



**Methane to Markets**



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## **Reducing Methane Emissions from Centrifugal and Reciprocating Compressors**

**Seminar with Russian Independent Oil and Gas Producers on Methane Mitigation Technologies and Strategies**

October 4, 2010, Moscow, Russia

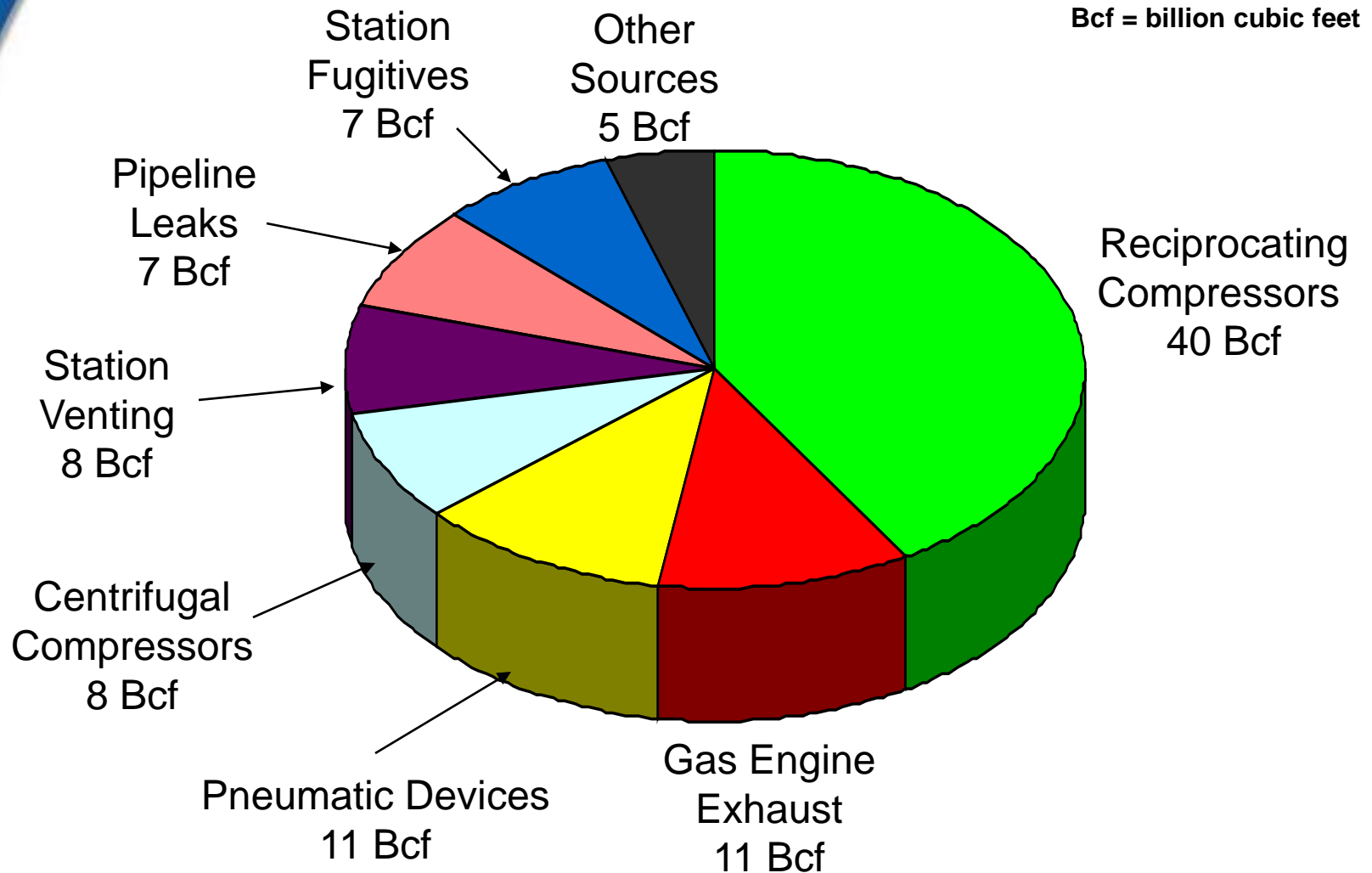
Don Robinson, Vice President  
ICF International

