Storage Tanks

Emission units: Tanks Number of Tanks 4

Used (<u> </u>	<u>Tank</u>
--------	----------	-------------

Volume	63	bbl
Height (shell)	5	ft
Diameter	10	ft
Throughput	2	bbl/day

Uncontrolled Emissions

VOCs	VOCs	_	
	0.075	lb/hr	Tanks 4.09d
	0.33	ton/yr	
HAPs	HAPs	_	
	0.002327626	lb/hr	Tanks 4.09d
	0.010	ton/yr	

Ethylene Glycol Tank

Volume	137	bbl
Height (shell)	20	ft
Diameter	7	ft
Throughput	4	bbl/day

Uncontrolled Emissions

VOCs	VOCs		
	Negligible Negligible	lb/hr ton/yr	Tanks 4.09d
HAPs	HAPs		
	5.8219E-05	lb/hr	Tanks 4.09d
	2.55E-04	ton/vr	

Wastewater Tank

Not a source of air emissions.

Mercaptan Tank

Pressurized storage vessel. Not a source of air emissions.

Pipeline Liquids Tank

47	bbl
10	ft
6	ft
1	bbl/day
	10 6

Uncontrolled Emissions

Oncome once			
VOCs	VOCs	_	
	0.041	lb/hr	Tanks 4.09d
	0.179725	ton/yr	
HAPs	HAPs		
•	1.8185E-03	lb/hr	Tanks 4.09d
	0.01	ton/yr	

Emissions Summary

*HAPs (lb/hr)*4.2043E-03 *HAPs (tpy) VOC (lb/hr VOC (tpy)*0.02
0.12
0.51

New Mexico Gas Company -- Redonda Compressor Station

Unit 3 - Baldor/GM 2.0 Electric Generator

SSION CALCULATION FOR CO and NOx

Rate (lb/hr) = Multiply EF (g/kW-hr) by Rating (kW) and divide by 453.6 to convert g to lb

1 lb = 453.60 gm

Rating (kW)	Emission Factor	or (EF) Sea Level Emission Rate Emiss				Uncontro Emissions (ton/ye	500 hr
	NOX + THC (g/kw-hr)	CO (g/kW-hr)	NOx (lb/hr)		CO (lb/hr)	NOx (ton/yr C	O (ton/yr)
37.90	7.22	29.4	·7	0.60	2.46	0.15	0.62

The manufacturer specifies deration rate of 3% every 1000' over 4000 ft.

Altitude at Redonda is \sim 5370 ft and a deration of 4.1% is applied

	Derated Rating (kW)	Emission Factor	De	Derated Emission Rate (lb/hr)		Uncontroll Emissions 50 (ton/year	ed O0hr
		NOX + THC (g/kw-hr) CO (g/kW-h	nr) NO	Ox (lb/hr) (CO (lb/hr) l	NOx (ton/yr CO	(ton/yr)
_	36.35	7.22	29.47	0.58	2.36	0.14	0.59

Calculations Basis: Manufacturer's data used for CO and NOx emission factors (see page 13 of 27 in manufacturer's data) Note: SO₂, VOC and VOC rates from EPA AP42 - Table 3.2-3.

Uncontrolled Emission Factors for 4-Stroke Rich-Burn Engines

Pollutant	EF (lb/MMBTU)	Emission Rate (lb/hr)	Emission Rate 500h	r (tpy)
SO_2	0.000588	0.00026	0.00006	
SO ₂ VOC	0.0296	0.01298	0.00325	
PM	0.00991	0.00435	0.00109	

PM = TSP; for this facility and this unit, emissions of PM = PM10 = PM2.5

1 MMBtu = 1020.0 MMScf (per AP-42)

emission rate (lb/hr) = (EF lb/MMBtu * 1020 MMBtu/MMScf * 3.77 MMScf/ year) /8760 hr/year

Fuel consumption = 3.77 MMScf/yr $(430 \text{ cf/hr}*8760 \text{hr/yr})/10^6 = 3.77 \text{ MMcf/yr}$

