



Reducing Methane Emissions from Transmission Pipelines

Turkmenistan Symposium on Gas Systems Management: Methane Mitigation

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ICF International

Reducing Methane Emissions from Transmission Pipelines: Agenda

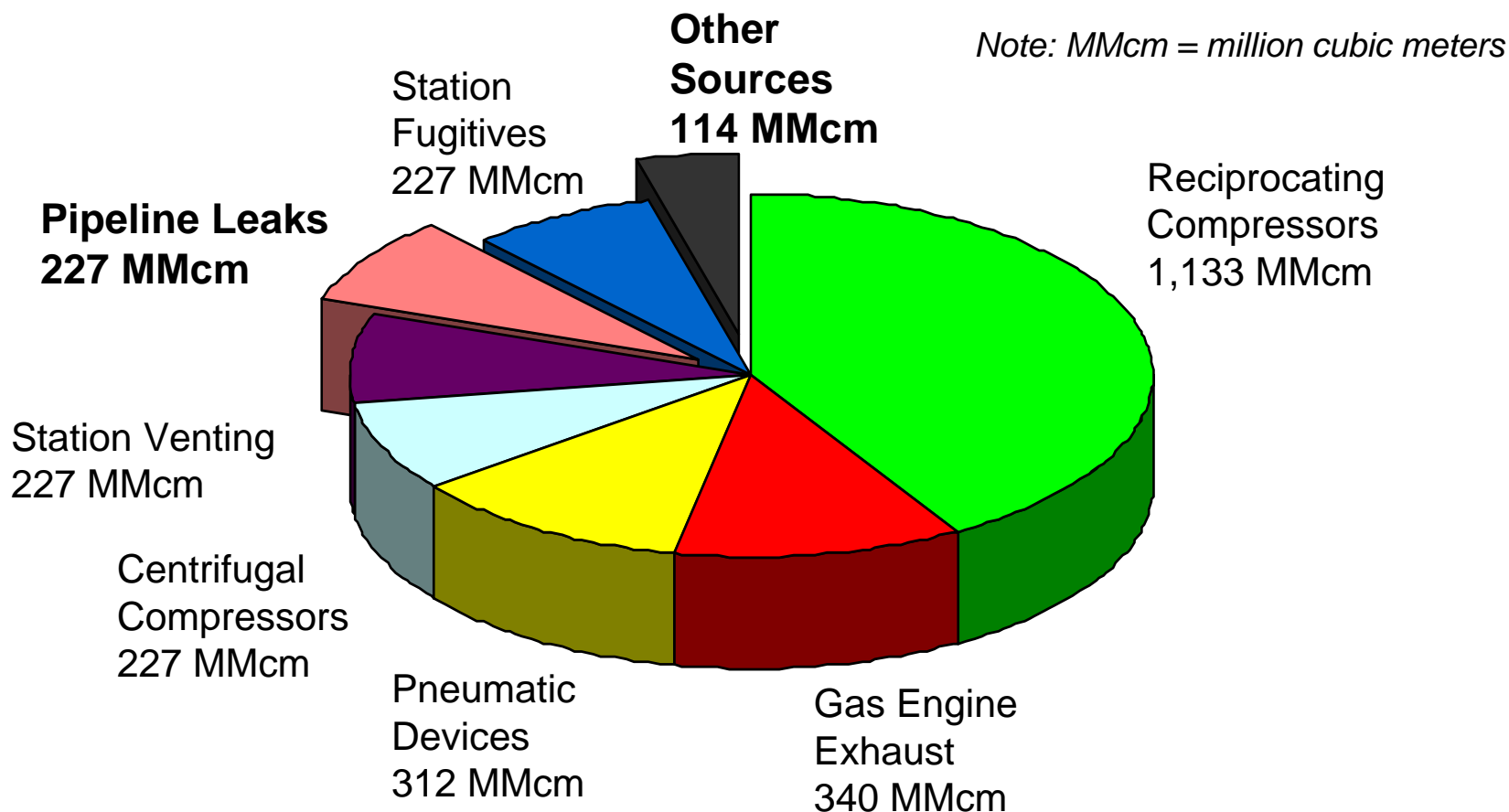
- Methane emissions from transmission pipelines
- Opportunities for methane recovery:
 - Pipeline pump-downs
 - Hot taps
 - Composite wrap
- Contact and further information