# Compressor Seals: Agenda

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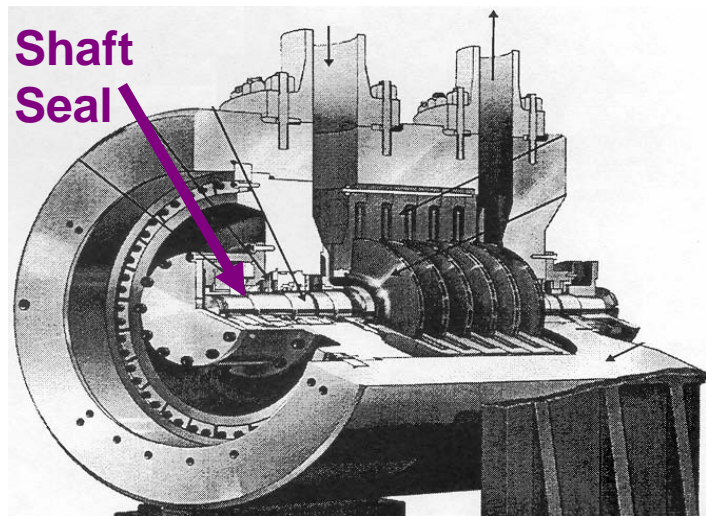
- U.S. Methane Emissions from Compressor Seals
- Centrifugal Compressor Wet Seals
  - Methane Losses
  - Solutions
  - Economics
  - Industry Experience / More Opportunities
- Reciprocating Compressor Rod Packing
  - Methane Losses
  - Solutions
  - Economics
  - More Opportunities / Industry Experience
- Contacts and Further Information

# 2008 Transmission Sector Methane Emissions (97 Bcf)



# Methane Losses from Centrifugal Compressors

- Centrifugal compressor wet seals leak little gas at the seal face
  - The majority of methane emissions occur through seal oil degassing which is vented to the atmosphere
  - Seal oil degassing may vent 1.1 to 5.7 m<sup>3</sup>/minute to the atmosphere
  - One Natural Gas STAR Partner reported emissions as high as 2,124 m<sup>3</sup>/day

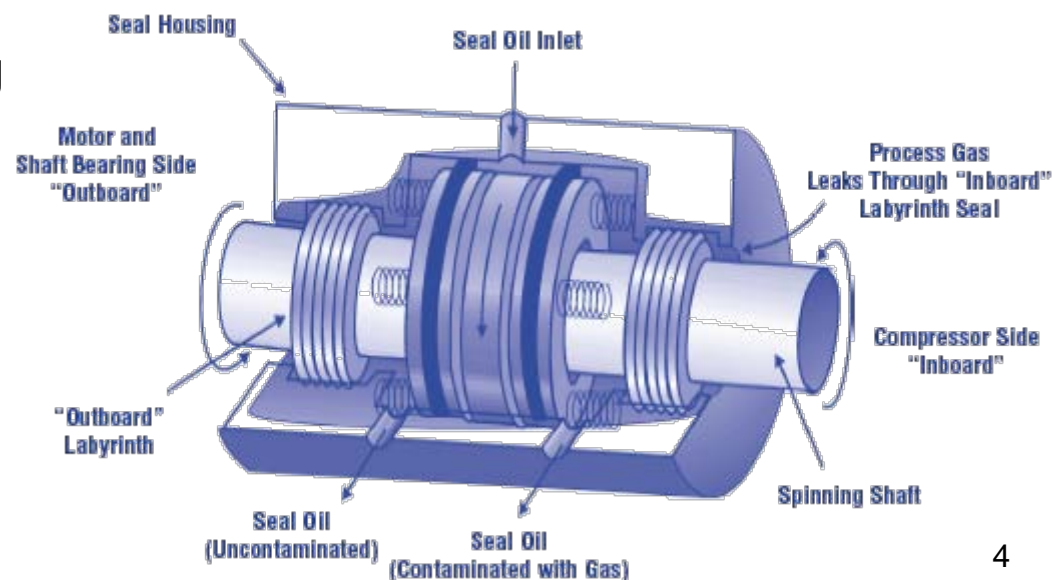


# Centrifugal Compressor Wet Seals

- High pressure seal oil circulates between rings around the compressor shaft
- Oil absorbs the gas on the inboard side
  - Little gas leaks through the oil seal
  - Seal oil degassing vents methane to the atmosphere

