

Mitigation Options for Key Sources

Overview of technologies and practices

Distribution Technology Transfer Workshop

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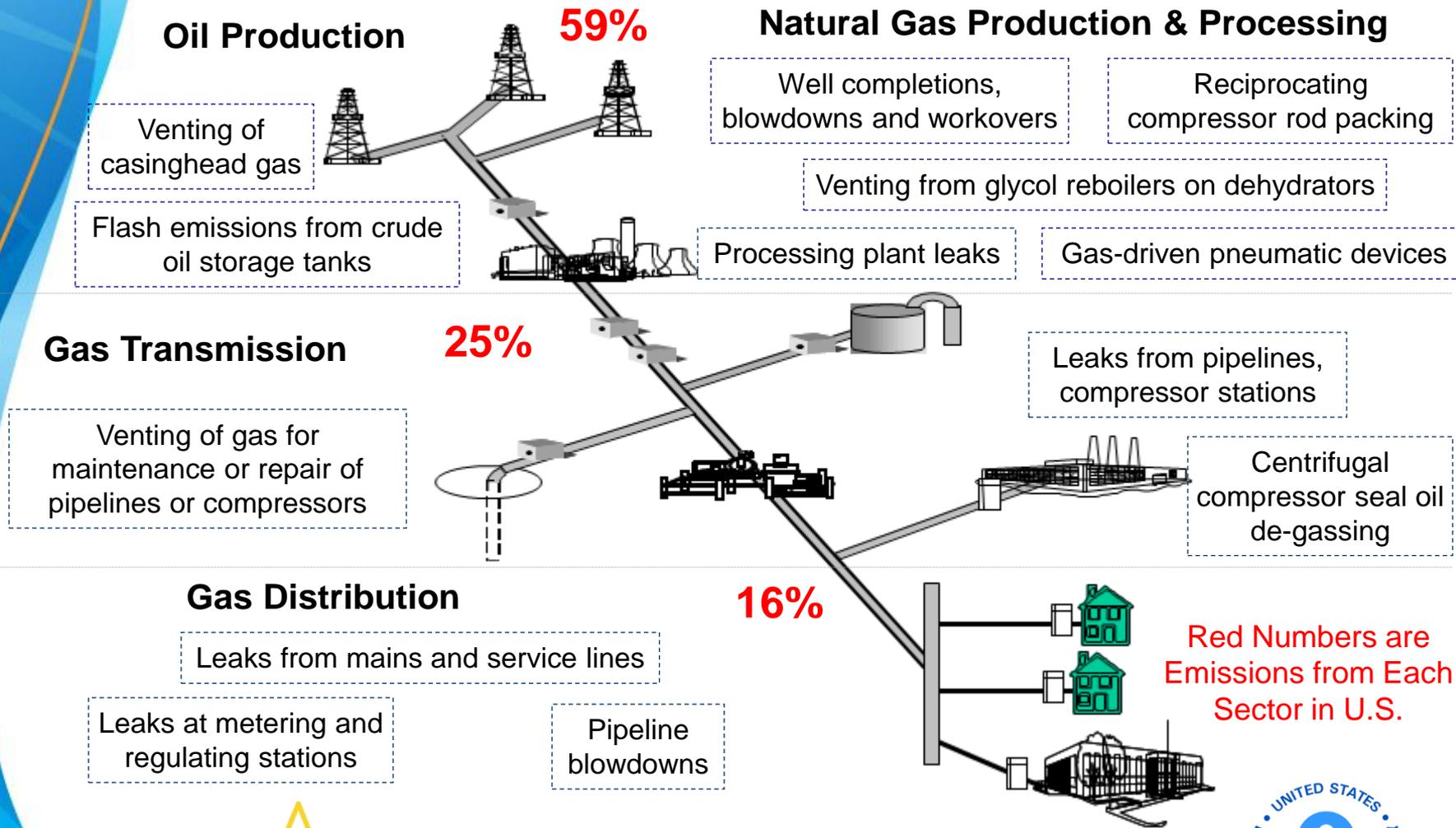


Distribution Emission Mitigation Options

- Compressor emission reductions
 - Rod packing replacement from reciprocating compressors
 - Re-routing wet seal degassing emissions from centrifugal compressors
 - Replacing wet seals with dry seals in centrifugal compressors
- Directed Inspection and Maintenance (DI&M)



