

Reciprocating Compressor Rod Packing



Lessons Learned from the
Natural Gas STAR Program

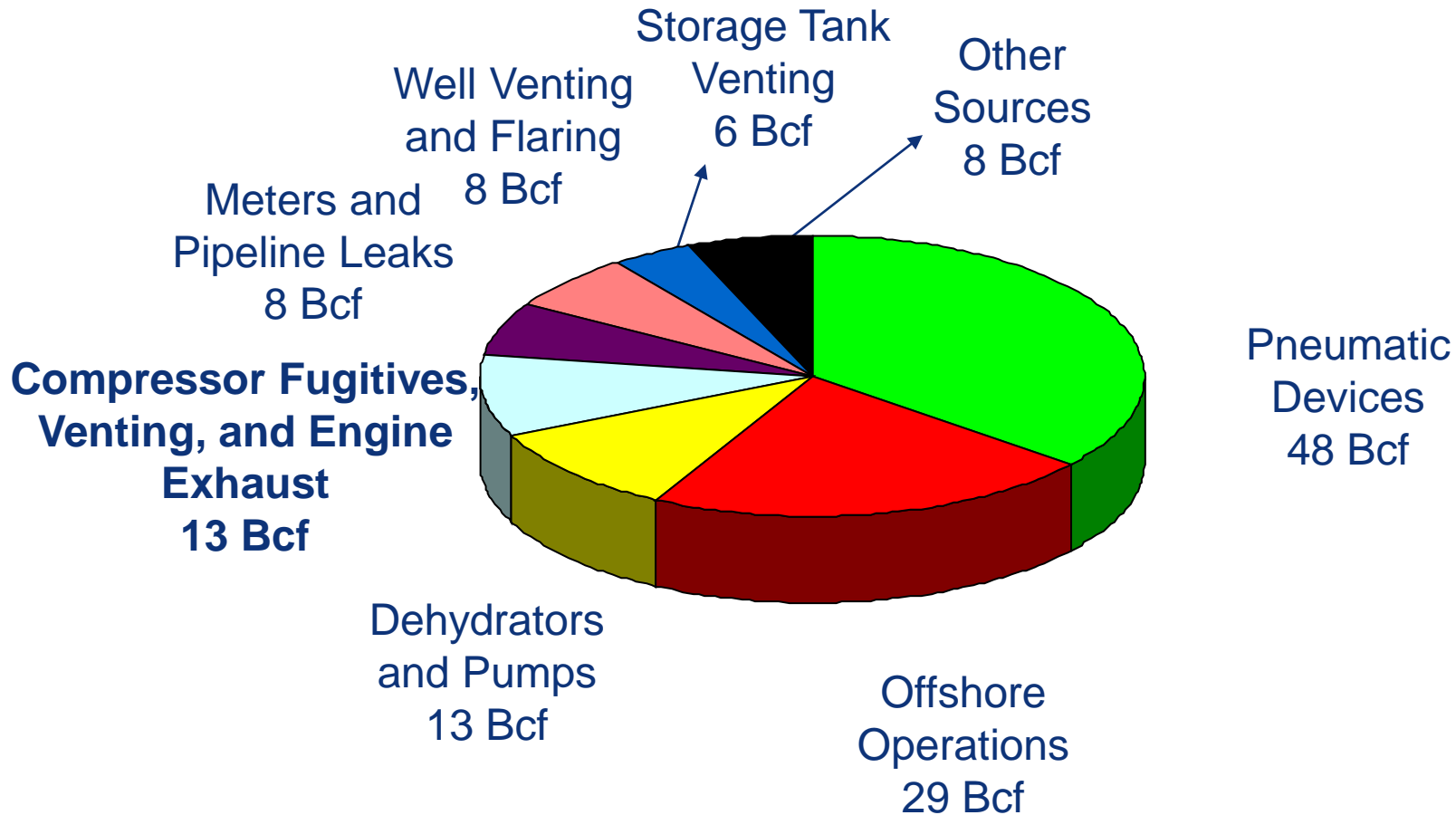
Chevron Corporation,
New Mexico Oil and Gas Association,
Texas Oil and Gas Association

Technology Transfer Workshop
Midland, Texas
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epa.gov/gasstar