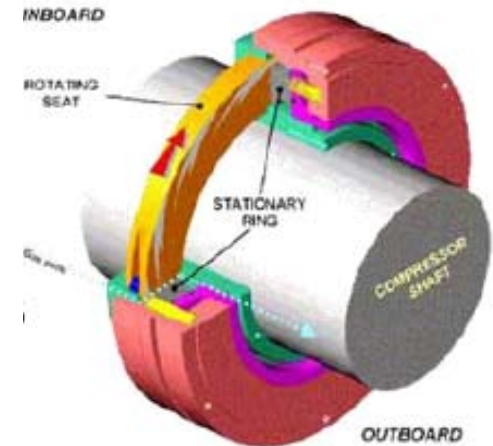


Source: PEMEX

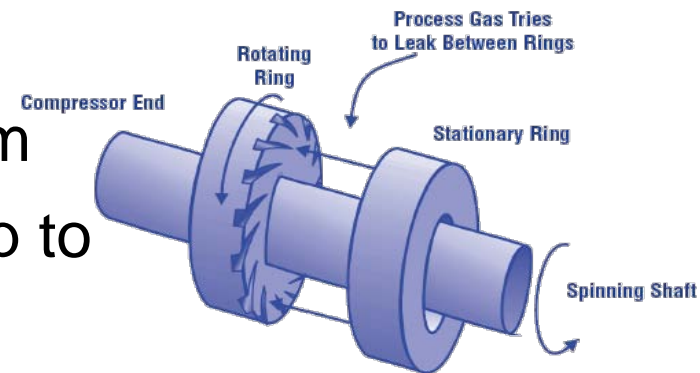


# Wet Seals Solution: Dry Seals

- Dry seal springs press stationary ring in seal housing against rotating ring when compressor is not rotating
- At high rotation speed, gas is pumped between seal rings by grooves in rotating ring creating a high pressure barrier to leakage
- Only a very small amount of gas escapes through the gap
- 2 seals are often used in tandem
- Can operate for compressors up to 206 atmospheres (atm) safely



Source: PEMEX

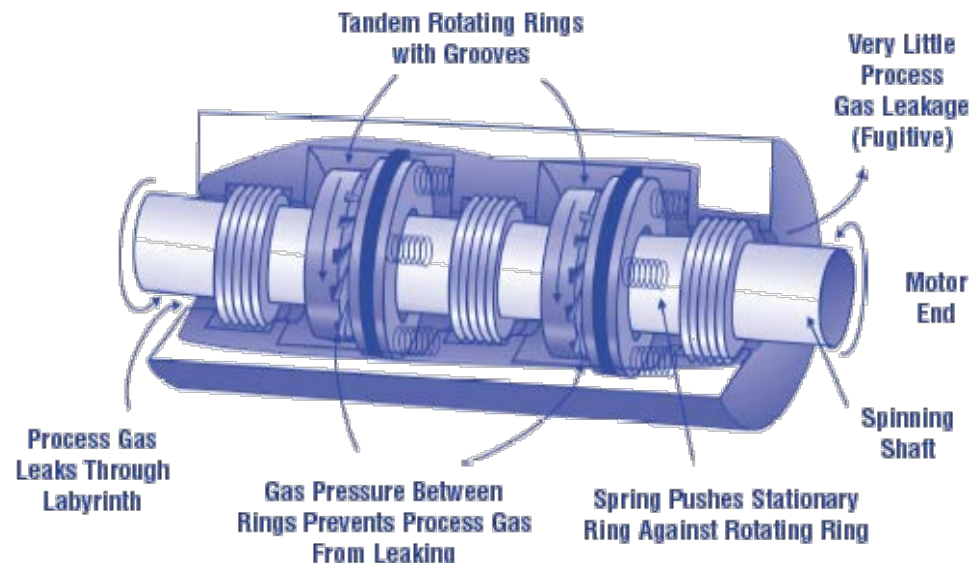


# Methane Savings through Dry Seals

- Dry seals typically leak at a rate of only 0.8 to 5.1 m<sup>3</sup>/hour (0.01 to 0.09 m<sup>3</sup>/ minute)
  - Significantly less than the 1.1 to 5.7 m<sup>3</sup>/minute emissions from wet seals
- Gas savings translate to approximately RUB 5,000,000 to RUB 30,000,000 at RUB 11,360/Mcm<sup>1</sup>



Source: PEMEX



<sup>1</sup>Mcm = thousand cubic meters

## Economics of Replacing Seals

- Compare costs and savings for a 15.2 cm (6-inch) shaft beam compressor

Cost Category	Dry Seal (RUB)	Wet Seal (RUB)
<b>Implementation costs<sup>1</sup></b>		
Seal costs (2 dry @ RUB 414,720/shaft-inch, with testing)	4,976,640	
Seal costs (2 wet @ RUB 207,390/shaft-inch)		2,488,680
Other costs (engineering, equipment installation)	4,976,640	0
<b>Total implementation costs</b>	<b>9,953,280</b>	<b>2,488,680</b>
<b>Annual operating and maintenance</b>	<b>433,150</b>	<b>3,145,730</b>
<b>Annual methane emissions</b> (@ RUB 11,360/thousand m <sup>3</sup> ; 8,000 hours/year)		
2 dry seals at a total of 12 m <sup>3</sup> /hour	1,090,560	
2 wet seals at a total of 168 m <sup>3</sup> /hour		15,267,840
<b>Total costs over 5-year period</b>	<b>12,119,030</b>	<b>18,217,330</b>
<b>Total dry seal savings over 5 years</b>		
Savings	6,098,300	
Methane Emissions Reductions (million m <sup>3</sup> )	6.24	

