

Arsenic Removal During Iron Removal

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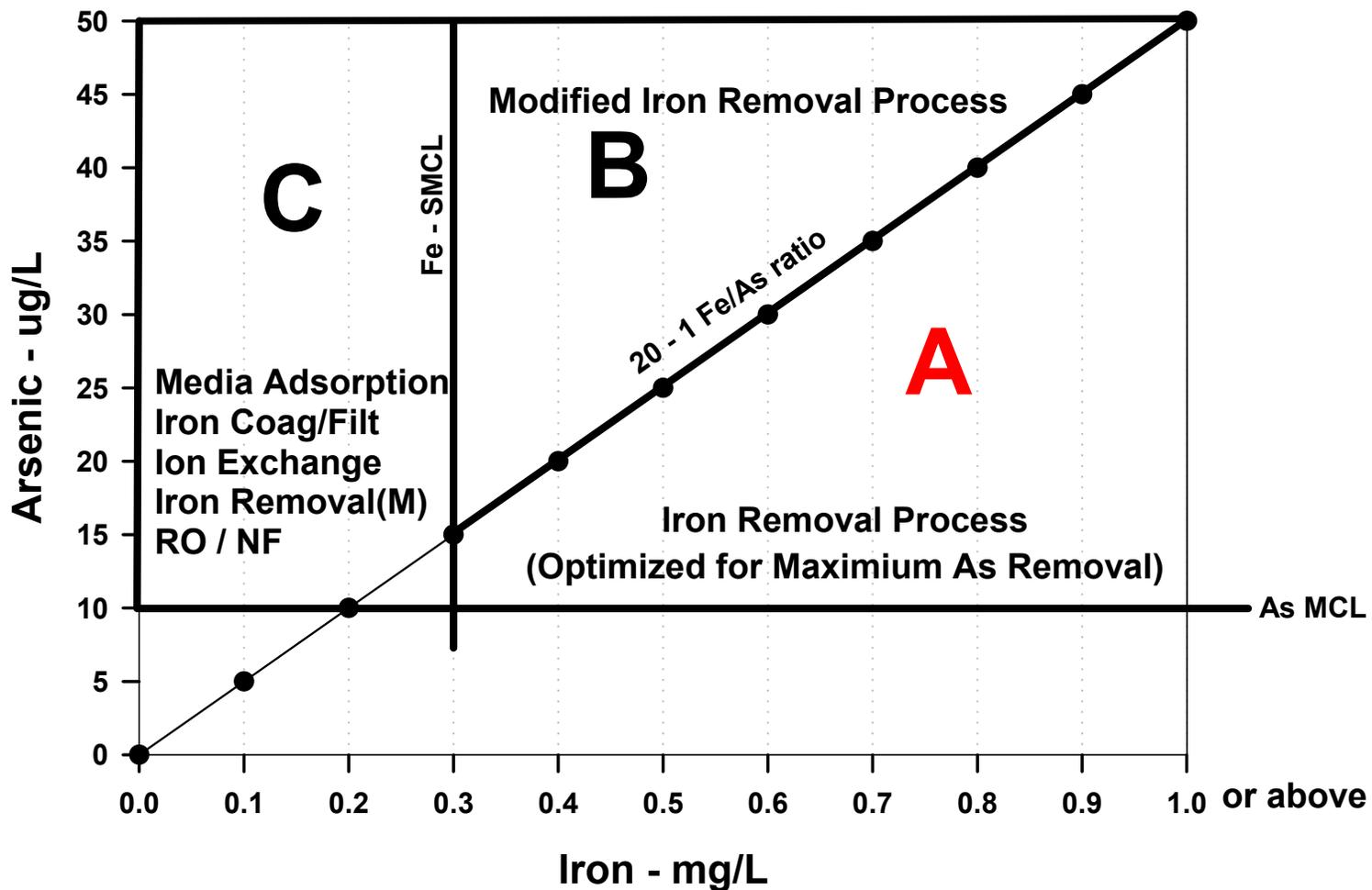
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Arsenic Rule Webcast
October 20, 2004

Iron-Based Arsenic Removal Processes

- Adsorptive properties of iron mineral toward arsenic are well known
- That knowledge is the basis for many arsenic treatment processes
 - **IRON REMOVAL**
 - Coagulation with iron coagulant
 - Iron-based adsorption media