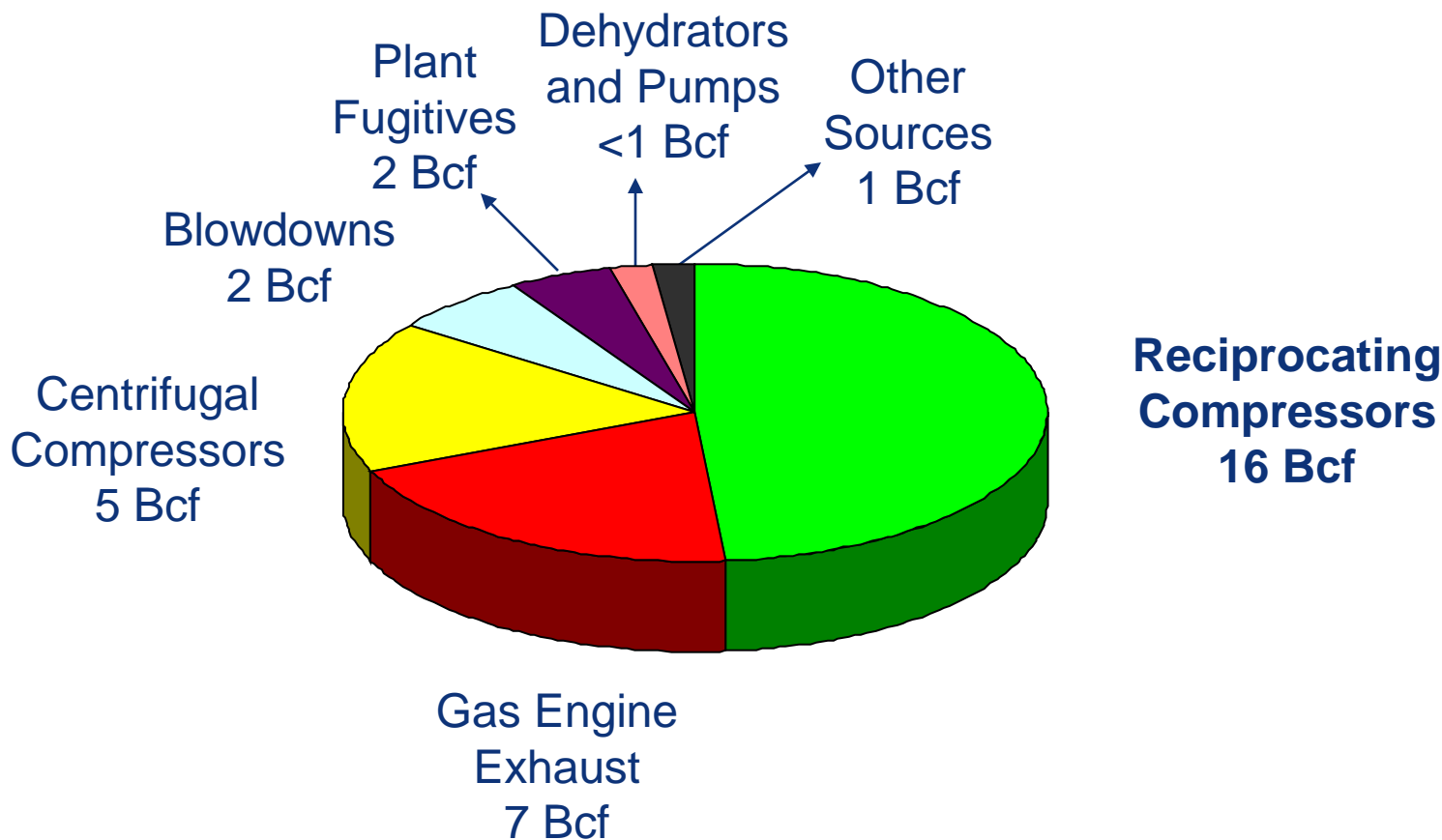
Industry Emissions: Production, Gathering, and Boosting



Source: EPA. *Inventory of U.S. Greenhouse Gas Emissions and Sinks 1990 – 2006*. April, 2008. Available on the web at: epa.gov/climatechange/emissions/usinventoryreport.html

Note: Natural Gas STAR reductions from gathering and boosting operations are reflected in the production sector.