<sup>1</sup>Flowserve Corporation (updated costs and savings)



# Industry Experience – PEMEX (Mexican Production Company)

- PEMEX had 46 compressors with wet seals at a production site
- Converted three to dry seals<sup>1</sup>
  - Cost RUB 13,639,680/compressor
  - Saves 580,500 m<sup>3</sup>/compressor/year
  - Saves RUB 6,594,480/compressor/year in gas<sup>1</sup>
- 2.1 year payback from gas savings alone<sup>2</sup>
- Plans for future dry seal installations



Source: PEMEX

<sup>1</sup>All data based on Partners' experiences and represented in U.S. economics, converted to Russian currency.

<sup>2</sup>Gas price at RUB 11,360/Mcm

# Industry Experience – Supersonic Gas Injector: TransCanada (Canadian Transmission Company)

- Developed for capturing very low pressure vent gases and re-injection into a high pressure gas stream without the use of rotating machinery
- Savings
  - 113,000 m<sup>3</sup>/year of gas savings from one compressor
  - Natural gas worth RUB 1,283,680/year/unit at RUB 11,360/Mcm
  - Zero operating cost



Source: TransCanada

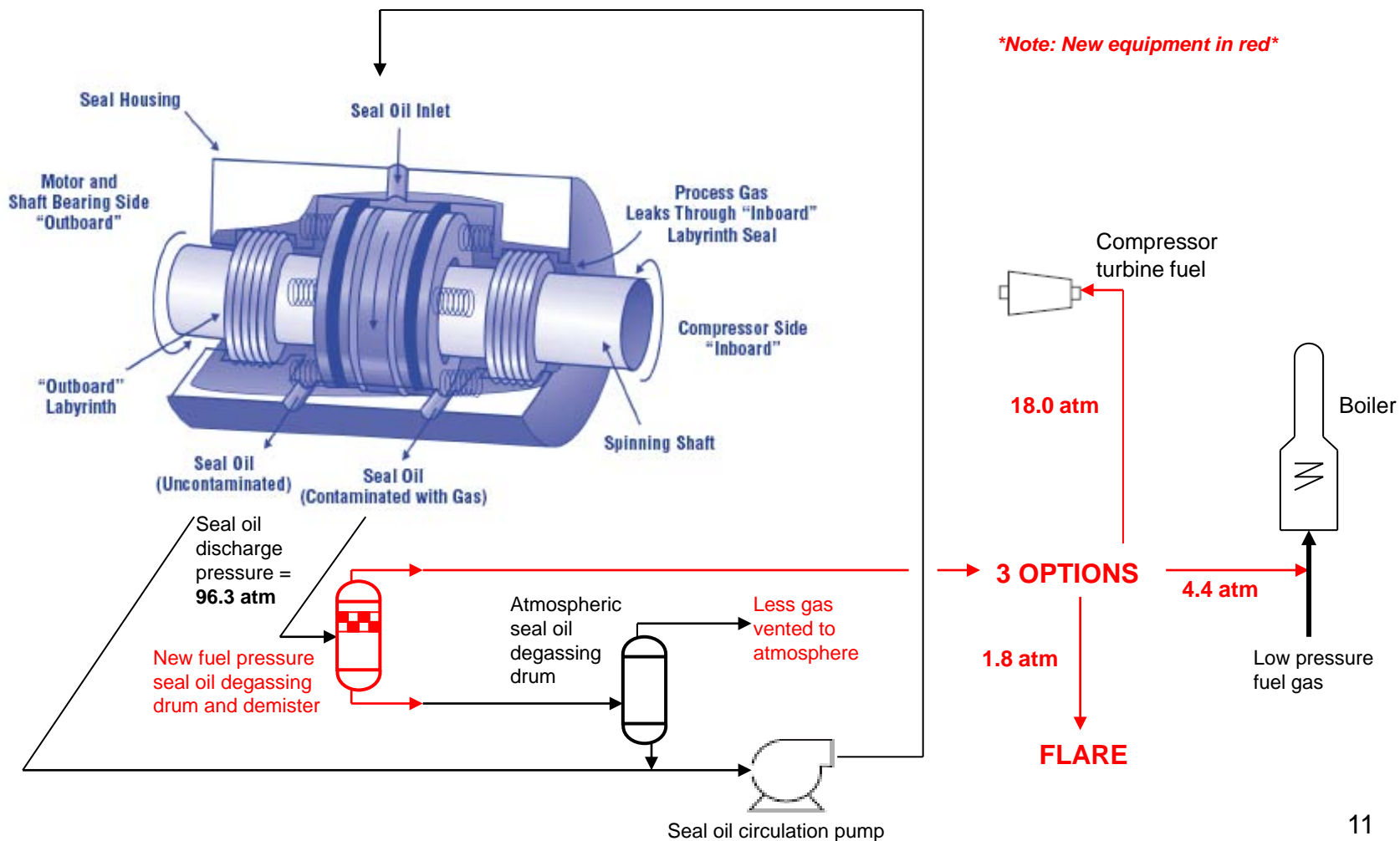
## More Opportunities

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- Partners are identifying other technologies and practices to reduce emissions
- One partner degasses seal oil in an intermediate pressure drum, with the gas used:
  - As turbine fuel
  - As low pressure fuel