Fuel Type Pipeline quality natural gas

Stack Velocity Calculation

Flow Rate 250 cf/m Flow Rate 4.17 cf/s diameter 0.21 ft Area 0.03 ft 2 Velocity 122.23 ft/s

Waukesha L7044 GSI

Emission Unit: 2

Source Description: Natural gas-fired reciprocating engine

Manufacturer: Waukesha Model: L7044 GSI

Type Naturally-aspirated, four-cycle, rich-burn engine with catalytic converter

 3-Year Average Operating Hours
 261
 2010, 2011, and 2012

 3-Year Average Number of Starts
 12
 2010, 2011, and 2013

Engine speed1200rpmSea level hp1680hpElevation5370msl

Derate 4.1% 3% per 1000 ft over 4000 ft

Site hp 1611 hp

Potential Emission Calculations

NOx	CO	VOC	SO_2	'PM2.5/P	M10	_
23	14	0.25			g/hp-hr	Mfg data 2001
81.7	49.7	0.9	0.2	0.4	lb/hr	Hourly emission rate
357.8	217.8	3.9	0.9	1.6	tpy	Annual emission rate (8760 hrs/yr)
1.1	0.6	0.0	0.0	0.0	tpy	SSM (assuming 52, 30 minute starts per year)

Allowable Emission Calculations

NOx	CO	VOC	SO_2	'PM2.5/I	PM10	
1.5	1.95	0.15			g/hp-hr	Catalyst controlled emissions (miratech specs)
2.0	3.0	0.5			g/hp-hr	Catalyst controlled with safety factor
7.1	10.7	1.8	0.2	0.4	lb/hr	$Hourly\ emission\ rate\ controlled\ w/safety\ factor$
31.0	47.0	7.7	0.9	1.6	tpy	Annual controlled emission rate (8760 hrs/yr)
32.1	47.7	7.7	0.9	1.6	tpy	Annual emission rate with SSM

Actual Emission Calculations

NOx	CO	VOC	SO ₂	'PM2.5/1	PM10	<u></u>
7.1	10.7	1.8	0.2	0.4	lb/hr	Hourly emission rate controlled w/safety factor
0.9	1.4	0.2	0.0	0.0	tpy	Annual emission rate (3-year average)
0.2	0.1	0.0	0.0	0.0	tpy	Annual emission rate of SSM (3-year ave)
1.2	1.5	0.2	0.0	0.0	tpy	Annual emission total with SSM (3-year ave)

Sample Calculations

NOx: Catalyst controlled emission factor manufaturer data =1.5 g/hp-hr

1.5 g/hp-hr * 1.33 = 2.0 g/hp-hr (safety factor) 2.0 g/hp-hr * 1611 hp / 453.6 g/lb = 7.1 lb/hr 7.1 lb/hr * 8760 hrs/yr / 2000 lb/ton = 31.0 tons/yr

CO: Catalyst controlled emission factor manufaturer data =1.95 g/hp-hr

1.95 g/hp-hr * 1.55 = 3.0 g/hp-hr (safety factor) 3.0 g/hp-hr * 1611 hp / 453.6 g/lb = 10.7 lb/hr 10.7 lb/hr * 8760 hrs/yr / 2000 lb/ton = 47.0 tons/yr

VOC: Catalyst controlled emission factor manufaturer data =0.25 g/hp-hr

0.25 g/hp-hr * 2.3 = 0.5 g/hp-hr (safety factor) 0.5 g/hp-hr * 1611 hp / 453.6 g/lb = 1.8 lb/hr 1.8 lb/hr * 8760 hrs/yr / 2000 lb/ton = 7.7 tons/yr

SO₂: Fuel sulfur content: 5 gr S/100 scf, or 0.00714 lb S/Mscf

0.00714 lb S/Mscf * fuel consumption (Mscf/hr) * 64 lb SO $_2/32$ lb S = lb/hr SO $_2$ 0.00714 lb S/Mscf * 13.9 (Mscf/hr) * 64 lb SO $_2/32$ lb S = 0.19 lb/hr SO $_2$

