



Methane Savings from Compressors

Lessons Learned from the Natural Gas STAR Program

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epa.gov/gasstar



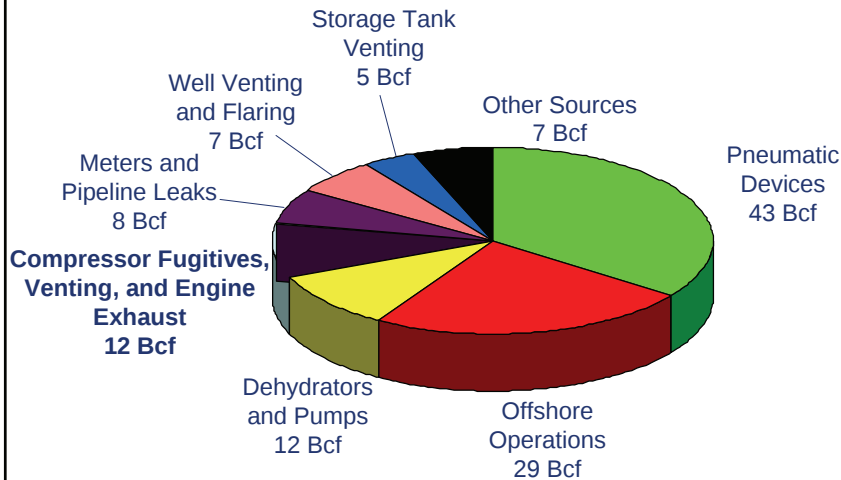
Compressors: Agenda

- 💧 Centrifugal Compressors
 - 💧 Methane Losses
 - 💧 Methane Savings
 - 💧 Industry Experience
- 💧 Reciprocating Compressors
 - 💧 Methane Losses
 - 💧 Methane Savings
 - 💧 Industry Experience
- 💧 Discussion

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2007 Production Sector Methane Emissions



EPA. *Inventory of U.S. Greenhouse Gas Emissions and Sinks 1990 – 2007*. April, 2009. Available on the web at: epa.gov/climatechange/emissions/usinventoryreport.html

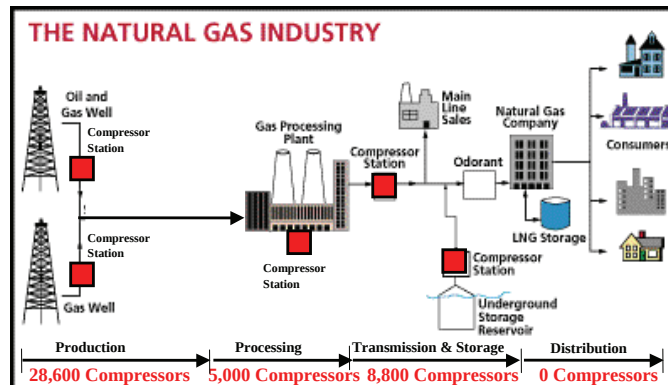
Note: Natural Gas STAR reductions from gathering and boosting operations are reflected in the production sector.

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Compressor Methane Emissions What is the problem?

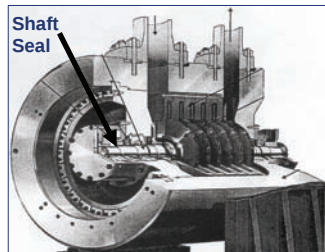
- ⚡ Methane emissions from the ~42,400 compressors in the natural gas industry account for 118 Bcf/year or about 33% of all methane emissions from the natural gas industry



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Methane Losses from Centrifugal Compressors

- 💧 Centrifugal compressor wet seals leak little gas at the seal face
 - 💧 Seal oil degassing may vent 40 to 200 cubic feet per **minute** (cf/minute) to the atmosphere
 - 💧 A Natural Gas STAR Partner reported wet seal emissions of 75 Mcf/day (52 cf/minute)



