.108
Daily Vapor Temperature Range (deg. R):	57.261
Dally Vapor Pressure Range (pala):	0.000
Breather Vent Press. Setting Range(pala):	0.060
Vapor Pressure at Daily Average Liquid	
Surface Temperature (psia):	0.019
Vapor Pressure at Daily Minimum Liquid	
Surface Temperature (psia):	0.019
Vapor Pressure at Daily Maximum Liquid	
Surface Temperature (pala):	0.019
Daily Avg. Liquid Surface Temp. (deg R):	511.427
Dally Min. Liquid Surface Temp. (deg R):	497.112
Daily Max. Liquid Surface Temp. (deg R):	525.742
Daily Ambient Temp. Range (deg. R):	35.433
Vented Vapor Saturation Factor	
Vented Vapor Saturation Factor:	0.998
Vapor Pressure at Daily Average Liquid:	0.019
Surface Temperature (pala): Vapor Space Outage (ft):	2.000
Working Losses (ib):	0.621
Vapor Molecular Weight (Ib/Ib-mole): Vapor Pressure at Dally Average Liquid	150.200
	0.019
Surface Temperature (psia):	9,000.000
Annual Net Throughput (gal/yr.):	18.000
Annual Turnovers:	1.000
Turnover Factor:	4.000
Tank Diameter (ft): Working Loss Product Factor:	1,000
Working Loss Froduct Factor:	1.000
Total Losses (lb):	1.442

#### TANKS 4.0.9d Emissions Report - Detail Format Individual Tank Emission Totals

**Emissions Report for: Annual** 

Ethylene Glycol Tanks - Horizontal Tank Ignacio, Colorado

Components	Losses(lbs)									
	Working Loss	Breathing Loss	Total Emissions							
Triethylene Glycol	0.62	0.82	1.44							

TANKS 4.0.9D OUTPUT WASTE OIL/SLOP TANKS

#### **TANKS 4.0.9d Emissions Report - Detail Format Tank Indentification and Physical Characteristics**

Waste Oil/Used Oil Storage Tank

Identification
User Identification:
City:
State:
Company:
Type of Tank:
Description:

Ignacio Colorado Samson Resources Horizontal Tank Spring Creek 500 gallon waste oil tanks

Tank Dimensions
Shell Length (ft):
Diameter (ft):
Volume (gallons):
Turnovers:
Net Throughput(gal/yr):
Is Tank Heated (y/n):
Is Tank Underground (y/n): 5.00 4.00 500.00 6.00 3,000.00

Paint Characteristics Shell Color/Shade: Shell Condition Gray/Medium Good

Breather Vent Settings Vacuum Settings (psig): Pressure Settings (psig) -0.03 0.03

Meterological Data used in Emissions Calculations: Alamosa, Colorado (Avg Atmospheric Pressure = 11.19 psia)

#### TANKS 4.0.9d Emissions Report - Detail Format Liquid Contents of Storage Tank

Waste Oil/Used Oil Storage Tank - Horizontal Tank Ignacio, Colorado

Mixture/Component	Month	Tem	ily Liquid So perature (de Min.		Liquid Bulk Temp (deg F)	Vapo Avg.	or Pressure Min.	(psia) Max.	Vapor Mol. Weight.	Liquid Mass Fract.	Vapor Mass Fract	Mol. Weight	Basis for Vapor Pressure Calculations
Used Oil	All	51.76	37.44	66.07	44.16	0.0004	0.0002	0.0006	700.0000			0.00	

#### TANKS 4.0.9d Emissions Report - Detail Format Detail Calculations (AP-42)

### Waste Oil/Used Oil Storage Tank - Horizontal Tank Ignacio, Colorado

Annual Emission Calcaulations	
Standing Losses (lb):	0.0795
Vapor Space Volume (cu ft):	40.0203
Vapor Density (lb/cu ft):	0.0001
Vapor Space Expansion Factor:	0.1086
Vented Vapor Saturation Factor:	1.0000
Tank Vapor Space Volume:	
Vapor Space Volume (cu ft):	40.0203
Tank Diameter (ft): Effective Diameter (ft):	5.0475
Vapor Space Outage (ft):	2.0000
Tank Shell Length (ft):	5.0000
Vapor Density	
Vapor Density (lb/cu ft):	0.0001
Vapor Molecular Weight (lb/lb-mole):	700.0000
Vapor Pressure at Daily Average Liquid	
Surface Temperature (psia):	0.0004 511.4276
Daily Avg. Liquid Surface Temp. (deg. R): Daily Average Ambient Temp. (deg. F):	41.0750
Ideal Gas Constant R	41.0750
(psia cuft / (lb-mol-deg R)):	10.731
Liquid Bulk Temperature (deg. R):	503.8250
Tank Paint Solar Absorptance (Shell): Daily Total Solar Insulation	0.6800
Factor (Btu/sqft day):	1,007.4918
Vapor Space Expansion Factor	
Vapor Space Expansion Factor:	0.1066
Daily Vapor Temperature Range (deg. R):	57.2610
Daily Vapor Pressure Range (psia):	0.0004
Breather Vent Press. Setting Range(psia): Vapor Pressure at Daily Average Liquid	0.0800
Surface Temperature (psia):	0.0004
Vapor Pressure at Daily Minimum Liquid	
Surface Temperature (psia):	0.0002
Vapor Pressure at Daily Maximum Liquid	
Surface Temperature (psia):	0.0006 511.4276
Daily Avg. Liquid Surface Temp. (deg R): Daily Min. Liquid Surface Temp. (deg R):	497.1123
Daily Max. Liquid Surface Temp. (deg R):	525.7428
Daily Ambient Temp. Range (deg. R):	35.4333
Vented Vapor Saturation Factor	
Vented Vapor Saturation Factor:	1.0000
Vapor Pressure at Daily Average Liquid: Surface Temperature (psia):	0.0004
Vapor Space Outage (ft):	2.0000
Working Losses (Ib):	0.0200
Vapor Molecular Weight (Ib/Ib-mole):	700.0000
Vapor Pressure at Daily Average Liquid Surface Temperature (psia):	0.0004
Annual Net Throughput (gal/yr.):	3,000.0000
Annual Tumovers:	6.000
Turnover Factor:	1.0000
Tank Diameter (ft):	4.0000
Working Loss Product Factor:	1.0000
Total Losses (lb):	0.0998

#### TANKS 4.0.9d Emissions Report - Detail Format Individual Tank Emission Totals

#### **Emissions Report for: Annual**

Waste Oil/Used Oil Storage Tank - Horizontal Tank Ignacio, Colorado

		Losses(lbs)	
Components	Working Loss	Breathing Loss	Total Emissions
Used Oil	0.02	0.08	0.10

## TANKS 4.0.9D OUTPUT SLOP TANK

Breather Vent Settings Vacuum Settings (psig): Pressure Settings (psig)

## TANKS 4.0.9d Emissions Report - Detail Format Tank Indentification and Physical Characteristics

Identification User Identification: City: State: Company: Type of Tank: Description:	Slop Tank Ignacio Colorado Samson Resources Vertical Fixed Roof Tank Spring Creek 400 bbl Slop Tank
Tank Dimensions Shell Height (ft): Diameter (ft): Liquid Height (ft): Avg. Liquid Height (ft): Volume (gallons): Turnovers: Net Throughput(gal/yr): Is Tank Heated (y/n):	20.00 12.50 19.00 10.00 17,442.02 12.00 209,304.20
Paint Characteristics Shell Color/Shade: Shell Condition Roof Color/Shade: Roof Condition:	Gray/Light Good Gray/Medium Good
Roof Characteristics Type: Height (ft) Slope (ft/ft) (Cone Roof)	Cone 1.00 0.00

Meterological Data used in Emissions Calculations: Alamosa, Colorado (Avg Atmospheric Pressure = 11.19 psia)

-0.03 0.03

#### TANKS 4.0.9d Emissions Report - Detail Format Liquid Contents of Storage Tank

Slop Tank - Vertical Fixed Roof Tank Ignacio, Colorado

Mixture/Component	Month		lly Liquid Su perature (de Min.		Liquid Bulk Temp (deg F)	Vapo Avg.	r Pressure	(peia) Max.	Vapor Mol. Weight.	Liquid Mass Fract.	Vapor Mass Fract.	Mol. Weight	Basis for Vapor Pressure Calculations
maximo component	Moliui	Ush.	IVIII.	IVIIIA.	(0091)	Little.		IVIIIA	Troigin.	11000	T Tarot.	TTOIGH	Cercuration
Slop/Lube Oil	All	50.60	37.10	64.10	43.74	0.0004	0.0002	0.0006	700.0000			0.00	