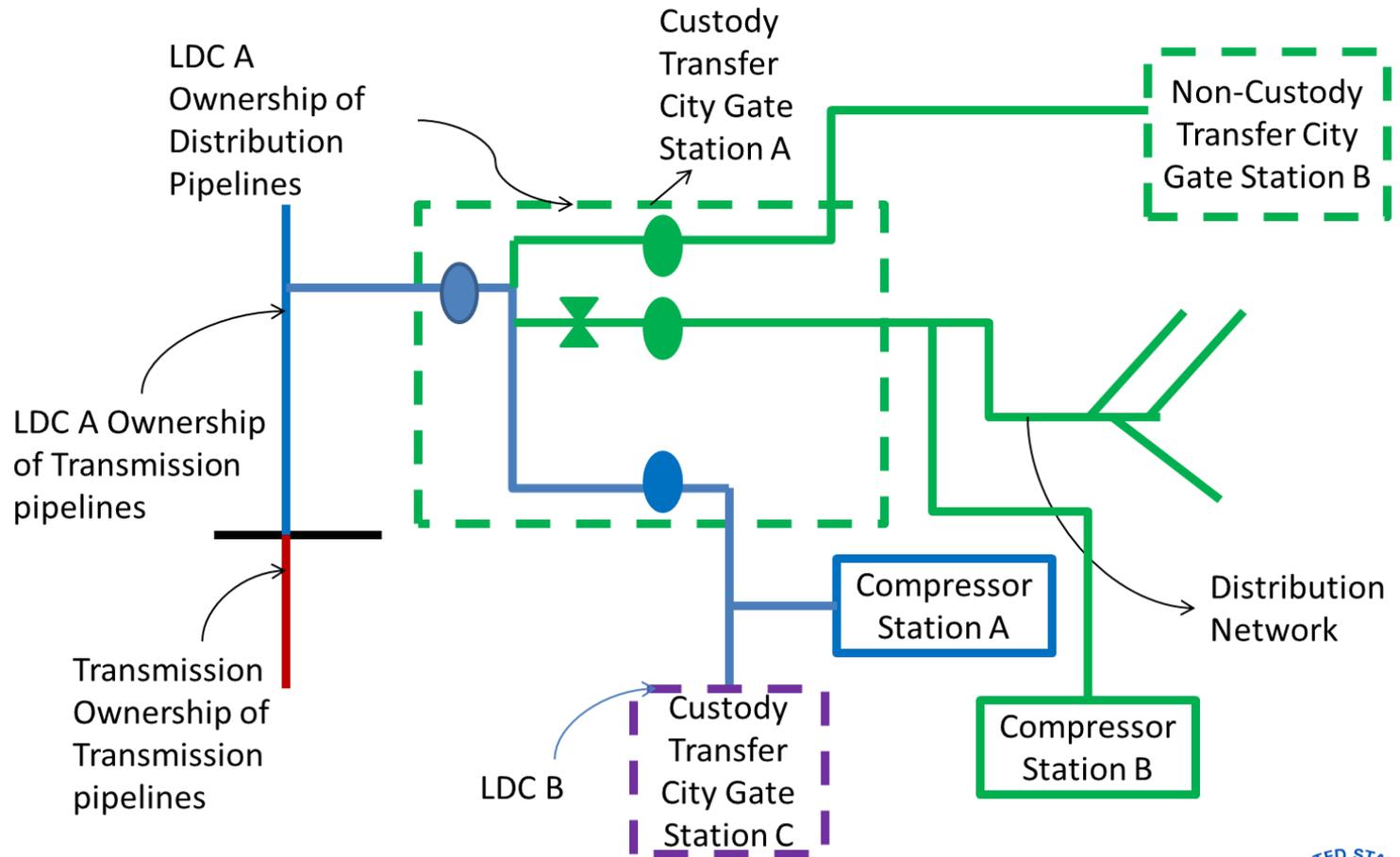
Sources of Methane Emissions from Oil and Gas Operations



Picture courtesy of American Gas Association
 Values Source: 2013 Inventory of U.S. Greenhouse
 Gas Emissions and Sinks: 1990-2011