0.19 lb/hr * 8760 hrs/yr / 2000 lb/ton = 0.87 tons/yr

PM 2.5/PM10: AP-42 EF = 0.029 lb/MMBtu (EF is the sum of PM2.5, PM10 and PM condensable)

AP-42 EF * Heat input = PM lb/hr

0.029 lb/MMBtu * 12.5 MMBtu/hr = 0.36 lb/hr

New Mexico Gas Company -- Redonda Compressor Station

Waukesha L7044 GSI

Emission Unit: 2

Source Description: Natural gas-fired reciprocating engine

Manufacturer: Waukesha Model: L7044 GSI

Type Naturally-aspirated, four-cycle, rich-burn engine with catalytic converter

Fuel Consumption

Heat Rate 7780 Btu/hp-hr Mfg data

Fuel heat value 900 Btu/scf Nominal; natural gas Heat Input 12.5 MMBtu/hr Heat Rate * hp

Fuel consumption 13.9 Mscf/hr Heat input / fuel heat value Annual fuel usage 122.0 MMcf/yr 8760 hrs/yr operation

Exhaust Parameters

Stack flow 7981 acfm Mfg. Data Flow(lb/hr)*Exhaust Temp(°R)/2250

Stack velocity 124.5 ft/s Mfg. Data

New Mexico Gas Company -Redonda Compressor Station

Waukesha 7042 GL

Emission	Unit:	1
LIIII331011	OIIIC.	_

Source Description: Natural gas-fired reciprocating engine

Manufacturer: Waukesha Model: 7042 GL

Type Turbocharged, four-cycle, lean burn engine

3-Year Average Operating Hours 2458 hrs years 2010,2011,2012

 $\begin{array}{ccc} \text{Engine speed} & 1200 & \text{rpm} \\ \text{Sea level hp} & 1478 & \text{hp} \\ \text{Elevation} & 5370 & \text{msl} \end{array}$

Derate 4.1% 3% per 1000 ft over 4000 ft

Site hp 1417 hp

Potential Emission Calculations

					PM2.5/		
	NOx	CO	VOC	SO_2^*	PM10**		_
-	1.5	2.65	1			g/hp-hr	Mfg. data
	4.7	8.3	3.1	0.2	0.1	lb/hr	Hourly emission rate
	6.2	9.1	3.1	0.2	0.1	Hourly E	mission rate with safety factor
	27.3	39.9	13.7	0.7	0.5	tpy	

^{*} SO₂ emissions based on fuel sulfur content of 5 gr S/100 scf, or 0.00714 lb S/Mscf. 0.00714 lb S/Mscf * fuel consumption (Mscf/hr) * 64 lb SO₂/32 lb S = lb/hr SO₂

(EF is the sum of PM2.5, PM10 and PM condensable)

0.01 lb/MMBtu * 10.3 MMBtu/hr = 0.1 lb/hr

Allowable Emission Calculations equal PTE (no controls)

Actual Emission Calculations (three year average: 2010-2012)

NOx	CO	VOC	SO_2	'PM2.5/I	PM10	
6.2	9.1	3.1	0.2	0.1	lb/hr	
7.7	11.2	3.8	0.2	0.1	tpy	

Sample Calculations

NOx: Emission factor manufaturer data = 1.5 g/hp-hr 1.5 g/hp-hr * 1.33 = 2.0 g/hp-hr (safety factor) 2.0 g/hp-hr * 1417 hp / 453.6 g/lb = 6.2 lb/hr 6.2 lb/hr * 8760 hrs/yr / 2000 lb/ton = 27.3 tons/yr