#### TANKS 4.0.9d Emissions Report - Detail Format Detail Calculations (AP-42)

## Slop Tank - Vertical Fixed Roof Tank Ignacio, Colorado

Vapor Space Volume (cu ft):	Annual Emission Calcaulations	
\( Vapor Space Volume (cu ft): \( 1,286.06 \) \( Vapor Density (blocu ft): \( 0,000 \) \( Vapor Density (blocu ft): \( 0,000 \) \( Vapor Space Expension Factor: \) \( Vapor Space Expension Factor: \) \( Vapor Space Volume (cu ft): \) \( Vapor Unage (Cone Roof) \) \( Roof Outage (Cone Roof) \) \( Roof Outage (Cone Roof) \) \( Roof Valtage (Cone Roof) \) \( Vapor Density \) \( Vapor Density \) \( Vapor Density \) \( Vapor Density \) \( Vapor Molecular Weight (blit)-mole) \) \( Vapor Molecular Meight (blit) \) \( Vapor Molecular Weight (blit) \) \( Vapor Molecular Weight (blit)-mole) \) \( Vapor Molecu	Standing Losses (lb):	2.377
Vapor Density (IbCut ft):         0.00           Vapor Space Expansion Factor:         0.10           Vapor Space Expansion Factor:         0.00           Vapor Space Expansion Factor:         0.00           Vapor Space Volume:         1.286.00           Tank Daroor Space Volume (cut ft):         1.286.00           Vapor Space Outinge (ft):         1.25.           Tank Shall Height (ft):         1.00.00           Roof Outinge (ft):         0.33           Roof Outinge (ft):         1.00           Roof Outinge (ft):         0.00           Roof Outinge (ft):         0.00           Roof Space (Cone Roof)         0.00           Vapor Density         0.00           Vapor Density         0.00           Vapor Density (IbCut ft):         0.00           Vapor Density         0.00           Vapor Density         0.00           Vapor Density         0.00           Vapor D	Vapor Space Volume (cu ft):	1,268.090
Vapor Space Expansion Factor:         0.16           Vented Vapor Space Volume:         1,286.06           Vapor Space Volume (cu ft):         1,286.07           Tank Vapor Space Volume (cu ft):         1,286.07           Tank Damelser (ft):         12.56           Vapor Space Cutlage (ft):         10.33           Tank Shaff Height (ft):         10.35           Tank Shaff Height (ft):         0.03           Roof Cuttage (Cone Roof)         Roof Cuttage (Cone Roof)           Roof Outage (Ift):         0.03           Roof Height (ft):         1.00           Roof Slope (ft/ft):         0.00           Vapor Badius (ft):         0.02           Vapor Melecular Weight (IbVIb-mole):         0.00           Vapor Melecular Weight (IbVIb-mole):         0.00           Vapor Melecular Weight (IbVIb-mole):         0.00           Vapor Melecular Weight (IbVIb-mole):         41.00           Vapor Pensure at Cally Average Liquid         0.00           Saliva Temperature (pale):         1.00           Ideal Cas Constant R         1.01           Ideal Cas Constant R         1.02           Ideal Cas Constant R         1.03           Ideal Cas Absorptance (Shell):         0.05           Inark Palnt Solar Absorptance (Sh	Vapor Density (lb/cu ft):	0.000
Venited Vapor Saturation Factor:         0,96           Tank Damos Space Volume (cu ft):         1,286.06           Vapor Space Volume (cu ft):         1,286.06           Tank Damester (ft):         12,56           Vapor Space Cuttage (ft):         10,56           Yapor Space Cuttage (ft):         10,56           Tank Shell Height (ft):         20,00           Average Liquid Height (ft):         0,33           Roof Outage (ft):         0,33           Roof Outage (ft):         0,00           Roof Outage (ft):         0,00           Roof Space (Mft):         0,00           Shell Radius (ft):         0,00           Appor Density         0,00           Shell Radius (ft):         0,00           Vapor Density (blou ft):         0,00           Vapor Pressure at Daily Average Liquid         0,00           Surface Temperature (deg, ft):	Vapor Space Expansion Factor:	0.100
\( Vapor Space Volume (cut ft): 1,286.00	Vented Vapor Saturation Factor:	0.999
\( Vapor Space Volume (cut ft): 1,286.00	Fank Vapor Space Volume:	
Vapor Space Outlage (ft): 10.33	Vapor Space Volume (cu ft):	1,268.090
Tank Shell Height (ft): 20.00  Roof Outage (Cone Roof)  Roof Outage (Cone Roof)  Roof Outage (Th): 0.33  Roof Height (ft): 1.00  Roof Outage (Th): 0.33  Roof Height (ft): 1.00  Roof Outage (Th): 0.33  Roof Height (ft): 1.00  Roof Stope (Th): 0.00  Roof Height (ft): 1.00  Roof Stope (Th): 0.00  Roof Density  Vapor Density (Ibcu ft): 0.00  Vapor Pressure at Daily Average Liquid  Surface Temperature (Roof): 0.00  Jaily Avy, Liquid Surface Temp. (deg. R): 510.21  Joint Jaily Average Ambient Temp. (deg. F): 541.07  Joint Jaily Average Ambient Temp. (deg. F): 540.21  Liquid Bulk Temperature (deg. R): 553.46  Tank Parist Soiar Absorptance (Roof): 0.66  Daily Yaor Space Expansion Factor  Vapor Pressure at Daily Average Liquid  Surface Temperature (pois): 0.00  Roof Space Expansion Factor 0.00  Vapor Pressure at Daily Average Liquid  Surface Temperature (pois): 0.00  Vapor Pressure at Daily Maximum Liquid  Surface Temperature (pois): 0.00  Jaily Ave, Liquid Surface Temp. (deg R): 50.21  Daily Average Liquid Surface	Tank Diameter (ft):	12.500
Average Liquid Height (ft): (10.00 Roof Outage (10): 0.33 Roof Outage (10): 0.33 Roof Outage (10): 0.33 Roof Height (ft): 1.00 Roof Outage (10): 0.33 Roof Height (ft): 1.00 Roof Stope (17/ft): 0.00 Sheel Radius (ft): 1.00 Vapor Density (10): 0.00 Vapor Molecular Weight (10/fb-mole): 0.00 Vapor Molecular Weight (10/fb-mole): 0.00 Vapor Molecular Weight (10/fb-mole): 0.00 Vapor Pressure at Daily Average Liquid 0.00 Surface Temperature (pola): 0.00 Surface Temperature (pola): 0.00 Daily Average Ambient Temp. (deg. R): 10.27 Daily Average Ambient Temp. (deg. R): 10.21 Daily Average Ambient Fector (Shell): 0.00 Vapor Space Expansion Factor (Shell): 0.00 Vapor Space Expansion Factor (10) Daily Vapor Temperature Range (deg. R): 10.21 Daily Vapor Temperature Range (pola): 0.00 Daily Vapor Temperature (pola): 0.00 Surface Temperature (pola): 0.00 Surface Temperature (pola): 0.00 Surface Temperature (pola): 0.00 Vapor Pressure at Daily Average Liquid 0.00 Surface Temperature (pola): 0.00 Daily Vap. Liquid Surface Temp. (deg. R): 10.27 Daily Max. Liquid	Vapor Space Outage (ft):	10.333
Roof Outage (R):		20.000
Roof Cutage (ft):		10.000
Roof Cutage (ft):	Poof Outene (Cone Boof)	
Roof Helgrit (ft):		0.333
Roof Slope (fifth);		1.000
Shell Radius (ft):		0.000
Vapor Density (libcu ft):         0.00           Vapor Molecular Weight (Ibrilb-mole):         700.00           Vapor Pressure at Daily Average Liquid         0.00           Surface Temperature (pola):         0.00           Daily Avy, Liquid Surface Temp. (deg. R):         41.07           Ideal Gas Constant R         10.21           Ideal Gas Constant R         10.21           Ideal Gas Constant R         10.21           Tank Pairt Solar Absorptance (Reof):         0.5           Tank Pairt Solar Absorptance (Reof):         0.6           Tank Pairt Solar Absorptance (Reof):         0.6           Pairt Total Solar Installation         0.6           Factor (Btu/agft day):         1,867.46           /apor Space Expansion Factor         0.1           Vapor Space Expansion Factor         0.1           Vapor Space Expansion Factor         0.1           Vapor Pressure at Daily Average Liquid         0.0           Surface Temperature (pola):         0.0           Vapor Pressure at Daily Maximum Liquid         0.0           Surface Temperature (pola):         0.0           Vapor Pressure at Daily Maximum Liquid         0.0           Surface Temperature (pola):         0.0           Vapor Pressure at Daily Maximum Liquid         0.0 </td <td></td> <td>6.250</td>		6.250
Vapor Molecular Weight (IbNb-mole):         700,000           Vapor Pressure at Daily Average Liquid         0.00           Surface Temperature (pola):         510,22           Daily Average Ambient Temp. (deg. R):         510,22           Daily Average Ambient Temp. (deg. R):         41,01           Ideal Gas Constant R         (pola cutt / (lb-mol-deg R)):         503,44           Liquid Bulk Temperature (deg. R):         503,44           Tank Plant Soler Absorptance (Roof):         0.56           Tank Plant Soler Absorptance (Roof):         0.57           Factor (Blusder) Barrier (Roof):         0.57           Factor (Blusder) Barrier (Roof):         0.57           Japor Space Expansion Factor:         0.10           Vapor Space Expansion Factor         0.10           Vapor Space Expansion Factor         0.1           Daily Vapor Pressure Rarge (deg. R):         53,06           Daily Vapor Pressure Rarge (deg. R):         53,06           Daily Vapor Pressure Rarge (deg. R):         0.00           Surface Temperature (pola):         0.00           Surface Temperature (pola):         0.00           Surface Temperature (pola):         0.00           Daily Ambient Temp. Range (deg. R):         510,22           Daily Ambient Temp. Range (deg. R):         <		
Vapor Pressure at Daily Average Liquid         0.00           Surface Temperature (poisa)         0.00           Daily Avy Liquid Surface Temp. (deg. R):         510.21           Daily Average Ambient Temp. (deg. F):         410.01           Ideal Gas Constant R         (poisa cutf. (bir-mol-deg R)):         503.40           Liquid Bulk Temperature (deg. R):         503.40           Tank Parist Solar Absorptance (Shell):         0.5           Tank Parist Solar Absorptance (Roof):         0.60           Daily Total Solar Insulation         1,667.46           Yapor Space Expansion Factor         Vapor Space Expansion Factor           Vapor Space Expansion Factor         1,667.46           Vapor Pressure Range (deg. R):         53.00           Daily Vapor Pressure Range (deg. R):         50.00           Vapor Pressure at Daily Average Liquid         50.00           Surface Temperature (poisa):         0.00           Vapor Pressure at Daily Maximum Liquid         50.00           Surface Temperature (poisa):         0.00           Vapor Pressure at Daily Maximum Liquid         50.00           Surface Temperature (poisa):         0.00           Daily Average Liquid Surface Temp. (deg R):         400.77           Daily Average Liquid Surface Temp. (deg R):         400.77      <		0.000
Surface Temperature (pola): Daily Average Ambient Temp. (deg. R): 510,22 Daily Average Ambient Temp. (deg. R): Daily Average Ambient Temp. (deg. F): (deal Gas Constant R (pola cuft / (lb-mol-deg R)): Liquid Bulk Temperature (deg. R): Tank Parist Solar Absorptance (Shell): Tank Parist Solar Absorptance (Roof): Daily Total Solar Insulation Factor (Bulker) Absorptance (Roof): Daily Total Solar Insulation Bulker) Ambient Temperature Range (deg. R): Daily Vepor Temperature Range (deg. R): Daily Vepor (Pressure at Daily Marianum Liquid Surface Temperature (pola): Daily Ambient Temp. (deg. R): Daily Ambient Temp. Range (		700.000
Daily Avg. Liquid Surface Temp. (deg. R): 510.21 Daily Average Ambient Temp. (deg. F): 41.05 Ideal Gas Constant R (pais cut/ (l/b-mol-deg R): 503.44 Tank Paint Solar Absorptance (Shell): 0.54 Tank Paint Solar Absorptance (Shell): 0.53 Tank Paint Solar Absorptance (Roof): 0.66 Daily Total Solar Insulation Factor (Blufar) day): 1,867.46 Tank Paint Solar Absorptance (Roof): 0.66 Daily Total Solar Insulation Factor (Blufar) day): 1,867.46 Tank Paint Solar Absorptance (Roof): 0.66 Daily Total Solar Insulation Factor (Blufar) day): 1,867.46 Tank Paint Solar Absorptance (Roof): 0.66 Daily Tagor Space Expansion Factor Vapor Space Expansion Factor Vapor Space Expansion Factor Vapor Pressure at Daily Average Liquid Surface Temperature Range (deg. R): 0.00 Tagor Pressure at Daily Average Liquid Surface Temperature (sola): 0.00 Tagor Pressure at Daily Maximum Liquid Surface Temperature (sola): 0.00 Daily Ayb, Liquid Surface Temp. (deg R): 510.21 Daily May, Liquid Surface Temp. (deg R): 52.77 Daily Max. Liquid		0.000
Dally Average Ambient Temp. (deg. F):  (deal Gas Constant R		
Ideal Gas Constant R	Daily Average Ambient Temp. (deg. R):	
(paia cuft / (lb-mol-deg R)): 10.1 Liquid Bulk Temperature (deg. R): 503.4 Tank Paint Solar Absorptance (Shell): 0.5 Tank Paint Solar Absorptance (Roof): 0.5 Daily Total Solar Insulation Factor (Shell): 1.6 Pactor (Blulydid My): 1.667.44 //spor Space Expansion Factor (Vapor Space Expansion Factor (Daily Vapor Pensure Range (deg. R): 53.0 Daily Vapor Pressure Range (gela): 0.00 Pressure at Daily Average Liquid 0.00 Surface Temperature (paia): 0.00 Surface Tem	Ideal Gas Constant R	41.070
Liquid Bulk Temperature (deg. R): 503.44 Tank Paint Solar Absorptance (Shell): 0.54 Tank Paint Solar Absorptance (Shell): 0.54 Tank Paint Solar Absorptance (Roof): 0.66 Daily Total Solar Insulation Factor (Bull/art) day): 1,667.44 Vapor Space Expansion Factor Vapor Space Expansion Factor Vapor Space Expansion Factor Vapor Space Expansion Factor Vapor Pressure Range (neig. S.3,68) Daily Vapor Pressure Range (psig. S.3,68) Daily Vapor Pressure at Daily Average Liquid Surface Temperature (psig.) 0.00 Vapor Pressure at Daily Average Liquid Surface Temperature (psig.) 0.00 Vapor Pressure at Daily Maximum Liquid Surface Temperature (psig.) 0.00 Vapor Pressure at Daily Maximum Liquid Surface Temperature (psig.) 0.00 Daily Avg. Liquid Surface Temp. (deg R): 510.27 Daily Max. Liquid Surface Temp. (deg R): 406.77 Daily Max. Liquid Surface Temp. (deg R): 523.77 Daily Max. Liquid Surface Temp.	(psia cuft / (lb-mol-deg R)):	10.73
Tank Paint Solar Absorptance (Shell): 0.5. Tank Paint Solar Absorptance (Roof): 0.6. Daily Total Solar Insulation Factor (Sapor Space Expansion Factor (Papor Space Expansion (	Liquid Bulk Temperature (deg. R):	503.405
Delily Total Solar Insulation Factor (Bluvgrid day):  /apor Space Expansion Factor:  Vapor Space Expansion Factor:  Vapor Space Expansion Factor:  0.16 Delily Vapor Pressure Range (deg. R): Delily Vapor Pressure Range (psia): Delily Vapor Pressure Range (psia): Delily Vapor Pressure (psia): Delily Vapor Pressure (psia): OX Surface Temperature (psia): Vapor Pressure at Delily Average Liquid Surface Temperature (psia): Delily Aport Delily Minimum Liquid Surface Temperature (psia): Delily Aput Liquid Surface Temp. (deg R): Delily Ambient Temp. Range (deg. R): Delily Ambient Temp. Range (deg. R): Delily Aput Liquid Surface Temp. (deg R): Delily Aput Liquid	Tank Paint Solar Absorptance (Shell):	0.540
Factor (Blu/lar)t day);	Tank Paint Solar Absorptance (Roof):	0.680
Appor Space Expansion Factor   0.11		1,667,491
Vapor Space Expansion Factor:         0.15           Daily Vapor Pressure Range (deg. R):         53.00           Daily Vapor Pressure Range (psia):         0.00           Breather Vent Press. Setting Range (psia):         0.00           Vapor Pressure at Daily Average Liquid         0.00           Surface Temperature (psia):         0.00           Vapor Pressure at Daily Monimum Liquid         0.00           Surface Temperature (psia):         0.00           Vapor Pressure at Daily Monimum Liquid         0.00           Surface Temperature (psia):         0.00           Daily Avg. Liquid Surface Temp. (deg R):         0.00           Daily Avg. Liquid Surface Temp. (deg R):         409.7           Daily Avg. Liquid Surface Temp. (deg R):         523.7           Daily Ambient Temp. Range (deg. R):         523.7           Daily Amolient Temp. Range (deg. R):         0.00           Vented Vapor Saturation Factor:         0.00           Vapor Pressure at Daily Average Liquid:         0.00           Surface Temperature (psia):         0.00           Vapor Space Outage (ft):         1.33           Vapor Molecular Weight (lb/lb-mole):         700.00           Vapor Melecular Weight (lb/lb-mole):         0.00           Vapor Pressure at Daily Average Liquid:         0		1,007.401
Daily Vapor Temperature Range (deg. R): Daily Vapor Temperature Range (deg. R): Daily Vapor Tessaure Range (psia): 0.00 Breather Vent Press. Setting Range(psia): 0.00 Vapor Pressure at Daily Versepe Liquid Surface Temperature (psia): 0.00 Vapor Pressure at Daily Manimum Liquid Surface Temperature (psia): 0.00 Vapor Pressure at Daily Manimum Liquid Surface Temperature (psia): 0.00 Daily Any. Liquid Surface Temp. (deg R): Daily Ann. Liquid Surface Temp. (deg R): Daily Ann. Liquid Surface Temp. (deg R): Daily Annbient Temp. Range (deg. R): 0.00 Verted Vapor Saturation Factor Verted Vapor Saturation Factor: 0.00 Vapor Pressure at Daily Average Liquid: Surface Temperature (psia): 0.00 Vapor Opisco Outlage (R): 0.00 Vapor Opisco Outlage (R): 0.00 Vapor Melecuter Weight (IbHt-mole): 0.00 Vapor Annual Net Throughput (gallyr): 0.00 Vannual Net Throughput (gallyr): 0.00 Maximum Liquid Volume (gal): 0.00 Tank Diameter (R): 0.00 Tank Dia	Venor Space Expansion Factor  Venor Space Expansion Factor	0.100
Delly Vapor Pressure Range (psla): 0.00 Presenter Vent Press. Setting Range(psla): 0.00 Vapor Pressure at Delly Average Liquid Surface Temperature (psla): 0.00 Vapor Pressure at Delly Monimum Liquid Surface Temperature (psla): 0.00 Vapor Pressure at Delly Monimum Liquid Surface Temperature (psla): 0.00 Vapor Pressure at Delly Monimum Liquid Surface Temperature (psla): 5.10.2 Delly Avg. Liquid Surface Temp. (deg R): 5.00 Delly Avg. Liquid Surface Temp. (deg R): 400.7 Delly Avg. Liquid Surface Temp. (deg R): 5.22.7 Delly Ambient Temp. Range (deg. R): 5.23.7 Delly Ambient Temp. Range (deg. R): 5.23.7 Delly Ambient Temp. Range (deg. R): 5.23.7 Delly Average Saturation Factor: 0.00 Vapor Pressure at Delly Average Liquid: Surface Temperature (psla): 0.00 Vapor Space Outage (ft): 1.33 Vapor Molecular Weight (lb/lb-mole): 700.00 Vapor Pressure at Delly Average Liquid Surface Temperature (psla): 0.00 Vapor Molecular Weight (lb/lb-mole): 700.00 Vapor Pressure at Delly Average Liquid Surface Temperature (psla): 0.00 Vapor Molecular Weight (lb/lb-mole): 700.00 Vapor Molecul	Daily Vapor Temperature Range (deg. R):	53.992
Breather Vent Press. Setting Range(psia):   0.00	Dally Vapor Pressure Range (nsia):	0.000
Vapor Pressure at Daily Average Liquid Surface Temperature (pois).         0.00           Surface Temperature (pois).         0.00           Vapor Pressure at Daily Minimum Liquid Surface Temperature (pois).         0.00           Vapor Pressure at Daily Maximum Liquid Surface Temperature (pois).         0.00           Daily Any Liquid Surface Temp. (deg R):         480.7           Daily Any Liquid Surface Temp. (deg R):         480.7           Daily Max Liquid Surface Temp. (deg R):         582.7           Daily Ambez Liquid Surface Temp. (deg R):         582.7           Daily Ambez Liquid Surface Temp. (deg R):         58.7           Vented Vapor Saturation Factor         0.00           Vented Vapor Saturation Factor:         0.00           Vapor Pressure at Deily Average Liquid:         0.00           Surface Temperature (pois):         0.00           Vapor Space Outage (ft):         1.33           Vapor Molecular Weight (Ib/Ib-mole):         700.00           Vapor Pressure at Deily Average Liquid         0.00           Surface Temperature (pois):         0.00           Vapor Pressure at Deily Average Liquid         0.00           Surface Temperature (pois):         0.00           Vapor Molecular Weight (Ibrib-mole):         700.00           Vapor Inverse Testor:         0.00	Breather Vent Press, Setting Range(psia):	0.060
Surface Temperature (pola):		
Vapor Pressure at Daily Minimum Liquid         0.00           Surface Temperature (pois)         0.00           Vapor Pressure at Daily Maximum Liquid         0.00           Surface Temperature (pois)         0.00           Daily Any, Liquid Surface Temp, (deg R):         480-7.           Daily May, Liquid Surface Temp, (deg R):         480-7.           Daily Max, Liquid Surface Temp, (deg R):         523-7.           Daily Max, Liquid Surface Temp, (deg R):         523-7.           Daily Ambert Temp, Range (deg, R):         58-4.           Vented Vapor Saturation Factor:         0.00           Vapor Pressure at Deily Average Liquid:         0.00           Surface Temperature (pois):         10.33           Vapor Space Outage (fi):         1.33           Vapor Molecular Weight (Ib/Ib-mole):         700.00           Vapor Pressure at Deily Average Liquid         50-7.           Surface Temperature (pois):         0.00           Vapor Pressure at Deily Average Liquid         0.00           Surface Temperature (pois):         0.00           Annual Neil Throughput (gallyri):         209,304-22           Annual Tumover Temperature (pois):         17.442.0           Maximum Liquid Maximum (gall):         19.00           Tank Diameter (ft):         19.00 </td <td>Surface Temperature (psia):</td> <td>0.000</td>	Surface Temperature (psia):	0.000
Vapor Pressure at Daily Meximum Liquid           Surface Temperature (pola):         0.00           Daily Avg. Liquid Surface Temp. (deg R):         400.7           Daily May. Liquid Surface Temp. (deg R):         400.7           Daily Max. Liquid Surface Temp. (deg R):         523.7           Daily Ambert Temp. Range (deg. R):         524.7           Vented Vapor Saturation Factor:         0.00           Vapor Pressure at Daily Average Liquid:         0.00           Surface Temperature (psis):         0.00           Vapor Space Outage (ft):         1.33           Voorling Losses (lb):         1.30           Vapor Pressure at Daily Average Liquid         5.00           Surface Temperature (psis):         0.00           Vapor Pressure at Daily Average Liquid         0.00           Surface Temperature (psis):         0.00           Annual Neit Throughput (gallyr.):         209.304.2           Annual Tumover:         1.00           Tumover Factor:         1.00           Modrimum Liquid Volume (gal):         1.00           Modrimum Liquid Volume (gal):         1.00           Volving Loss Product Factor:         1.00	Vapor Pressure at Daily Minimum Liquid	
Surface Temperature (psia):		0.000
Daily Avg. Liquid Surface Temp. (deg R): 510.21 Daily Avg. Liquid Surface Temp. (deg R): 400.7. Daily Max. Liquid Surface Temp. (deg R): 523.70 Daily Max. Liquid Surface Temp. (deg R): 523.71 Daily Ambient Temp. Range (deg. R): 523.74 Vented Vapor Saturation Factor Vented Vapor Saturation Factor Vented Vapor Saturation Factor: 0,00 Vapor Pressurs at Daily Average Liquid: 51.00 Surface Temperature (psia): 0,00 Verpor Space Outage (ft): 10,33 Verpor Molecular Weight (b/th-mole): 700.00 Vapor Pressurs at Daily Average Liquid Surface Temperature (psia): 0,00 Annual Net Throughput (gallyr.): 200,304.22 Annual Net Throughput (gallyr.): 200,304.23 Annual Net Throughput (gallyr.): 17,442.01 Maximum Liquid Volume (gall): 17,442.01 Maximum Liquid Velogint (ft): 19,00 Tank Diameter (ft): 12,56 Worlding Loss Product Factor: 1,00		
Daily Mir. Liquid Surface Temp. (deg R): 400.7. Daily Amblent Temp. Range (deg. R): 523.7. Daily Amblent Temp. Range (deg. R): 525.4. Verland Vapor Saturation Factor: 0.06 Vented Vapor Saturation Factor: 0.06 Vapor Pressure at Daily Average Liquid: 52.7. Vapor Pressure at Daily Average Liquid: 0.00 Vapor Space Outlage (R): 10.3. Vapor Space Outlage (R): 700.00 Vapor Pressure at Daily Average Liquid: 700.00 Vapor Moderna at Daily Average Liquid: 700.00 Vapor Pressure at Daily Average Liquid: 700.00 Vapor Moderna at Daily Average Liquid: 700.00 Vapor Modern		0.000
Daily Max. Liquid Surface Temp. (deg R): 523.7t Daily Ambient Temp. Range (deg. R): 35.4t   /ented Vapor Saturation Factor   Vented Vapor Saturation Factor   Vented Vapor Saturation Factor   Vented Vapor Saturation Factor   Vented Vapor Saturation Factor: 0,00   Vapor Pressure at Daily Average Liquid: 10.00   Vapor Space Outage (ft): 10.3t   Vapor Molecular Weight (Ib/Ib-mole): 700.00   Vapor Pressure at Daily Average Liquid   Surface Temperature (pale): 0,00   Annual Net Throughput (gallyr.): 200,304.2t   Annual Tumovers: 12.00   Tumover Factor: 1,00   Maximum Liquid Volume (gal): 17,442.0t   Maximum Liquid Velogint (ft): 19.00   Tank Diameter (ft): 12.5t   Worlding Lose Product Factor: 1,00   Tank Diameter (ft): 12.5t   Volving Lose Product Factor: 1,00   Temperature (gall Lose Product Facto	Daily Avg. Liquid Surface Temp. (deg R):	
Daily Ambient Temp. Range (deg. R): 35.43  Vented Vapor Saturation Factor  Vented Vapor Saturation Factor: 0.06  Vapor Pressure at Daily Average Liquid: 3  Surface Temperature (psis): 10.33  Vorking Losses (lib: 70.00  Vapor Space Cuttage (lb/lb-mole): 700.00  Vapor Melecular Weight (lb/lb-mole): 700.00  Vapor Melecular Weight (lb/lb-mole): 0.00  Surface Temperature (psis): 0.00  Surface Temperature (psis): 0.00  Annual Net Throughput (gallyr): 20.03042  Annual Net Throughput (gallyr): 12.00  Tumover Factor: 1.00  Mesimum Liquid Velume (gal): 17.442.01  Mesimum Liquid Velume (gal): 19.00  Tank Clarmeter (ft): 10.00  Tank Clarmeter (ft): 10.00  Tank Clarmeter (ft): 10.00		490.772
Vented Vapor Seturation Factor:	Daily Ambient Temp. Range (deg. R):	35.433
Vented Vapor Seturation Factor:	Vented Vapor Saturation Factor	
Vapor Pressure at Deily Average Liquid:         0.00           Surface Temperature (psia):         0.00           Vapor Space Outlage (ft):         10.33           Vforful Loesse (lb:         700.00           Vapor Melecular Weight (lb/lb-mole):         700.00           Vapor Pressure at Daily Average Liquid         0.00           Surface Temperature (psia):         0.00           Annual Nell Throughput (pallyr):         209,304.22           Annual Nell Throughput (pallyr):         12.00           Macimum Liquid Volume (psi):         17.442.01           Macimum Liquid Height (ft):         19.00           Tank Clarester (ft):         1.00           Working Loss Product Factor:         1.00	Vented Vapor Saturation Factor:	0.999
Surface Temperature (psie)   0.00	Vapor Pressure at Daily Average Liquid:	
Working Losses (Ib):         1.38           Vapor Molecular Weight (Ib/Ib-mole):         700.00           Vapor Molecular Weight (Ib/Ib-mole):         700.00           Surface Temperature (psle):         0.00           Annual Net Throughput (gallyr.):         200,304.20           Annual Turmovers:         12.00           Turmover Factor:         1.00           Maximum Liquid Volume (gall):         17.442.01           Maximum Liquid Height (It):         19.00           Tank Diameter (It):         12.56           Working Loss Product Factor:         1.00	Surface Temperature (psia):	0.000
Vapor Molecular Weight (Ibfh-mole):         700.00           Vapor Pressurs at Delily Average Liquid         0.00           Surface Temperature (psla):         0.00           Annual Net Throughput (gallyr.):         200,304.20           Annual Net Throughput (gallyr.):         12.00           Turmover Factor:         1.00           Maximum Liquid Volume (gall):         17.442.01           Maximum Liquid Height (ft):         19.00           Tank Diameter (ft):         12.56           Working Loss Product Factor:         1.00	Vapor Space Outage (ft):	10.333
Surface Temperature (psla): 0.00   Annual Net Throughput (gallyr.): 200,304.24   Annual Net Throughput (gallyr.): 12.00   Tumover Factor: 1.00   Maximum Liquid Volume (gal): 17,442.01   Maximum Liquid Height (ft): 19,00   Tank Diameter (ft): 12.56   Worlding Loss Product Factor: 1.00	Vorking Losses (ib):	1.395
Surface Temperature (psia): 0.00   Annual Net Throughput (gallyr.): 200,304.24   Annual Net Throughput (gallyr.): 12.00   Tumnover Factor: 1.00   Maximum Liquid Volume (gall): 17,442.01   Maximum Liquid Height (ft): 19,00   Tank Diameter (ft): 12.56   Working Lose Product Factor: 1.00	Vapor Molecular Weight (lb/lb-mole):	700.000
Annual Net Throughput (gal/vr.): 209,304.20 Annual Turnover: 120,20 Turnover Factor: 1,00 Maximum Liquid Volume (gal): 17,442.01 Maximum Liquid Volume (fil): 19,00 Tarik Diarneter (ft): 12,56 Working Loss Product Factor: 1,00	Vapor Pressure at Dally Average Liquid	
Annual Tumoveres: 12.00 Tumover Factor: 1.00 Maximum Liquid Volume (gal): 17.442.01 Maximum Liquid Height (ft): 19.00 Tank Dlameter (ft): 12.56 Working Lose Product Factor: 1.00	Surface remperature (pala):	0.000
Turnover Factor:	Annual Turnoughput (gal/yr.):	209,304.203
Meadmum Liquid Volume (gal):   17,4(2.0"   Meadmum Liquid Height (ft):   19,00   Tank Dlameter (ft):   12,56   Working Loss Product Factor:   1,00		1.000
Maximum Liquid Height (ft): 19.00 Tank Diameter (ft): 12.56 Working Loss Product Factor: 1.00	Maximum Liquid Volume (nel):	17.442.017
Tank Diameter (ft): 12.50 Working Loss Product Factor: 1.00	Maximum Liquid Helaht (ft):	17,442.017
Working Loss Product Factor: 1.00	Tank Diameter (ft):	12.500
	Working Loss Product Factor:	1.000
Total Losses (lb): 3.77	Total Losses (lb):	3.773