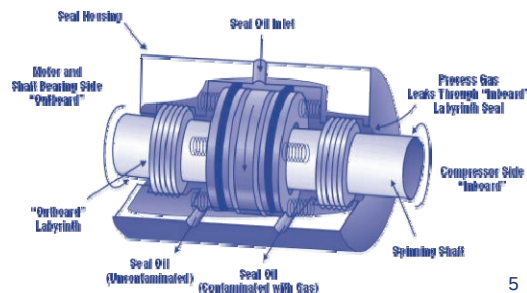
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Centrifugal Compressor Wet Seals

- 💧 High pressure seal oil circulates between rings around the compressor shaft
- 💧 Oil absorbs the gas on the inboard side
- 💧 Little gas leaks through the oil seal
- 💧 Seal oil degassing vents methane to the atmosphere



Source: PEMEX

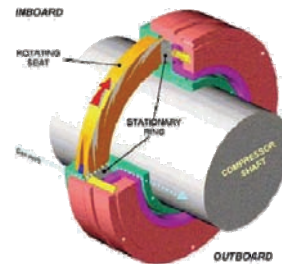


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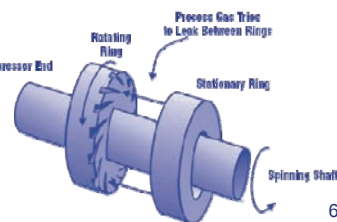


Natural Gas STAR Partners Reduce Emissions with Dry Seals

- ⚡ Dry seal springs press the stationary ring in the seal housing against the rotating ring when the compressor is not rotating
- ⚡ Sealing at high rotation speed pump gas between the seal rings creating a high pressure barrier to leakage
- ⚡ Only a very small volume of gas escapes through the gap
- ⚡ Two seals are often used in tandem
- ⚡ Can operate for compressors up to 3,000 pounds per square inch gauge (psig) safely



Source: PEMEX



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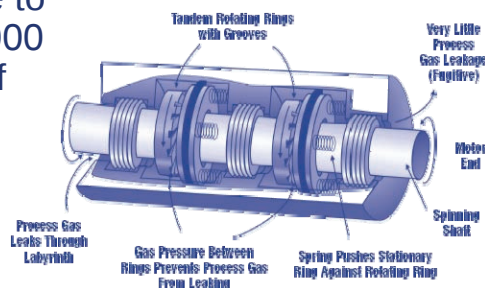


Methane Savings through Dry Seals

- ⚡ Dry seals typically leak 0.5 to 3 cf/minute
 - ⚡ Significantly less than the 40 to 200 cf/minute emissions from wet seals
- ⚡ Gas savings translate to approximately \$112,000 to \$651,000 at \$7/Mcf



Source: PEMEX



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Economics of Replacing Seals

- Compare costs and savings for a 6-inch shaft beam compressor

Cost Category	Dry Seal (\$)	Wet Seal (\$)
Implementation Costs¹		
Seal costs (2 dry @ \$13,500/shaft-inch, with testing)	\$162,000	
Seal costs (2 wet @ \$6,750/shaft-inch)		\$81,000
Other costs (engineering, equipment installation)	\$162,000	\$0
Total implementation costs	\$324,000	\$81,000
Annual Operating and Maintenance	\$14,100	\$102,400
Annual Methane Emissions (@ \$7/Mcf; 8,000 hours/year)		
2 dry seals at a total of 6 cf/minute	\$20,160	
2 wet seals at a total of 100 cf/minute		\$336,000
Total Costs Over 5-Year Period	\$495,300	\$2,273,000
Total Dry Seal Savings Over 5 Years		
Savings	\$1,777,700	
Methane Emissions Reductions (Mcf; at 45,120 Mcf/year)	225,600	

¹ Flowserve Corporation (updated costs and savings)

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Is Wet Seal Replacement Profitable?