LDC System Schematic



Compressor Reductions



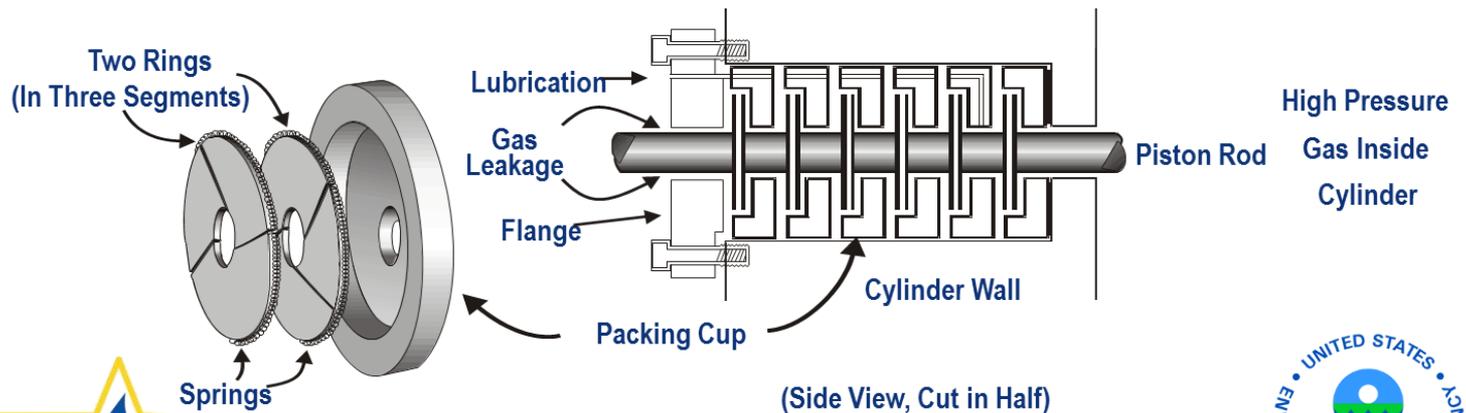
Methane Losses from Compressors in Distribution

- LDCs use compressors to move gas from custody transfer gates to other sections of distribution system
- Typically reciprocating compressors are in operation
 - Resulting in methane emissions from worn rod packing
- Centrifugal compressors can also be used
 - Resulting in wet seal degassing methane emissions



Methane Losses from Reciprocating Compressors

- Reciprocating compressor rod packing leaks some gas by design
 - Newly installed packing may leak 60 cubic feet per hour (cf/hour)
 - Worn packing has been reported to leak up to 900 cf/hour
- A series of flexible rings fit around the shaft to prevent leakage
- Leakage may still occur through nose gasket, between packing cups, around the rings, and between rings and shaft



Steps to Determine Economic Rod Packing Replacement

- Measure rod packing leakage
 - When new packing installed – after worn-in
 - Periodically afterwards
- Determine cost of packing replacement
- Calculate economic leak reduction
- Replace packing when leak reduction expected will pay back cost



Cost of Rod Packing Replacement

- Assess costs of replacements

- A set of rings: \$ 675 to \$ 1,100
(with cups and case) \$ 2,100 to \$ 3,400
- Rods: \$2,500 to \$ 13,500

Special coatings such as ceramic, tungsten carbide, or chromium can increase rod costs



Source: CECO

Calculate Economic Leak Reduction

- Determine economic replacement threshold
 - Partners can determine economic threshold for all replacements
 - This is a capital recovery economic calculation

$$\text{Economic Replacement Threshold (cf/hour)} = \frac{CR * DF * 1,000}{(H * GP)}$$

Where:

CR = Cost of replacement (\$)

DF = Discount factor at interest i =

$$DF = \frac{i(1+i)^n}{(1+i)^n - 1}$$

H = Hours of compressor operation per year

GP = Gas price (\$/thousand cubic feet)



Economic Replacement Threshold

- Example: Payback calculations for new rings and rod replacement

CR = \$1,620 for rings + \$9,450 for rod

CR = \$11,070

HR = 8,000 hours per year

GP = \$3/Mcf

DF @ $i = 10\%$ and $n = 1$ year

DF @ $i = 10\%$ and $n = 2$ years

One year payback

$$ER = \frac{\$11,070 \times 1.1 \times 1,000}{(8,000 \times \$3)}$$

$$= 508 \text{ scf per hour}$$

Rings Only:

Leak Reduction Expected (cf/hour)	Payback (months)
55	15
29	28
20	41
16	51

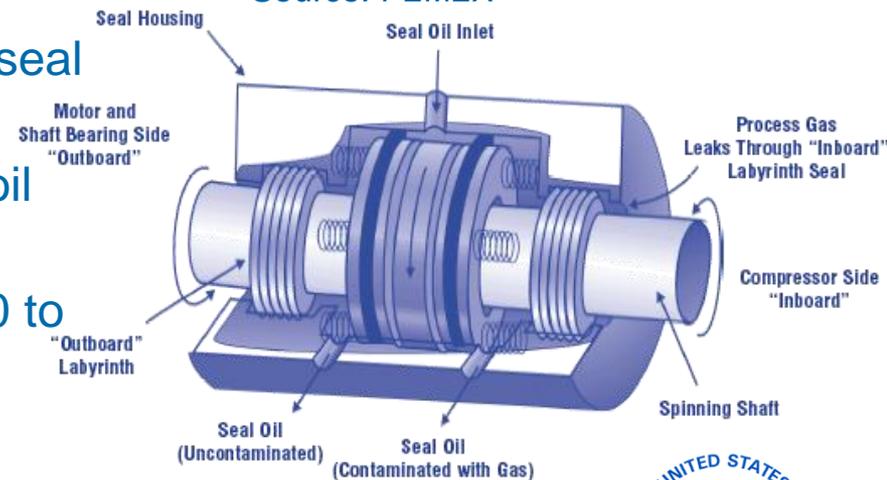


Methane Emissions from Centrifugal Compressors

- High pressure seal oil circulates between rings around the compressor shaft
- Oil absorbs the gas on the inboard side
 - Little gas leaks through the oil seal
 - Seal oil degassing vents methane to the atmosphere
- Wet seals leak little gas at the seal face
- Most emissions are from seal oil degassing
- Seal oil degassing may vent 40 to 200 cf/minute