#### TANKS 4.0.9d Emissions Report - Detail Format Individual Tank Emission Totals

**Emissions Report for: Annual** 

Slop Tank - Vertical Fixed Roof Tank Ignacio, Colorado

		Losses(lbs)	
Components	Working Loss	Breathing Loss	Total Emissions
Slop/Lube Oil	1.40	2.38	3.77





ANALYTICAL RESULTS FOR GREEN ANALYTICAL LABORATORIES, INC. ATTN: DEBBIE ZUFELT 75 SUTTLE STREET DURANGO, CO 81303 FAX TO: (970) 247-4227

Receiving Date: 06/24/10
Reporting Date: 07/01/10
Project Number: 1006-125-01
Project Name: LT ENVIRONMENTAL

Project Location: NOT GIVEN Sample ID: SPRING CREEK TANK

Lab Number: H20199-1

Analysis Date: 06/28/10 Sampling Date: 06/22/10 Sample Type: WATER

Sample Condition: COOL & INTACT @ 5 °C

Sample Received By: JH

Analyzed By: ZL

VC	PLATILES - 8260	Sample Result	Method	QC	QC	QC
		H20199-1	Blank	Measured	True Value	Recovery
	Compound Name		mg/L			%
1	Dichlorodifluoromethane	<0.002	<0.002	0.009	0.010	90.0
2	Chloromethane	<0.002	<0.002	0.010	0.010	104
3	Vinyl chloride	<0.002	< 0.002	0.010	0.010	102
4	Bromomethane	<0.002	<0.002	0.010	0.010	95.5
5	Chloroethane	<0.002	<0.002	0.008	0.010	80.7
6	Trichlorofluoromethane	<0.002	< 0.002	0.011	0.010	111
7	1,1-Dichloroethene	<0.002	< 0.002	0.010	0.010	97.9
8	Carbon Disulfide	ND	ND	NR	NR	NR
9	lodomethane	ND	ND	NR	NR	NR
10	Acrolein	<0.200	<0.200	0.057	0.050	114
11	Methylene chloride	0.013	<0.002	0.009	0.010	88.0
12	Acetone	ND	ND	NR	NR	NR
13	trans-1,2-Dichloroethene	<0.002	< 0.002	0.009	0.010	90.3
14	Methyl-t-butyl ether *	<0.002	<0.002	0.009	0.010	88.7
15	1,1-Dichloroethane	<0.002	<0.002	0.009	0.010	94.0
16	Vinyl Acetate	ND	ND	NR	NR	NR
17	cis-1,2-Dichloroethene	<0.002	< 0.002	0.008	0.010	84.3
18	Acrylonitrile	<0.002	< 0.002	0.056	0.050	111
19	2,2-Dichloropropane	<0.002	<0.002	0.012	0.010	120
20	Bromochloromethane	<0.002	< 0.002	0.009	0.010	94.0
21	Chloroform	<0.002	< 0.002	0.009	0.010	86.9
22	Carbon tetrachloride	<0.002	< 0.002	0.011	0.010	114
23	1,1,1-Trichloroethane	<0.002	< 0.002	0.009	0.010	86.2
24	1,1-Dichloropropene	<0.002	< 0.002	0.009	0.010	90.8
25	2 Butanone	ND	ND	NR	NR	NR
26	Benzene	<0.002	< 0.002	0.010	0.010	104
27	1,2-Dichloroethane	<0.002	< 0.002	0.009	0.010	88.1
28	Trichloroethene	<0.002	<0.002	0.011	0.010	106
29	Dibromomethane	<0.002	<0.002	0.008	0.010	81.6



ANALYTICAL RESULTS FOR GREEN ANALYTICAL LABORATORIES, INC.

ATTN: DEBBIE ZUFELT 75 SUTTLE STREET DURANGO, CO 81303 FAX TO: (970) 247-4227

Receiving Date: 06/24/10
Reporting Date: 07/01/10
Project Number: 1006-125-01
Project Name: LT ENVIRONMENTAL

Project Location: NOT GIVEN Sample ID: SPRING CREEK TANK

Lab Number: H20199-1

Analysis Date: 06/28/10 Sampling Date: 06/22/10 Sample Type: WATER

Sample Condition: COOL & INTACT @ 5 °C

Sample Received By: JH

Analyzed By: ZL

VO	LATILES - 8260	Sample Result H20199-1	Method Blank	QC Measured	QC True Value	QC Recovery
_	Compound Name	1120199-1	mg/L	Measured	11de value	%
30	1,2-Dichloropropane	<0.002	<0.002	0.009	0.010	87.7
31	Bromodichloromethane	<0.002	<0.002	0.008	0.010	81.9
32	cis-1,3-Dichloropropene	<0.002	<0.002	0.010	0.010	99.0
33	Toluene	<0.002	<0.002	0.010	0.010	96.9
34	4-Methyl-2-pentanone	ND ND	ND	NR	NR	NR
35	Tetrachloroethene	<0.002	<0.002	0.009	0.010	92.4
36	trans-1,3-Dichloropropene	<0.002	<0.002	0.012	0.010	120
37	1,1,2-Trichloroethane	<0.002	<0.002	0.012	0.010	120
38	Dibromochloromethane	<0.002	<0.002	0.011	0.010	112
39	1,3-Dichloropropane	<0.002	<0.002	0.011	0.010	110
40	1,2-Dibromoethane	<0.002	<0.002	0.010	0.010	96.6
41	2-Hexanone	ND	ND	NR	NR	NR
42	Chlorobenzene	<0.002	<0.002	0.010	0.010	99.1
43	Ethylbenzene	<0.002	<0.002	0.009	0.010	92.8
44	1,1,1,2-Tetrachloroethane	<0.002	<0.002	0.011	0.010	108
45	m+p - Xylene	0,117	<0.002	0.019	0.020	94.5
46	o-Xylene	0.007	< 0.004	0.009	0.010	89.3
47	Bromoform	<0.002	< 0.002	0.009	0.010	86.6
48	Styrene	<0.002	< 0.002	0.009	0.010	88.5
49	Isopropylbenzene	<0.002	<0.002	0.009	0.010	92.6
50	Bromobenzene	<0.002	<0.002	0.008	0.010	82.2
51	n-Propylbenzene	<0.002	< 0.002	0.009	0.010	91.6
52	1,1,2,2-Tetrachloroethane	<0.002	< 0.002	0.009	0.010	85.0
53	2-Chlorotoluene	<0.002	<0.002	0.009	0.010	89.9
54	1,2,3-Trichloropropane	<0.002	< 0.002	0.010	0.010	95.1
55	1,3,5-Trimethylbenzene	<0.002	< 0.002	0.009	0.010	93.8
56	trans-1,4-Dichloro-2-butene	ND	ND	NR	NR	NR
57	4-Chlorotoluene	<0.002	< 0.002	0.009	0.010	86.5
58	tert-Butylbenzene	<0.002	< 0.002	0.009	0.010	88.6



ANALYTICAL RESULTS FOR GREEN ANALYTICAL LABORATORIES, INC.