Arsenic Treatment - Process Selection Guide

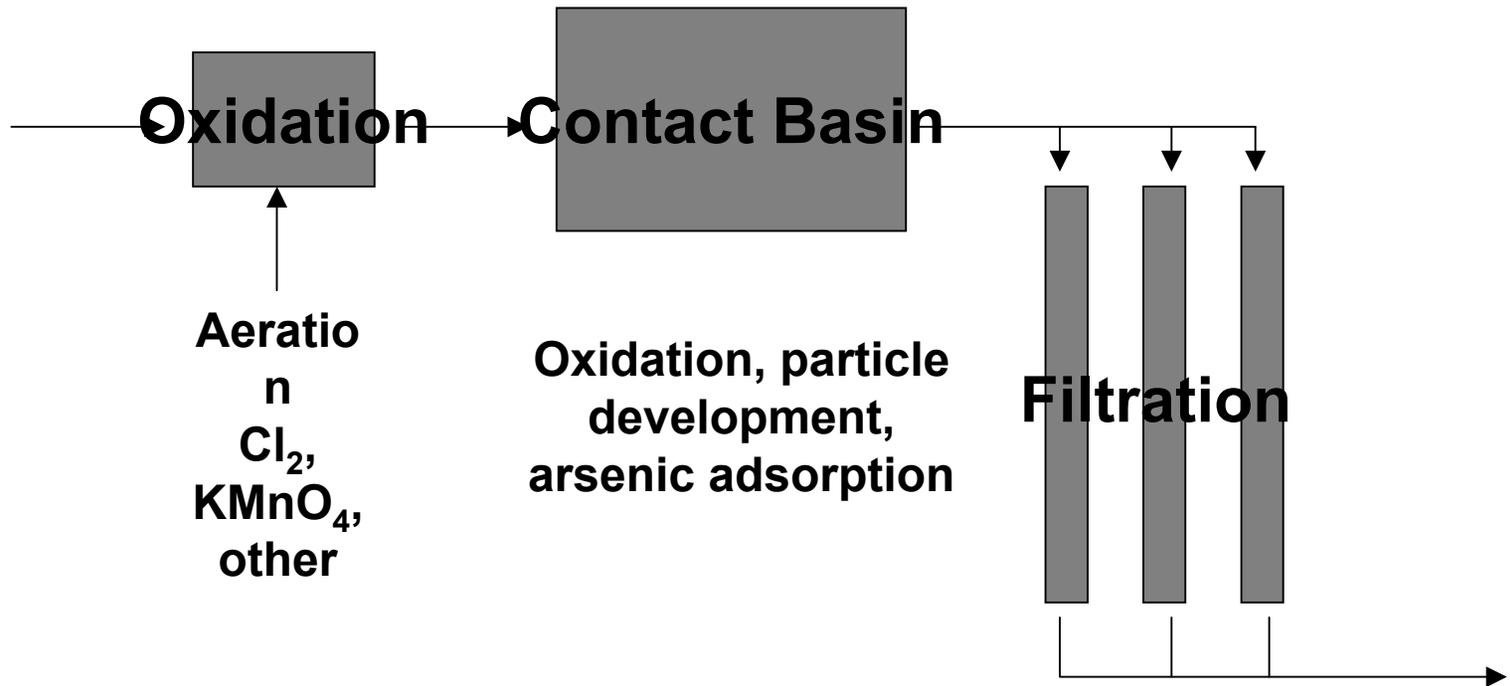


Removal of 1 mg/L of iron

achieves

removal of 50 ug/L arsenic
(Optimized conditions and As[V])

Iron and Arsenic (and Mn) Removal



Iron and Arsenic (and Mn) Removal

Fe(II),
As(III)

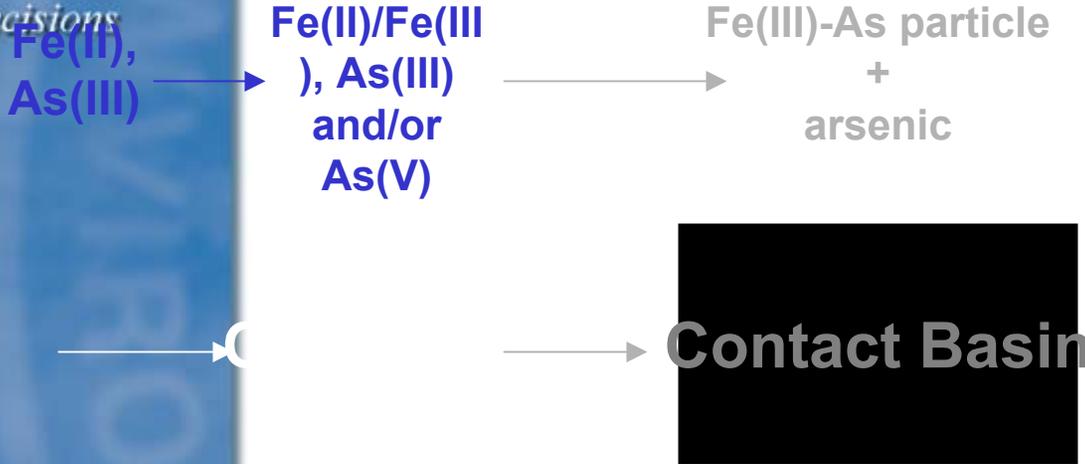
Fe(II)/Fe(III)
, As(III)
and/or
As(V)