  - To flare
- Prevents most seal oil gas emissions from venting to atmosphere
- Less expensive capital costs compared to dry seals
- Partner reported emission reductions of 3.1 m<sup>3</sup>/minute (110 ft<sup>3</sup>/minute) per seal when routing gas back to turbine fuel

# More Opportunities—cont.

- Partner's seal oil degassing vent recovery and use:



## More Opportunities—cont.

- Investment includes cost of:
  - Intermediate degassing drum
  - New piping
  - Gas demister/filter
  - Pressure regulator for fuel gas line
- Project summary:
  - Less capital intensive than dry seals
  - Reduce emissions while also improving site efficiency
  - Positive cash flow after less than a month

PROJECT SUMMARY: CAPTURE AND USE OF SEAL OIL DEGASSING EMISSIONS			
Operating Requirements	<ul style="list-style-type: none"> <li>■ Centrifugal compressor with seal oil system</li> <li>■ Nearby use for low pressure fuel gas</li> <li>■ New intermediate pressure flash drum, fuel filter, pressure regulator</li> </ul>		
Capital & Installation Costs	RUB 675,840 <sup>1</sup>		
Annual Labor & Maintenance Costs	Minimal		
Methane saved	1.8 MMcm		
Gas Price per Mcm	RUB 5,680	<b>RUB 11,360</b>	RUB 17,040
Value of Gas Saved	RUB 10,224,000	<b>RUB 20,448,000</b>	RUB 30,672,000
Payback Period in Months	0.8	<b>0.4</b>	0.3

<sup>1</sup>Assuming a typical seal oil flow rate of 14.20 liters/minute (3.75 gallons/minute)