2006 Processing Sector Methane Emissions



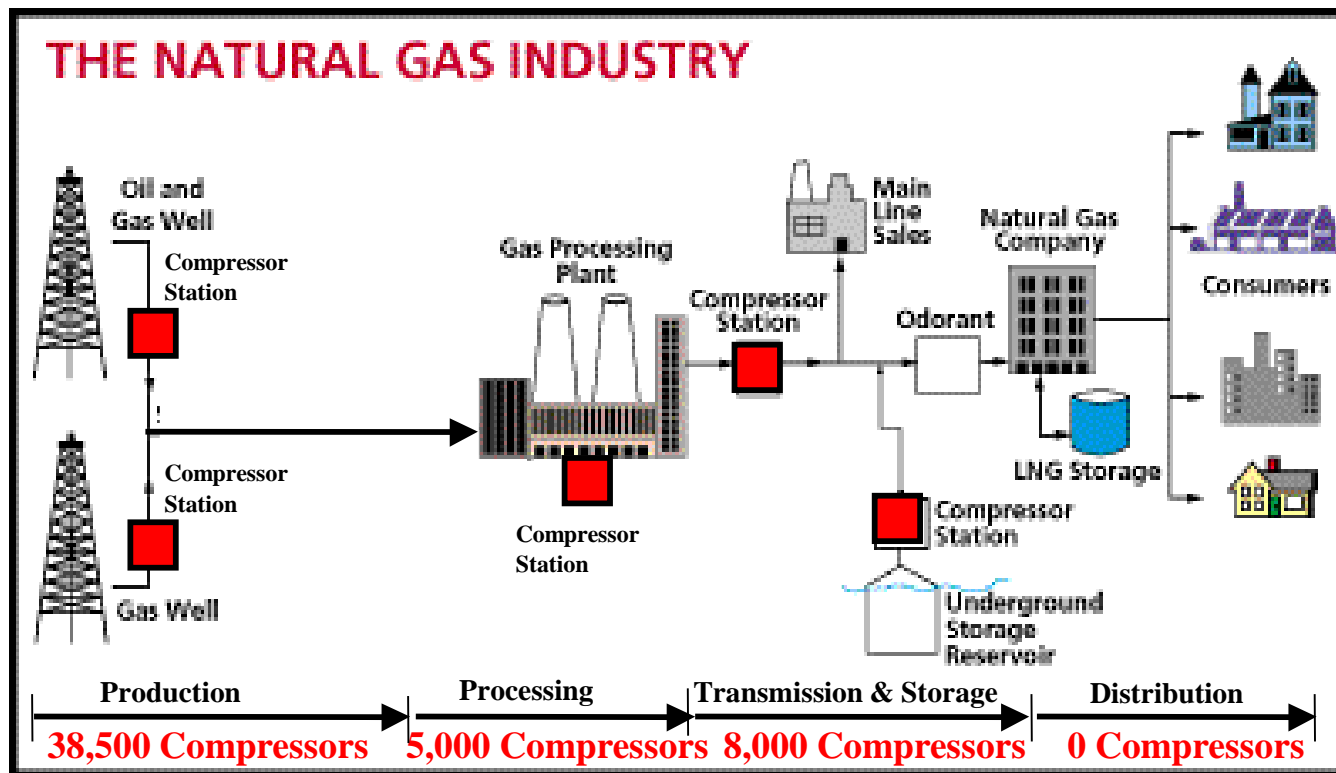
EPA. *Inventory of U.S. Greenhouse Gas Emissions and Sinks 1990 – 2006*. April, 2008. Available on the web at: epa.gov/climatechange/emissions/usinventoryreport.html

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Compressor Methane Emissions

What is the problem?

- Methane emissions from the ~51,500 compressors in the natural gas industry account for 89 Bcf/year or about 24% of all methane emissions from the natural gas industry