Oxidation

Aeration
Cl₂,
KMnO₄,
other

Building a scientific foundation for sound environmental decisions

Iron and Arsenic (and Mn) Removal



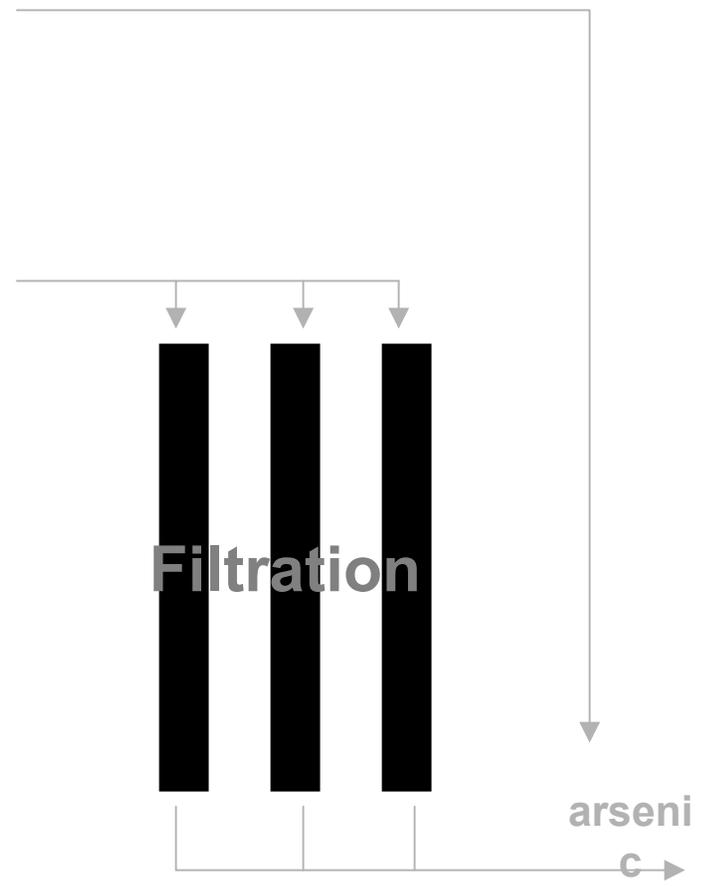
Oxidation, particle development, arsenic adsorption/coprec.

Iron and Arsenic (and Mn) Removal

Fe(II),
As(III)

Fe(II)/Fe(III)
, As(III)
and/or
As(V)

Fe(III)-As particle
+
arsenic



Case Studies

**Factors the impact arsenic
removal during iron removal.**

Form of Arsenic

As(III) vs As(V)

- **As(III) is removed during iron removal and other iron-based processes- just not as well as As(V)**
- **Aeration will oxidize Fe(II) to Fe(III) but not As(III) to As(V)**

Case Study 1-Ohio

As Oxidation State-Removal of As (III)

Fe(II)=2.7 mg/L, As=0.043 mg/L (80% As(III))

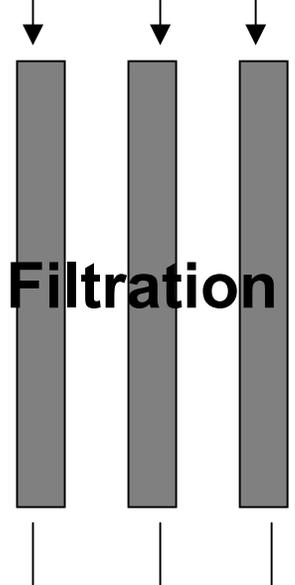


Aeration

As= 0.033 mg/L (80% As(III))
Ammonia > 1 mg/L



No contactor
Fe(III)-As particle + Arsenic (III)



As= 0.008 mg/L
Ammonia > nd

As (III) Oxidation

Effective!

- Free Chlorine
- Potassium Permanganate
- Ozone
- Solid Oxidizing Media (MnO_2 solids)

Ineffective

- Chloramine
- Chlorine Dioxide
- UV Radiation
- Oxygen

Oxidant Type

- Depends on As, Fe and Mn
- Aeration
 - May need contact basin
 - Will not address Mn and As oxidation
 - Iron particles have less surface area
 - May have longer filter run lengths
- Strong oxidants (chlorine, permanganate, etc)
 - Address Mn and As oxidation
 - Shorter filter run time possible
 - More particle surface area
 - Difficult to feed
 - Probably no contactor needed