Source: PEMEX

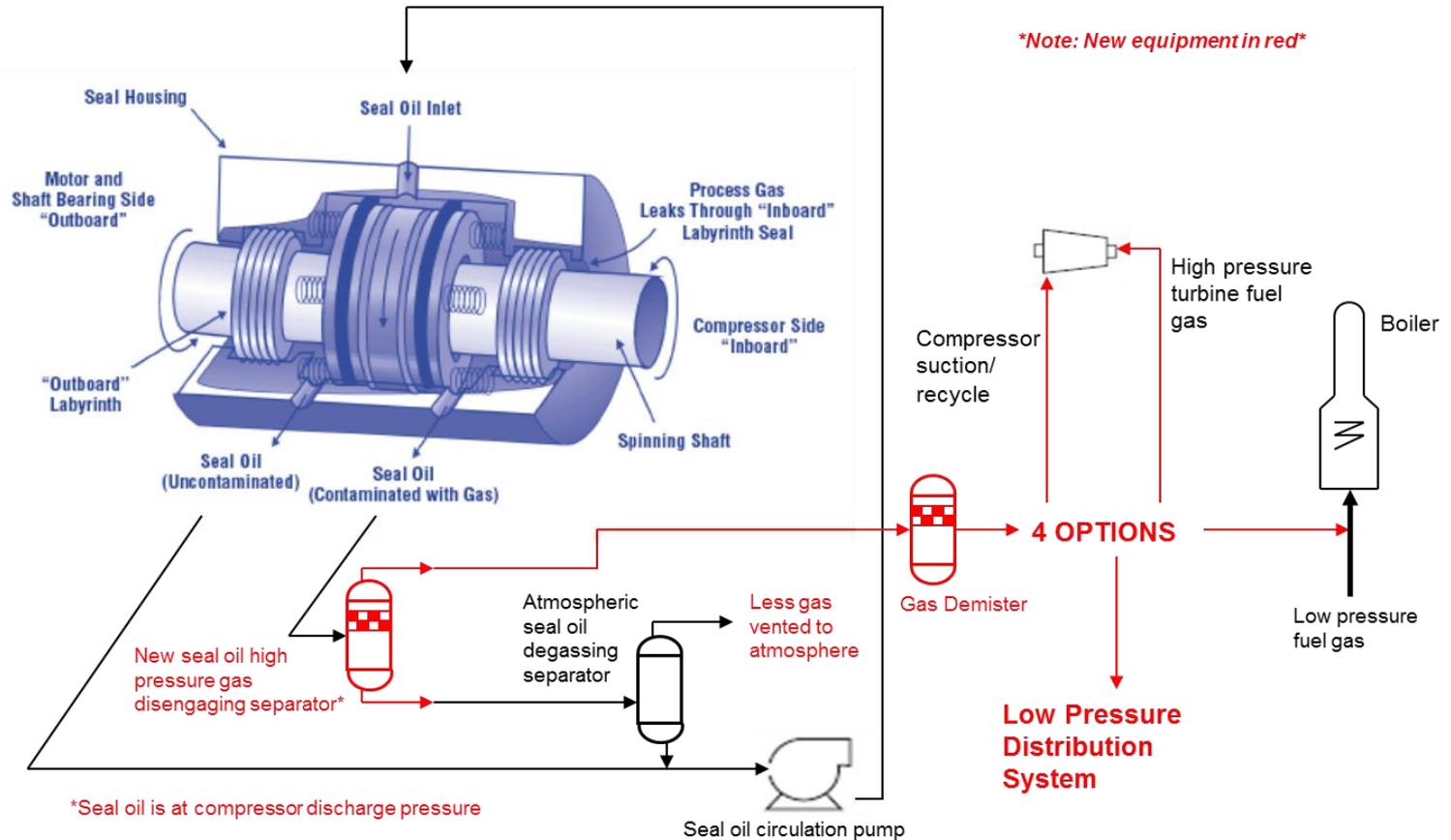


Gas Recovery from Centrifugal Compressors

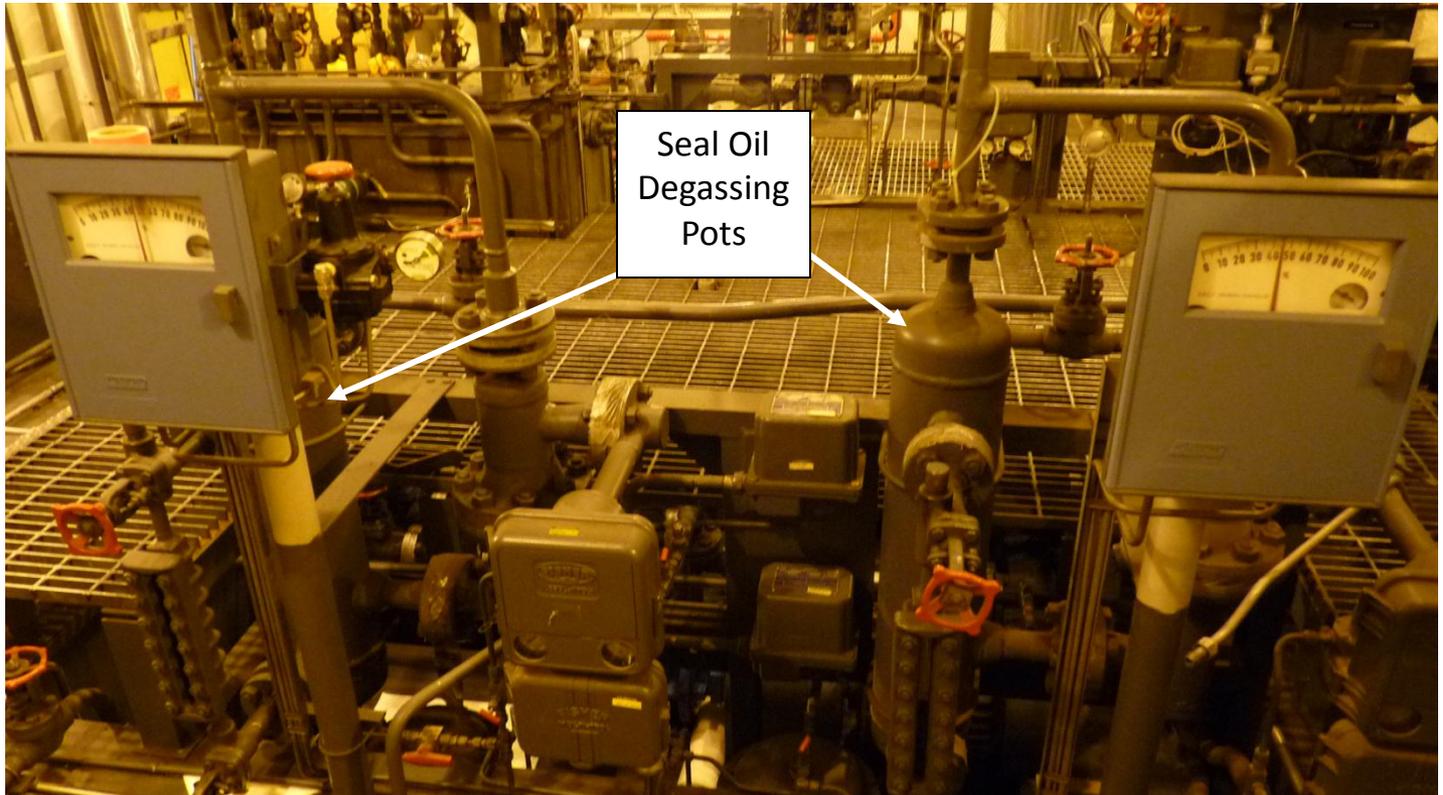
- Gas capture system currently used by BP on the North Slope of Alaska
 - Wet seal oil degassing emissions recovered with 4 possible destinations for gas
 - Flare
 - Low pressure suction side of compressor
 - Low pressure fuel gas for boiler
 - Compressor turbine fuel
- Recovering gas eliminates cost for conventional retrofit with dry seals
- In distribution, gas may be sent to low pressure section of distribution system



