

Partner Reported Opportunities for Small and Medium Sized Producers

Lessons Learned
from Natural Gas STAR



Small and Medium Sized Producer Technology Transfer Workshop

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EPA's Natural Gas STAR Program

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Producer PROs: Agenda

- Introduction to Partner Reported Opportunities (PROs) and Lessons Learned
- Selected PRO Overviews
- DI&M
- DI&M Industry Experience
- Discussion Questions



EPA POLLUTION PREVENTER

Reducing Emissions, Increasing Efficiency, Maximizing Profits

Why Are Partner Reported Opportunities Important?

- Partner Annual Reports document Program accomplishments
 - ◆ **Best Management Practices (BMPs): the consensus best practices**
 - ◆ **PROs: Partner Reported Opportunities**
- Simple vehicles for sharing successes and continuing Program's future
 - ◆ **Lessons Learned: expansion on the most advantageous BMPs and PROs**
 - ◆ **PRO Fact Sheets**
 - ◆ **Technology Transfer Workshops**
 - ◆ **Posted on www.epa.gov/gasstar**



Why Are Partner Reported Opportunities Important?

- Many production facilities have identified practical, cost effective reduction practices
- Production partners report saving 187 Bcf since 1990, 80% from PROs
 - ◆ Vapor recover units (VRUs) account for 30% of PRO emissions reductions
 - ◆ Plunger lift installations account for 16%
 - ◆ Flare installations account for 13%



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Production Best Management Practices

- ❑ BMP 1: Install and replace high-bleed pneumatics
- ❑ BMP 2: Install flash tank separators (FTS) on glycol dehydrators
- ❑ BMP 3: Partner Reported Opportunities



Lessons Learned

- 11 applicable to small and medium sized producers
 - ◆ 2 focused on operating practices
 - ◆ 9 focused on technology

- All 16 Lessons Learned studies on the EPA web site
 - ◆ www.epa.gov/gasstar/lessons.htm



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Technology Focused Lessons Learned for Small and Medium Producers

- ❑ Installing Vapor Recovery Units on Crude Oil Storage Tanks
- ❑ Optimize Glycol Circulation and Installation of Flash Tank Separators in Dehydrators
- ❑ Options for Reducing Methane Emissions from Pneumatic Devices in the Natural Gas Industry
- ❑ Convert Gas Pneumatic Controls to Instrument Air
- ❑ Reducing Methane Emissions from Compressor Rod Packing Systems
- ❑ Replacing Gas-Assisted Glycol Pumps with Electric Pumps
- ❑ Installing Plunger Lift Systems in Gas Wells
- ❑ Composite Wrap for Non-Leaking Pipeline Defects
- ❑ Replace Glycol Dehydrators with Desiccant Dehydrators



Gas STAR PRO Fact Sheets

- 16 applicable to small and medium sized producers

- ◆ 38 PROs applicable to production

- 12 focused on operating practices
- 26 focused on technology

- PRO Fact Sheets from Annual Reports 1994-2002

- ◆ Total 56 posted PROs at epa.gov/gasstar/pro/index.htm



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PROs

- ❑ Replace Gas Starters with Air
- ❑ Replace Ignition – Reduce False Starts
- ❑ Install Electric Starters
- ❑ Rerouting of Glycol Skimmer Gas
- ❑ Convert Gas-Driven Chemical Pumps to Instrument Air
- ❑ Pipe Glycol Dehydrator to Vapor Recovery Unit
- ❑ Convert Pneumatics to Mechanical Controls
- ❑ Install Electronic Flare Ignition Devices
- ❑ Use ClockSpring® Repair



More PROs

- ❑ Inspect Flowlines Annually
- ❑ Install BASO® Valves
- ❑ Use Ultrasound to Identify Leaks
- ❑ Connect casing to VRU
- ❑ Lower Heater-Treater Temperature
- ❑ Begin DI&M at Remote Facilities
- ❑ Install Compressors to Capture Casinghead Gas
- ❑ Install Pumpjacks on Low Water Production Gas Wells
- ❑ Replace Glycol Dehydration Units with Methanol Injection