- Replacing wet seals in a 6 inch shaft beam compressor operating 8,000 hours/year
 - Net present value = \$1,337,769
 - Assuming a 10% discount over 5 years
 - Internal rate of return = 129%
 - Payback period = 10 months
 - Ranges from 3 to 11 months based on wet seal leakage rates between 40 and 200 cf/minute
- Economics are better for new installations
 - Vendors report that 90% of compressors sold to the natural gas industry are centrifugal with dry seals

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Industry Experience – PEMEX

- 💧 PEMEX had 46 compressors with wet seals at its PGPB production site
- 💧 Converted three to dry seals
 - 💧 Cost \$444,000/compressor
 - 💧 Saves 20,500 Mcf/compressor/year
 - 💧 Saves \$126,690/compressor/year in gas
- 💧 3.5 year payback from gas savings alone
- 💧 Plans for future dry seal installations



Source: PEMEX

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Finding More Opportunities

- 💧 Partners are identifying other technologies and practices to reduce emissions
 - 💧 TransCanada has successfully conducted pilot studies on the use of an ejector to recover dry seal leakage
 - 💧 Prospective project not yet reported: route seal oil flash gas to low pressure fuel system
 - 💧 Reduces methane emissions from the significant source of centrifugal compressor wet seal oil degassing but without significant capital investment of dry seal retrofit

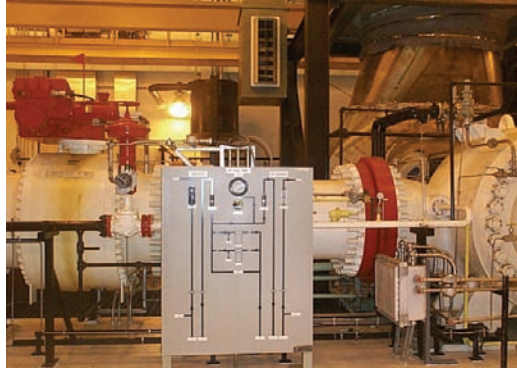


Source: TransCanada

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TransCanada Experience: Supersonic Gas-Gas Ejector

- Compressor Package Components
Winchell Lk

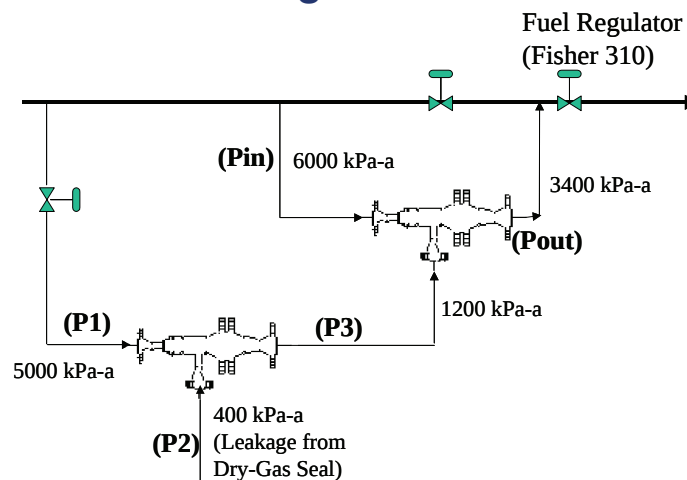


Source: TransCanada

Dry seal panel, continuous gas venting by design

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Supersonic Gas-Gas Ejector for Capturing Low Pressure Vent gases