Methane Savings from Compressors: Agenda

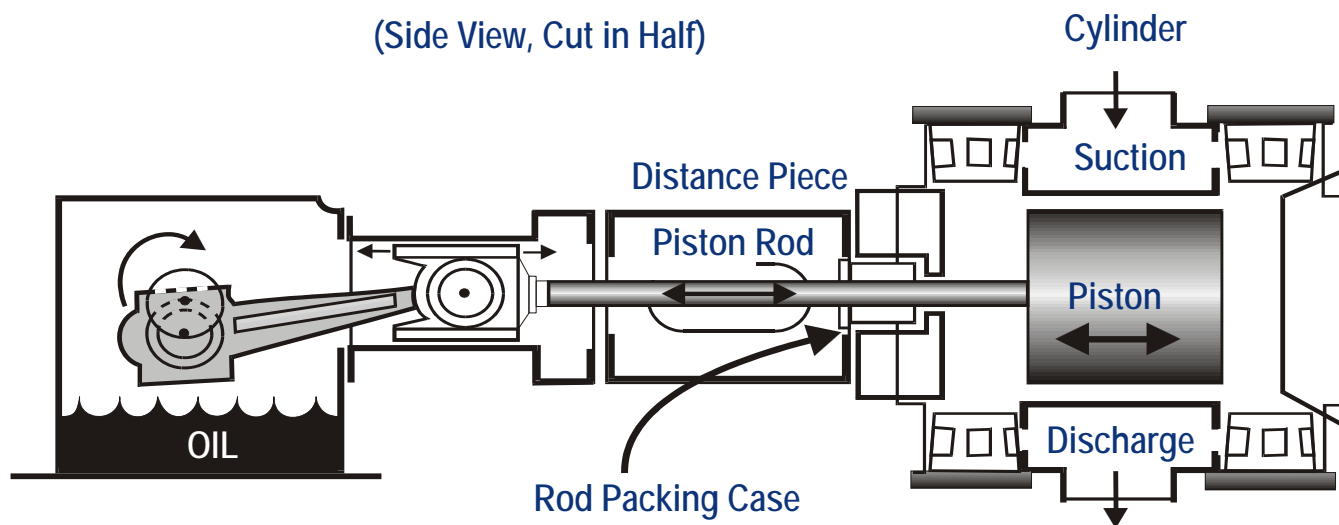
🔥 Reciprocating Compressors

- 🔥 Methane Losses
- 🔥 Methane Savings
- 🔥 Industry Experience

🔥 Discussion

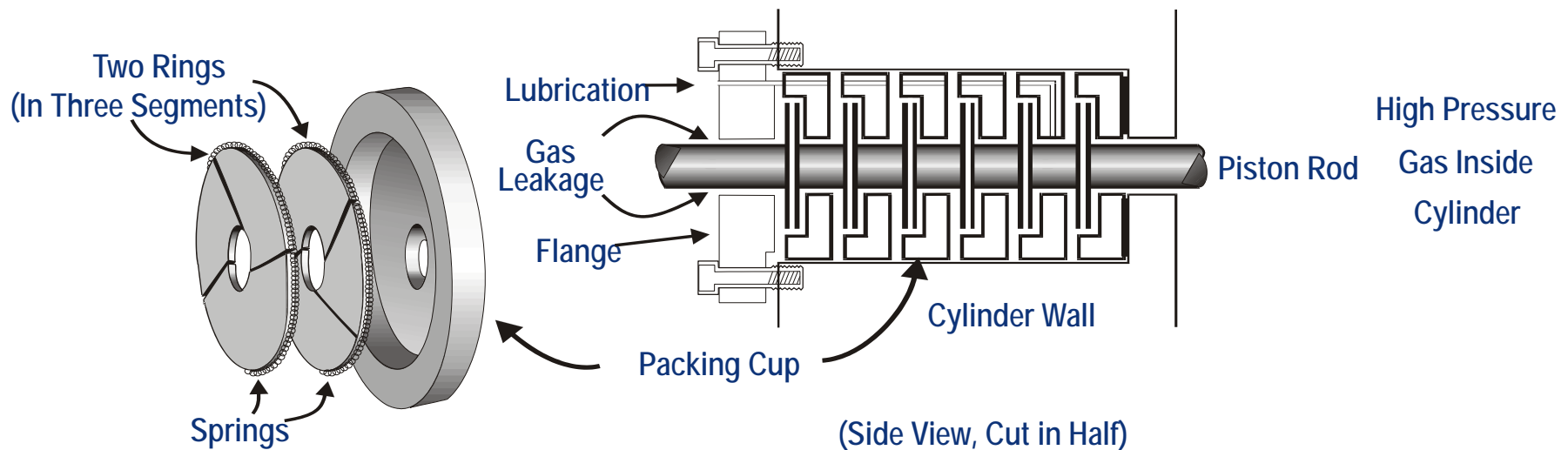
Methane Losses from Reciprocating Compressors

- 🔥 Reciprocating compressor rod packing leaks some gas by design
 - 🔥 Newly installed packing may leak 60 cubic feet per hour (cf/hour)
 - 🔥 Worn packing has been reported to leak up to 900 cf/hour



Reciprocating Compressor Rod Packing

- 🔥 A series of flexible rings fit around the shaft to prevent leakage
- 🔥 Leakage may still occur through nose gasket, between packing cups, around the rings, and between rings and shaft



Impediments to Proper Sealing

Ways packing case can leak

- 🔥 Nose gasket (no crush)
- 🔥 Packing to rod (surface finish)
- 🔥 Packing to cup (lapped surface)
- 🔥 Packing to packing (dirt/lube)
- 🔥 Cup to cup (out of tolerance)

What makes packing leak?