CO: Emission factor manufaturer data = 2.65 g/hp-hr 2.65 g/hp-hr * 1.1 = 8.3 g/hp-hr (safety factor) 8.3 g/hp-hr * 1417 hp / 453.6 g/lb = 9.1 lb/hr 9.1 lb/hr * 8760 hrs/yr / 2000 lb/ton = 39.9 tons/yr

VOC: Emission factor manufaturer data = 1.0 g/hp-hr 1.0 g/hp-hr * 1417 hp / 453.6 g/lb = 3.1 lb/hr 3.1 lb/hr * 8760 hrs/yr / 2000 lb/ton = 13.7 tons/yr

Engine BMEP

Displacement	7040	cubic in.	Mfg data
Engine BMEP	133	psia	(hp * 792,000) / (rpm * displacement)

Fuel Consumption

Heat Rate	/292	Btu/np-nr	Mig data	

Fuel heat value 900 Btu/scf Nominal; natural gas

^{**} PM based on AP-42 EF * Heat input = PM lb/hr

Heat Input	10.3	MMBtu/hr	Heat Rate * hp

Fuel consumption 11.5 Mscf/hr Heat input / fuel heat value Annual fuel usage 100.6 MMcf/yr 8760 hrs/yr operation

Exhaust Parameters

Exhaust temp	725.0 deg F	Mfg Data
	14760.0 lb/hr	Mfg Data

Exhaust flow 7688.2 acfm Flow(lb/hr)*Exhaust Temp(°R)/2275

Stack diameter 1.17 ft Design

Exhaust velocity 119.2 ft/sec Exhaust flow / stack area

Stack height 45 ft Design

PTE Total - Emission Summary

Potential Emission Calculations (uncontrolled, 8760 operating hours)

	NO _x (lb/hr)	NO _x (tpy)	CO (lb/hr)	CO (tpy)	VOC (lb/hr)	VOC (tpy)	SO ₂ (lb/hr)	SO ₂ (tpy)	CH ₂ O (lb/hr)	CH ₂ O (tpy)*	HAPs (tpy)*	PM2.5/ PM10 (lb/hr)	PM10	CO ₂ e (facility wide, tpy)
1 7042 GL	6.23	27.30	9.11	39.89	3.12	13.69	0.16	0.72	1.05	4.61	5.47	0.10	0.45	
2 7044 GSI	81.68	357.78	49.72	217.78	0.89	3.89	0.20	0.87	0.18	0.77	1.52	0.36	1.59	
Baldor														
3 Emergency														
Gen**	0.58	0.14	2.36	0.59	0.01	0.00	0.00	0.00	0.01	0.05	0.07	0.00	0.00	
Tanks	-	-	-	-	0.12	0.51	-	-	-	-	0.02	-	-	
SSM (Unit 2)	-	1.06	-	0.65	-	-	-	-	-	-	-	-	-	
Total	88.50	386.28	61.19	258.91	4.14	18.08	0.36	1.59	1.24	5.43	7.08	0.47	2.05	13,623.3

^{*}Formaldehdye (tpy) and total HAPs come from GRI-HAPCalc 3.01 Report. Tpy is converted to lb/hr

Allowables Total - Emission Summary

Allowables Emission Calculations (controlled emissions, 8760 operating hours)

	NO _x (lb/hr)	NO _x (tpy)	CO (lb/hr)	CO (tpy)	VOC (lb/hr)	VOC (tpy)	SO ₂ (lb/hr)	SO ₂ (tpy)	CH ₂ O (lb/hr)	CH ₂ O (tpy)*	HAPs (tpy)*	PM2.5/ PM10 (lb/hr)	PM2.5/ PM10 (tpy)	CO ₂ e (facility wide, tpy)
1 7042 GL	6.23	27.30	9.11	39.89	3.12	13.69	0.16	0.72	1.05	4.61	5.47	0.10	0.45	
2 7044 GSI	7.09	31.03	10.73	47.02	1.76	7.70	0.20	0.87	0.18	0.77	1.52	0.36	1.59	
Baldor														
3 Emergency														
Gen*	0.58	0.14	2.36	0.59	0.01	0.00	0.00	0.00	0.01	0.05	0.07	0.00	0.00	
Tanks	-	-	-	-	0.12	0.51	-	-	-	-	0.02	-	-	
SSM (Unit 2	-	1.06	-	0.65	-	-	-	-	-	-	-	-	-	
Total	13.90	59.54	22.20	88.15	5.01	21.90	0.36	1.59	1.24	5.43	7.08	0.47	2.05	13,623.3