Source: TransCanada

U.S. Methane Emissions from Transmission Pipelines

- Emissions from transmission pipelines accounts for a significant portion of transmission sector emissions



Reducing Methane Emissions from Transmission Pipelines: Agenda

- Methane emissions from transmission pipelines
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 - **Pipeline pump-downs**
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Source: TransCanada

Pipeline Pump-down: Overview

- Most applicable to large pipelines operating at high pressures
- Use in-line compressors to “pull down” the pressure to minimum suction pressure
- Use portable compressor to “pull down” pressure even further
- Cost is justified by immediate payback in gas savings
- About 90% of gas usually vented is recoverable

Pipeline Pump-down: Process

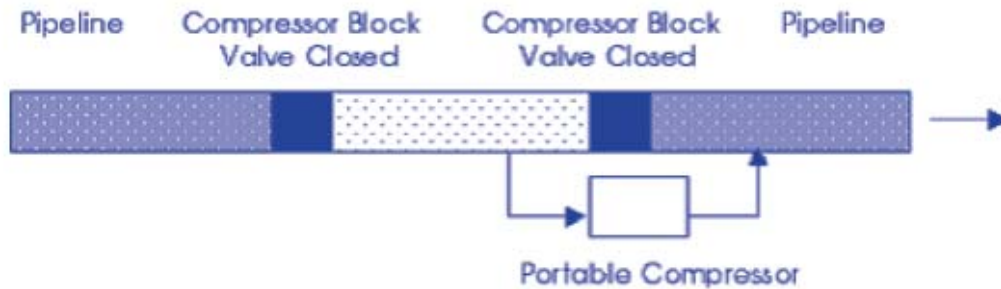
1. Identify Pipeline Segment Needing Repair



2. Depressurize Segment by 50% Using In-line Pipeline Compressor



3. Depressurize Segment Further by 90% Using Portable Compressor In Sequence With an In-line Compressor



-  Normal pipeline pressure
-  Pipeline with pressure reduced by 50%
-  Pipeline with pressure reduced by 90%

Pipeline Pump-down: Economics

- Quantity of gas saved by pump-down:

- Total gas in pipeline segment:

$$M = L * (1,000 \text{ m/km}) * (\pi/4 * D^2) * (P/101.3 \text{ kPa}) * (1 \text{ Mcm}/1,000 \text{ m}^3)$$

- Gas saved by in-line compressor:

Note: 1 Mcm = 1,000 cubic meters

$$N_i = M - (M/R_i)$$

- Gas saved by portable compressor:

$$N_p = N_i - (N_i / R_p)$$

- Example:

- Pipeline isolated length (L) = 16.1 km
- Pipeline interior diameter (D) = 0.724 m
- Pipeline operating pressure (P) = 4,134 kPa

- In-line compression ratio (R_i) = 2
- Portable compression ratio (R_p) = 8

Note: TMT = Turkmenistan New Manat
Gas Value = 855 TMT per thousand cubic meters

| | Volume of Gas (Mcm) | Value of Gas Saved |
|--|------------------------|-----------------------|
| Total gas in pipeline segment (M) | 270 | - |
| Gas saved by in-line compressor (N _i) | 135 | TMT 115,425 |
| Gas saved by portable compressor (N _p) | 118 | TMT 100,890 |
| Total gas saved by pump-down | 253 | TMT 216,315 |

Pipeline Pump-down: Economics

- Potential costs associated with using a portable compressor:
 - Capital or compressor lease cost
 - Labor costs
 - Fuel costs to run compressor
 - Installation costs
 - Maintenance costs of compressors
 - Freight costs
 - Pipeline stopple for valve leaks
 - Parallel pipeline for extra fuel gas
- Example: Lease portable compressor for one year, perform 30 pump-downs per year
 - Lease portable compressor = TMT 88,350/month x 12 months = TMT 1,060,000 for one year
 - Maintenance & fuel = TMT 1,425/month x 12 months = TMT 17,100 for one year
 - Freight costs = TMT 54,150 for one year
 - Total costs = TMT 1,131,450 for one year
- Net value = gas savings in-line + (gas savings portable – portable compressor costs)
 - = $[30 \times \text{TMT } 115,425] + ([30 \times \text{TMT } 100,890] - [\text{TMT } 1,131,450])$
 - = TMT 5,358,000

Pipeline Pump-down: Time

- Time required for pump-down affects:
 - Potential service interruptions
 - Fuel use by portable compressor
 - Fuel use by downstream compressors
 - Labor costs