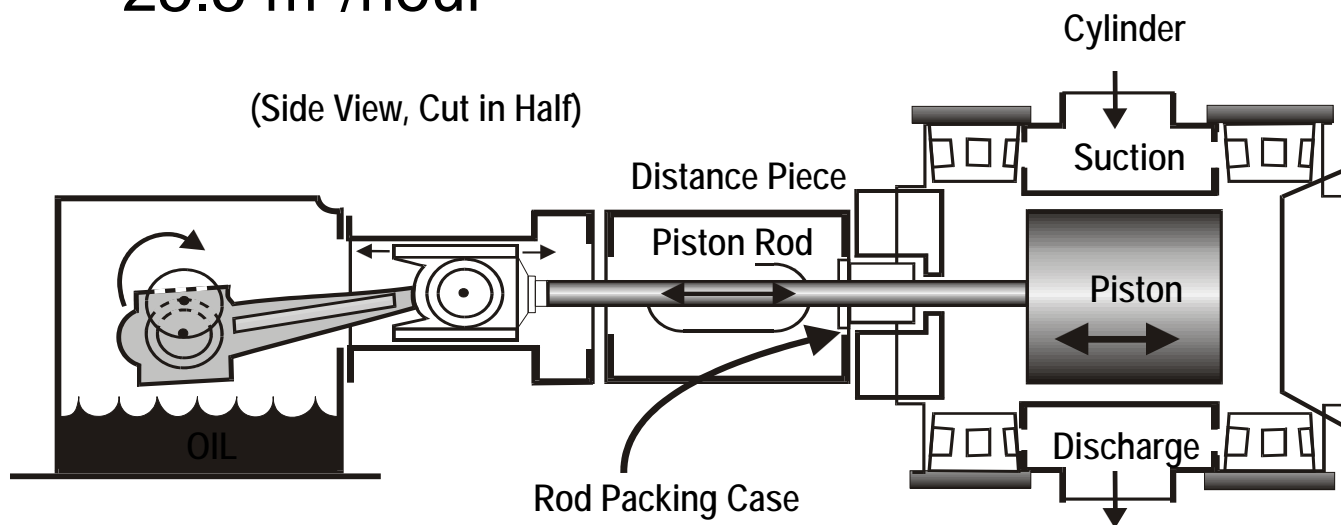
# Compressor Seals: Agenda

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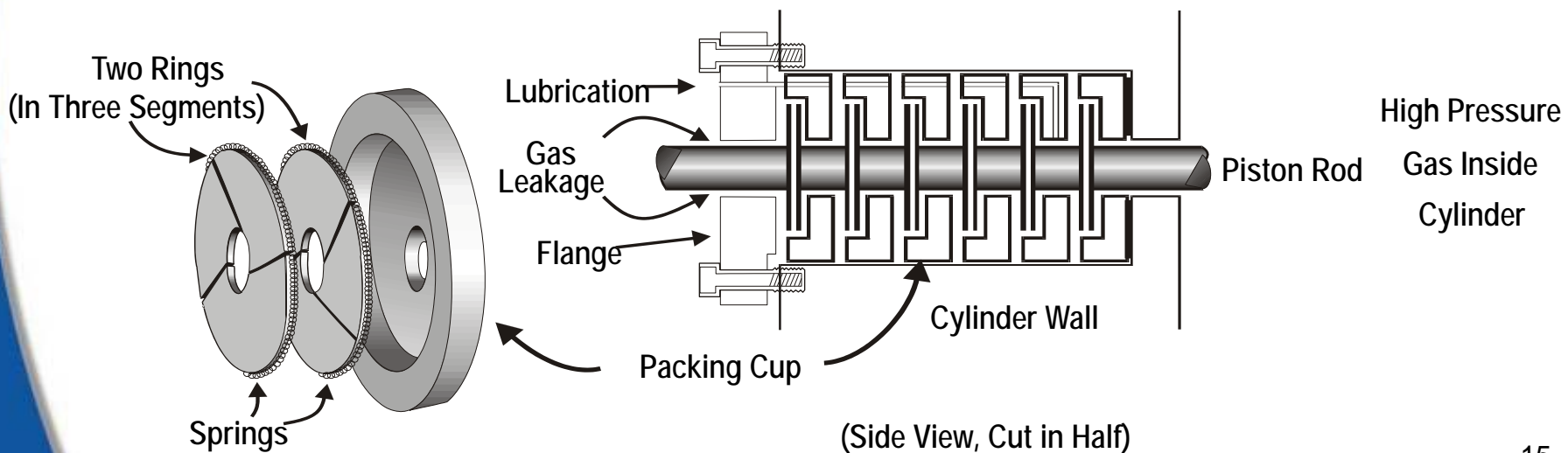
# Methane Losses from Reciprocating Compressors

- Reciprocating compressor rod packing leaks some gas by design
  - Newly installed packing may leak 0.3 to 1.7 m<sup>3</sup>/hour
  - Worn packing has been reported to leak up to 25.5 m<sup>3</sup>/hour



# Reciprocating Compressor Rod Packing

- A series of flexible rings fit around the shaft to prevent leakage
- Leakage may still occur through nose gasket, between packing cups, around the rings, and between rings and shaft





# Methane Losses from Rod Packing

Emission from Running Compressor	24,600	m <sup>3</sup> /year-packing
Emission from Idle/Pressurized Compressor	36,000	m <sup>3</sup> /year-packing
Leakage from Packing Cup	19,500	m <sup>3</sup> /year-packing
Leakage from Distance Piece	8,500	m <sup>3</sup> /year-packing

Leakage from Rod Packing on Running Compressors				
Packing Type	Bronze	Bronze/Steel	Bronze/Teflon	Teflon
Leak Rate (m <sup>3</sup> /year)	17,300	15,700	37,300	5,900

Leakage from Rod Packing on Idle/Pressurized Compressors				
Packing Type	Bronze	Bronze/Steel	Bronze/Teflon	Teflon
Leak Rate (m <sup>3</sup> /year)	17,400	N/A	36,500	5,400

# Solution: Economic Replacement

- Measure rod packing leakage
  - When new packing installed—after worn-in
  - Periodically afterwards
- Determine cost of packing replacement
- Determine economic replacement threshold
  - Partners can determine economic threshold for all replacements
  - This is a capital recovery economic calculation
- Replace packing when leak reduction expected will pay back cost

**Economic Replacement Threshold (m<sup>3</sup>/hour) =**

$$\frac{CR * DF * 1,000}{(H * GP)}$$

Where:

**CR = Cost of replacement (RUB)**

**DF = Discount factor at interest *i***

**H = Hours of compressor operation per year**

**GP = Gas price RUB/thousand cubic meters)**

$$DF = \frac{i(1+i)^n}{(1+i)^n - 1}$$

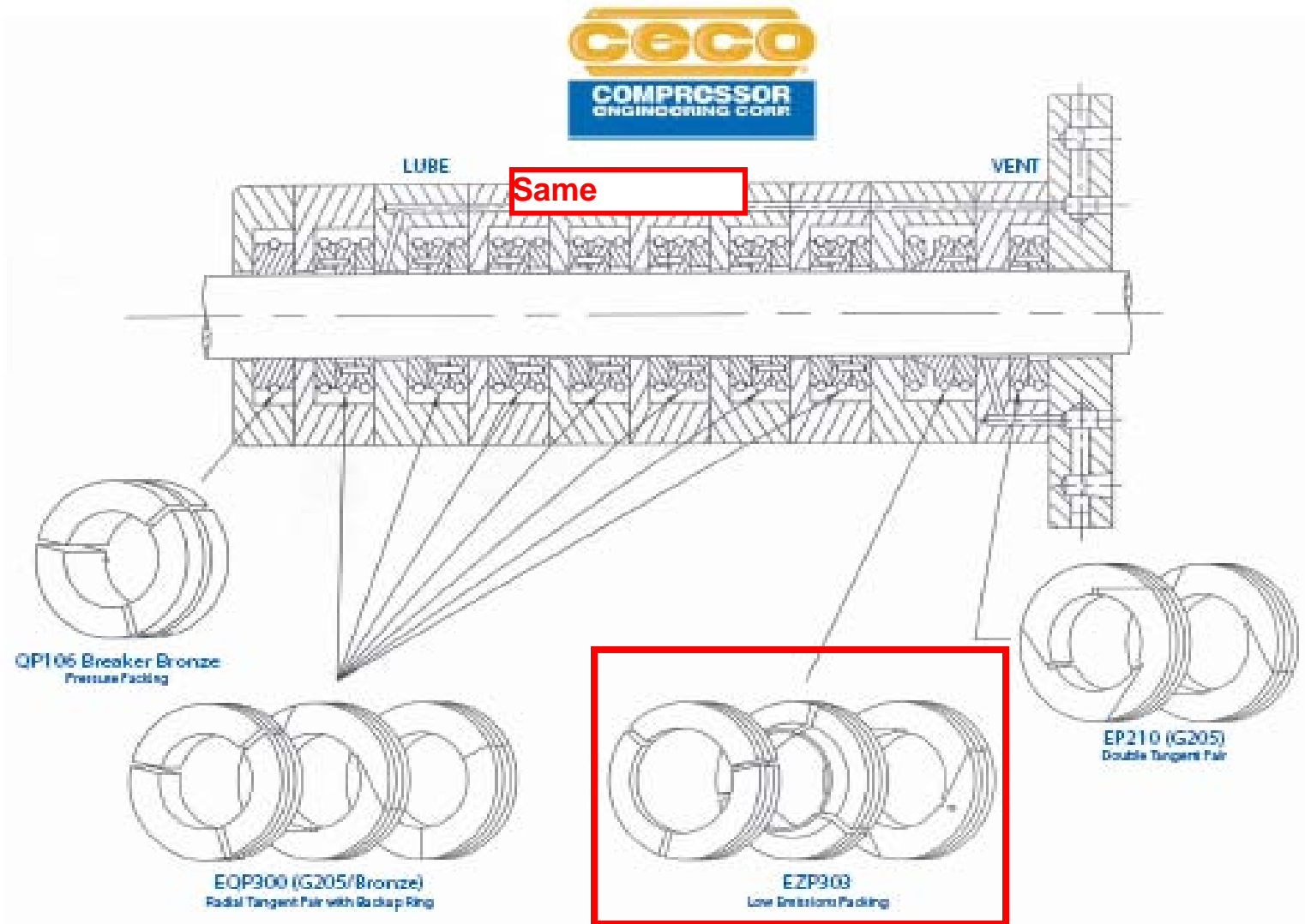
## More Opportunities: Low Emission Packing (LEP)