ATTN: DEBBIE ZUFELT 75 SUTTLE STREET DURANGO, CO 81303 FAX TO: (970) 247-4227

Receiving Date: 06/24/10 Reporting Date: 07/01/10 Project Number: 1006-125-01

Project Name: LT ENVIRONMENTAL Project Location: NOT GIVEN Sample ID: SPRING CREEK TANK

Lab Number: H20199-1

Analysis Date: 06/28/10 Sampling Date: 06/22/10 Sample Type: WATER

Sample Condition: COOL & INTACT @ 5 °C

Sample Received By: JH

Analyzed By: ZL

VO	LATILES - 8260	Sample Result H20199-1	Method Blank	QC Measured	QC True Value	QC Recovery
	Compound Name		mg/L			%
59	1,2,4-Trimethylbenzene	<0.002	<0.002	0.009	0.010	88.5
60	sec-Butylbenzene	<0.002	<0.002	0.009	0.010	88.3
61	p-Isopropyltoluene	< 0.002	< 0.002	0.009	0.010	88.3
62	1,3-Dichlorobenzene	< 0.002	< 0.002	0.008	0.010	84.7
63	1,4 Dichlorobenzene	<0.002	< 0.002	0.010	0.010	101
64	n-Butylbenzene	<0.002	<0.002	0.010	0.010	101
65	1,2-Dichlorobenzene	<0.002	<0.002	0.010	0.010	95.3
66	1,2-Dibromo-3-chloropropane	<0.002	<0.002	0.008	0.010	80.0
67	Hexachlorobutadiene	< 0.002	< 0.002	0.011	0.010	108
68	1,2,4-Trichlorobenzene	<0.002	< 0.002	0.009	0.010	85.6
69	Naphthalene	0.006	< 0.002	0.008	0.010	80.0
70	1,2,3-Trichlorobenzene	<0.002	< 0.002	0.009	0.010	91.0

Surrogates	% Recovery	
Dibromodifluoromethane	92.9	
Toluene-d8	102	
4-Bromofluorobenzene	84.8	

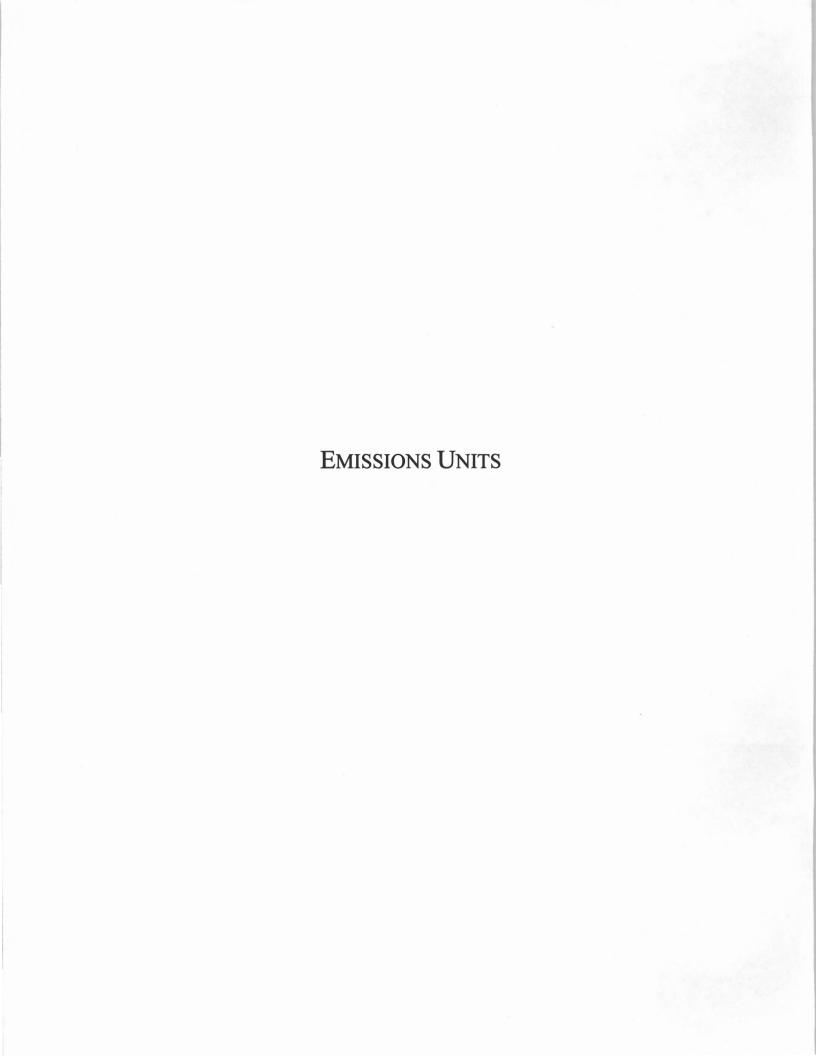
METHODS: EPA SW-846-8260. Reported on wet weight.

ND - Not detected NR - Not reported.

\* MTBE WAS ANALYZED SEPERATELY

Chemist

Date



CATERPILLAR G3516LE COMPRESSOR ENGINES

# Emission Unit Description Caterpillar G3516LE Compressor Engines Spring Creek Compressor Station

There are currently nine, with future expansion to ten, 1340 horsepower Caterpillar G3516LE compressor engines installed at the Spring Creek Compressor Station. These engines are natural gas-fired 4-stroke lean burn internal combustion engines. These units have a site rating of 1092 horsepower. The fuel for the engines is pipeline quality natural gas. All of the engines are equipped with oxidation catalysts. Detailed emission calculations are attached for each unit. The manufacturer's specification sheet is also attached. Table 5 lists the serial number, manufacture date and installation/startup date for each of the engines at the Spring Creek Compressor Station.

**Table 5: Spring Creek Compressor Station Engine Information** 

Unit ID	Serial Number	Manufacture Date	Installation/Commence Construction Date	Startup Date
E1	WPW1905	12/19/2007	06/20/2011	06/20/2011
E2	WPW1778	10/30/2007	06/23/2011	06/23/2011
E3	WPW02104	03/11/2008	09/15/2010	09/15/2010
E4	WPW00797	03/09/2007	02/23/2010	02/23/2010
E5	WPW00938	05/16/2007	02/23/2010	02/23/2010
E6	WPW00174	05/19/2006	02/25/2010	02/25/2010
E7	WPW00177	05/22/2006	02/25/2010	02/25/2010
E8	WPW00178	05/22/2006	02/24/2010	02/24/2010
E9	WPW00724	02/05/2007	02/23/2010	02/23/2010
E10	TBD	TBD	TBD	TBD

This facility is subject to the National Emission Standard for Hazardous Air Pollutants (NESHAP) for reciprocating internal combustion engines (RICE) regulation 40 CFR 63, Subpart ZZZZ because it emits or has the potential to emit a single Hazardous Air Pollutant (HAP) at a rate greater than 10 tons per year. Per 40 CFR 63, Subpart ZZZZ §63.6640, an affected facility is required to develop a Startup, Shutdown and Malfunction Plan (SSMP). The Spring Creek Compressor Station operates in accordance with the current facility SSMP that was last revised in January 2009.

Unit E3 is subject to the requirements of 40 CFR Part 60, Subpart JJJJ. Performance test are conducted on Unit E3 in accordance with 40 CFR 60.4244 every 8760 hours of operating or every three years, whichever comes first.

Each of the Caterpillar G3516LE compressor engines is equipped with either a  $NO_X$  sensor or  $O_2$  sensor as part of the air fuel ration controller system (AFRC) and an oxidation catalytic converter to reduce emissions in the exhaust stream. A continuous parameter monitoring system (CPMS) is used to record the catalyst inlet temperature of each engine to ensure that the inlet temperature remains between 450 °F and 1350 °F. The CPMS continuously monitors the catalyst inlet temperature and reduces the data to a 4-hour rolling average. The CPMS also logs the shutdown times and events and displays the unit process and fuel flows for each engine. The pressure drop across the catalyst is manually recorded at least once a month. Facility data is recorded in accordance with applicable parts of Section §63.6640.

Performance tests are conducted on the engines at the Spring Creek Compressor Station to demonstrate compliance with the NO<sub>X</sub> emission limit. The NO<sub>X</sub> emissions from each engine are limited to 2.0 g/bhp-hr or 21.1 tpy. All engines at the facility are tested semi-annually to assess NO<sub>X</sub> emissions. The performance tests for NO<sub>X</sub> are conducted in accordance with the test methods specified in 40 CFR Part 60, Appendix A. EPA Reference Method 7E is used to measure NO<sub>X</sub> emissions. The VOC performance tests required on Unit E3 are conducted in accordance with EPA Reference Method 25A and 18 of 40 CFR Part 63, Appendix A. All tests are performed at a maximum operating rate, 90% to 110% of engine design capacity. Each source test consists of at least three 1-hour or longer valid test runs. Emission results are reported as the arithmetic average of all valid test runs. During each test run data is collected on all parameters necessary to document how formaldehyde emissions were measured or calculated.

Exhaust  $NO_X$  ceiling monitoring and  $O_2$  concentration floor monitoring values shall be established for each engine equipped with  $NO_X$  and  $O_2$  sensors as part of the AFRC during the performance tests. The  $NO_X$  emissions of all operating engines will be monitored with one 20 minute portable analyzer test quarterly to confirm that the unit's respective set points are adequate to achieve compliance with the  $NO_X$  emissions limits.

Reference method performance tests will be conducted for all replacement catalysts and engines to measure  $NO_X$  emissions to demonstrate compliance with the engine emission limits. The performance tests will be conducted within 90 calendar days of catalyst change out or startup of the replacement engine. A portable analyzer test will be conducted to establish the new set-point for replacement  $NO_X$  and  $O_2$  sensors to ensure that  $NO_X$  emissions remain within permitted limits.

### **Spring Creek Compressor Station Engine Emission Calculations**

### **Basis**

Unit(s) E1, E2, E4-E10

Type Caterpillar G3516LE Control Oxidation Catalyst

Horsepower 1340 hp Site Rated Horsepower 1092 hp Hours of Operation 8760 hrs

Fuel Usage 7500 BTU/hp-hr
Fuel Heat Content 975.0 BTU/SCF
Annual Fuel Consumption 73.58 MMscf
Fuel Use Rate 8400 scf/hr

**Emissions Estimate (per engine)** 

		U	ncontrolled			Controlled					Reduction
	<b>Emissions Factor</b>			Emissions		<b>Emissions Factor</b>			Emissions		
Pollutant	(lb/MMbtu)	(g/hp-hr)	(lb/hr)	(lb/yr)	(tpy)	(lb/MMbtu)	(g/hp-hr)	(lb/hr)	(lb/yr)	(tpy)	Efficiency
$NO_X$	0.5874	2.000	4.81		21.07	0.5874	2.000	4.81		21.07	0%
CO	0.5463	1.860	4.47		19.60	0.5463	1.860	4.47		19.60	0%
VOC	0.1028	0.350	0.84		3.69	0.1028	0.350	0.84		3.69	0%
Formaldehyde	0.0816	0.278	0.67	5858	2.93	0.0411	0.140	0.34	2950	1.47	50%
SO <sub>2</sub>	0.0006	0.002	0.00		0.02	0.0006	0.002	0.00		0.02	0%
TSP	0.0100	0.034	0.08		0.36	0.0100	0.034	0.08		0.36	0%
$PM_{10}$	0.0001	0.000	0.00		0.00	0.0001	0.000	0.00		0.00	0%
$PM_{2.5}$	0.0001	0.000	0.00		0.00	0.0001	0.000	0.00		0.00	0%
Acetaldehyde	0.0084	0.028	0.07	600	0.30	0.0017	0.006	0.01	120	0.06	80%
Acrolein	0.0051	0.018	0.04	369	0.18	0.0010	0.004	0.01	74	0.04	80%
Benzene	0.0004	0.001	0.00	32	0.02	0.0001	0.000	0.00	6	0.00	80%
Toluene	0.0004	0.001	0.00	29	0.01	0.0001	0.000	0.00	6	0.00	80%
Xylene	0.0002	0.001	0.00	13	0.01	0.0000	0.000	0.00	3	0.00	80%
n-Hexane	0.0011	0.004	0.01	80	0.04	0.0002	0.001	0.00	16	0.01	80%
Methanol	0.0025	0.009	0.02	179	0.09	0.0005	0.002	0.00	36	0.02	80%

Emission Factors from Manufacturer's Specifications or

AP-42 Table 3.2-2 Uncontrolled Emission Factors for 4-Stroke Lean Burn Engines

### **Spring Creek Compressor Station Engine Emission Calculations**

### **Basis**

Unit(s) E3

Type Caterpillar G3516LE Control Oxidation Catalyst

Horsepower 1340 hp

Site Rated Horsepower 1092 hp Hours of Operation 8760 hrs

Fuel Usage 7500 BTU/hp-hr
Fuel Heat Content 975.0 BTU/SCF
Annual Fuel Consumption 73.58 MMscf
Fuel Use Rate 8400 scf/hr

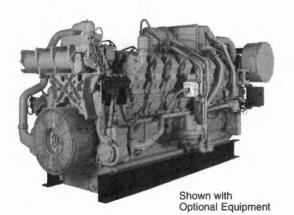
**Emissions Estimate (per engine)** 

		U	ncontrolled			Controlled					Reduction	
	Emission	s Factor		Emissions		Emission	s Factor	Emissions			THE RESERVE THE PERSON NAMED IN THE PERSON NAM	
Pollutant	(lb/MMbtu)	(g/hp-hr)	(lb/hr)	(lb/yr)	(tpy)	(lb/MMbtu)	(g/hp-hr)	(lb/hr)	(lb/yr)	(tpy)	Efficiency	
NO <sub>X</sub>	0.5874	2.000	4.81		21.07	0.5874	2.000	4.81		21.07	0%	
CO	0.5463	1.860	4.47		19.60	0.5463	1.860	4.47		19.60	0%	
VOC	0.2937	1.000	2.41		10.54	0.2937	1.000	2.41		10.54	0%	
Formaldehyde	0.0816	0.278	0.67	5858	2.93	0.0411	0.140	0.34	2950	1.47	50%	
$SO_2$	0.0006	0.002	0.00		0.02	0.0006	0.002	0.00		0.02	0%	
TSP	0.0100	0.034	0.08		0.36	0.0100	0.034	0.08		0.36	0%	
$PM_{10}$	0.0001	0.000	0.00		0.00	0.0001	0.000	0.00		0.00	0%	
PM <sub>2.5</sub>	0.0001	0.000	0.00		0.00	0.0001	0.000	0.00		0.00	0%	
Acetaldehyde	0.0084	0.028	0.07	600	0.30	0.0017	0.006	0.01	120	0.06	80%	
Acrolein	0.0051	0.018	0.04	369	0.18	0.0010	0.004	0.01	74	0.04	80%	
Benzene	0.0004	0.001	0.00	32	0.02	0.0001	0.000	0.00	6	0.00	80%	
Toluene	0.0004	0.001	0.00	29	0.01	0.0001	0.000	0.00	6	0.00	80%	
Xylene	0.0002	0.001	0.00	13	0.01	0.0000	0.000	0.00	3	0.00	80%	
n-Hexane	0.0011	0.004	0.01	80	0.04	0.0002	0.001	0.00	16	0.01	80%	
Methanol	0.0025	0.009	0.02	179	0.09	0.0005	0.002	0.00	36	0.02	80%	

Emission Factors from Manufacturer's Specifications or

AP-4/2 Table 3.2-2 Uncontrolled Emission Factors for 4-Stroke Lean Burn Engines

## CATERPILLAR®



## Gas Petroleum Engine

G3516 809-1000 bkW 1085-1340 bhp 1200-1400 rpm

### **CATERPILLAR® ENGINE SPECIFICATIONS**

V-16, 4-Stroke-Cycle	
Bore — mm (in) 1	70 (6.7)
Stroke — mm (in)	90 (7.5)
Displacement — L (cu in) 69	(4,210)
Aspiration Turbocharged-Afte	rcoolec
Capacity for Liquids — L (U.S. gal)	
Cooling System <sup>1</sup>	205 (54)
Lube Oil System (refill) 42	23 (112
Package Shipping Weight	
(Dry) — kg (lb) 8015 (	17,670
Engine only.	