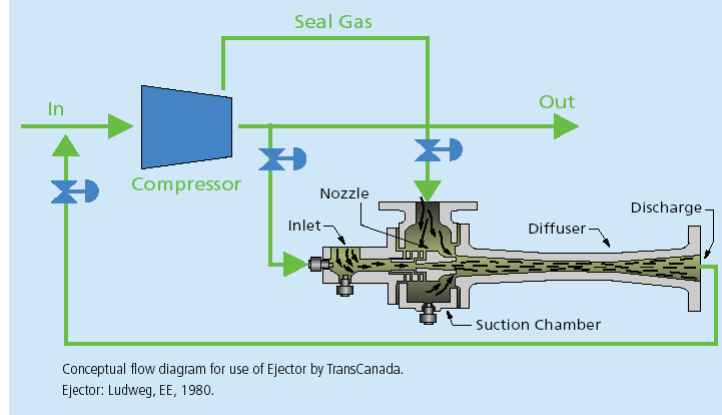
Source: TransCanada

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Supersonic Gas-Gas Ejector for Dry Gas Seal Leak Capture

Conceptual Flow Diagram

US & Canadian patent filed



Source: TransCanada

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Supersonic Gas-Gas Ejector

- 💧 Developed for capturing very low pressure vent gases and re-injection into a high pressure gas stream without the use of rotating machinery
- 💧 Savings
 - 💧 4 MMcf/yr of gas savings from one compressor
 - 💧 Natural gas worth \$28,000/yr/unit @\$7/GJ
 - 💧 GHG emissions
 - 💧 Zero operating cost



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Finding More Opportunities

Wet Seal Degassing

- Potential new method to capture emissions from wet seal compressors
- Can be more economical than replacing wet seals with dry seals

POTENTIAL PROJECT EXAMPLE ECONOMICS: CAPTURE AND USE OF SEAL OIL DEGASSING EMISSIONS

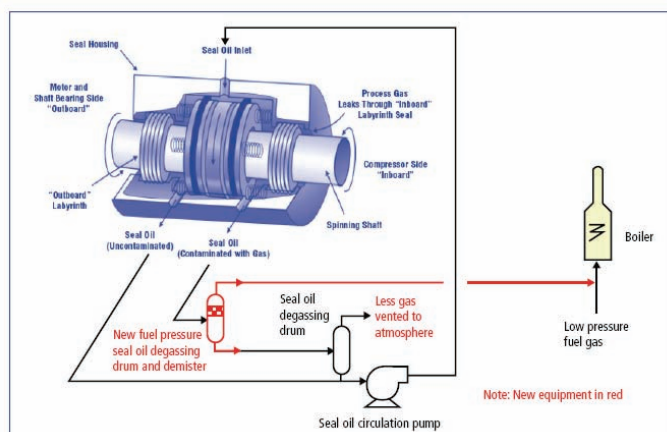
OPERATING REQUIREMENTS	- Centrifugal compressor with seal oil system - Nearby use for low pressure fuel gas - New intermediate pressure flash drum, fuel filter, pressure regulator		
CAPITAL & INSTALLATION COSTS	\$22,000		
ANNUAL LABOR & MAINTENANCE COSTS	Minimal		
METHANE SAVED	63 MMcf per year		
GAS PRICE PER Mcf	\$3	\$7	\$10
VALUE OF GAS SAVED	\$189,000	\$442,000	\$631,000
PAYBACK PERIOD IN MONTHS	2	1	0.5

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Finding More Opportunities

Wet Seal Degassing

- Requires nearby boiler or engine to make use of fuel gas



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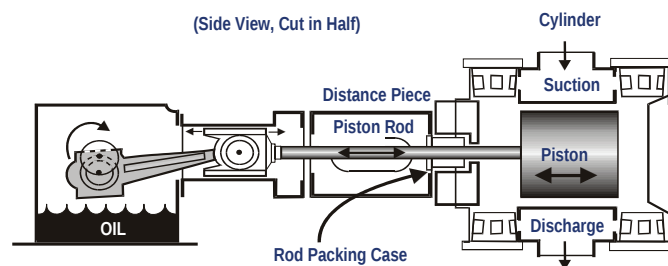
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Methane Losses from Reciprocating Compressors