^{*}Formaldehdye (tpy) and total HAPs come from GRI-HAPCalc 3.01 Report. Tpy is converted to lb/hr

Actual Total - Emission Summary

$\label{lem:condition} \textbf{Actual Emission Calculations (based on 3-year average operating hours)}$

	NO _x (lb/hr)	NO _x (tpy)	CO (lb/hr)	CO (tpy)	VOC (lb/hr)	VOC (tpy)	SO ₂ (lb/hr)	SO ₂ (tpy)	CH ₂ O (lb/hr)	CH ₂ O (tpy)	HAPs (tpy)	PM2.5/ PM10 (lb/hr)	PM2.5/ PM10 (tpy)	CO ₂ e (facility wide, tpy)
1 7042 GL	6.23	7.66	9.11	11.19	3.12	3.84	0.16	0.20	1.05	1.29	1.54	0.10	0.45	2459 hours
2 7044 GSI Baldor	7.09	0.92	10.73	1.40	1.76	0.23	0.20	0.03	0.18	0.02	0.05	0.36	1.59	261 hours
3 Emergency														
Gen	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0.00	0 hrs
Tanks	-	-	-	-	0.12	0.51	-	-	-	-	0.02	-	-	
Total	13.32	8.59	19.84	12.60	5.00	4.58	0.36	0.23	1.23	1.32	1.60			4,230.1

 $\underline{\textbf{Emissions are provided for informational purposes only and are not intended to be an enforceable limit.}$

^{**}Assumes 500 hours of operation per year except for CH20 and HAP which assumes 8760 hours

^{**}Assumes 500 hours of operation per year except for CH20 and HAP which assumes 8760 hours

NMGC--Redonda Compressor Station

CAT G3516

Emission Unit: NA- previous unit

Source Description: Natural gas-fired reciprocating engine

Manufacturer: Caterpillar Model: 3516

Type Turbocharged, four-cycle, lean burn engine

 $\begin{array}{ccc} \text{Engine speed} & 1200 & \text{rpm} \\ \text{Sea level hp} & 1151 & \text{hp} \\ \text{Elevation} & 5000 & \text{msl} \end{array}$

Derate 0.0% 3% per 1000 ft over 4000 ft

 $\begin{array}{ccc} \text{Site hp} & & 1151 & \text{hp} \\ \text{Hours of Operation} & & 8760 & \text{hr/yr} \end{array}$

Emission Calculations

Uncontrolled Emissions

	NOx	CO	NMHC	SO_2^{1}	НСНО		<u></u>
	1.5	1.8	0.5		0.34	g/hp-hr	Mfg. data,
Hourly Emissions	3.8	4.6	1.2	0.021	0.9	lb/hr	hp*g/hp-hr/453.6 g/lb
Annual Emissions	16.7	20.0	5.4	0.09	3.8	tons/yr	

 $^{^1}$ SO₂ emissions based on fuel sulfur content of 5 gr S/100 scf, or 0.00714 lb S/Mscf. 0.00714 lb S/Mscf * fuel consumption (Mscf/hr) * 64 lb SO₂/32 lb S = lb/hr SO₂

Engine BMEP

Displacement	7040	cubic in.	Mfg data
Engine BMEP	108	psia	(hp * 792,000) / (rpm * displacement)

Fuel Consumption

r acr consumption			
Heat Rate	2370	Btu/hp-hr	Mfg data
Fuel heat value	920	Btu/scf	Nominal; natural gas
Heat Input	2.7	MMBtu/hr	Heat Rate * hp
Fuel consumption	3.0	Mscf/hr	Heat input / fuel heat value
Annual fuel usage	26.0	MMcf/yr	8760 hrs/yr operation