### **FEATURES**

- Advisor Panel Compact, remote-mounted advisor gauge panel with fully electronic display
- · Expanded monitoring features:
  - Unfiltered oil pressure
  - Filtered oil pressure
  - Coolant (water) temperature
  - Oil temperature
  - Engine speed
  - Battery voltage
  - Service hours
  - Oil filter differential pressure
  - Detonation
  - Manifold inlet air pressure
  - Coolant (JW) outlet pressure
  - Coolant (JW) inlet pressure
  - Left turbocharger inlet temperature
  - Right turbocharger inlet temperature
  - Cylinder port temperature
  - Cylinder port temperature deviation from average (high or low)
  - Engine oil to engine coolant differential temperature
  - Improper gas control valve response
  - O<sub>2</sub> level sensor

- · Expanded alarm and shutdown capability
- Full range of diagnostics for troubleshooting electrical or electronic faults
- Advisor panel standard containing digital display of electronic control unit (ECU) parameters, diagnostic codes, engine start/stop switch, prelube and postlube integrated into ADEM<sup>TM</sup> A3 ECU with control switch mounted in Advisor panel
- Remote speed input 4-20 ma or 0-5 volts
- Integrated governing, AFRC, safeties, start/stop logic and ignition
- The standard ignition and control system is certified by the Canadian Standards Association (CSA) for use in Class I, Division 2, Group D hazardous locations
- · Modular wiring concept
- PL1000E provides direct translation of engine operating parameters from Cat Data Link to Modbus, with an available mounting location for the PL1000E in the Advisor panel

Factory-designed systems built at Caterpillar ISO 9001:2000 certified facilities.

### **BENEFITS**

### Reliable and durable product

- Components are proven and reliable based upon experience with G3600, G3500B, and diesel engine platforms
- Performance and system validation completed via lab and field test

### · Serviceable product

- Common ADEM A3 ECU with G3600, G3500B, and diesel C280 and 3500 products
- Improved access to engine sides due to removal of mechanical gauge panel
- Expanded diagnostics which are linked to troubleshooting procedures

- One common serviceable engine harness reducing parts stocking requirements and reducing repair time
- One common Advisor panel, reducing parts stocking requirements

### Easy to use

- Engine monitoring parameters communicated via MODBUS or ethernet by optional PL1000E
- Engine monitoring parameters and exhaust temperatures displayed and alarmed on Advisor panel

### Web Site

For all your petroleum power requirements, visit www.cat-oilandgas.com.

## **CATERPILLAR®**

### G3516 **GAS PETROLEUM ENGINE**

809-1000 bkW (1085-1340 bhp)

### STANDARD EQUIPMENT

**Air Inlet System** 

Air cleaner — intermediate-duty with service indicator

**Control System** 

ADEM™ A3 ECU

Air-fuel ratio control

**Cooling System** 

Thermostats and housing

Jacket water pump

Aftercooler water pump

Aftercooler core for sea-air atmosphere

Aftercooler thermostats and housing

**Exhaust System** 

Watercooled exhaust manifolds

Flywheels & Flywheel Housings

SAE No. 00 flywheel

SAE No. 00 flywheel housing

SAE standard rotation

**Fuel System** 

Gas pressure regulator

Natural gas carburetor

**Ignition System** 

ADEM A3 ECU

Instrumentation

PL1000 Advisor panel

**Lubrication System** 

Crankcase breather — top mounted

Oil cooler

Oil filter - RH

Oil bypass filter

Oil pan - shallow

Oil sampling valve

Turbo oil accumulator

**Mounting System** 

Rails, engine mounting — 254 mm (10 in)

**Protection System** 

Electronic shutoff system

Gas shutoff valve

General

Paint — Caterpillar yellow

Vibration damper and guard — dual 484 mm (23 in)

### OPTIONAL EQUIPMENT

Air Inlet System

Remote air inlet adapters

Precleaner

**Charging System** 

Battery chargers

Charging alternators

**Cooling System** 

Aftercooler core

Thermostatic valve

Temperature switch

Connections

Expansion and overflow tank

Water level switch gauge

**Exhaust System** 

Flexible fittings

**Elbows** 

Flange

Flange and exhaust expanders

Rain cap

Mufflers

**Fuel System** 

Low pressure gas conversions

Propane gas valve and jet kits

Fuel filter

Instrumentation

PL1000 communications modules

**Lubrication System** 

Oil bypass filter removal and oil pan accessories

Sump pump

Air prelube pump

Manual prelube pump

Lubricating oil

**Mounting System** 

Rails

Vibration isolators

**Power Take-Offs** 

Front accessory drives

Auxiliary drive shafts and pulleys

Front stub shaft

**Pulleys** 

**Protection System** 

Explosion relief valves, status control box interconnect

wiring harness

Starting System

Air starting motor

Air pressure regulator Air silencer

Electric air start controls

Electric starting motors — dual 24-volt

Starting aids

Battery sets (24-volt dry), cables, and rack

General

Flywheel intertia weight

Guard removal

Engine barring group

Premium 8:1 pistons

Premium cylinder heads

### **TECHNICAL DATA**

### G3516 Gas Petroleum Engine — 1400 rpm

		DM9540.00	DM0E44 00	DM8542-00	DM8543-00
Fuel System		DM8540-00 w/o AFRC	DM8541-00 w/o AFRC	with AFRC	w/o AFRC
Fuel System		W/O AFRC	W/O AFRO	WILLIAFIC	W/U AFRO
Engine Power  @ 100% Load  @ 75% Load	bkW (bhp) bkW (bhp)	969 (1300) 727 (975)	943 (1265) 707 (949)	999 (1340) 749 (1005)	999 (1340) 749 (1005)
Engine Speed	rpm	1400	1400	1400	1400
SCAC Temperature	°C (°F)				
Compression Ratio		8:1	8:1	8:1	8:1
Emissions* NO <sub>X</sub> CO Total Hydrocarbons	mg/N•m³ dry (g/bhp-hr) mg/N•m³ dry (g/bhp-hr) mg/N•m³ dry (g/bhp-hr)	829 (2.0) 772 (1.86)	824 (2.0) 777 (1.89)	604 (1.5) 759 (1.89)	837 (2.0) 767 (1.83)
Fuel Consumption @ 100% Load @ 75% Load	MJ/bkW-hr (Btu/bhp-hr) MJ/bkW-hr (Btu/bhp-hr)	10.45 (7392) 10.69 (7561)	10.48 (7407) 10.70 (7564)	10.47 (7401) 10.83 (7657)	10.43 (7377) 10.69 (7558)
Heat Balance Heat Rejection to Jacket Water @ 100% Load @ 75% Load  Heat Rejection to Aftercooler @ 100% Load	bkW (Btu/mn) bkW (Btu/mn)	711 (40,443) 464 (26,402) 175 (9976)	708 (40,277) 602 (34,223) 145 (8276)	725 (41,216) 606 (34,469) 183 (10,426)	719 (40,893) 325 (18,476) 206 (11,752)
@ 75% Load  Heat Rejection to Exhaust @ 100% Load (LHV to 77°) (LHV to 77° F / 25° C) @ 75% Load (LHV to 77°) (LHV to 77° F / 25° C)	bkW (Btu/mn) bkW (Btu/mn) bkW (Btu/mn)	138 (7829) 794 (45,180) 707 (40,232)	90 (5115) 782 (44,486) 557 (31,677)	124 (7047) 833 (47,381) 631 (35,910)	195 (11,086) 807 (45,870) 856 (48,690)
Exhaust System Exhaust Gas Flow Rate @ 100% Load @ 75% Load  Exhaust Stack Temperature @ 100% Load @ 75% Load	N•m³/bkW-hr (cfm) N•m³/bkW-hr (cfm) °C (°F) °C (°F)	4.69 (7283) 5.68 (6579) 460 (860) 456 (854)	4.71 (7151) 4.56 (5171) 465 (868) 461 (862)	4.80 (7651) 4.96 (5853) 457 (854) 449 (840)	4.67 (7416) 6.72 (7970) 455 (852) 452 (845)
Intake System Air Inlet Flow Rate @ 100% Load @ 75% Load	N•m³/bkW-hr (scfm) N•m³/bkW-hr (scfm)	4.39 (2732) 5.37 (2506)	4.40 (2666) 4.24 (1929)	4.50 (2886) 4.64 (2282)	4.36 (2798) 6.40 (3084)
Gas Pressure	kPag (psig)	242-276 (35-40)	242-276 (35-40)	242-276 (35-40)	242-276 (35-4

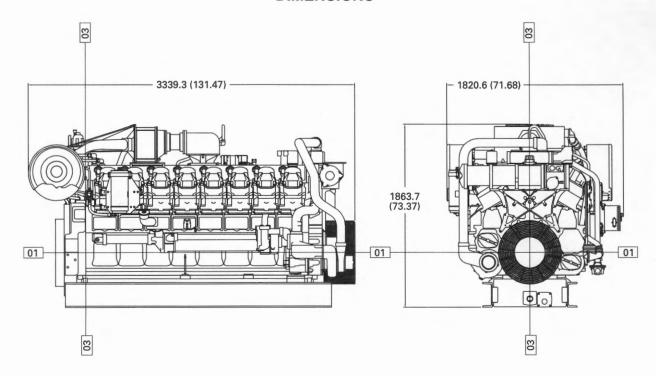
<sup>\*</sup>at 100% load and speed

## **CATERPILLAR®**

## G3516 GAS PETROLEUM ENGINE

809-1000 bkW (1085-1340 bhp)

### **DIMENSIONS**



DIMENSIONS							
Length	mm (in)	3339.3 (131.47)					
Width	mm (in)	1820.6 (71.68)					
Height	mm (in)	1863.7 (73.37)					
Shipping Weight	kg (lb)	8015 (17,670)					

Note: General configuration not to be used for installation. See general dimension drawings for detail (drawing #289-2971).

Dimensions are in mm (inches).

## **CATERPILLAR®**

### G3516 GAS PETROLEUM ENGINE

809-1000 bkW (1085-1340 bhp)

### **RATING DEFINITIONS AND CONDITIONS**

Engine performance is obtained in accordance with SAE J1995, ISO3046/1, BS5514/1, and DIN6271/1 standards.

Transient response data is acquired from an engine/generator combination at normal operating temperature and in accordance with ISO3046/1 standard ambient conditions. Also in accordance with SAE J1995, BS5514/1, and DIN6271/1 standard reference conditions.

Conditions: Power for gas engines is based on fuel having an LHV of 33.74 kJ/L (905 Btu/cu ft) at 101 kPa (29.91 in. Hg) and 15° C (59° F). Fuel rate is based on a cubic meter at 100 kPa (29.61 in. Hg) and 15.6° C (60.1° F). Air flow is based on a cubic foot at 100 kPa (29.61 in. Hg) and 25° C (77° F). Exhaust flow is based on a cubic foot at 100 kPa (29.61 in. Hg) and stack temperature.

## **CATERPILLAR**

Materials and specifications are subject to change without notice. The International System of Units (SI) is used in this publication. CAT, CATERPILLAR, ADEM, their respective logos and "Caterpillar Yellow," as well as corporate and product identity used herein, are trademarks of Caterpillar and may not be used without permission.

## Emission Estimates Emission Unit E1 Spring Creek Compressor Station

Unit E1 is a 1,340 horsepower Caterpillar G3516LE, a 4-stroke lean burn internal combustion engine. The engine is equipped with an oxidation catalyst for the control of formaldehyde. Potential to emit calculations are presented below.

Potential to Emit: Uncontrolled Configuration
Lean-burn Engine with Oxidation Catalyst for formaldehyde control

### **Estimated Emission Factors**

NO<sub>X</sub> 2.00 g/hp-hr (Manufacturer Quotation)
CO 1.86 g/hp-hr (Manufacturer Quotation)
VOC 0.35 g/hp-hr (Manufacturer Quotation)
Formaldehvde 13.6 ppmyd ~ 0.14 "

Formaldehyde 13.6 ppmvd  $\approx$  0.14 g/hp-hr (40 CFR 63, Subpart ZZZZ Limitation, Engineering Estimate)

$$NO_{x} = \frac{(2.00 \text{ g/hp - hr})(1,092 \text{ hp})(8,760 \text{ hr/yr})}{(454 \text{ g/lb})(2,000 \text{ lb/ton})} = 21.1 \text{ tpy}$$

CO = 
$$\frac{(1.86 \text{ g/hp - hr})(1,092 \text{ hp})(8,760 \text{ hr/yr})}{(454 \text{ g/lb})(2,000 \text{ lb/ton})}$$
 = 19.6 tpy

VOC = 
$$\frac{(0.35 \text{ g/hp - hr})(1,092 \text{ hp})(8,760 \text{ hr/yr})}{(454 \text{ g/lb})(2,000 \text{ lb/ton})}$$
 = 3.7 tpy

$$CH_2O = \frac{(0.14 \text{ g/hp - hr})(1,092 \text{ hp})(8,760 \text{ hr/yr})}{(454 \text{ g/lb})(2,000 \text{ lb/ton})} = 1.5 \text{ tpy}$$

# Emission Estimates Emission Unit E2 Spring Creek Compressor Station

Unit E2 is a 1,340 horsepower Caterpillar G3516LE, a 4-stroke lean burn internal combustion engine. The engine is equipped with an oxidation catalyst for the control of formaldehyde. Potential to emit calculations are presented below.

Potential to Emit: Uncontrolled Configuration
Lean-burn Engine with Oxidation Catalyst for formaldehyde control

### **Estimated Emission Factors**

NO $_{\rm X}$  2.00 g/hp-hr (Manufacturer Quotation) CO 1.86 g/hp-hr (Manufacturer Quotation) VOC 0.35 g/hp-hr (Manufacturer Quotation) Formaldehyde 13.6 ppmvd  $\approx$  0.14 g/hp-hr (40 CFR 63, Subpart ZZZZ Limitation, Engineering Estimate)

$$NO_X = \frac{(2.00 \text{ g/hp - hr})(1,092 \text{ hp})(8,760 \text{ hr/yr})}{(454 \text{ g/lb})(2,000 \text{ lb/ton})} = 21.1 \text{ tpy}$$

CO = 
$$\frac{(1.86 \text{ g/hp - hr})(1,092 \text{ hp})(8,760 \text{ hr/yr})}{(454 \text{ g/lb})(2,000 \text{ lb/ton})}$$
 = 19.6 tpy

VOC = 
$$\frac{(0.35 \text{ g/hp - hr})(1,092 \text{ hp})(8,760 \text{ hr/yr})}{(454 \text{ g/lb})(2,000 \text{ lb/ton})}$$
 = 3.7 tpy

$$CH_2O = \frac{(0.14 \text{ g/hp - hr})(1,092 \text{ hp})(8,760 \text{ hr/yr})}{(454 \text{ g/lb})(2,000 \text{ lb/ton})} = 1.5 \text{ tpy}$$

### **Emission Estimates Emission Unit E3 Spring Creek Compressor Station**

Unit E3 is a 1,340 horsepower Caterpillar G3516LE, a 4-stroke lean burn internal combustion engine. The engine is equipped with an oxidation catalyst for the control of formaldehyde. Potential to emit calculations are presented below.