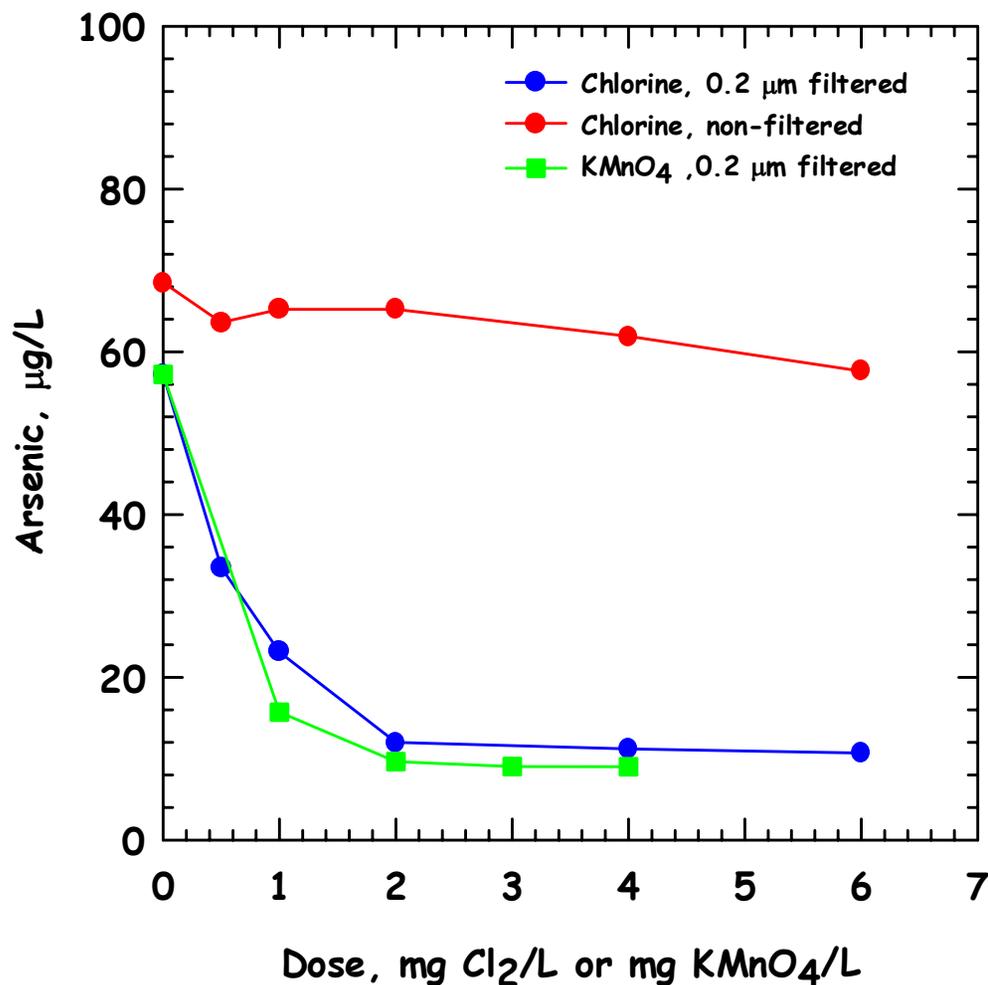
Oxidation- Case Study 2- Ohio

Source Water Quality

| <u>Parameter</u> | <u>Concentration</u> |
|------------------|----------------------|
| Arsenic - ug/L | 69 - 132 |
| As III | 85 % |
| As V | 15 % |
| Calcium - mg/L | 115 |
| Magnesium - mg/L | 58 - 60 |
| Iron - mg/L | 0.5 - 1.4 |
| Manganese -mg/L | 0.2 - 0.9 |
| Sulfate - mg/L | 1.2 - 10.0 |
| Silica - mg/L | NA |
| pH - units | 7.9 |

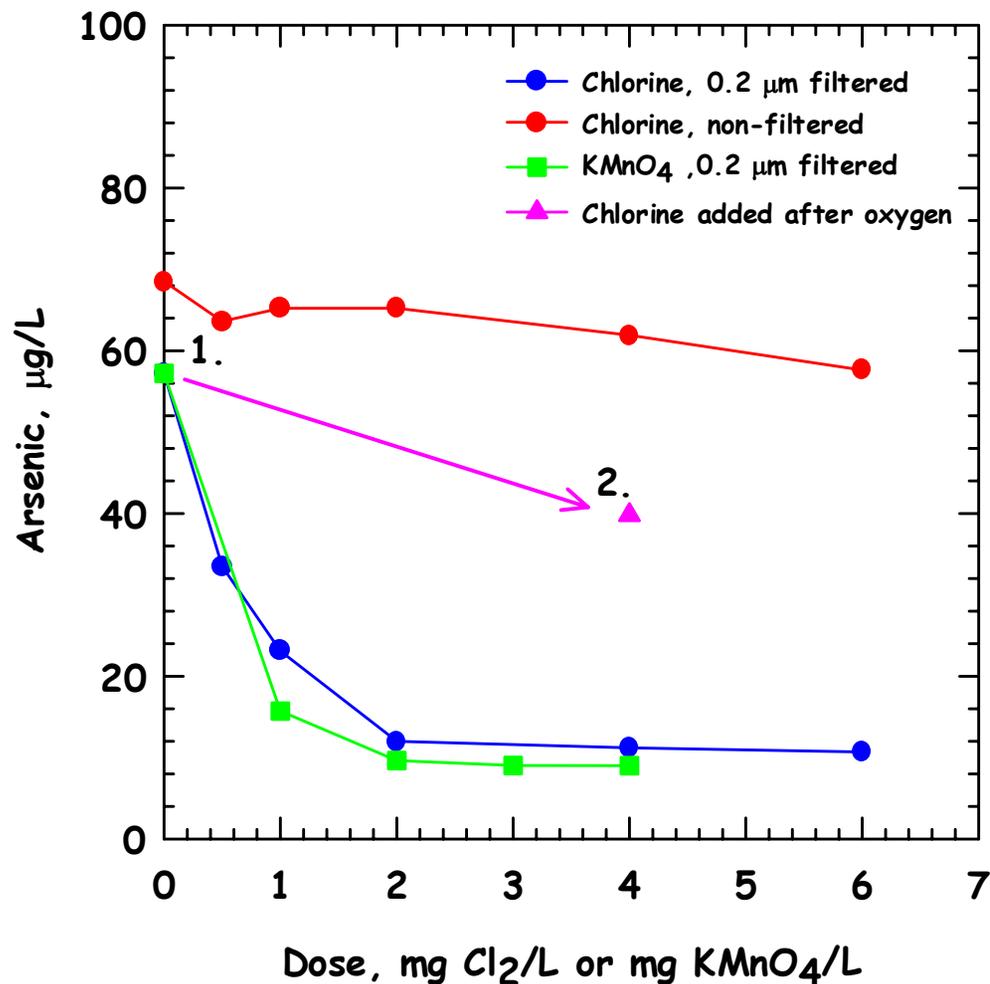
Effect of Oxidant Type and Concentration