Source: Ariel Corporation

Sm³/hr = standard cubic meters per hour

| ARIEL JGA/4 WITH 2X7-1/2JG+1X6-12JG+1X4-1/8JG AND CATERPILLAR G3406TA GAS ENGINE AT 1800RPM | | | | | | | | |
|---|---|--------|-----------------------|--|---|---|------------------------------|-------------------------------|
| ASSUMPTIONS: | | | | | | | | |
| Flow (Sm ³ /hr at 1.01325BarA & 15DegC) | | | | | | Pipe length(mile) | 10 | |
| Gas Temperature (DegC) | | | | | | Pipe dia.(inches) | 48 | |
| | | | | | | Volume (m3) = | 18791 | |
| Pipe line pressure (BarG) | Compressor capacity (Sm ³ /hr) | Stages | Calculated power (kw) | Avg. Flow Rate During Interval (Sm ³ /hr) | Total Gas Volume in Pipeline (Sm ³) | Volume Removed During Interval (Sm ³) | Interval Time Required (hrs) | Cumulative Running Time (hrs) |
| 31.03 | 10048 | 3 | 85 | | 613080.9 | | | 0 |
| 29.65 | 9609 | 3 | 95 | 9828.5 | 599081.6 | 27959.695 | 2.84 | 2.84 |
| 28.96 | 9429 | 3 | 100 | 9519 | 585121.2 | 13982.611 | 1.47 | 4.31 |
| 27.58 | 8776 | 3 | 106 | 9102.5 | 571138.6 | 27724.882 | 3.05 | 7.36 |
| 24.13 | 7591 | 3 | 125 | 8183.5 | 543413.7 | 72227.952 | 8.83 | 16.19 |
| 20.68 | 6307 | 3 | 137 | 6949 | 471185.7 | 66715.975 | 9.60 | 25.79 |
| 17.24 | 7165 | 3 | 248 | 6736 | 404469.8 | 66903.964 | 9.93 | 35.72 |
| 13.79 | 5744 | 3 | 244 | 6454.5 | 337565.8 | 65518.72 | 10.15 | 45.87 |
| 10.34 | 5708 | 3 | 283 | 5726 | 272047.1 | 64579.849 | 11.28 | 57.15 |
| 6.89 | 4657 | 3 | 283 | 5132.5 | 207467.2 | 63642.176 | 12.40 | 69.55 |
| 3.45 | 2963 | 3 | 261 | 3760 | 143825 | 102908.8 | 27.37 | 96.92 |
| 0 | 635 | 3 | 102 | 1799 | 40916.24 | 40916.243 | 22.74 | 119.66 |
| TOTAL TIME TAKEN TO EVACUATE A SECTION OF THE PIPELINE (HRS) | | | | | | | = | 119.66 |

Pipeline Pump-down: Case Study

- TransCanada implements pump-downs on:
 - 32 to 48 kilometer segments
 - 64 atm operating pressure
 - 1.1 meter pipeline
- Performs 30 pump-downs per year
 - In-line compressors draw down to 48 atm
 - Portable compressor draw down to 5 to 14 atm
- Uses trailer-mounted centrifugal compressor
 - 8 stages
 - Fuel gas for compressor drawn off discharge side
- Saves 1.38 million m³ per pump-down of 32 kilometer segment
 - 41.6 million m³ per year with 30 implementations annually