Examples of PROs Applicable to Small/Medium Producers

- PROs enabled by instrument air
 - ◆ Replace Gas Starters with Instrument Air
 - ◆ Convert Gas-Driven Chemical Pumps to Instrument Air
- PROs enabled by glycol dehydrators
 - ◆ Reroute Glycol Skimmer Gas
 - ◆ Reroute Glycol Dehydrator to Vapor Recovery
- PROs enabled by electric power
 - ◆ Install Electric Starters
 - ◆ Install Compressors to Capture Casinghead Gas



Replace Gas Starters with Air

- What is the Problem?
 - ◆ Pressurized gas used to start engines is exhausted to atmosphere
- Partner Solution
 - ◆ Replace gas with compressed air
- Methane Savings
 - ◆ Based on one 3,000 HP reciprocating compressor with 10 start-ups per year
- Applicability
 - ◆ Natural gas pneumatic starter motors
 - ◆ Needs electric power to run air compressor

Methane Savings

1,356 Mcf/yr

Project Economics

Project Cost	< \$1,000
Annual O&M Costs	\$100 - \$1,000
Payback	< 1 yr



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Convert Gas-Driven Chemical Pumps to Instrument Air

❑ What is the Problem?

- ◆ Chemical pumps powered by pressurized natural gas vent methane

❑ Partner Solution

- ◆ Replace natural gas with instrument air to power pumps

❑ Methane Savings

- ◆ Based on glycol unit pump

❑ Applicability

- ◆ Use excess capacity of existing instrument air
- ◆ Needs electric power to run air compressor

Methane Savings

2,500 Mcf/yr

Project Economics

Project Cost	\$1,000 - \$10,000
Annual O&M Costs	\$100 - \$1,000
Payback	< 1 yr



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PROs Enabled by Glycol Dehydrators

Dehydrators present an excellent place to reduce emissions

□ How much methane is emitted?

◆ A 1 MMcf/d dehydrator with vent condenser, no flash tank separator and gas pump can produce 460 Mcf/yr of losses

□ How can these losses be reduced?

◆ BMP 2: install flash tank separator

◆ Many PROs



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Reroute Glycol Skimmer Gas

□ What is the Problem?

- ◆ Gas from condensate separator vented to atmosphere

□ Partner Solution

- ◆ Reroute condensate separator gas for fuel use

□ Methane Savings

- ◆ Based on 20 MMcf/d dehydrator w/o FTS, circulating 300 gph

□ Applicability

- ◆ All dehydrators with vent condensers
- ◆ Condensate separator must operate at higher pressure than gas destination

Methane Savings

7,600 Mcf/yr

Project Economics

Project Cost	<\$1,000
Annual O&M Costs	\$100 - \$1,000
Payback	< 1 yr



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Pipe Glycol Dehydrator to Vapor Recovery

□ What is the Problem?

- ◆ High pressure gas used to drive gas pumps in dehydrators are vented

□ Partner Solution

- ◆ Reroute gas vent to VRU

□ Methane Savings

- ◆ Based on a 10 MMcf/d gas dehydration unit with FTS and gas assist pump

□ Applicability

- ◆ Sufficient spare capacity in existing VRU
- ◆ Capacity of VRU outlet

Methane Savings

3,300 Mcf/yr

Project Economics

Project Cost	\$1,000 - \$10,000
Annual O&M Costs	> \$1,000
Payback	< 1 yr



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Install Electric Starters

□ What is the Problem?