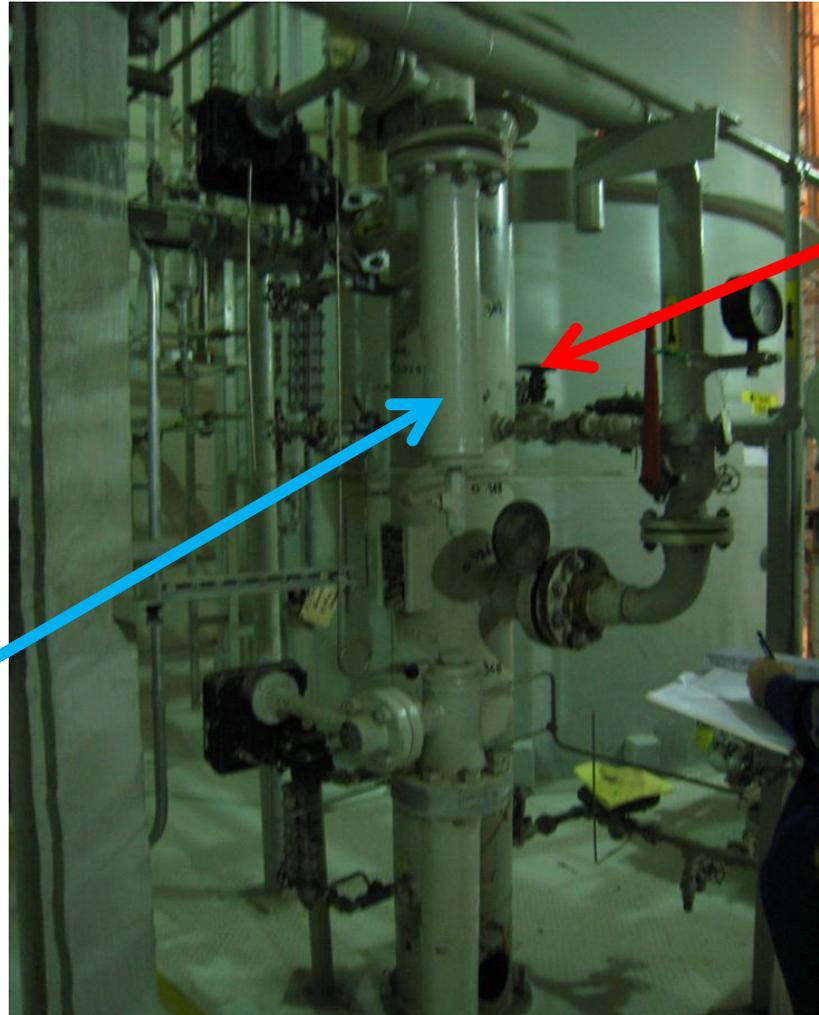
Gas Capture System in Distribution



Seal Oil Degassing Pots



First Stage Gas Filter Vessel



This is the first stage gas demister/filter vessel.

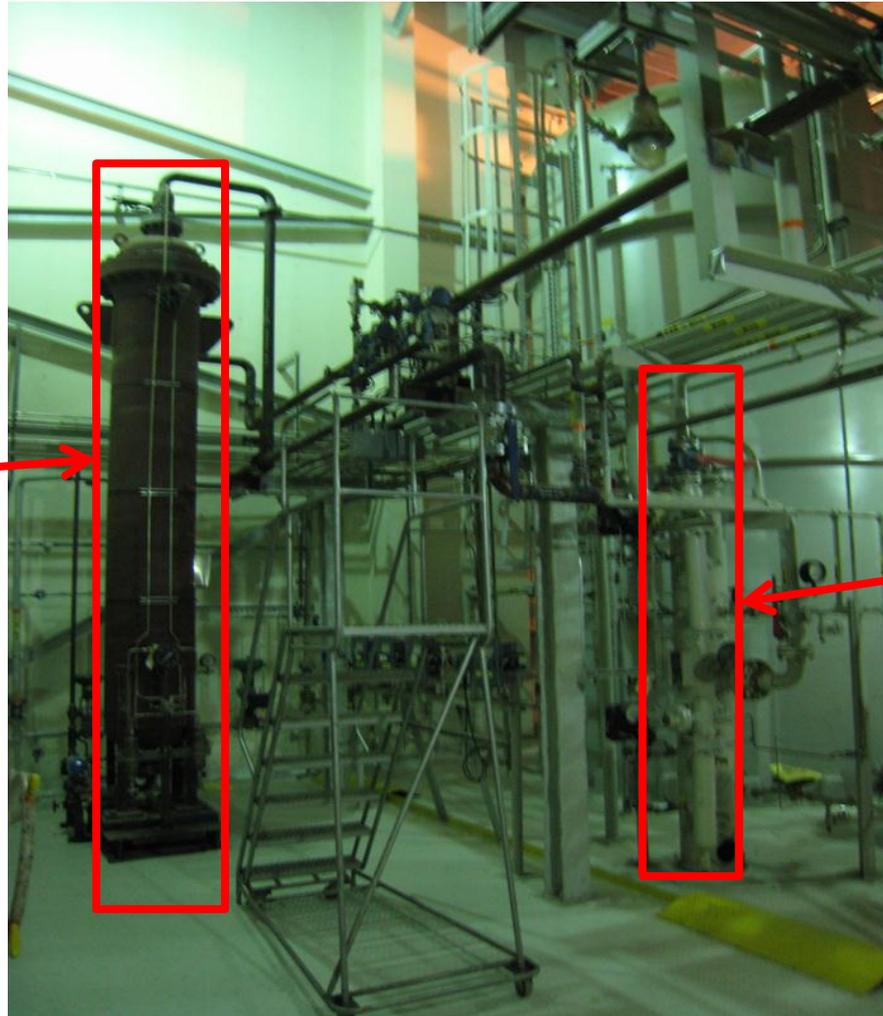
This pipe is NOT the demister/filter vessel.