Case Study 2- Ohio- pH 8.2, 1.7 mg O₂/L



Effect of Oxidant Type and Concentration

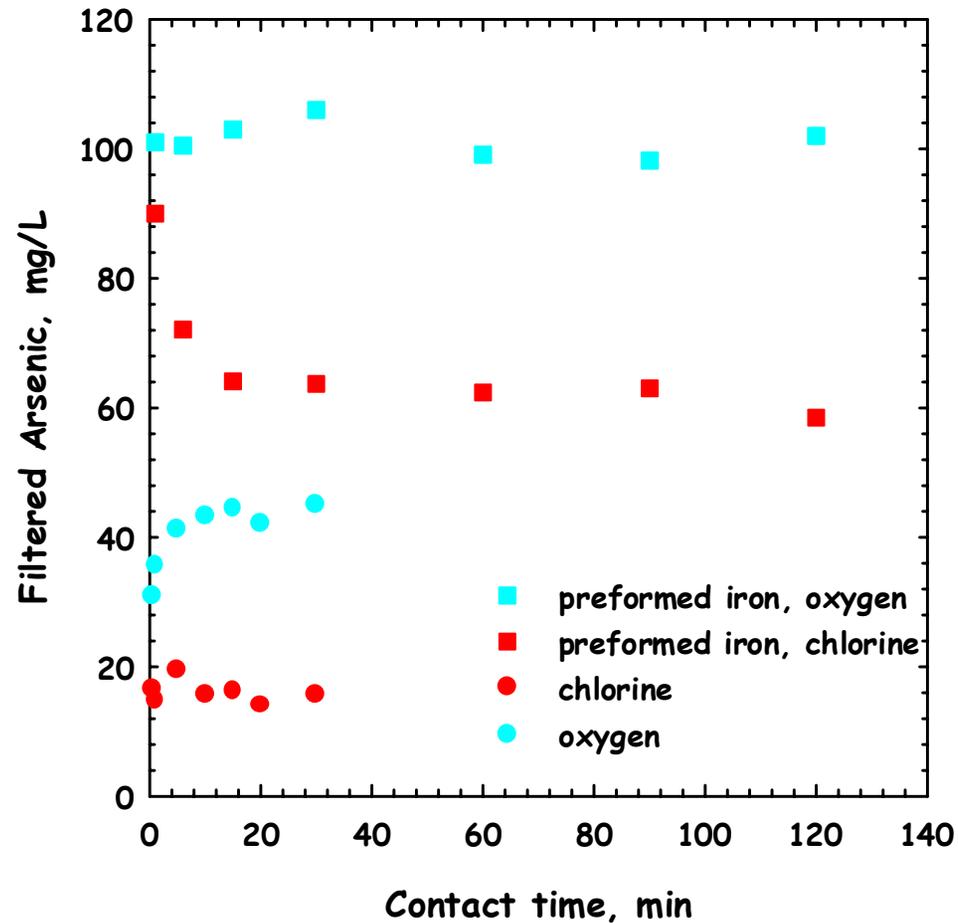
Case Study 2- Ohio- pH 8.2, 1.7 mg O₂/L



Oxidation

pH=8, DIC=10 mg C/L, As(V)=100 ug/L, Fe=1 mg/L

Point of Application and Contact Time



Oxidation- Point of Application

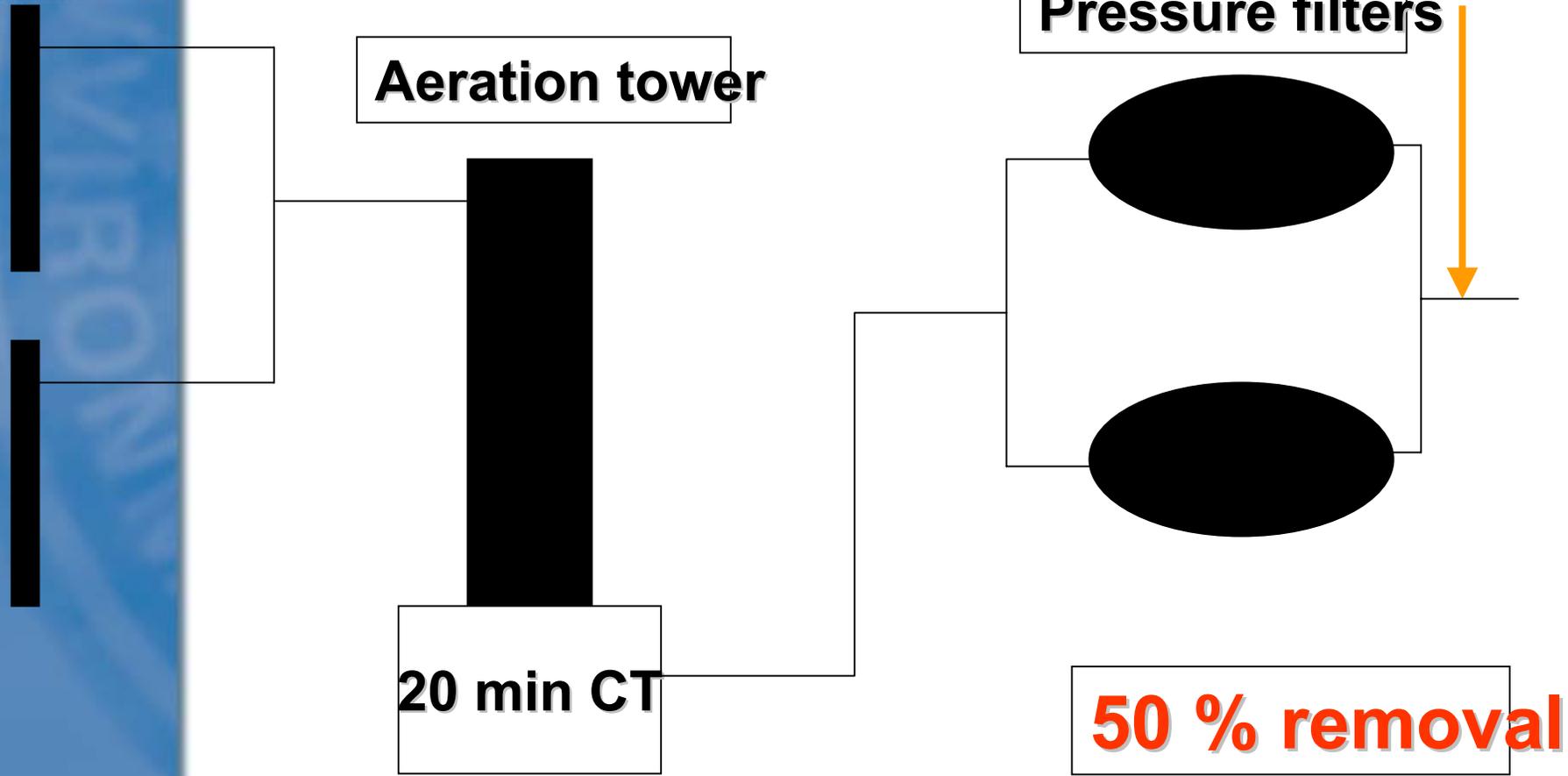
Case Study 3- Michigan

| <u>Parameter</u> | <u>Concentration</u> |
|------------------|----------------------|
| Arsenic - ug/L | 19 - 24 |
| As III | 95 % |
| As V | 5 % |
| Calcium - mg/L | 74 - 84 |
| Magnesium - mg/L | 30 - 33 |
| Iron - mg/L | 0.5 - 0.6 |
| Manganese -mg/L | 0.02 |
| Sulfate - mg/L | 50 - 60 |
| Silica - mg/L | 12 - 13 |
| pH - units | 7.1 - 7.3 |