Potential to Emit: Uncontrolled Configuration Lean-burn Engine with Oxidation Catalyst for formaldehyde control

### **Estimated Emission Factors**

 $NO_X$ 2.00 g/hp-hr (Manufacturer Quotation) 1.00 g/hp-hr 13.6 pp-(Manufacturer Quotation) CO

(40 CFR 60, Subpart JJJJ Limitation) VOC

Formaldehyde 13.6 ppmvd ≈ 0.14 g/hp-hr (40 CFR 63, Subpart ZZZZ Limitation, Engineering Estimate)

$$NO_{X} = \frac{(2.00 \text{ g/hp - hr})(1,092 \text{ hp})(8,760 \text{ hr/yr})}{(454 \text{ g/lb})(2,000 \text{ lb/ton})} = 21.1 \text{ tpy}$$

CO = 
$$\frac{(1.86 \text{ g/hp - hr})(1,092 \text{ hp})(8,760 \text{ hr/yr})}{(454 \text{ g/lb})(2,000 \text{ lb/ton})}$$
 = 19.6 tpy

VOC = 
$$\frac{(1.00 \text{ g/hp - hr})(1,092 \text{ hp})(8,760 \text{ hr/yr})}{(454 \text{ g/lb})(2,000 \text{ lb/ton})}$$
 = 10.5 tpy

$$CH_2O = \frac{(0.14 \text{ g/hp - hr})(1,092 \text{ hp})(8,760 \text{ hr/yr})}{(454 \text{ g/lb})(2,000 \text{ lb/ton})} = 1.5 \text{ tpy}$$

# Emission Estimates Emission Unit E4 Spring Creek Compressor Station

Unit E4 is a 1,340 horsepower Caterpillar G3516LE, a 4-stroke lean burn internal combustion engine. The engine is equipped with an oxidation catalyst for the control of formaldehyde. Potential to emit calculations are presented below.

Potential to Emit: Uncontrolled Configuration
Lean-burn Engine with Oxidation Catalyst for formaldehyde control

### **Estimated Emission Factors**

NO $_{\rm X}$  2.00 g/hp-hr (Manufacturer Quotation) CO 1.86 g/hp-hr (Manufacturer Quotation) VOC 0.35 g/hp-hr (Manufacturer Quotation) Formaldehyde 13.6 ppmvd  $\approx$  0.14 g/hp-hr (40 CFR 63, Subpart ZZZZ Limitation, Engineering Estimate)

$$NO_{X} = \frac{(2.00 \text{ g/hp - hr})(1,092 \text{ hp})(8,760 \text{ hr/yr})}{(454 \text{ g/lb})(2,000 \text{ lb/ton})} = 21.1 \text{ tpy}$$

CO = 
$$\frac{(1.86 \text{ g/hp - hr})(1,092 \text{ hp})(8,760 \text{ hr/yr})}{(454 \text{ g/lb})(2,000 \text{ lb/ton})}$$
 = 19.6 tpy

VOC = 
$$\frac{(0.35 \text{ g/hp - hr})(1,092 \text{ hp})(8,760 \text{ hr/yr})}{(454 \text{ g/lb})(2,000 \text{ lb/ton})}$$
 = 3.7 tpy

$$CH_2O = \frac{(0.14 \text{ g/hp - hr})(1,092 \text{ hp})(8,760 \text{ hr/yr})}{(454 \text{ g/lb})(2,000 \text{ lb/ton})} = 1.5 \text{ tpy}$$

# Emission Estimates Emission Unit E5 Spring Creek Compressor Station

Unit E5 is a 1,340 horsepower Caterpillar G3516LE, a 4-stroke lean burn internal combustion engine. The engine is equipped with an oxidation catalyst for the control of formaldehyde. Potential to emit calculations are presented below.

Potential to Emit: Uncontrolled Configuration
Lean-burn Engine with Oxidation Catalyst for formaldehyde control

### **Estimated Emission Factors**

NO<sub>X</sub> 2.00 g/hp-hr (Manufacturer Quotation)
CO 1.86 g/hp-hr (Manufacturer Quotation)
VOC 0.35 g/hp-hr (Manufacturer Quotation)

Formaldehyde 13.6 ppmvd  $\approx$  0.14 g/hp-hr (40 CFR 63, Subpart ZZZZ Limitation, Engineering Estimate)

$$NO_{X} = \frac{(2.00 \text{ g/hp - hr})(1,092 \text{ hp})(8,760 \text{ hr/yr})}{(454 \text{ g/lb})(2,000 \text{ lb/ton})} = 21.1 \text{ tpy}$$

$$CO = \frac{(1.86 \text{ g/hp - hr})(1,092 \text{ hp})(8,760 \text{ hr/yr})}{(454 \text{ g/lb})(2,000 \text{ lb/ton})} = 19.6 \text{ tpy}$$

VOC = 
$$\frac{(0.35 \text{ g/hp - hr})(1,092 \text{ hp})(8,760 \text{ hr/yr})}{(454 \text{ g/lb})(2,000 \text{ lb/ton})}$$
 = 3.7 tpy

$$CH_2O = \frac{(0.14 \text{ g/hp - hr})(1,092 \text{ hp})(8,760 \text{ hr/yr})}{(454 \text{ g/lb})(2,000 \text{ lb/ton})} = 1.5 \text{ tpy}$$

# Emission Estimates Emission Unit E6 Spring Creek Compressor Station

Unit E6 is a 1,340 horsepower Caterpillar G3516LE, a 4-stroke lean burn internal combustion engine. The engine is equipped with an oxidation catalyst for the control of formaldehyde. Potential to emit calculations are presented below.

Potential to Emit: Uncontrolled Configuration
Lean-burn Engine with Oxidation Catalyst for formaldehyde control

### **Estimated Emission Factors**

NO<sub>X</sub> 2.00 g/hp-hr (Manufacturer Quotation) CO 1.86 g/hp-hr (Manufacturer Quotation) VOC 0.35 g/hp-hr (Manufacturer Quotation) Formaldehyde 13.6 ppmyd  $\approx 0.14$  g/hp-hr (40 CFR 63, Subpart ZZZZ Limitation, I

Formaldehyde 13.6 ppmvd  $\approx$  0.14 g/hp-hr (40 CFR 63, Subpart ZZZZ Limitation, Engineering Estimate)

$$NO_{X} = \frac{(2.00 \text{ g/hp - hr})(1,092 \text{ hp})(8,760 \text{ hr/yr})}{(454 \text{ g/lb})(2,000 \text{ lb/ton})} = 21.1 \text{ tpy}$$

$$CO = \frac{(1.86 \text{ g/hp - hr})(1,092 \text{ hp})(8,760 \text{ hr/yr})}{(454 \text{ g/lb})(2,000 \text{ lb/ton})} = 19.6 \text{ tpy}$$

VOC = 
$$\frac{(0.35 \text{ g/hp - hr})(1,092 \text{ hp})(8,760 \text{ hr/yr})}{(454 \text{ g/lb})(2,000 \text{ lb/ton})}$$
 = 3.7 tpy

$$CH_2O = \frac{(0.14 \text{ g/hp - hr})(1,092 \text{ hp})(8,760 \text{ hr/yr})}{(454 \text{ g/lb})(2,000 \text{ lb/ton})} = 1.5 \text{ tpy}$$

# Emission Estimates Emission Unit E7 Spring Creek Compressor Station

Unit E7 is a 1,340 horsepower Caterpillar G3516LE, a 4-stroke lean burn internal combustion engine. The engine is equipped with an oxidation catalyst for the control of formaldehyde. Potential to emit calculations are presented below.

Potential to Emit: Uncontrolled Configuration
Lean-burn Engine with Oxidation Catalyst for formaldehyde control

### **Estimated Emission Factors**

NO $_{\rm X}$  2.00 g/hp-hr (Manufacturer Quotation) CO 1.86 g/hp-hr (Manufacturer Quotation) VOC 0.35 g/hp-hr (Manufacturer Quotation) Formaldehyde 13.6 ppmvd  $\approx$  0.14 g/hp-hr (40 CFR 63, Subpart ZZZZ Limitation, Engineering Estimate)

$$NO_{X} = \frac{(2.00 \text{ g/hp - hr})(1,092 \text{ hp})(8,760 \text{ hr/yr})}{(454 \text{ g/lb})(2,000 \text{ lb/ton})} = 21.1 \text{ tpy}$$

CO = 
$$\frac{(1.86 \text{ g/hp - hr})(1,092 \text{ hp})(8,760 \text{ hr/yr})}{(454 \text{ g/lb})(2,000 \text{ lb/ton})}$$
 = 19.6 tpy

VOC = 
$$\frac{(0.35 \text{ g/hp - hr})(1,092 \text{ hp})(8,760 \text{ hr/yr})}{(454 \text{ g/lb})(2,000 \text{ lb/ton})}$$
 = 3.7 tpy

$$CH_2O = \frac{(0.14 \text{ g/hp - hr})(1,092 \text{ hp})(8,760 \text{ hr/yr})}{(454 \text{ g/lb})(2,000 \text{ lb/ton})} = 1.5 \text{ tpy}$$

# Emission Estimates Emission Unit E8 Spring Creek Compressor Station

Unit E8 is a 1,340 horsepower Caterpillar G3516LE, a 4-stroke lean burn internal combustion engine. The engine is equipped with an oxidation catalyst for the control of formaldehyde. Potential to emit calculations are presented below.

Potential to Emit: Uncontrolled Configuration
Lean-burn Engine with Oxidation Catalyst for formaldehyde control

### **Estimated Emission Factors**

NO<sub>X</sub>
2.00 g/hp-hr (Manufacturer Quotation)
CO
1.86 g/hp-hr (Manufacturer Quotation)
VOC
0.35 g/hp-hr (Manufacturer Quotation)

Formaldehyde 13.6 ppmvd  $\approx$  0.14 g/hp-hr (40 CFR 63, Subpart ZZZZ Limitation, Engineering Estimate)

$$NO_X = \frac{(2.00 \text{ g/hp - hr})(1,092 \text{ hp})(8,760 \text{ hr/yr})}{(454 \text{ g/lb})(2,000 \text{ lb/ton})} = 21.1 \text{ tpy}$$

$$CO = \frac{(1.86 \text{ g/hp - hr})(1,092 \text{ hp})(8,760 \text{ hr/yr})}{(454 \text{ g/lb})(2,000 \text{ lb/ton})} = 19.6 \text{ tpy}$$

VOC = 
$$\frac{(0.35 \text{ g/hp - hr})(1,092 \text{ hp})(8,760 \text{ hr/yr})}{(454 \text{ g/lb})(2,000 \text{ lb/ton})}$$
 = 3.7 tpy

$$CH_2O = \frac{(0.14 \text{ g/hp - hr})(1,092 \text{ hp})(8,760 \text{ hr/yr})}{(454 \text{ g/lb})(2,000 \text{ lb/ton})} = 1.5 \text{ tpy}$$

# Emission Estimates Emission Unit E9 Spring Creek Compressor Station

Unit E9 is a 1,340 horsepower Caterpillar G3516LE, a 4-stroke lean burn internal combustion engine. The engine is equipped with an oxidation catalyst for the control of formaldehyde. Potential to emit calculations are presented below.

Potential to Emit: Uncontrolled Configuration
Lean-burn Engine with Oxidation Catalyst for formaldehyde control

### **Estimated Emission Factors**

NO $_{\rm X}$  2.00 g/hp-hr (Manufacturer Quotation) CO 1.86 g/hp-hr (Manufacturer Quotation) VOC 0.35 g/hp-hr (Manufacturer Quotation) Formaldehyde 13.6 ppmvd  $\approx$  0.14 g/hp-hr (40 CFR 63, Subpart ZZZZ Limitation, Engineering Estimate)

$$NO_{X} = \frac{(2.00 \text{ g/hp - hr})(1,092 \text{ hp})(8,760 \text{ hr/yr})}{(454 \text{ g/lb})(2,000 \text{ lb/ton})} = 21.1 \text{ tpy}$$

CO = 
$$\frac{(1.86 \text{ g/hp - hr})(1,092 \text{ hp})(8,760 \text{ hr/yr})}{(454 \text{ g/lb})(2,000 \text{ lb/ton})}$$
 = 19.6 tpy

VOC = 
$$\frac{(0.35 \text{ g/hp - hr})(1,092 \text{ hp})(8,760 \text{ hr/yr})}{(454 \text{ g/lb})(2,000 \text{ lb/ton})}$$
 = 3.7 tpy

$$CH_2O = \frac{(0.14 \text{ g/hp - hr})(1,092 \text{ hp})(8,760 \text{ hr/yr})}{(454 \text{ g/lb})(2,000 \text{ lb/ton})} = 1.5 \text{ tpy}$$

# Emission Estimates Emission Unit E10 Spring Creek Compressor Station

Unit E10 is a 1,340 horsepower Caterpillar G3516LE, a 4-stroke lean burn internal combustion engine. The engine is equipped with an oxidation catalyst for the control of formaldehyde. Potential to emit calculations are presented below.

Potential to Emit: Uncontrolled Configuration
Lean-burn Engine with Oxidation Catalyst for formaldehyde control

### **Estimated Emission Factors**

NO $_{\rm X}$  2.00 g/hp-hr (Manufacturer Quotation) CO 1.86 g/hp-hr (Manufacturer Quotation) VOC 0.35 g/hp-hr (Manufacturer Quotation) Formaldehyde 13.6 ppmvd  $\approx$  0.14 g/hp-hr (40 CFR 63, Subpart ZZZZ Limitation, Engineering

Estimate)

$$NO_{X} = \frac{(2.00 \text{ g/hp - hr})(1,092 \text{ hp})(8,760 \text{ hr/yr})}{(454 \text{ g/lb})(2,000 \text{ lb/ton})} = 21.1 \text{ tpy}$$

$$CO = \frac{(1.86 \text{ g/hp - hr})(1,092 \text{ hp})(8,760 \text{ hr/yr})}{(454 \text{ g/lb})(2,000 \text{ lb/ton})} = 19.6 \text{ tpy}$$

VOC = 
$$\frac{(0.35 \text{ g/hp - hr})(1,092 \text{ hp})(8,760 \text{ hr/yr})}{(454 \text{ g/lb})(2,000 \text{ lb/ton})}$$
 = 3.7 tpy

$$CH_2O = \frac{(0.14 \text{ g/hp - hr})(1,092 \text{ hp})(8,760 \text{ hr/yr})}{(454 \text{ g/lb})(2,000 \text{ lb/ton})} = 1.5 \text{ tpy}$$

# EMISSION UNIT D1 TEG DEHYDRATION UNIT

# Emission Estimates Emission Unit D1 60 MMscfd Dehydration Unit Spring Creek Compressor Station

VOC and HAP emissions may occur when triethylene glycol is regenerated. The emission model GRI-GLYCalc, a thermodynamic-based process simulator for dehydration units, was utilized to estimate emissions from this unit. A facility inlet gas analysis with the highest sampled VOC content and maximum anticipated benzene concentration was input to the model. Following is a summary of other worse-case operating parameter model input values:

<u>Parameter</u>	Va	<u>llue</u>
Inlet Gas Throughput	60	MMscfd
Inlet Gas Temperature	60	°F
Inlet Gas Pressure	120	psig
Inlet Benzene Concentration	2	ppm
Glycol Circulation	15	gpm
Flash Vessel Temperature	140	°F
Flash Vessel Pressure	40	psig

### **Model Results (Output Follows)**

VOC Emissions	8.7	tpy
Benzene Emissions	0.9	tpy
<b>Total HAP Emissions</b>	6.6	tpy

### D1 PTE (150% of modeled emissions)

<b>VOC Emissions</b>	13.1	tpy
HAP Emissions	9.9	tpy

### **Emission Estimates Dehydration Unit Reboiler Spring Creek Compressor Station**

## Reboilers and Heaters Type

<100 MMBtu/hr

Operation	8760 hrs
Heat Content	975 Btu/SCF

D-II-dd	<b>Emission Factor*</b>
Pollutant	(lb/MMSCF)
$NO_X$	100
CO	84
VOC	5.5
Formaldehyde	0.075
SO2	0.6
PM	7.6

<sup>\*</sup>Emission factors obtained from AP-42 Tables 1.4-1, 1.4-2 and 1.5-2.