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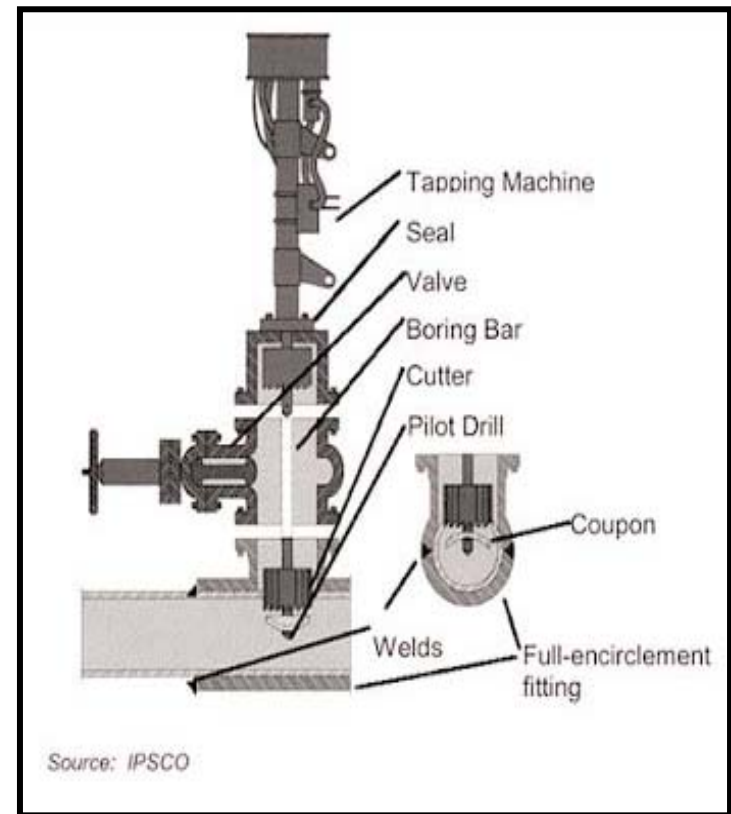
- Methane emissions from transmission pipelines
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Source: Williamson Industries Inc.

Hot Taps: Overview

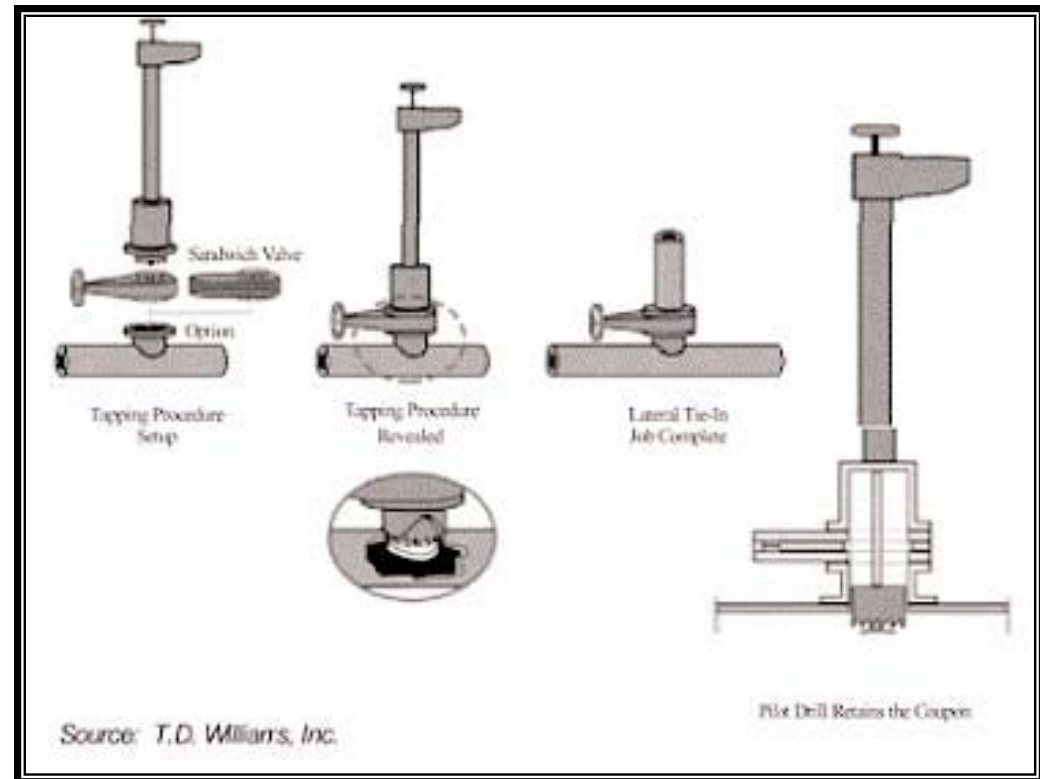
- New branch connection while the pipeline remains in service
 - Attach a branch connection and valve to the main pipeline
 - Cut-out a section of the main pipeline wall through the valve to connect the branch to the main pipeline
- Current technology has improved reliability and reduced complications
- Hot tapping can be used to add connections to a wide range of pipelines
 - Transmission pipelines
 - Distribution mains



Schematic of hot tapping machine

Hot Taps: Process

- Connect fitting and permanent valve on the existing pipeline
- Install hot tapping machine on the valve
- Perform hot tap and extract coupon through the valve
- Close valve and remove hot tapping machine
- Connect branch line