Oxidation- Point of Application

Case Study 3- Michigan

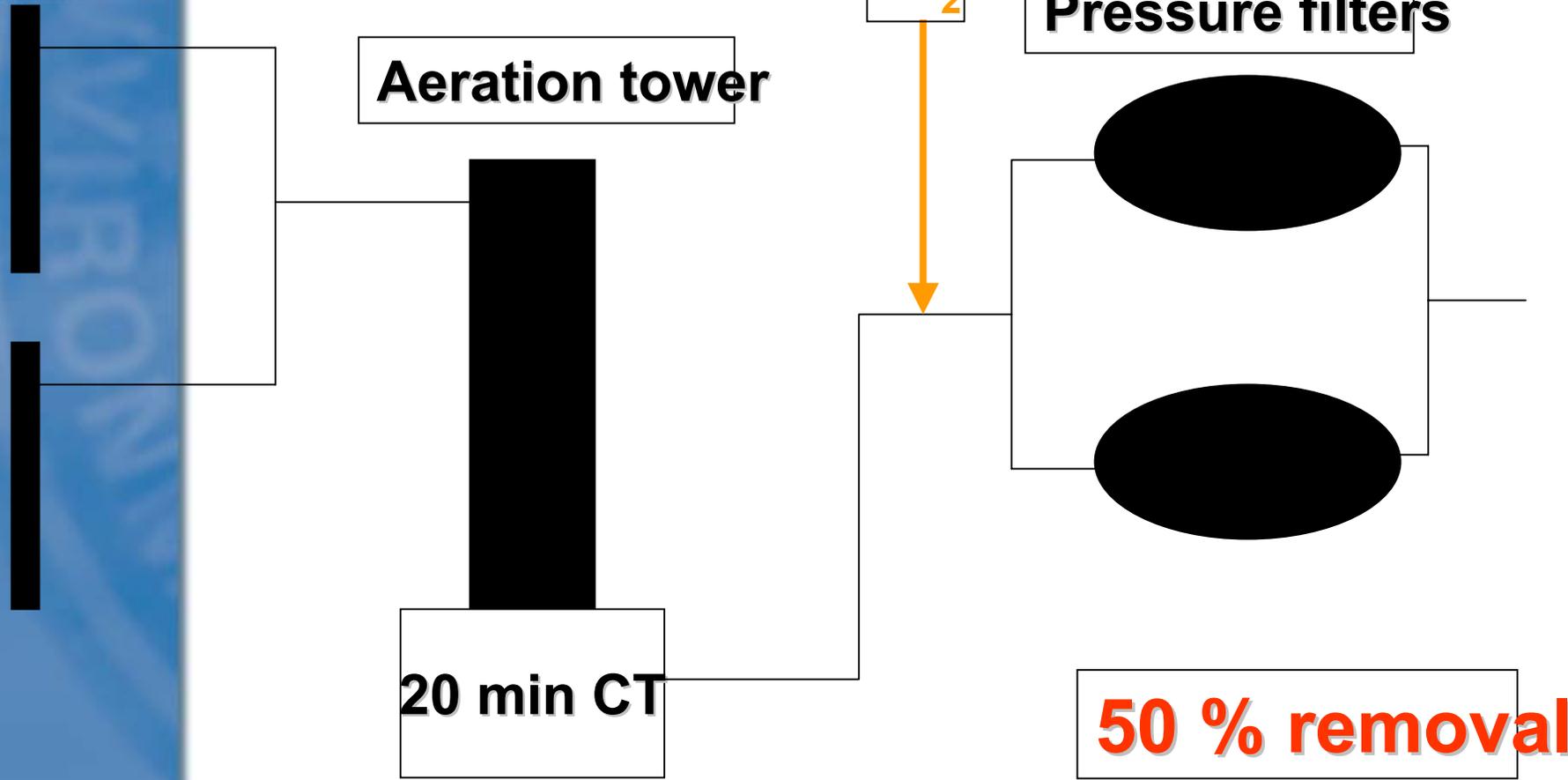
Wells



Oxidation- Point of Application

Case Study 3- Michigan

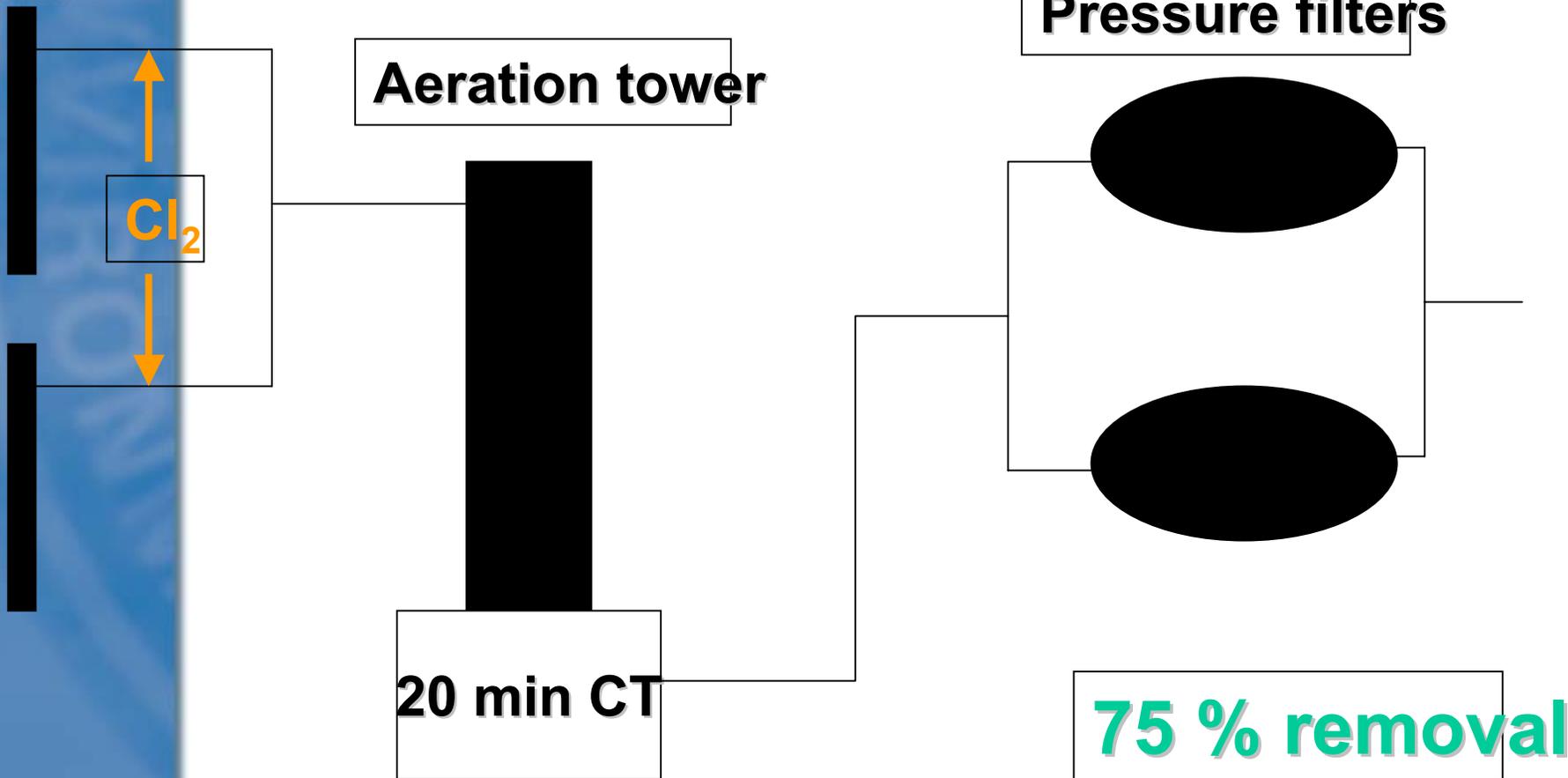
Wells



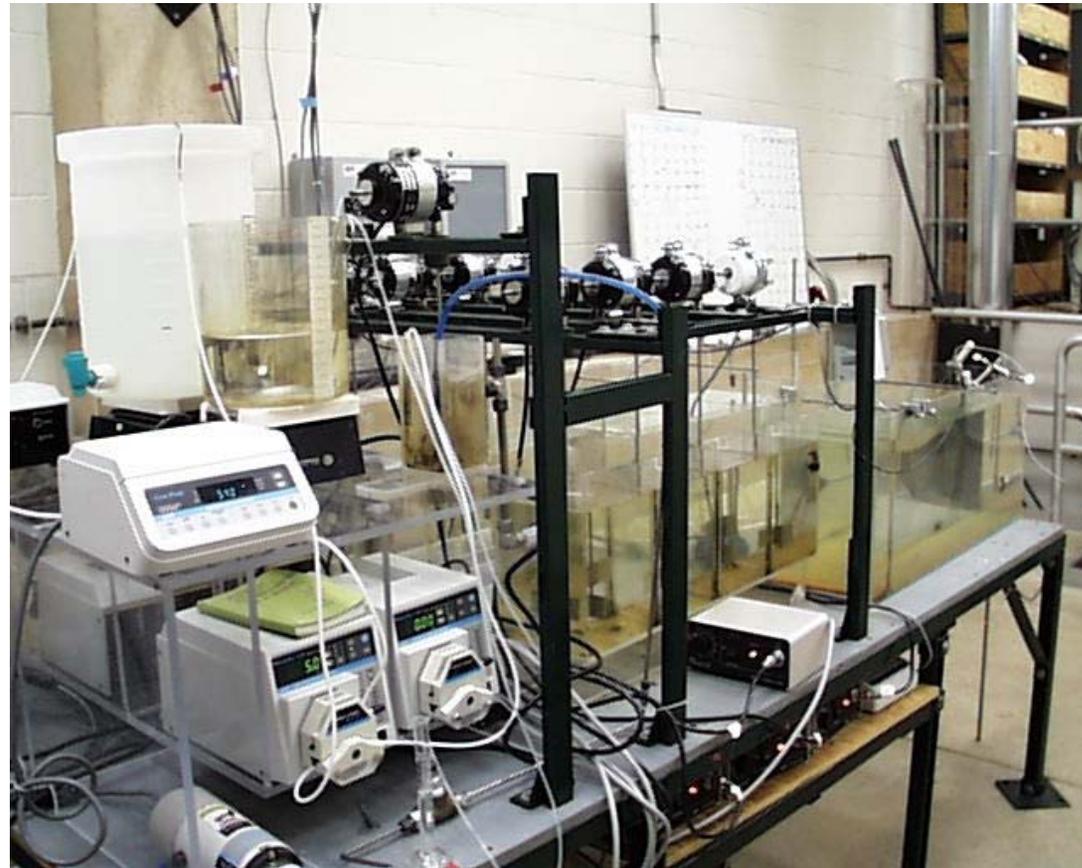
Oxidation- Point of Application

Case Study 3- Michigan

Wells



Pilot Plant Rapid Mix, Flocculation, Sedimentation



Pilot Plant Filters



Arsenic Pilot Plant Screening Runs

Arsenic Removal

(pH 7.2 with 20 mg/L DIC and 1.5 mg/L Fe)

| <u>Date</u> | <u>Floc</u> | <u>Cl₂ (mg/L)</u> | <u>As (mg/L)</u> | <u>As(mg/L)*_{final}</u> |