### Reboilers

	Description	Heater Size	NC	x	C	0	VO	C	Formal	dehyde	SC	)2	PM	110
Unit	Description	(MMBtu/hr)	(lb/hr)	(tpy)	(lb/hr)	(tpy)	(lb/hr)	(tpy)	(lb/hr)	(tpy)	(lb/hr)	(tpy)	(lb/hr)	(tpy)
D1	Dehy Reboiler	0.75	0.07	0.31	0.06	0.26	0.004	0.02	0.00	0.00	0.00	0.00	ე.005	0.02

## QUESTAR APPLIED TECHNOLOGY

## 1210 D. Street, Rock Springs, Wyoming 82901 (307) 352-7292

4:43 PM

LIMS ID:

N/A

Description:

Spring Creek CDP Inlet

Analysis Date/Time:

1/7/2013

Field:

La Plata

Analyst Initials: Instrument ID:

ABK Instrument 1 ML#:

Lease# 038105

Data File:
Date Sampled:

QPC16.D 1/1/2013 GC Method: Quesbtex

Component	Mol%		V	Vt%	LV%
Methane	95.3680		88.6938	95.32	255
Ethane	0.2304		0.4017	0.364	4
Propane	0.0094		0.0241	0.015	3
Isobutane	0.0016		0.0053	0.003	30
n-Butane	0.0012		0.0042	0.002	23
Neopentane	0.0004		0.0018	0.001	0
Isopentane	0.0019		0.0078	0.004	0
n-Pentane	0.0005		0.0020	0.001	0
2,2-Dimethylbutane	0.0002		0.0010	0.000	5
2,3-Dimethylbutane	0.0002		0.0010	0.000	5
2-Methylpentane	0.0000		0.0000	0.000	0
3-Methylpentane	0.0002		0.0009	0.000	)4
n-Hexane	0.0002		0.0009	0.000	5
Heptanes	0.0005		0.0033	0.001	4
Octanes	0.0000		0.0000	0.000	00
Nonanes	0.0003		0.0018	0.000	7
Decanes plus	0.0006		0.0046	0.002	20
Nitrogen	0.3667		0.5955	0.237	<b>'</b> 2
Carbon Dioxide	4.0177		10.2503	4.040	3
Oxygen	0.0000		0.0000	0.000	00
Hydrogen Sulfide	0.0000		0.0000	0.000	00
Total	100.0000		100.0000	100.0	0000
Global Properties		Jnits			
Gross BTU/Real CF	972.2		BTU/SCF a	t 60°F and 14.73 ps	sia
Sat.Gross BTU/Real CF	956.4		BTU/SCF a	t 60°F and14.73 ps	sia
Gas Compressibility (Z)	0.9979				
Specific Gravity	0.5969		air=1		
Avg Molecular Weight	17.250		gm/mole		
Propane GPM	0.002576		gal/MCF		
Butane GPM	0.000900		gal/MCF		
Gasoline GPM	0.001502		gal/MCF		
26# Gasoline GPM	0.001880		gal/MCF		
Total GPM	0.791064		gal/MCF		
Base Mol%	100.221		%v/v		
Sample Temperature:	39		°F		
Sample Pressure:	32		psig		
H2SLength of Stain Tube	e N/A		ppm		

Component	Mol%	Wt%	LV%
Benzene	0.0000	0.0000	0.0000
Toluene	0.0002	0.0011	0.0004
Ethylbenzene	0.0001	0.0006	0.0002
M&P Xylene	0.0001	0.0006	0.0002
O-Xylene	0.0000	0.0000	0.0000
2,2,4-Trimethylpentane	0.0000	0.0000	0.0000
Cyclopentane	0.0000	0.0000	0.0000
Cyclohexane	0.0000	0.0000	0.0000
Methylcyclohexane	0.0002	0.0014	0.0006
Description:	Spring Creek CDP Inlet		

### GRI GlyCalc Information

Component	Mol%	Wt%	LV%
Carbon Dioxide	4.0177	10.2503	4.0403
Hydrogen Sulfide	0.0000	0.0000	0.0000
Nitrogen	0.3667	0.5955	0.2372
Methane	95.3680	88.6938	95.3255
Ethane	0.2304	0.4017	0.3644
Propane	0.0094	0.0241	0.0153
Isobutane	0.0016	0.0053	0.0030
n-Butane	0.0012	0.0042	0.0023
Isopentane	0.0023	0.0096	0.0050
n-Pentane	0.0005	0.0020	0.0010
Cyclopentane	0.0000	0.0000	0.0000
n-Hexane	0.0002	0.0009	0.0005
Cyclohexane	0.0000	0.0000	0.0000
Other Hexanes	0.0006	0.0029	0.0014
Heptanes	0.0001	0.0008	0.0004
Methylcyclohexane	0.0002	0.0014	0.0006
2,2,4 Trimethylpentane	0.0000	0.0000	0.0000
Benzene	0.0000	0.0000	0.0000
Toluene	0.0002	0.0011	0.0004
Ethylbenzene	0.0001	0.0006	0.0002
Xylenes	0.0001	0.0006	0.0002
C8+ Heavies	0.0007	0.0052	0.0023
Subtotal	100.0000	100.0000	100.0000
Oxygen	0.0000	0.0000	0.0000
Total	100.0000	100.0000	100.0000

Page: 1

### GRI-GLYCalc VERSION 4.0 - AGGREGATE CALCULATIONS REPORT

Case Name: Spring Creek Dehy

File Name: C:\Work\Projects\Samson\Spring Creek\Permit Work\March 2013\dehy.ddf

Date: March 15, 2013

### DESCRIPTION:

Description: Samson Resources

Spring Creek Compressor Station

Dehydration Unit with 60 MMSCFD capacity

Annual Hours of Operation: 8760.0 hours/yr

### EMISSIONS REPORTS:

### UNCONTROLLED REGENERATOR EMISSIONS

Component	lbs/hr	lbs/day	tons/yr
	1.3334	32 003	5 8405
	0.0518		
Propage	0.0097	0.233	0.0426
	0.0042		
n-Butane			
II Dacaire	0.0017	0.112	0.0203
Isopentane	0.0146	0.349	0.0638
n-Pentane		0.105	
n-Hexane		0.114	
Other Hexanes	0.0099	0.238	0.0434
Heptanes	0.0071	0.170	0.0310
-			
Methylcyclohexane	0.0348	0.835	0.1523
Benzene	0.1952	4.684	0.8549
	0.4096		
Ethylbenzene	0.3970	9.528	1.7388
Xylenes			
C8+ Heavies	0.3852	9.245	1.6871
Total Emissions	3.3613	80.670	14.7223
Total Hydrocarbon Emissions		80.670	
Total VOC Emissions			8.6550
Total HAP Emissions			
Total BTEX Emissions	1.4968	35.923	6.5559

### FLASH TANK OFF GAS

Component	lbs/hr	lbs/day	tons/yr
Methane	2.5751	61.803	11.2791
Ethane	0.0300	0.719	0.1312
Propane	0.0026	0.061	0.0112
Isobutane	0.0008	0.018	0.0033
n-Butane	0.0006	0.016	0.0028
Isopentane	0.0018	0.043	0.0078
n-Pentane	0.0004	0.010	0.0019
n-Hexane	0.0003	0.006	0.0012
Other Hexanes	0.0007	0.018	0.0032
Heptanes	0.0002	0.005	0.0009

Methylcyclohexane Benzene Toluene Ethylbenzene Xylenes	0.0004 0.0004 0.0006 0.0003	0.010 0.010 0.014 0.008 0.007	Page: 2 0.0018 0.0018 0.0025 0.0014 0.0012
C8+ Heavies	0.0013	0.030	0.0055
Total Emissions	2.6157	62.777	11.4569
Total Hydrocarbon Emissions Total VOC Emissions Total HAP Emissions Total BTEX Emissions	2.6157 0.0106 0.0019 0.0016	62.777 0.255 0.044 0.038	11.4569 0.0466 0.0081 0.0069

### EQUIPMENT REPORTS:

### ABSORBER

Specified Absorber Stages: 2.11
Calculated Dry Gas Dew Point: 2.99 lbs. H2O/MMSCF
Temperature: 60.0 deg. F
120.0 psig
Dry Gas Flow Rate: 60.0000 MMSCF/day
Glycol Losses with Dry Gas: 0.0373 lb/hr

Wet Gas Water Content: Saturated

Calculated Wet Gas Water Content: 94.28 lbs. H2O/MMSCF Calculated Lean Glycol Recirc. Ratio: 3.94 gal/lb H2O

Component	Remaining in Dry Gas		
Water	3.17%	96.83%	
Carbon Dioxide	99.92%	0.08%	
Nitrogen	100.00%	0.00%	
Methane			
Ethane	99.98%	0.02%	
Propane	99.96%	0.04%	
Isobutane	99.92%	0.08%	
n-Butane	99.88%	0.12%	
Isopentane	99.85%	0.15%	
n-Pentane	99.80%	0.20%	
n-Hexane	99.56%	0.44%	
Other Hexanes	99.69%	0.31%	
Heptanes	98.90%	1.10%	
Methylcyclohexane	97.28%	2.72%	
Benzene	81.00%	19.00%	
Toluene	66.22%	33.78%	
Ethylbenzene	43.20%	56.80%	
Xylenes	29.19%	70.81%	
C8+ Heavies	95.08%	4.92%	

### FLASH TANK

Flash Control: Vented to atmosphere Flash Temperature: 140.0 deg. F Flash Pressure: 40.0 psig

Page: 3

Component		Removed in Flash Gas
Water	99.99%	
Carbon Dioxide	85.11%	
Nitrogen		
Methane	34.12%	
Ethane	63.35%	36.65%
Propane	79.14%	20.86%
Isobutane	84.80%	15.20%
n-Butane	87.84%	12.16%
Isopentane	89.10%	10.90%
n-Pentane	91.02%	8.98%
n-Hexane	94.66%	5.34%
Other Hexanes	93.19%	6.81%
Heptanes	97.23%	2.77%
Methylcyclohexane	98.90%	
Benzene	99.80%	0.20%
Toluene	99.87%	0.13%
Ethylbenzene	99.93%	0.07%
Xylenes	99.95%	0.05%
C8+ Heavies	99.71%	0.29%

### REGENERATOR

No Stripping Gas used in regenerator.

Component	Remaining in Glycol	
Water Carbon Dioxide Nitrogen Methane Ethane	35.65% 0.00% 0.00% 0.00% 0.00%	100.00% 100.00% 100.00%
Propane Isobutane n-Butane Isopentane n-Pentane	0.00% 0.00% 0.00% 0.56% 0.55%	100.00% 99.44%
n-Hexane Other Hexanes Heptanes Methylcyclohexane Benzene	0.53% 1.07% 0.51% 4.04% 5.01%	98.93% 99.49%
Toluene Ethylbenzene Xylenes C8+ Heavies	7.91% 10.41% 12.91% 12.06%	

STREAM	REPORTS:			

WET GAS STREAM

Temperature: 60.00 deg. F Pressure: 134.70 psia Flow Rate: 2.51e+006 scfh

Component		Loading (lb/hr)
Carbon Dioxide Nitrogen Methane	1.99e-001 4.01e+000 3.66e-001 9.52e+001 2.30e-001	1.17e+004 6.77e+002 1.01e+005
Isobutane n-Butane Isopentane	9.38e-003 1.60e-003 1.20e-003 2.30e-003 4.99e-004	6.13e+000 4.60e+000 1.09e+001
Other Hexanes Heptanes Methylcyclohexane	9.98e-005	3.41e+000 6.60e-001 1.29e+000
Ethylbenzene	9.98e-005 6.99e-004	7.00e-001 7.00e-001

### DRY GAS STREAM

Temperature: 60.00 deg. F Pressure: 134.70 psia Flow Rate: 2.50e+006 scfh

Flow Rate: 2.50e+006 Scin			
Component		Loading (lb/hr)	
Carbon Dioxide Nitrogen Methane	6.31e-003 4.01e+000 3.67e-001 9.54e+001 2.30e-001	1.16e+004 6.77e+002 1.01e+005	
Isobutane n-Butane Isopentane	9.40e-003 1.60e-003 1.20e-003 2.30e-003 4.99e-004	6.12e+000 4.59e+000 1.09e+001	
Other Hexanes Heptanes Methylcyclohexane	9.89e-005	3.40e+000 6.53e-001 1.26e+000	
Ethylbenzene	2.92e-005 6.66e-004	3.02e-001 2.04e-001 7.47e+000	

### LEAN GLYCOL STREAM

Temperature: 60.00 deg. F
Flow Rate: 1.50e+001 gpm

Conc. Loading (wt%) (lb/hr) Component \_\_\_\_\_ TEG 9.85e+001 8.32e+003 Water 1.50e+000 1.27e+002 Carbon Dioxide 1.13e-011 9.53e-010 Nitrogen 3.04e-014 2.57e-012 Methane 1.56e-018 1.31e-016 Ethane 4.57e-010 3.86e-008 Propane 5.92e-012 5.00e-010 Isobutane 1.77e-012 1.49e-010 n-Butane 1.56e-012 1.32e-010 Isopentane 9.73e-007 8.22e-005 n-Pentane 2.86e-007 2.42e-005 n-Hexane 2.99e-007 2.52e-005 Other Hexanes 1.27e-006 1.08e-004 Heptanes 4.33e-007 3.66e-005 Methylcyclohexane 1.74e-005 1.47e-003 Benzene 1.22e-004 1.03e-002 Toluene 4.17e-004 3.52e-002 Ethylbenzene 5.46e-004 4.62e-002 Xylenes 8.69e-004 7.34e-002 C8+ Heavies 6.26e-004 5.28e-002 -----Total Components 100.00 8.45e+003

### RICH GLYCOL STREAM

\_\_\_\_\_

Temperature: 60.00 deg. F Pressure: 134.70 psia Flow Rate: 1.55e+001 gpm

NOTE: Stream has more than one phase.