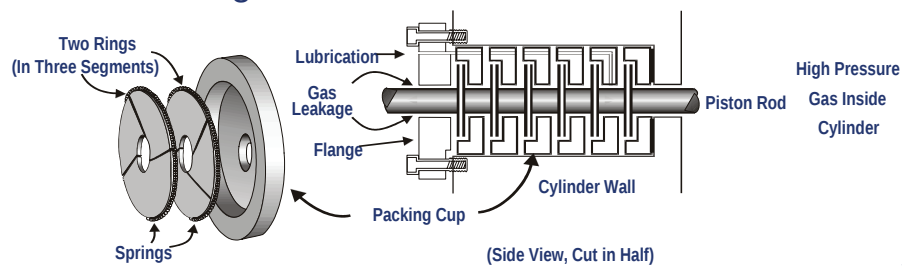
- 💧 Reciprocating compressor rod packing leaks some gas by design
 - 💧 Newly installed packing may leak 60 cubic feet per hour (cf/hour)
 - 💧 Worn packing has been reported to leak up to 900 cf/hour



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Reciprocating Compressor Rod Packing

- ⚡ A series of flexible rings fit around the shaft to prevent leakage
- ⚡ Leakage may still occur through nose gasket, between packing cups, around the rings, and between rings and shaft



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Impediments to Proper Sealing

Ways packing case can leak

- ⚡ Nose gasket (no crush)
- ⚡ Packing to rod (surface finish)
- ⚡ Packing to cup (lapped surface)
- ⚡ Packing to packing (dirt/lube)
- ⚡ Cup to cup (out of tolerance)

What makes packing leak?

- ⚡ Dirt or foreign matter (trash)
- ⚡ Worn rod (.0015"/per inch dia.)
- ⚡ Insufficient/too much lubrication
- ⚡ Packing cup out of tolerance ($\leq 0.002"$)
- ⚡ Improper break-in on startup
- ⚡ Liquids (dilutes oil)
- ⚡ Incorrect packing installed (backward or wrong type/style)

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Methane Losses from Rod Packing

Emission from Running Compressor	99	cf/hour-packing
Emission from Idle/Pressurized Compressor	145	cf/hour-packing
Leakage from Idle Compressor Packing Cup	79	cf/hour-packing
Leakage from Idle Compressor Distance Piece	34	cf/hour-packing

Leakage from Rod Packing on Running Compressors				
Packing Type	Bronze	Bronze/Steel	Bronze/Teflon	Teflon
Leak Rate (cf/hour)	70	63	150	24

Leakage from Rod Packing on Idle/Pressurized Compressors				
Packing Type	Bronze	Bronze/Steel	Bronze/Teflon	Teflon
Leak Rate (cf/hour)	70	N/A	147	22

PRCI/ GRI/ EPA. *Cost Effective Leak Mitigation at Natural Gas Transmission Compressor Stations*

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Steps to Determine Economic Replacement

- 💧 Measure rod packing leakage
 - 💧 When new packing installed – after worn-in
 - 💧 Periodically afterwards
- 💧 Determine cost of packing replacement
- 💧 Calculate economic leak reduction
- 💧 Replace packing when leak reduction expected will pay back cost

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Cost of Rod Packing Replacement

Assess costs of replacements

- A set of rings: \$ 1,350 to \$ 1,700
 - (with cups and case) \$ 2,025 to \$ 3,375
 - Rods: \$ 2,430 to \$13,500
 - Special coatings such as ceramic, tungsten carbide, or chromium can increase rod costs



Source: CECO

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Calculate Economic Leak Reduction

Determine economic replacement threshold

- Partners can determine economic threshold for all replacements
 - This is a capital recovery economic calculation

$$\text{Economic Replacement Threshold (cf/hour)} = \frac{CR * DF * 1,000}{(H * GP)}$$

Where:

CR = Cost of replacement (\$)

DF = Discount factor at interest i =

H = Hours of compressor operation per year

GP = Gas price (\$/thousand cubic feet)

$$DF = \frac{i(1+i)^n}{(1+i)^n - 1}$$

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Economic Replacement Threshold