- ◆ Pressurized gas used to start engines is exhausted to atmosphere

□ Partner Solution

- ◆ Replacing starter expansion turbine with electric motor starter

□ Methane Savings

- ◆ Based on one engine starter, ten start-ups per year and methane leakage through gas shut-off valve

□ Applicability

- ◆ All sectors of the gas industry
- ◆ Requires access to power supply

Methane Savings

1,350 Mcf/yr

Project Economics

Project Cost	\$1,000 - \$10,000
Annual O&M Costs	< \$100
Payback	1- 3 yrs



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Install Compressors to Capture Casinghead Gas

□ What is the Problem?

- ◆ Casinghead gas vented to atmosphere

□ Partner Solution

- ◆ Install compressor to capture casinghead gas and pump to sales line

□ Methane Savings

- ◆ Based on 180 Mcf/d associated gas containing 50% methane, 30 HP electric rotary compressor, 100 psig sales line

□ Applicability

- ◆ Oil wells that produce significant volume of casinghead gas
- ◆ Access to electricity for compressor

Methane Savings

32,850 Mcf/yr

Project Economics

Project Cost	> \$10,000
Annual O&M Costs	> \$1,000
Payback	<1 yrs



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Directed Inspection & Maintenance



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What is the Problem?

- ❑ Gas leaks are invisible, unregulated and go unnoticed
- ❑ STAR Partners find that valves, connectors, compressor seals and open-ended lines (OELs) are major sources
 - ◆ 27 Bcf methane emitted per year by reciprocating compressor seals and OELs
 - ◆ OELs contribute half these emissions
- ❑ Fugitive methane emissions depend on operating practices, equipment age and maintenance



How Can These Losses Be Reduced?

- Implementing a Directed Inspection and Maintenance (DI&M) Program



Source: CLEARSTONE ENGINEERING LTD



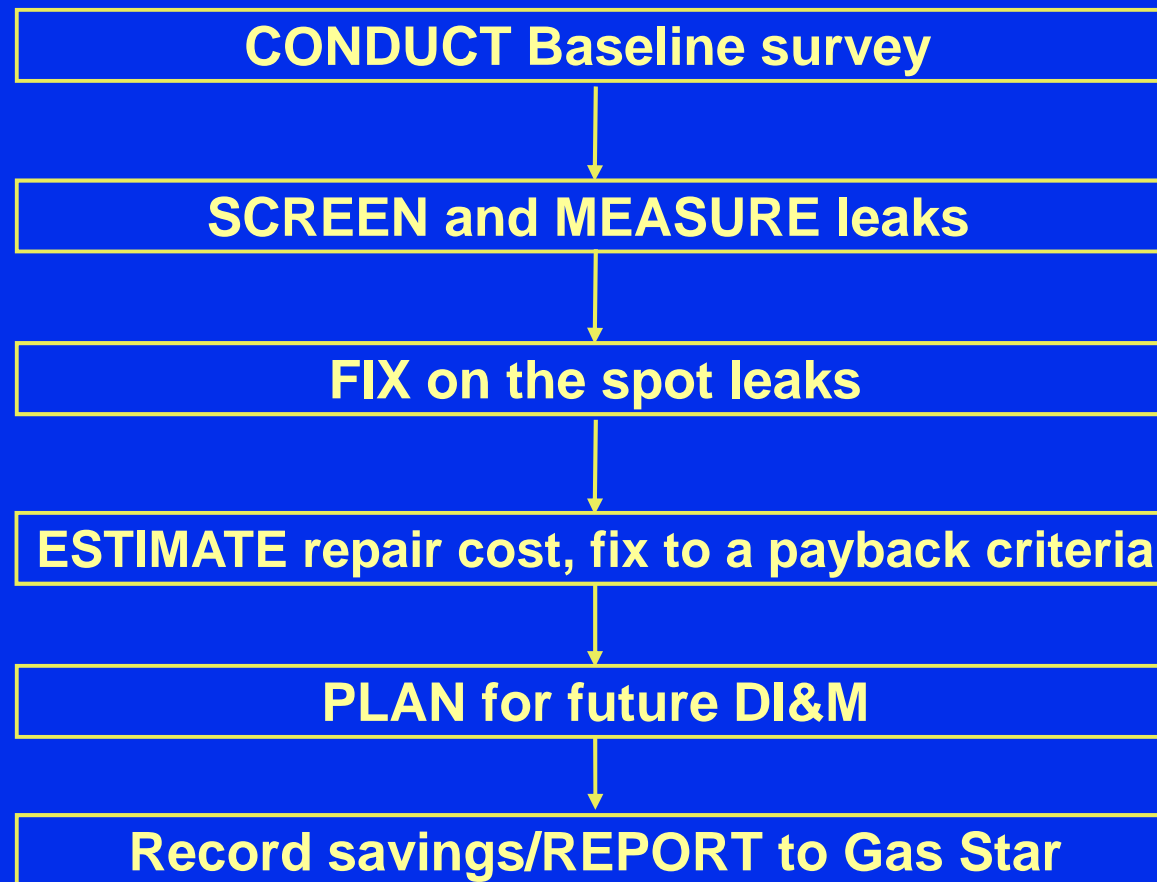
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What is a DI&M Program?