Component		Loading (lb/hr)
Water Carbon Dioxide Nitrogen	9.57e+001 4.09e+000 1.10e-001 2.95e-004 4.50e-002	3.55e+002 9.53e+000 2.57e-002
Propane Isobutane	9.41e-004 1.41e-004 5.74e-005 6.12e-005 1.89e-004	1.23e-002 4.98e-003 5.32e-003
n-Hexane Other Hexanes	8.42e-005	5.05e-003 1.08e-002 7.32e-003
Toluene Ethylbenzene	6.55e-003	4.45e-001 4.43e-001 5.69e-001

Total Components 100.00 8.69e+003

### FLASH TANK OFF GAS STREAM

Temperature: 140.00 deg. F Pressure: 54.70 psia Flow Rate: 7.42e+001 scfh

Component Conc. Loading (vol%) (lb/hr) Water 5.31e-001 1.87e-002 Carbon Dioxide 1.65e+001 1.42e+000 Nitrogen 3.13e-001 1.72e-002 Methane 8.21e+001 2.58e+000 Ethane 5.09e-001 3.00e-002 Propane 2.97e-002 2.56e-003 Isobutane 6.66e-003 7.57e-004 n-Butane 5.69e-003 6.47e-004 Isopentane 1.27e-002 1.79e-003 n-Pentane 3.07e-003 4.34e-004 n-Hexane 1.60e-003 2.70e-004 Other Hexanes 4.34e-003 7.32e-004 Heptanes 1.03e-003 2.03e-004 Methylcyclohexane 2.09e-003 4.02e-004 Benzene 2.67e-003 4.08e-004 Toluene 3.14e-003 5.66e-004 Ethylbenzene 1.57e-003 3.26e-004 Xylenes 1.36e-003 2.82e-004 C8+ Heavies 3.76e-003 1.25e-003 Total Components 100.00 4.07e+000

### FLASH TANK GLYCOL STREAM

Temperature: 140.00 deg. F Flow Rate: 1.55e+001 gpm

C	component	Conc. (wt%)	Loading (lb/hr)	
,	Water Carbon Dioxide Nitrogen	9.58e+001 4.09e+000 9.34e-002 9.80e-005 1.54e-002	3.55e+002 8.11e+000 8.51e-003	
	Propane Isobutane	5.96e-004 1.12e-004 4.87e-005 5.38e-005 1.69e-004	9.72e-003 4.22e-003 4.67e-003	
м	n-Hexane Other Hexanes	8.19e-005	4.78e-003 1.00e-002 7.11e-003	
	Toluene Ethylbenzene	2.37e-003 5.12e-003 5.10e-003 6.55e-003	4.45e-001 4.43e-001	

C8+ Heavies 5.05e-003 4.38e-001 Total Components 100.00 8.68e+003

### REGENERATOR OVERHEADS STREAM

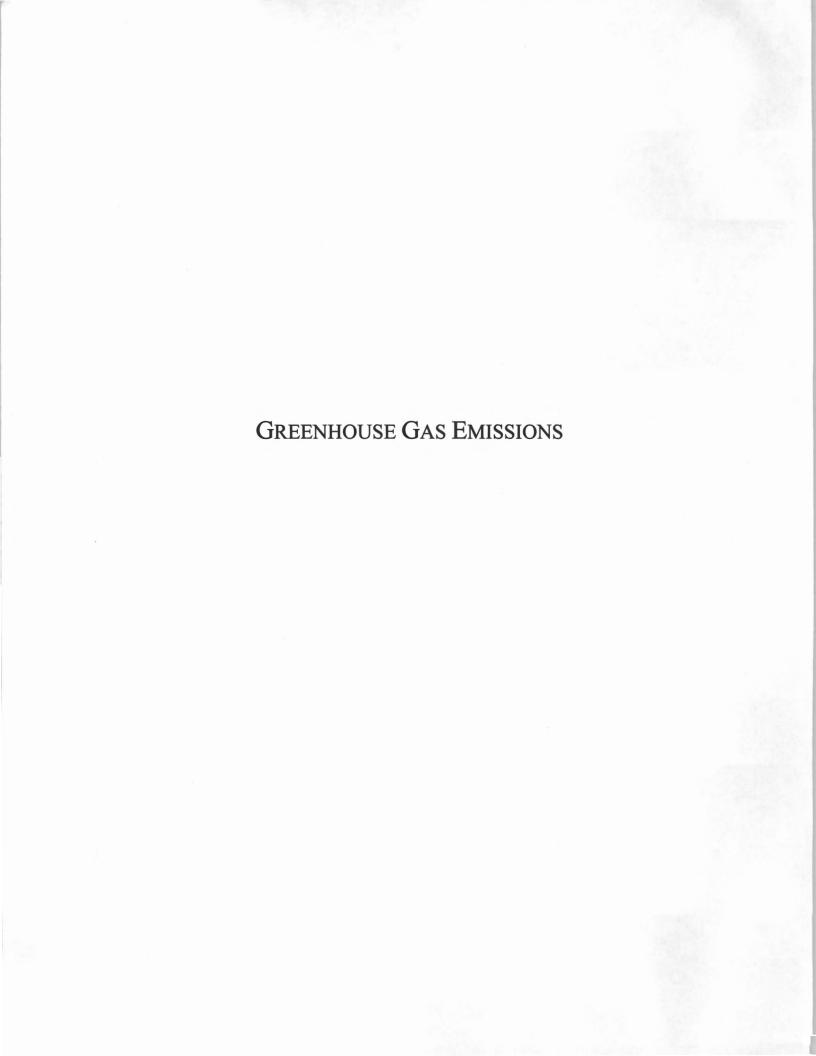
Temperature: 212.00 deg. F Pressure: 14.70 psia Flow Rate: 4.93e+003 scfh

Component		Loading (lb/hr)
Carbon Dioxide Nitrogen Methane	9.78e+001 1.42e+000 2.34e-003 6.40e-001 1.33e-002	8.11e+000 8.51e-003 1.33e+000
Isobutane n-Butane Isopentane	1.70e-003 5.60e-004 6.19e-004 1.55e-003 4.67e-004	4.22e-003 4.67e-003 1.46e-002
Other Hexanes Heptanes Methylcyclohexane	5.44e-004	9.91e-003 7.08e-003 3.48e-002
Ethylbenzene	3.59e-002 1.74e-002	3.97e-001 4.95e-001 3.85e-001
_		

EMISSION UNIT FUG FUGITIVE EMISSIONS

# Emission Estimates Emission Unit FUG Spring Creek Compressor Station

Service Compor	Component	Count	Emission factor	VOC	
Service	Component		(lb/component/hr)	(lb/hr)	(tpy)
		VOC W	t. % = 0.06		
	Valves	258	0.00992	0.00	0.01
	Connectors	86	0.00044	0.00	0.00
Gas	Flanges	40	0.00086	0.00	0.00
5	Other	116	0.01940	0.00	0.01
	Open End	0	0.00441	0.00	0.00
	Pump Seals	0	0.00529	0.00	0.00
		VOC Wt.	% = 100.00		
	Valves	76	0.00551	0.42	1.83
_	Connectors	14	0.00046	0.01	0.03
, Oi	Flanges	2	0.00024	0.00	0.00
Slop/Oil	Other	2	0.01653	0.03	0.14
02	Open End	0	0.00309	0.00	0.00
	Pump Seals	0	0.02866	0.00	0.00
		VOC Wt.	% = 1.00.00		
	Valves	33	0.00551	0.18	0.80
	Connectors	10	0.00046	0.00	0.02
col	Flanges	0	0.00024	0.00	0.00
Glycol	Other	2	0.01653	0.00	0.00
	Open End	0	0.00309	0.00	0.00
	Pump Seals	2	0.02866	0.06	0.25
		VOC Wt	% = 50.00		
	Valves	65	0.000216	0.01	0.03
	Connectors	40	0.000243	0.00	0.02
ter	Flanges	2	0.000006	0.00	0.00
Water	Other	19	0.000053	0.00	0.00
	Open End	0	0.030865	0.00	0.00
	Pump Seals	1	0.000551	0.00	0.00
		768		0.72	3.15



### Total Greenhouse Gas PTE Samson Resources Company Spring Creek Compressor Station

		Green	House Gases En	Total GHG PTE	CO <sub>2</sub> e PTE	
Source ID	Description	Description CO <sub>2</sub>			N <sub>2</sub> O	CO2CTIE
	/ Lancard Control of the Control of	tpy	tpy	tpy	tpy	tpy
E1	Caterpillar G3516LE	4199.8	58.1	0.01	4257.9	5423.0
E2	Caterpillar G3516LE	4199.8	58.1	0.01	4257.9	5423.0
E3	Caterpillar G3516LE	4199.8	58.1	0.01	4257.9	5423.0
E4	Caterpillar G3516LE	4199.8	58.1	0.01	4257.9	5423.0
E5	Caterpillar G3516LE	4199.8	58.1	0.01	4257.9	5423.0
E6	Caterpillar G3516LE	4199.8	58.1	0.01	4257.9	5423.0
E7	Caterpillar G3516LE	4199.8	58.1	0.01	4257.9	5423.0
E8	Caterpillar G3516LE	4199.8	58.1	0.01	4257.9	5423.0
E9	Caterpillar G3516LE	4199.8	58.1	0.01	4257.9	5423.0
E10	Caterpillar G3516LE	4199.8	58.1	0.01	4257.9	5423.0
D1	0.75 MMBtu/hr Reboiler	369.4	0.0	0.01	369.4	372.5
D1	Glycol Process Vents	41.7	17.1	0.00	58.8	400.8
FUG	Fugitive Leaks	2.2	18.9	0.00	21.1	399.1
otal		42411.3	617.0	0.11	43,028.4	55,402.4
O <sub>2</sub> e		42411.3	12957.0	34.1		

Total GHG PTE Total CO<sub>2</sub>e 43,028.4 tpy 55,402.4 tpy

### Compressor Engine GHG Emission Estimate Samson Resources Company Spring Creek Compressor Station

### **Basis**

Units Caterpillar G3516LE Compressor Engines

Combustion 4 Stroke Lean Burn
Rating 1092 hp

Operating Hours 8760 hours/year
Fuel Consuption 7500 Btu/hp-hr
Fuel Heat Content 975 Btu/scf

Blowdown Volume 40927 scf
Blowdown Events 20 per year

Packing Vent Volume 60 scf/cylinder
Number of cylinders 4 cylinders/engine

Starter Gas Usage 1100 scfm
Start Time 0.167 min
Starting Events 52 per year

**Emissions Estimate (per engine)** 

	E	xhaust		Rod Packing Vents		Blowdowns		Starter		Totals		
Pollutant	<b>Emission Factor</b>	Emissions		Emissions		Emissions		Emissions		Totals	Emission Factor Source	
	(lb/MMBtu)	(lb/hr)	(tpy)	(lb/hr)	(tpy)	(lb/event)	(tpy)	(lb/event)	(tpy)	(tpy)		
$\mathbb{CO}_2$	116.889	957	4,193	1.10	4.83	187.92	1.88	0.84	0.02	4,199.79	40 CFR Part 98, Subpart C, Table C-1	
Methane	0.002	0.016	0.072	9.51	41.66	1622.08	16.22	7.28	0.19	58.14	40 CFR Part 98, Subpart C, Table C-2	
N <sub>2</sub> O	0.0002	0.002	0.008	0	0	0	0	0	0	0.01	40 CFR Part 98, Subpart C, Table C-2	

### Glycol Dehydration Process Vents GHG Emission Estimate Samson Resources Company Spring Creek Compressor Station

### **Basis**

Unit Dehydration Unit
Annual Throughput 60 MMscfd
Hours of Operation 8760 hrs

Emissions Based on GLYCalc 3.0 Model

### **Emissions Estimate**

Pollutant	lb/hr	tpy	
CO <sub>2</sub>	9.53	41.74	
Methane	3.91	17.13	
N <sub>2</sub> O	0.0	0	

### Natural Gas Fired Burner GHG Emission Estimate Samson Resources Company **Spring Creek Compressor Station**

**Basis** Units

Dehydration Unit Reboiler

Hours of Operation

8760 hrs

Fuel Heat Content

975 Btu/scf

Heat Input Rate

0.75 MMBtu/hr

### **Emissions**

Dellestant	<b>Emission Factor</b>	r Emissions		Eii Et S
Pollutant	(lb/MMscf)	(lb/hr)	(tpy)	Emission Factor Source
CO <sub>2</sub>	120,000	84.34	369.42	AP-42 Table 1.4-2
Methane	2.3	0.00	0.01	AP-42 Table 1.4-2
N <sub>2</sub> O	2.2	0.00	0.01	AP-42 Table 1.4-2

### Fugitive GHG Emission Estimate Samson Resources Company Spring Creek Compressor Station

### **Basis**

 Units
 Fugitive Emissions

 CO2
 10.273 wt%

 CH4
 88.671 wt%

### **Emissions Estimate**

Component	Count	Emission Factor	CC	)2	Methane	
	Count	(kg/component-hr)	(lb/hr)	(tpy)	(lb/hr)	(tpy)
Flanges	40	3.90E-04	0.00	0.02	0.03	0.13
Valves	258	4.50E-03	0.26	1.15	2.27	9.93
Connectors	86	2.00E-04	0.00	0.02	0.03	0.15
Press Relief	0	2.00E-03	0.00	0.00	0.00	0.00
Pump Seals	0	2.40E-03	0.00	0.00	0.00	0.00
Other	116	8.80E-03	0.23	1.01	1.99	8.73
Total			0.50	2.19	4.33	18.95

Emission factors obtained from the 1995 Protocol for Equipment Leak Emission Estimates Document EPA-453/R-95-017 Table 2-4: Oil and Gas Production

### **Example GHG Emission Calculations Spring Creek Compressor Station**

Exhaust/Combustion

$$1092 \; hp \; * \frac{7500 \; Btu}{hp \; hr} * \frac{MMBtu}{1,000,000 \; Btu} * \frac{116.889 \; lb \; CO_2}{MMBtu} = 957 \; \frac{lb \; CO_2}{hr}$$

957 
$$\frac{lb\ CO_2}{hr} * \frac{ton}{2000\ lb} * \frac{8760\ hr}{yr} = 4,193\ tpy\ CO_2$$

$$1092 \ hp \ *\frac{7500 \ Btu}{hp \ hr} *\frac{MMBtu}{1,000,000 \ Btu} *\frac{0.002 \ lb \ CH_4}{MMBtu} = 0.016 \ \frac{lb \ CH_4}{hr}$$

$$0.016 \frac{lb CH_4}{hr} * \frac{ton}{2000 lb} * \frac{8760 hr}{yr} = 0.072 tpy CH_4$$

$$1092 hp * \frac{7500 Btu}{hp hr} * \frac{MMBtu}{1,000,000 Btu} * \frac{0.0002 lb N_2 O}{MMBtu} = 0.002 \frac{lb N_2 O}{hr}$$

$$0.002 \; \frac{lb \; N_2O}{hr} * \frac{ton}{2000 \; lb} * \frac{8760 \; hr}{yr} = \; 0.008 \; tpyN_2O$$

Cylinder Rod Packing Vents

$$\frac{60\,scf}{hr*cylinder}*\frac{4\,cylinder}{compressor}*\frac{mole}{385\,scf}*\frac{4.0177\,mole\,CO_2}{100\,mole}*\frac{44\,lb\,CO_2}{mole\,CO_2}=1.10\,\frac{lb\,CO_2}{hr}$$

$$1.10 \frac{lb CO_2}{hr} * \frac{ton}{2000 lb} * \frac{8760 hr}{yr} = 4.83 tpy CO_2$$

$$\frac{60 \, scf}{hr*cylinder}*\frac{4 \, cylinder}{compressor}*\frac{mole}{385 \, scf}*\frac{95.368 \, mole \, CH_4}{100 \, mole}*\frac{16 \, lb \, CH_4}{mole \, CH_4}=9.51 \, \frac{lb \, CH_4}{hr}$$

$$9.51 \frac{lb CH_4}{hr} * \frac{ton}{2000 lb} * \frac{8760 hr}{yr} = 41.66 tpy CH_4$$

### **Blowdown Emissions**

$$\frac{40,927\ scf}{event}*\frac{mole}{385\ scf}*\frac{4.0177\ mole\ CO_2}{100\ mole}*\frac{44\ lb\ CO_2}{mole\ CO_2}=187.92\ \frac{lb\ CO_2}{event}$$

$$187.92 \frac{lb CO_2}{event} * \frac{20 \ events}{yr} * \frac{ton}{2000 \ lb} = 1.88 \ tpy \ CO_2$$

$$\frac{40,927\ scf}{event}*\frac{mole}{385\ scf}*\frac{95.368\ mole\ CH_{4}}{100\ mole}*\frac{16\ lb\ CH_{4}}{mole\ CH_{4}}=1622.08\ \frac{lb\ CH_{4}}{event}$$

$$1622.08 \frac{lb CH_4}{event} * \frac{20 events}{vr} * \frac{ton}{2000 lb} = 16.22 tpy CH_4$$

### Starter Emissions

$$\frac{1100 \ scf}{min} * \frac{mole}{385 \ scf} * \frac{4.0177 \ mole \ CO_2}{100 \ mole} * \frac{44 \ lb \ CO_2}{mole \ CO_2} * \frac{0.167 \ min}{event} = 0.84 \ \frac{lb \ CO_2}{event}$$

$$0.84 \frac{lb CO_2}{event} * \frac{52 \ events}{yr} * \frac{ton}{2000 \ lb} = 0.02 \ tpy CO_2$$

$$\frac{1100 \ scf}{min} * \frac{mole}{385 \ scf} * \frac{95.368 \ mole \ CH_4}{100 \ mole} * \frac{16 \ lb \ CH_4}{mole \ CH_4} * \frac{0.167 \ min}{event} = 7.28 \ \frac{lb \ CH_4}{event}$$

7.28 
$$\frac{lb \ CH_4}{event} * \frac{52 \ events}{yr} * \frac{ton}{2000 \ lb} = 0.19 \ tpy \ CH_4$$