- 🔥 Dirt or foreign matter (trash)
- 🔥 Worn rod (.0015"/per inch dia.)
- 🔥 Insufficient/too much lubrication
- 🔥 Packing cup out of tolerance (≤ 0.002 ")
- 🔥 Improper break-in on startup
- 🔥 Liquids (dilutes oil)
- 🔥 Incorrect packing installed (backward or wrong type/style)

Methane Losses from Rod Packing

Emission from Running Compressor	99	cf/hour-packing
Emission from Idle/Pressurized Compressor	145	cf/hour-packing
Leakage from Idle Compressor Packing Cup	79	cf/hour-packing
Leakage from Idle Compressor Distance Piece	34	cf/hour-packing

Leakage from Rod Packing on Running Compressors				
Packing Type	Bronze	Bronze/Steel	Bronze/Teflon	Teflon
Leak Rate (cf/hour)	70	63	150	24

Leakage from Rod Packing on Idle/Pressurized Compressors				
Packing Type	Bronze	Bronze/Steel	Bronze/Teflon	Teflon
Leak Rate (cf/hour)	70	N/A	147	22

PRCI/ GRI/ EPA. *Cost Effective Leak Mitigation at Natural Gas Transmission Compressor Stations*

Steps to Determine Economic Replacement

- 🔥 Measure rod packing leakage
 - 🔥 When new packing installed – after worn-in
 - 🔥 Periodically afterwards
- 🔥 Determine cost of packing replacement
- 🔥 Calculate economic leak reduction
- 🔥 Replace packing when leak reduction expected will pay back cost

Calculate Economic Leak Reduction

- 🔥 Determine economic replacement threshold
 - 🔥 Partners can determine economic threshold for all replacements
 - 🔥 This is a capital recovery economic calculation

$$\text{Economic Replacement Threshold (cf/hour)} = \frac{CR * DF * 1,000}{(H * GP)}$$

Where:

CR = Cost of replacement (\$)

DF = Discount factor at interest i =

$$DF = \frac{i(1+i)^n}{(1+i)^n - 1}$$

H = Hours of compressor operation per year

GP = Gas price (\$/thousand cubic feet)

Economic Replacement Threshold

🔥 Example: Payback calculations for new rings and rod replacement

$$\begin{aligned} \text{CR} &= \$1,620 \text{ for rings} + \$9,450 \text{ for rod} \\ &= \$11,070 \end{aligned}$$

$$H = 8,000 \text{ hours per year}$$

$$\text{GP} = \$7/\text{Mcf}$$

DF @ $i = 10\%$ and $n = 1$ year

$$\text{DF} = \frac{0.1(1+0.1)^1}{(1+0.1)^1 - 1} = \frac{0.1(1.1)}{1.1-1} = \frac{0.11}{0.1} = 1.1$$

DF @ $i = 10\%$ and $n = 2$ years

$$\text{DF} = \frac{0.1(1+0.1)^2}{(1+0.1)^2 - 1} = \frac{0.1(1.21)}{1.21-1} = \frac{0.121}{0.21} = 0.576$$

One year payback

$$\begin{aligned} ER &= \frac{\$11,070 \times 1.1 \times 1,000}{(8,000 \times \$7)} \\ &= 217 \text{ scf per hour} \end{aligned}$$

Is Rod Packing Replacement Profitable?

- Replace packing when leak reduction expected will pay back cost
 - “leak reduction expected” is the difference between current leak rate and leak rate with new rings

Rings Only

Rings: \$1,620
 Rod: \$0
 Gas: \$7/Mcf
 Operating: 8,000 hours/year

Leak Reduction Expected (cf/hour)	Payback (months)
55	7
29	12
20	18
16	22

Rod and Rings

Rings: \$1,620
 Rod: \$9,450
 Gas: \$7/Mcf
 Operating: 8,000 hours/year

Leak Reduction Expected (cf/hour)	Payback (months)
376	7
197	13
137	18
108	22

Based on 10% interest rate
 Mcf = thousand cubic feet

Industry Experience – Northern Natural Gas

- 🔥 Monitored emission at two locations
 - 🔥 Unit A leakage as high as 301 liters/min (640 cf/hour)
 - 🔥 Unit B leakage as high as 105 liters/min (220 cf/hour)
- 🔥 Installed Low Emission Packing (LEP)
 - 🔥 Testing is still in progress
 - 🔥 After 3 months, leak rate shows zero leakage increase