	Pre-Control	Post-Control
Nox	Major	Minor
CO	Major	Minor
VOC	Minor	Minor
Formaldehyde	Minor	Minor
Total HAPs	Minor	Minor
Greenhouse Gas	Minor	Minor

Subpart C - General Stationary Fuel Combustion - Tier 1 Calculation Methodology Using Equations C-1 and C-8

OPTIONAL SPREADSHEET FOR FACILITY RECORDKEEPING PURPOSES

Version e-GGRT RY2011.R.01

Today's date 9/28/2016

Use one spreadsheet for each fuel. Make additional copies as needed.

This spreadsheet is protected and contains locked cells to ensure that you do not inadvertently alter any of the included formulas and/or calculations. To remove this protection and alter this spreadsheet, right-click the "worksheet" tab near the bottom of the screen and select "Unprotect Sheet." When prompted for the password, type "GHG" and click "OK." Please note that making changes to an unprotected sheet could result in incorrect calculations and that you are responsible for the accuracy of the data you report to EPA. For additional help, visit the Microsoft Excel Support website (http://office.microsoft.com/en-us/excel-help).

Equation C-1:

$$CO_2 = 1 \times 10^{-3} * Fuel * HHV * EF$$

Equation C-8:

$$CH_4 \text{ or } N_2O = 1 \times 10^{-3} * Fuel * HHV * EF$$

Facility Name:	Redonda Compressor Station
Reporter Name:	New Mexico Gas Company
Unit or Group Name/ ID:	
Configuration Type:	
Fuel/ Fuel Type:	Natural Gas
Reporting Period:	
Comments:	
Unit Type:	General Stationary Fuel Combustion

Fuel Input Data

[Fuel] = Mass or volume of fuel combusted per year, from company records as defined in §98.6 (express mass in short tons for solid fuel, volume in standard cubic feet for gaseous fuel, and volume in gallons for liquid fuel)	226,346,955.41429
[HHV] = Default High heat value of the fuel, from Table C-1 (mmBtu/mass or mmBtu/volume)	0.00103

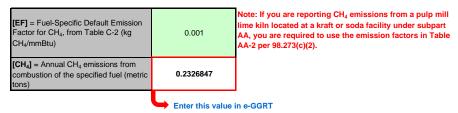
Constants

[1 x 10 ⁻³] = Conversion Factor from kg	0.001
to metric tons (constant)	0.001

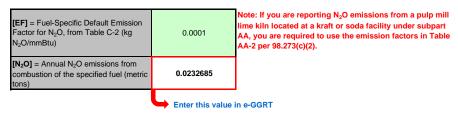
Annual CO₂ Mass Emissions For the Specific Fuel Type (metric tons) from Equation C-1

[EF] = Fuel-Specific Default CO ₂ Emission Factor, from Table C-1 (kg CO ₂ /mmBtu)	53.06	
[CO ₂] = Annual CO ₂ emissions from combustion of the specified fuel (metric tons)	12346.2485990	
	Enter this value i	n e-GG

Annual CH₄ Mass Emissions For the Specific Fuel Type (metric tons) from Equation C-8



Annual N₂O Mass Emissions For the Specific Fuel Type (metric tons) from Equation C-8



Subpart C - General Stationary Fuel Combustion - Tier 1 Calculation Methodology Using Equations C-1 and C-8

OPTIONAL SPREADSHEET FOR FACILITY RECORDKEEPING PURPOSES

Version e-GGRT RY2011.R.01

Today's date 9/28/2016

INFORMATION ONLY: Annual CH₄ Mass Emissions For the Specific Fuel Type Converted to Carbon Dioxide Equivalent (metric tons CO₂e)

[GWP _{CH4}] = Global Warming Potential for CH ₄	21
[CH ₄] = Annual CH ₄ emissions from combustion of the specified fuel (metric tons CO ₂ e)	4.886378073