- Implementing a Directed Inspection and Maintenance Program
 - ◆ Voluntary program to identify and fix leaks that are cost-effective to repair
 - ◆ Outside of mandatory Leak Detection and Repair (LDAR)
 - ◆ Survey cost will pay out in the first year
 - ◆ Provides valuable data on leakers



How Do You Implement A DI&M Program?



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One of the New PROs

- ❑ Begin Directed Inspection and Maintenance at Remote Facilities
 - ◆ **SAVES: 362 Mcf/yr**
 - ◆ **PAYOUT: < 1 yr**
- ❑ Enables several PROs
 - ◆ **Inspect and Repair Compressor Station Blowdown Valve**
 - ◆ **Use Ultrasound to Identify Leaks**
 - ◆ **Test and Repair Pressure Safety Valves**



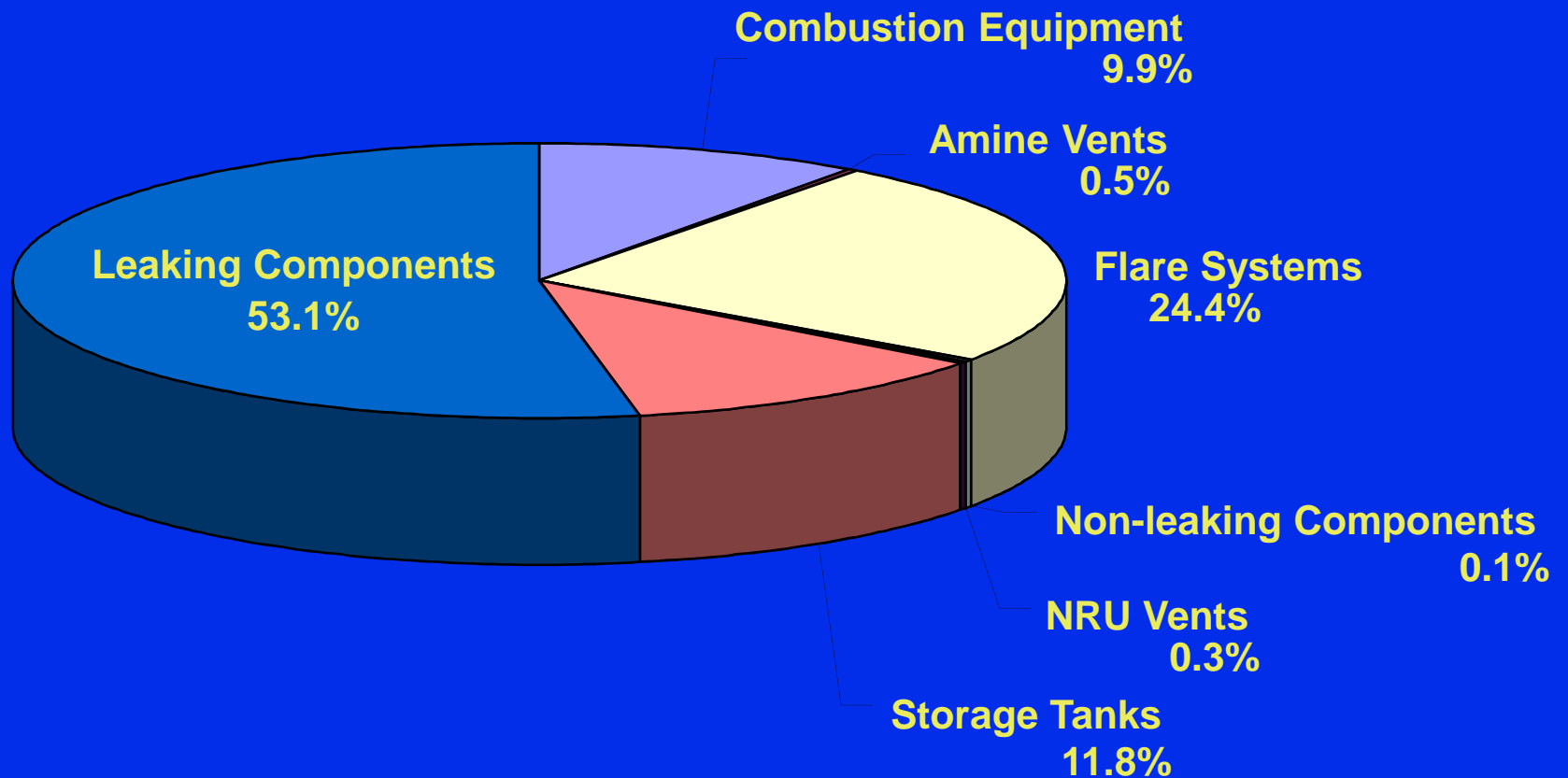
Bubble test on leaking valve

Source: CLEARSTONE ENGINEERING LTD



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Natural Gas Losses by Source