Example: Payback calculations for new rings and rod replacement

CR = \$1,620 for rings + \$9,450 for rod
= \$11,070

H = 8,000 hours per year

GP = \$7/Mcf

DF @ i = 10% and n = 1 year

$$DF = \frac{0.1(1+0.1)^1}{(1+0.1)^1 - 1} = \frac{0.1(1.1)}{1.1 - 1} = \frac{0.11}{0.1} = 1.1$$

DF @ i = 10% and n = 2 years

$$DF = \frac{0.1(1+0.1)^2}{(1+0.1)^2 - 1} = \frac{0.1(1.21)}{1.21 - 1} = \frac{0.121}{0.21} = 0.576$$

One year payback

$$ER = \frac{\$11,070 \times 1.1 \times 1000}{(8,000 \times \$7)} = 217 \text{ scf per hour}$$

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Is Rod Packing Replacement Profitable?

Replace packing when leak reduction expected will pay back cost

“leak reduction expected” is the difference between current leak rate and leak rate with new rings

Rings Only

Rings: \$1,620
Rod: \$0
Gas: \$7/Mcf
Operating: 8,000 hours/year

Leak Reduction Expected (cf/hour)	Payback (months)
61	6
32	12
17	24
12	36

Rod and Rings

Rings: \$1,620
Rod: \$9,450
Gas: \$7/Mcf
Operating: 8,000 hours/year

Leak Reduction Expected (cf/hour)	Payback (months)
415	6
217	12
114	24
75	36

Based on 10% interest rate
Mcf = thousand cubic feet

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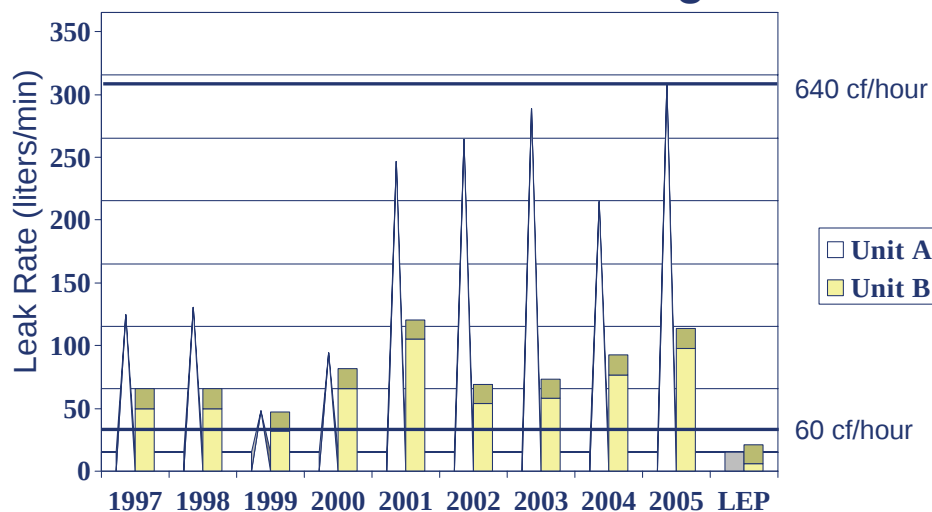
Industry Experience – Northern Natural Gas

- Monitored emission at two locations
 - Unit A leakage as high as 301 liters/min (640 cf/hour)
 - Unit B leakage as high as 105 liters/min (220 cf/hour)
- Installed Low Emission Packing (LEP)
 - Testing is still in progress
 - After 3 months, leak rate shows zero leakage increase

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Northern Natural Gas - Leakage Rates



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Northern Natural Gas Packing Leakage Economic Replacement Point