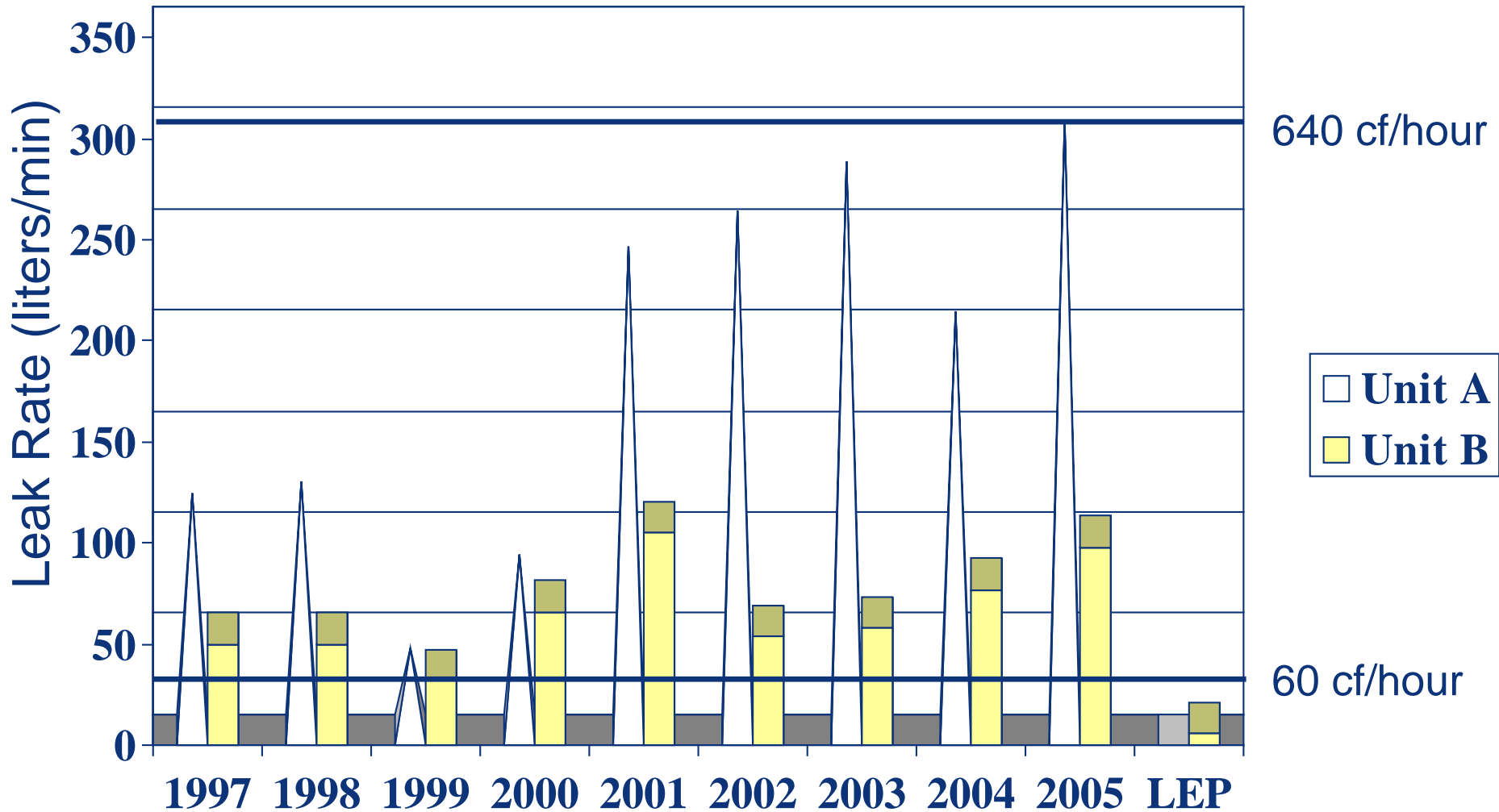
Industry Experience – Occidental

- Occidental upgraded compressor rod packing at its Elk Hills facility in southern California
- Achieved reductions of 400 Mcf/day/compressor
- Savings 145 MMcf/yr
- Payback in under 3 years