Here is a person for size reference.



Second Stage Gas Filter Vessel

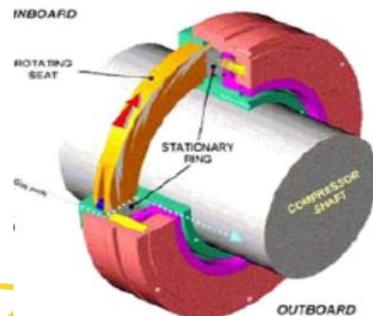
This is the second stage, high efficiency gas demister/filter vessel required for turbine fuel gas. It is newly installed and not yet painted.



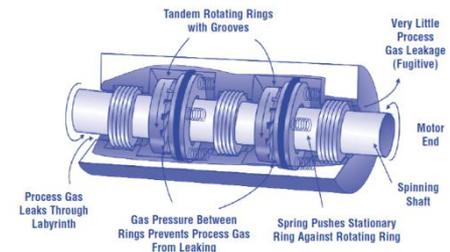
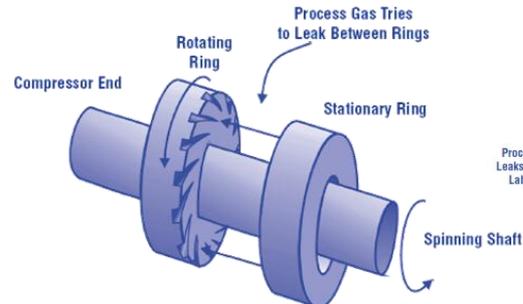
This is the first stage gas demister/filter vessel (behind a vertical pipe).

Traditional Solution: Retrofitting/Installing Dry Seals

- Dry seals:
 - 30 to 180 cf/hour (0.5 to 3 cf/minute) leak rate
 - Significantly less than the 40 to 200 cf/minute from wet seals
- Very cost-effective option for new compressors
- Significant capital costs and downtime for retrofitting compressors
 - See *Lessons Learned* for more info
- Alternative exists for more cost-effective seal oil degassing and vapor recovery retrofit with less downtime
- Dry seals keep gas from escaping while rotating with the shaft



Source: PEMEX



Directed Inspection and Maintenance



What is the Problem?

- Gas leaks are invisible, unregulated and go unnoticed
- Fugitives account for most distribution emissions¹
 - 18 Bcf of from metering and regulator stations in 2011
 - 11 Bcf from other regulator stations in 2011
 - 6 Bcf from customer meter leaks in 2011
- Distribution fugitive methane emissions depend on the technology in use, operating practices, equipment age and maintenance