INFORMATION ONLY: Annual N2O Mass Emissions For the Specific Fuel Type Converted to Carbon Dioxide Equivalent (metric tons CO2e)

[GWP _{N2O}] = Global Warming Potential for N ₂ O	310	
$[N_2O]$ = Annual N_2O emissions from combustion of the specified fuel (metric tons CO_2e)	7.213224775	

Table C-1 to Subpart C - Default ${\rm CO_2}$ Emission Factors and High Heat Values for Various Types of Fuel

Fuel Type	Default High	Default CO ₂ Emission
1001 1770	Heat Value	Factor
Coal and Coke	mmBtu/short ton	kg CO ₂ /mmBtu
Anthracite	25.09	103.54
Bituminous	24.93	93.40
Subbituminous	17.25	97.02
Lignite	14.21	96.36
Coke	24.80	102.04
Mixed (Commercial sector)	21.39	95.26
Mixed (Industrial coking)	26.28	93.65
Mixed (Industrial sector)	22.35	93.91
Mixed (Electric Power sector)	19.73	94.38
Natural Gas	mmBtu/scf	kg CO ₂ /mmBtu
(Weighted U.S. Average)	1.028E-03	53.02
Petroleum Products	mmBtu/gallon	kg CO ₂ /mmBtu
Distillate Fuel Oil No. 1	0.139	73.25
Distillate Fuel Oil No. 2	0.138	73.96
Distillate Fuel Oil No. 4	0.146	75.04
Residual Fuel Oil No. 5	0.140	72.93
Residual Fuel Oil No. 6	0.150	75.10
Used Oil	0.135	74.00
Kerosene	0.135	75.20
Liquefied petroleum gases (LPG)	0.092	62.98
Propane	0.091	61.46
Propylene	0.091	65.95
Ethane	0.069	62.64
Ethanol	0.084	68.44
Ethylene	0.100	67.43
Isobutane	0.097	64.91
Isobutylene	0.103	67.74
Butane	0.101	65.15
Butylene	0.103	67.73
Naphtha (<401 deg F)	0.125	68.02
Natural Gasoline	0.110	66.83
Other Oil (>401 deg F)	0.139	76.22
Pentanes Plus	0.110	70.02
Petrochemical Feedstocks	0.129	70.97
Petroleum Coke	0.143	102.41
Special Naphtha	0.125	72.34
Unfinished Oils	0.139	74.49
Heavy Gas Oils	0.148	74.92
Lubricants	0.144	74.27
Motor Gasoline	0.125	70.22
Aviation Gasoline	0.120	69.25
Kerosene-Type Jet Fuel	0.135	72.22
		l .

Table C-1 to Subpart C - Default CO₂ Emission Factors and High Heat Values for Various Types of Fuel

Fuel Type	Default High	Default CO ₂ Emission
	Heat Value	Factor
Asphalt and Road Oil	0.158	75.36
Crude Oil	0.138	74.49
Other Fuels (Solid)	mmBtu/short ton	kg CO ₂ /mmBtu
Municipal Solid Waste ¹	9.95	90.70
Tires	26.87	85.97
Plastics	38.00	75.00
Petroleum Coke	30.00	102.41
Other Fuels (Gaseous)	mmBtu/scf	kg CO ₂ /mmBtu
Blast Furnace Gas	9.20E-05	274.32
Coke Oven Gas	5.99E-04	46.85
Propane Gas	2.52E-03	61.46
Fuel Gas ²	1.39E-03	59.00
Biomass Fuels - Solid	mmBtu/short ton	kg CO ₂ /mmBtu
Wood and Wood Residuals	15.38	93.80
Agricultural Byproducts	8.25	118.17
Peat	8.00	111.84
Solid Byproducts	25.83	105.51
Biomass Fuels - Gaseous	mmBtu/scf	kg CO ₂ /mmBtu
Biogas (Captured methane)	8.41E-04	52.07
Biomass Fuels - Liquid	mmBtu/gallon	kg CO ₂ /mmBtu
Ethanol	0.084	68.44
Biodiesel	0.128	73.84
Rendered Animal Fat	0.125	71.06
Vegetable Oil	0.120	81.55

¹ Use of this default HHV is allowed only for: (a) units that combust MSW, do not generate steam, and are allowed to use Tier 1; (b) units that derive no more than 10 percent of their annual heat input from MSW and/or tires; and (c) small batch incinerators that combust no more than 1,000 tons of MSW per year.