Hot Taps: Economics

| Estimated Annual Gas Savings for the Example Scenario ¹ | | | | | | |
|--|-------------------|---------------------|--------------|----------------------------|-------------|-------------------|
| Tap scenario | Annual tap number | Natural gas savings | | Nitrogen purge gas savings | | Total gas savings |
| Pipeline | | Per tap Mcm | Annual Mcm | Per tap Mcm | Annual Mcm | TMT |
| 10.2 cm pipeline, 24.8 atm, 3.2 km | 250 | 0.6 | 155.7 | 0.05 | 14.1 | 144,474 |
| 20.3 cm pipeline, 7.8 atm, 1.6 km | 30 | 0.4 | 11 | 0.1 | 3.4 | 12,142 |
| 25.4 cm pipeline, 69.0 atm, 4.8 km | 25 | 16.7 | 417 | 0.5 | 13.4 | 367,322 |
| 45.7 cm pipeline, 14.6 atm, 3.2 km | 15 | 7.2 | 108.3 | 1.2 | 17.4 | 106,604 |
| Total Annual | 320 | | 692.1 | | 48.4 | 630,708 |

Note: Natural Gas Value: TMT 855 per thousand cubic meters
 Nitrogen Gas Value: TMT 805 per thousand cubic meters

¹ Source: EPA Natural Gas STAR Lessons Learned document "Using Hot Taps for In Service Pipeline Connections" 13

Hot Taps: Economics

Economic Analysis for Five Year Hot Tap Program (320 taps/yr)¹

| | Year 0 | Year 1 | Year 2 | Year 3 | Year 4 | Year 5 |
|----------------------------|-----------|-----------|-----------|-----------|-----------|-----------|
| Capital cost, TMT | (135,115) | 0 | 0 | 0 | 0 | 0 |
| Contract service cost, TMT | 0 | (154,650) | (154,650) | (154,650) | (154,650) | (154,650) |
| O&M cost, TMT | 0 | (22,683) | (22,683) | (22,683) | (22,683) | (22,683) |
| Total cost, TMT | (135,115) | (62,222) | (62,222) | (62,222) | (62,222) | (62,222) |
| Natural gas savings, TMT | | 591,746 | 591,746 | 591,746 | 591,746 | 591,746 |
| Inert gas savings, TMT | | 38,962 | 38,962 | 38,962 | 38,962 | 38,962 |
| Net benefit, TMT | (135,115) | 740,386 | 740,386 | 740,386 | 740,386 | 740,386 |
| Payback (months) | | | | | | 2 |
| IRR | | | | | | 548% |
| NPV ² , TMT | | | | | | 2,428,664 |

¹ Source: EPA Natural Gas STAR Lessons Learned document "Using Hot Taps for In Service Pipeline Connections"

² Net present value (NPV) based on 10% discount rate for 5 years.

Hot Taps: Case Study

- One hot tap vendor reported helping a gas transmission client avoid a service outage
 - One-day gas delivery in a 914.4 millimeters natural gas pipeline operating at 68.07 atm is worth TMT 1,732,800 in gross revenue*
 - Performing shutdown connection required 4 days
 - TMT 6,962,550 estimated revenue savings*



*Gas valued at TMT 855 / Mcm

Source: TransCanada

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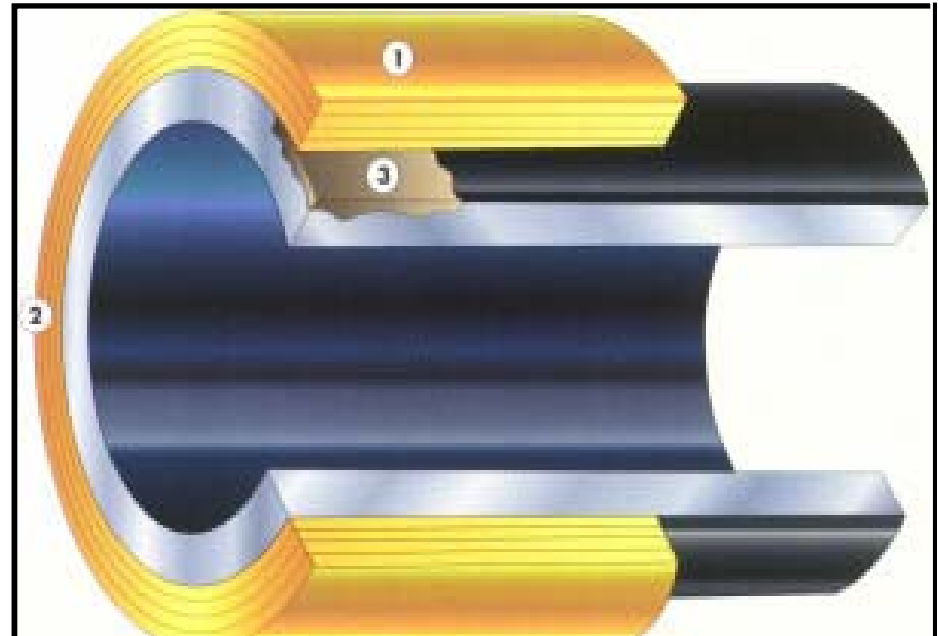
Source: Armor Plate