1. Inventory of U.S. Greenhouse Gas Emissions and Sinks 1990 – 2011, USEPA, April, 2013

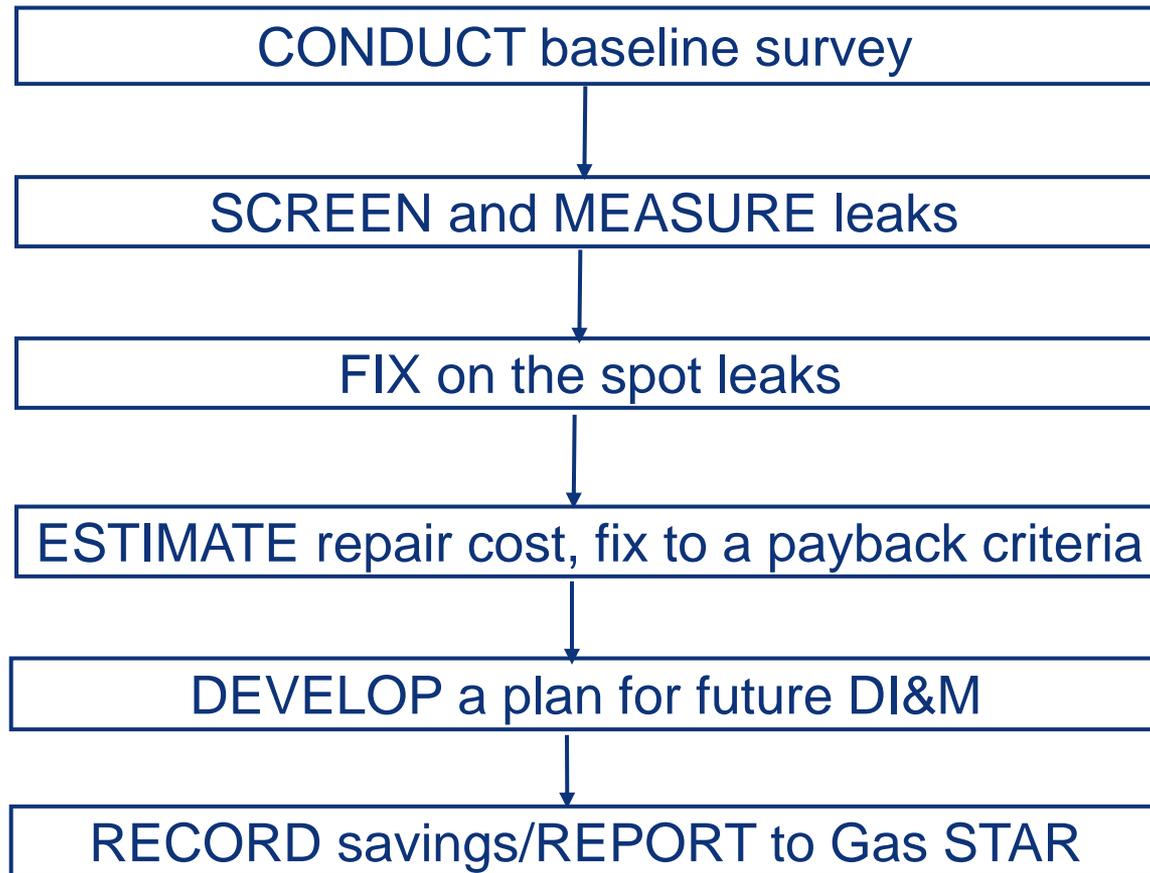


What is Directed Inspection & Maintenance?

- Directed Inspection and Maintenance (DI&M)
 - Cost-effective practice by definition
 - Find and fix significant leaks
 - Choice of leak detection technologies
 - Strictly tailored to company's needs
- DI&M is NOT the regulated volatile organic compound leak detection and repair (VOC LDAR) program



How Do You Implement DI&M?



How Do You Detect the Leaks?

- **Screening - find the leaks**
 - Soap bubble screening
 - Electronic screening (sniffer)
 - Toxic Vapor Analyzer (TVA)
 - Organic Vapor Analyzer (OVA)
 - Ultrasound Leak Detection
 - Acoustic Leak Detection
 - Optical Leak Imaging

Toxic Vapor Analyzer



Acoustic Leak Detection



Screening and Measurement Summary

Summary of Screening and Measurement Techniques		
Instrument/Technique	Effectiveness	Approximate
Soap Solution	★ ★	\$
Electronic Gas Detectors	★	\$\$
Acoustic Detection/ Ultrasound Detection	★ ★	\$\$\$
TVA (FID)	★	\$\$\$
Optical Leak Imaging	★ ★ ★	\$\$\$
Bagging	★	\$\$\$
High Volume Sampler	★ ★ ★	\$\$\$
Rotameter	★ ★	\$\$

Source: EPA's Lessons Learned Study

* - Least effective at screening/measurement

\$ - Smallest capital cost

*** - Most effective at screening/measurement

\$\$\$ - Largest capital cost



How Do You Measure the Leaks?

- **Evaluate the leaks detected - measure results**
 - High Volume Sampler
 - Toxic Vapor Analyzer (correlation factors)
 - Rotameters
 - Calibrated Bag
 - Engineering Method

Leak Measurement Using a High Volume Sampler



DI&M by Remote Leak Detection

- The trick has always been finding those few needles in the haystack of leaking components
 - Most large leaks (>3 scf/hr) clearly seen
- Real-time detection of gas leaks
 - Quicker identification & repair of leaks
 - Aerial surveillance applications
 - Screen hundreds of components an hour
 - Easily screen inaccessible areas



**Picarro Engineering
Survey Vehicle**



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Natural Gas STAR Program:

epa.gov/gasstar/index.html

Recommended Technologies:

epa.gov/gasstar/tools/recommended.html