Reporters subject to subpart X of this part that are complying with $\S98.243$ (d) or subpart Y of this part may only use the default HHV and the default CO_2 emission factor for fuel gas combustion under the conditions prescribed in $\S98.243$ (d) (2) (i) and (d) (2) (ii) and $\S98.252$ (a) (1) and (a) (2), respectively. Otherwise, reporters subject to subpart X or subpart Y shall use either Tier 3 (Equation C-5) or Tier 4.

Table C-2 to Subpart C - Default CH₄ and N₂O Emission Factors for Various Types of Fuel

Fuel Type	Default CH ₄ Emission Factor (kg CH ₄ /mmBtu)	Default N ₂ O Emission Factor (kg N ₂ O/mmBtu)
Coal and Coke (All fuel types in Table C-1)	1.1E-02	1.6E-03
Natural Gas	1.0E-03	1.0E-04
Petroleum (All fuel types in Table C-1)	3.0E-03	6.0E-04
Municipal Solid Waste	3.2E-02	4.2E-03
Tires	3.2E-02	4.2E-03
Blast Furnace Gas	2.2E-05	1.0E-04
Coke Oven Gas	4.8E-04	1.0E-04
Biomass Fuels - Solid (All fuel types in Table C-1)	3.2E-02	4.2E-03
Biogas	3.2E-03	6.3E-04
Biomass Fuels - Liquid (All fuel types in Table C-1)	1.1E-03	1.1E-04

Note: Those employing this table are assumed to fall under the IPCC definitions of the "Energy Industry" or "Manufacturing Industries and Construction". In all fuels except for coal the values for these two categories are identical. For coal combustion, those who fall within the IPCC "Energy Industry" category may employ a value of 1 g of CH4/mmBtu.

The emission factors in the table below should only be used for calculating CH₄ and N₂O emissions from located at a kraft or soda facilities under subpart AA per 98.273(c)(2).

Table AA-2 to Subpart AA of Part 98— Kraft Lime Kiln and Calciner Emissions Factors for Fossil Fuel-Based

	Fossil f	fuel-based emissic	ons factors (kg/mml
Fuel	Kraft lime kilns		Kraft ca
	CH ₄	N ₂ O	CH ₄
Residual Oil			
Distillate Oil	7		0.0027
Natural Gas	0.0027	0	0.0027
Biogas			
Petroleum coke	7		NA

^a Emission factors for kraft calciners are not available.

pulp mill lime kilns

CH₄ and N₂O

Btu HHV)	
alciners	
N ₂ O	
	0.0003
	0.0004
	0.0001
	0.0001
	^a NA

Redonda		Mcf fuel used		
Total	2010 2011 2012	36,482 19,423 1,472 57,377		
Fuel Usage CO2 Emissions		32,833.80 1,742,161.43	kg/yr	
CH4 Emissions N2O Emissions			ton/yr ton/yr ton/yr	
Fuel Usage		2,011 19.4 17,480.70	MMcf/yr	
CO2 Emissions		927,525.94 1,020.28	kg/yr	
CH4 Emissions N2O Emissions		0.02 0.00	ton/yr	
Fuel Usage		2012 1.5	MMcf/yr	
CO2 Emissions		1,324.80 70,293.89	kg/yr	
CH4 Emissions N2O Emissions		77.32 0.00 0.00	ton/yr	

total GHG

3,017.09