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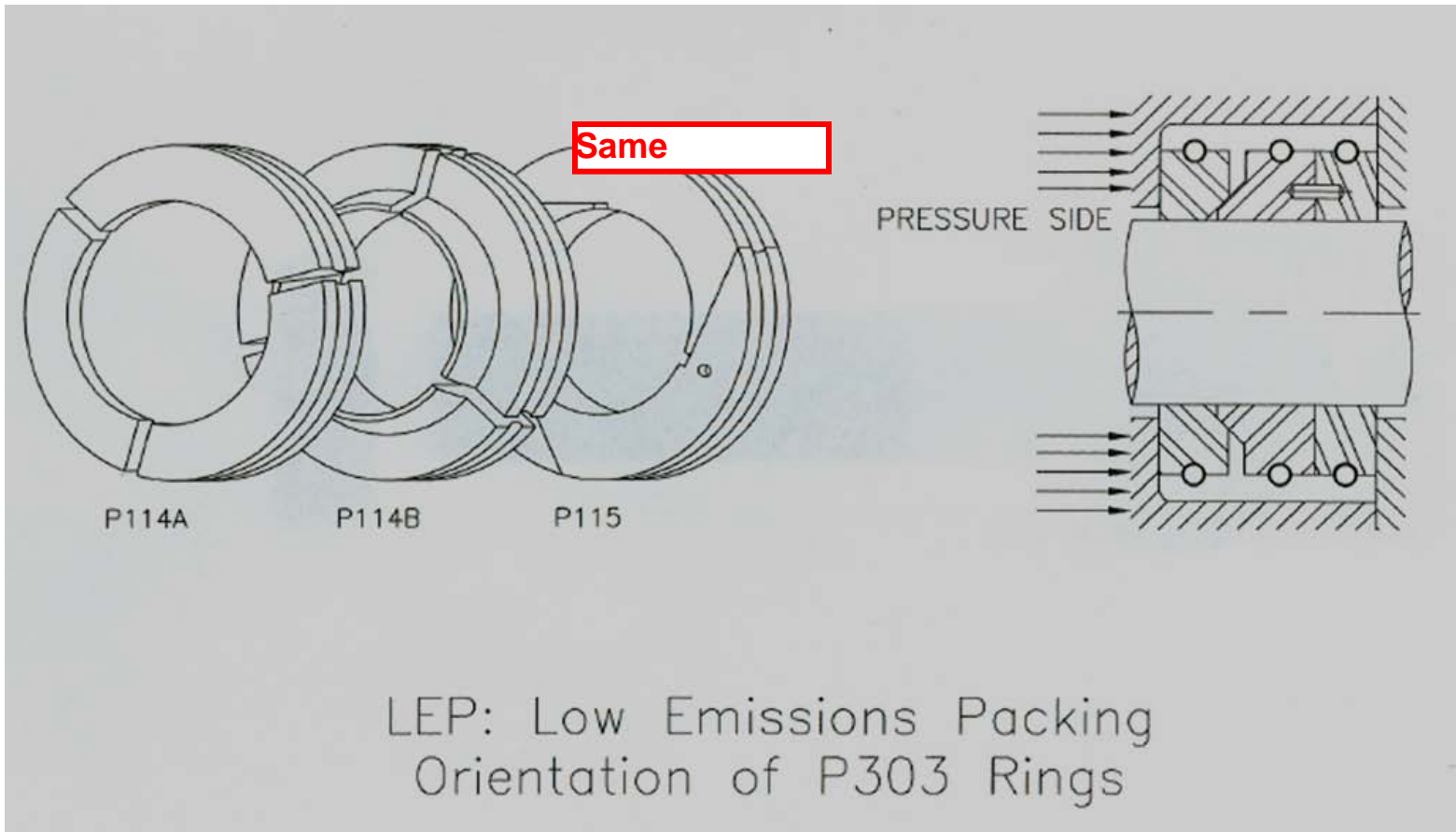
- The side load eliminates clearance and maintains positive seal on cup face
- LEP is a static seal, not a dynamic seal. No pressure is required to activate the packing
- This design works in existing packing case with limited, to no modifications required

Same

# LEP Packing Configuration



# Orientation in Cup



## Reasons to Use LEP

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- Upgrade is inexpensive
- Significant reduction of greenhouse gas is major benefit
- Refining, petrochemical, and air separation plants have used this design for many years to minimize fugitive emissions

## Industry Experience – Northern Natural Gas (U.S. Transmission Company)

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- Monitored emissions at two locations
  - Unit A leakage as high as 301 liters/minute (18 m<sup>3</sup>/hour)
  - Unit B leakage as high as 105 liters/minute (6 m<sup>3</sup>/hour)
- Installed low emission packing (LEP)
  - Testing is still in progress
  - After 3 months, leak rate showed zero leakage increase

# Contact Information and Further Information

- More detail is available on these practices and over 80 others online at:  
[epa.gov/gasstar/tools/recommended.html](http://epa.gov/gasstar/tools/recommended.html)
- For further assistance, direct questions to:

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