Composite Wrap: Overview

- Non-leaking pipeline defects can only be fixed in one of three ways:
 - Cut out damaged segment and replace with new pipes
 - Install a full-encirclement steel split sleeve over the damaged area
 - Install a composite sleeve over the damaged area
- Composite wrap advantages:
 - Can be performed without taking pipeline out of service
 - Repair is quick and less costly than replacement or sleeve options
 - Eliminates venting associated with replacement

Composite Wrap: Overview

- 1) A high-strength glass fiber composite or laminate
- 2) An adhesive or resin bonding system
- 3) A high-compressive-strength load transfer filler compound
- 4) Replaces lost hoop strength



Source: Clock Spring® Company L. P.

Composite Wrap: Installation

- After excavation and pipe preparation
 - External defects filled with filler
 - Composite wrap wound around pipe with adhesive or laminating agents
 - Typically 5 cm of wrap must extend beyond damage
 - Excavation site refilled after mandated curing time
- Reducing pressure improves quality of repair



Source: Armor Plate

Composite Wrap: Economics

| Cost Factors | At 285 TMT/Mcm (\$100/Mcm) | | | | At 855 RUB/Mcm (\$300/Mcm) | | | |
|--------------------------|----------------------------|-------------------|----------------|-------------------|----------------------------|-------------------|----------------|-------------------|
| | 15 cm defect | | 595 cm defect | | 15 cm defect | | 595 cm defect | |
| | Composite wrap | Pipeline replace. | Composite wrap | Pipeline replace. | Composite wrap | Pipeline replace. | Composite wrap | Pipeline replace. |
| Natural gas lost (Mcm) | 0 | 112 | 0 | 112 | 0 | 112 | 0 | 112 |
| Purge gas (Mcm) | 0 | 5.64 | 0 | 5.64 | 0 | 5.64 | 0 | 5.64 |
| Number of wrap kits | 1 | 0 | 20 | 0 | 1 | 0 | 20 | 0 |
| Cost of natural gas lost | 0 | 31,920 | 0 | 31,920 | 0 | 95,760 | 0 | 95,760 |
| Cost of purge Gas | 0 | 4,540 | 0 | 4,540 | 0 | 4,540 | 0 | 4,540 |
| Labor | 1,065 | 3,824 | 2,129 | 5,736 | 1,065 | 3,824 | 2,129 | 5,736 |
| Equipment and materials | 4,408 | 11,505 | 88,159 | 20,807 | 4,408 | 11,505 | 88,159 | 20,807 |
| Indirect costs | 2,736 | 4,908 | 45,145 | 10,617 | 2,736 | 4,908 | 45,145 | 10,617 |
| Total cost of repair | 8,209 | 30,923 | 135,433 | 47,845 | 8,209 | 125,706 | 135,433 | 142,629 |
| Most economical option | X | | X | | X | | X | |

¹ Based on repair of a small versus large defect on a 61 cm diameter pipeline operated at 24 atm, with 16.1 km between shut-off valves

Composite Wrap: Case Study

- One Partner reported installing over 300 wraps on 254 millimeter or greater lines since 1995
- Limits repairs to 4 butted wraps then replaces
- 51-cm defects in line near creek bed:
 - Limited environmental exposure
 - Wrapped in 2 hours
 - Total repair 2 days from start to finish

Contact Information and Further Information

- More detail is available on these practices and over 80 others online at:
epa.gov/gasstar/tools/recommended.html
- For further assistance, direct questions to:

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