Source: Occidental

Northern Natural Gas - Leakage Rates



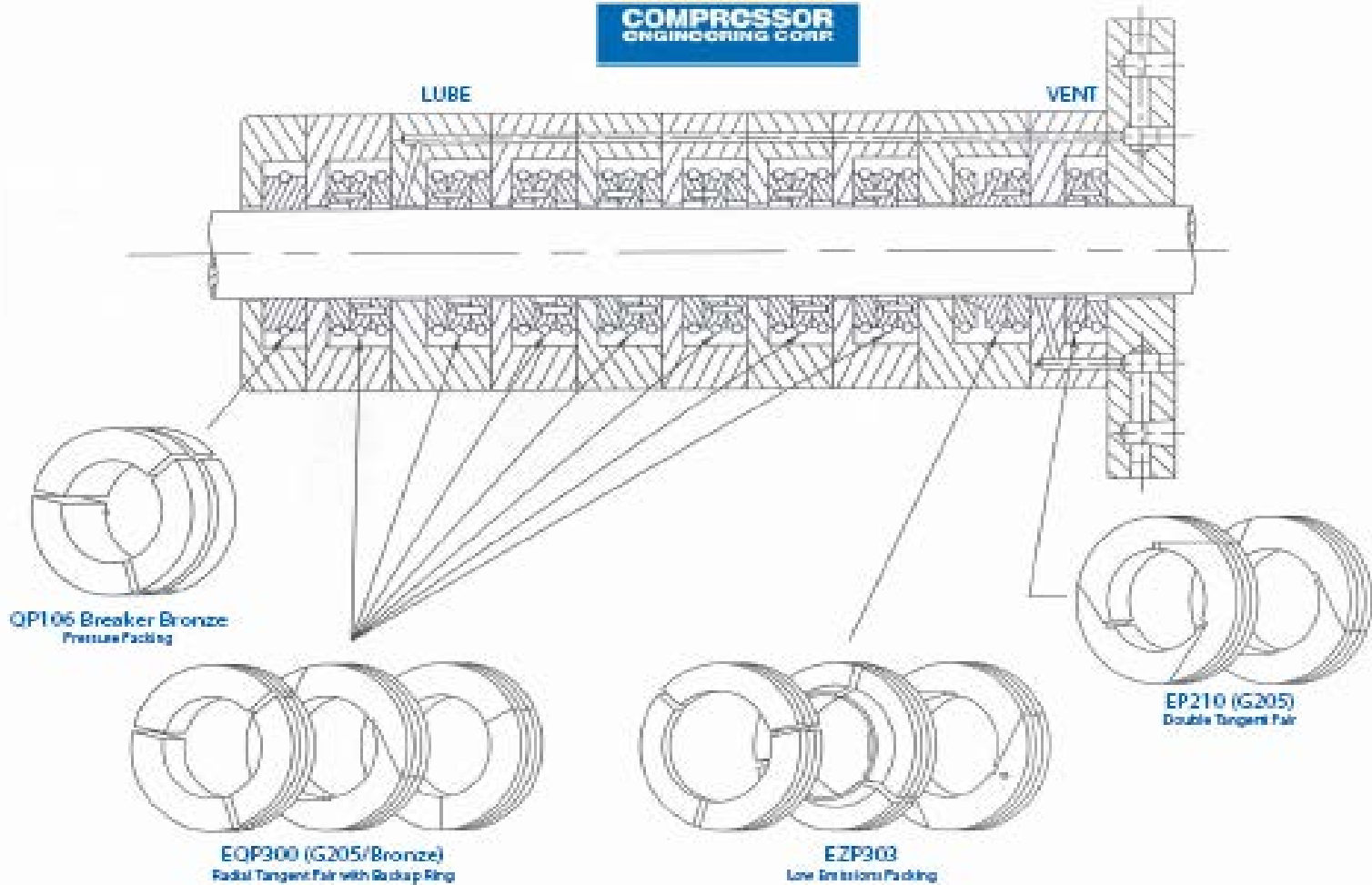
Northern Natural Gas Packing Leakage Economic Replacement Point

- 💧 Approximate packing replacement cost is \$3,000 per compressor rod (parts/labor)
- 💧 Assuming gas at \$7/Mcf:
 - 1 cubic foot/minute = 28.3 liters/minute
 - 💧 $50 \text{ liters/minute} / 28.316 = 1.8 \text{ scf/minute}$
 - 💧 $1.8 \times 60 \text{ minutes/hour} = 108 \text{ scf/hr}$
 - 💧 $108 \times 24 / 1000 = 2.6 \text{ Mcf/day}$
 - 💧 $2.6 \times 365 \text{ days} = 950 \text{ Mcf/year}$
 - 💧 $950 \times \$7/\text{Mcf} = \$6,650 \text{ per year leakage}$
 - 💧 This replacement pays back in <6 months