|-------------|-------------|------------------------------|--------------------------|----------------------------------|
| 8/12 | Yes | 1 | 100 (V) | 7 |
| 8/13 | Yes | - | 100 (V) | 13 |
| 8/14 | No | - | 100 (V) | 30** |
| 8/18 | No | 1 | 100 (V) | 7 |
| 8/19 | Yes | - | 100 (V) added after floc | 85 |
| 8/20 | Yes | 1 | 100 (V) added after floc | 48 |
| 8/22 | Yes | - | 100 (III) | 44 |
| 8/25 | Yes | 1 | 100 (III) | 8 |

* Average filter effluent value over complete test run

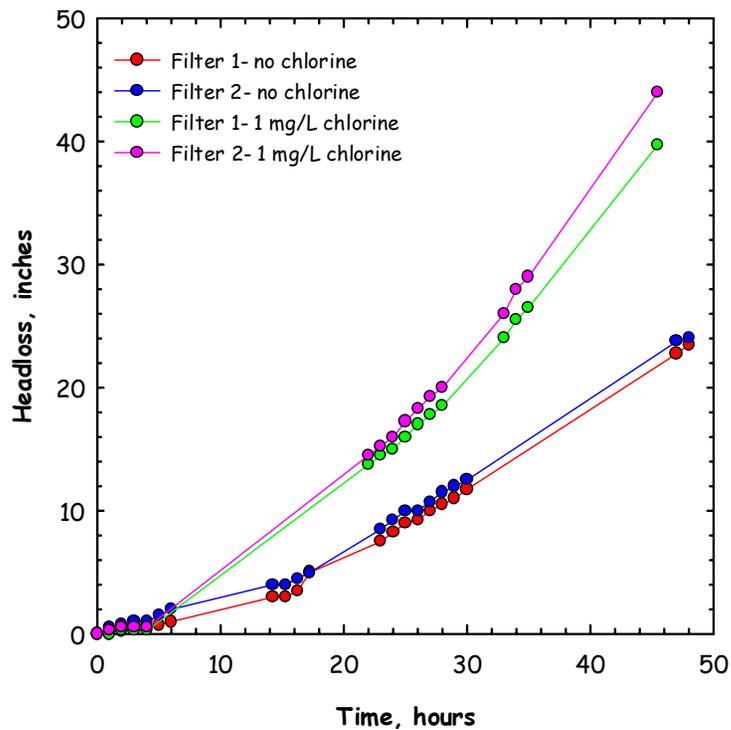
** Soluble iron passed filter

Arsenic Pilot Plant Runs

Headloss Build-Up

(pH 7.2 with 20 mg/L DIC and 1.5 mg/L Fe)

NO Calcium



Process Modifications

Increasing As Removal

Utility with iron removal in place or will be in place but can not meet MCL:

- Increase iron concentration
- Adjust pH
- Replace media w/ As adsorption media
- Change point of oxidant addition

Conclusions

- **Iron removal = arsenic removal**
- **Arsenic speciation is important**
- **Oxidant type is important**
- **Point of oxidant application is important**
 - **Arsenic removal impacted**
 - **Plant operation impacted**



Thank-you.