- 💧 Approximate packing replacement cost is \$3,000 per compressor rod (parts/labor)
- 💧 Assuming gas at \$7/Mcf:
 - 1 cubic foot/minute = 28.3 liters/minute
 - 💧 50 liters/minute/28.316 = 1.8 scf/minute
 - 💧 1.8 x 60 minutes/hour = 108 scf/hr
 - 💧 108 x 24/1000 = 2.6 Mcf/day
 - 💧 2.6 x 365 days = 950 Mcf/year
 - 💧 950 x \$7/Mcf = \$6,650 per year leakage
 - 💧 This replacement pays back in <6 months

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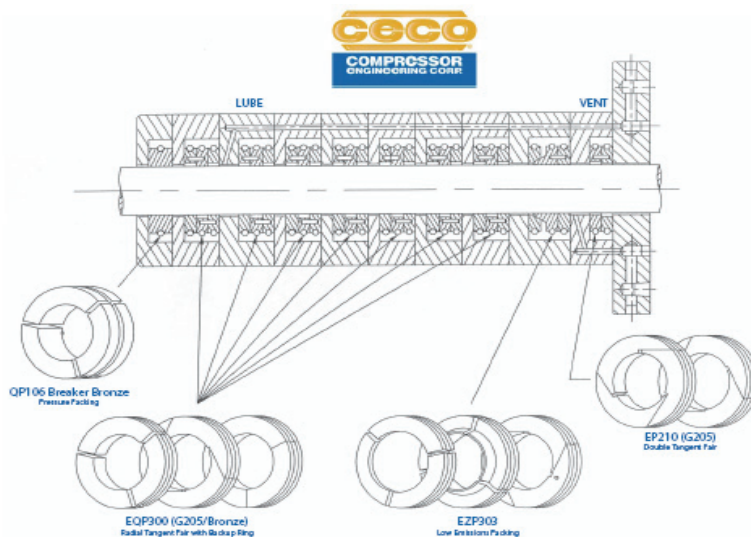


Low Emission Packing

- 💧 Low emission packing (LEP) overcomes low pressure to prevent leakage
- 💧 The side load eliminates clearance and maintains positive seal on cup face
- 💧 LEP is a static seal, not a dynamic seal. No pressure is required to activate the packing
- 💧 This design works in existing packing case with limited to no modifications required

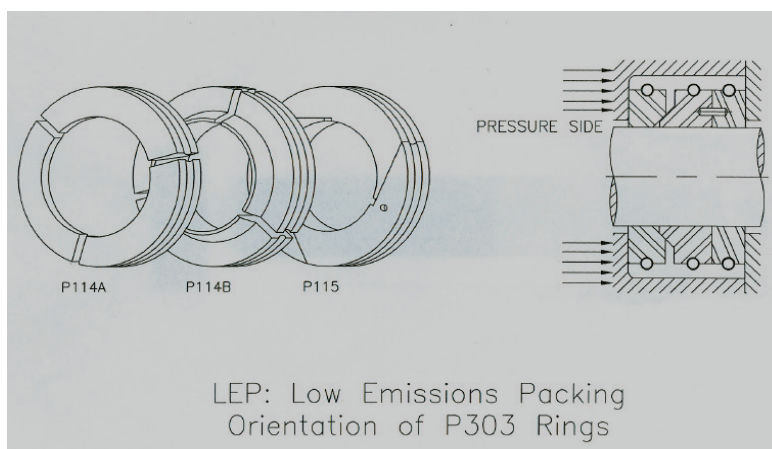
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LEP Packing Configuration



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Orientation in Cup



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Reasons to Use LEP

- ⚡ Upgrade is inexpensive
- ⚡ Significant reduction of greenhouse gas are major benefit
- ⚡ Refining, petrochemical and air separation plants have used this design for many years to minimize fugitive emissions
- ⚡ With gas at \$7/Mcf, packing case leakage should be identified and fixed.

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Discussion

- ⚡ Industry experience applying these technologies and practices
- ⚡ Limitations on application of these technologies and practices
- ⚡ Actual costs and benefits

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