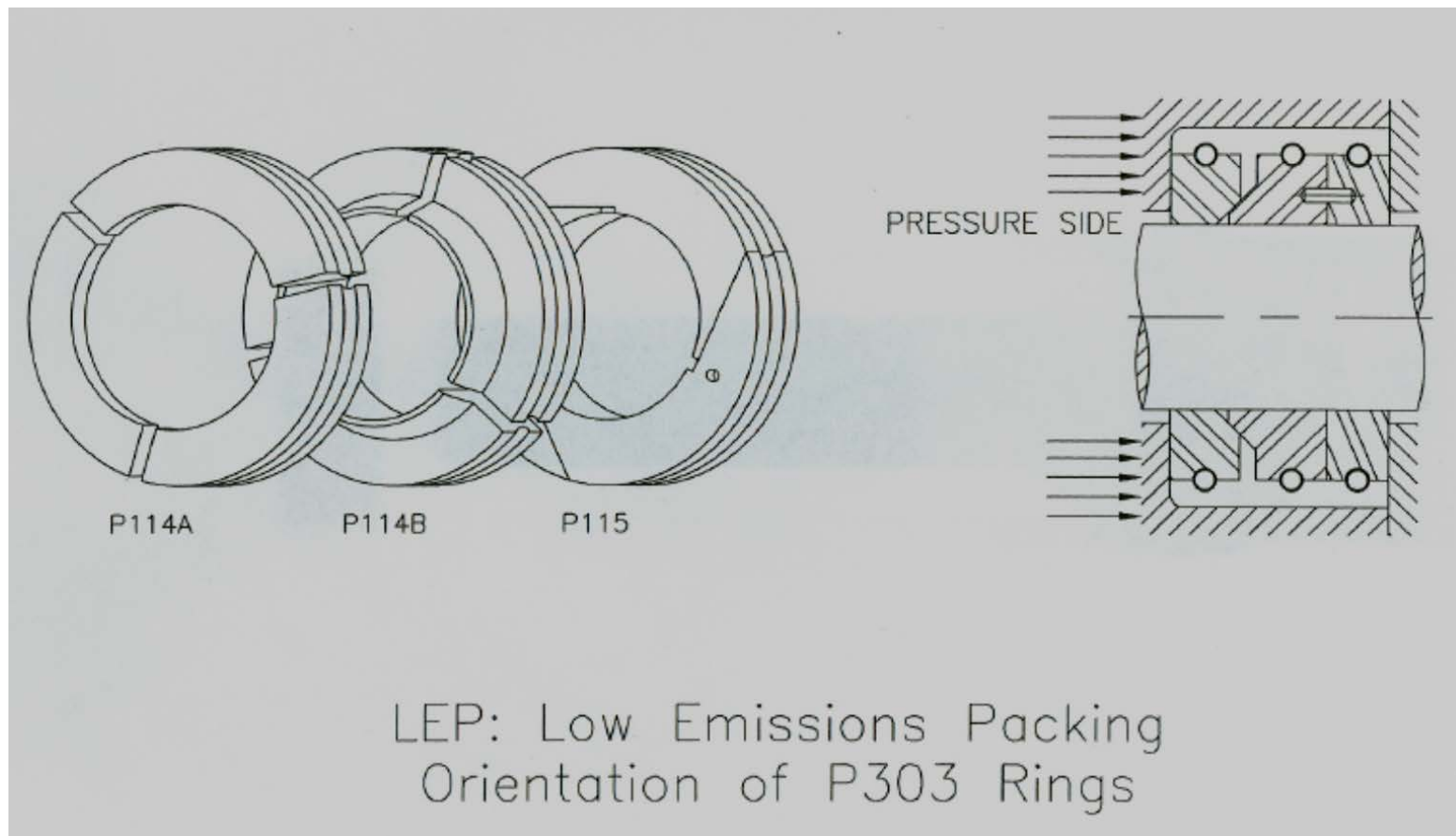
Low Emission Packing

- 🔥 Low emission packing (LEP) overcomes low pressure to prevent leakage
- 🔥 The side load eliminates clearance and maintains positive seal on cup face
- 🔥 LEP is a static seal, not a dynamic seal. No pressure is required to activate the packing
- 🔥 This design works in existing packing case with limited to no modifications required

LEP Packing Configuration



Orientation in Cup



LEP: Low Emissions Packing
Orientation of P303 Rings

Reasons to Use LEP

- 🔥 Upgrade is inexpensive
- 🔥 Significant reduction of greenhouse gas are major benefit
- 🔥 Refining, petrochemical and air separation plants have used this design for many years to minimize fugitive emissions
- 🔥 With gas at \$7/Mcf, packing case leakage should be identified and fixed.

Discussion

- 🔥 Industry experience applying these technologies and practices
- 🔥 Limitations on application of these technologies and practices
- 🔥 Actual costs and benefits