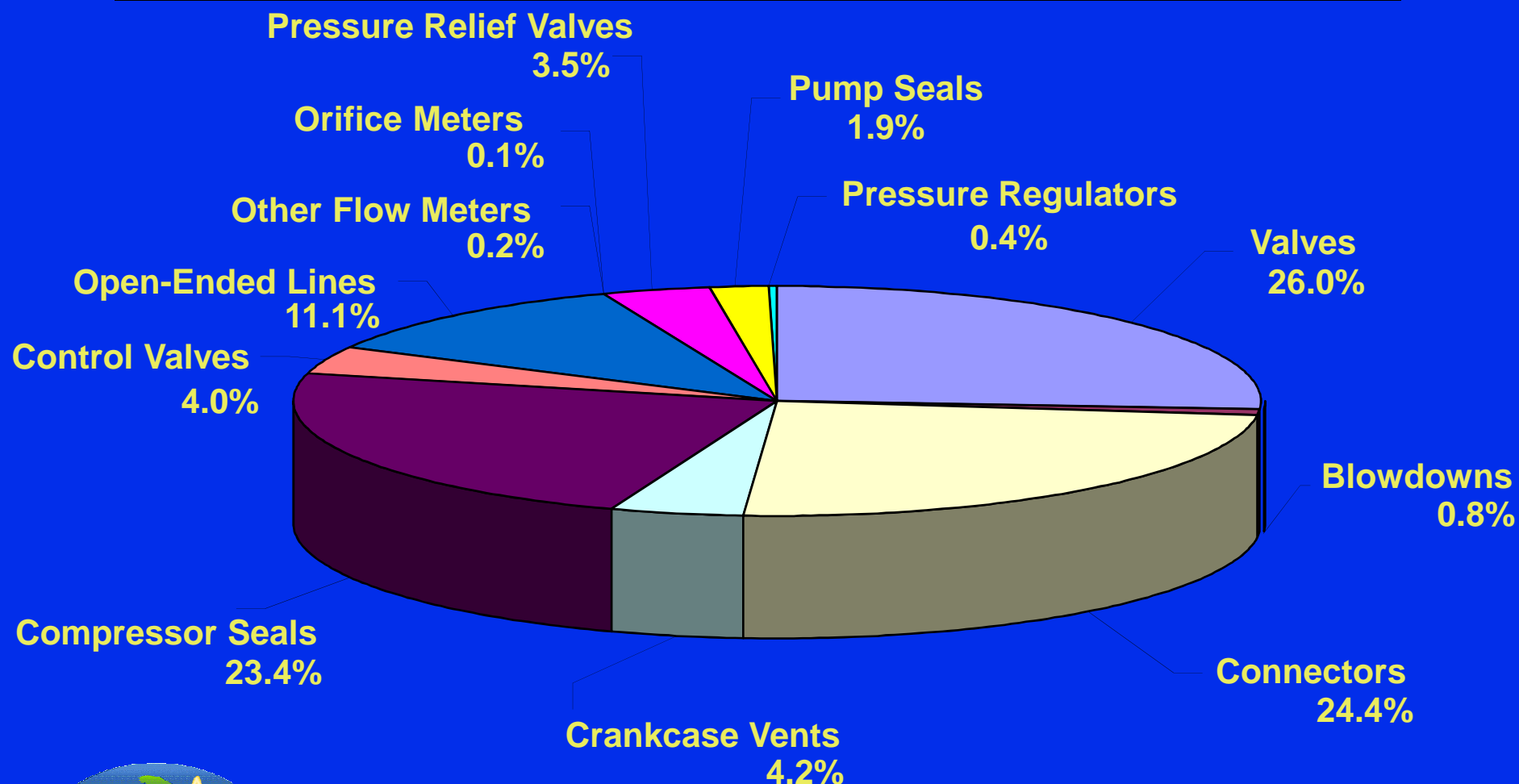


Source: Clearstone Engineering, 2002



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Natural Gas Losses by Equipment Type



Source: Clearstone Engineering, 2002

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How Much Methane is Emitted?

Methane Emissions from Leaking Components at Gas Plants			
Component Type	% of Total Methane Emissions	% Leaks	Estimated Average Methane Emissions per Leaking Component (Mcf/Year)
Valves (Block & Control)	26.0%	7.4%	66
Connectors	24.4%	1.2%	80
Compressor Seals	23.4%	8.1%	372
Open-Ended Lines	11.1%	10.0%	186
Pressure Relief Valves	3.5%	2.9%	844

Source: Clearstone Engineering, 2002, Identification and Evaluation of Opportunities to Reduce Methane Losses at Four Gas Processing Plants. Report of results from field study of 4 gas processing plants in WY and TX to evaluate opportunities to economically reduce methane emissions.



How Much Methane is Emitted?

Summary of Natural Gas Losses from the Top Ten Leakers¹.

Plant No.	Gas Losses From Top 10 Leakers (Mcf/d)	Gas Losses From All Equipment Leakers (Mcf/d)	Contribution By Top 10 Leakers (%)	Contribution By Total Leakers (%)
1	43.8	122.5	35.7	1.78
2	133.4	206.5	64.6	2.32
3	224.1	352.5	63.6	1.66
4	76.5	211.3	36.2	1.75
Combined	477.8	892.84	53.5	1.85

¹Excluding leakage into flare system



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Screening and Measurement

Summary of Screening and Measurement Techniques		
Instrument/ Technique	Effectiveness	Approximate Capital Cost
Soap Solution	★ ★	\$
Electronic Gas Detectors	★	\$\$
Acoustic Detection/ Ultrasound Detection	★ ★	\$\$\$
TVA (FID)	★	\$\$\$
Bagging	★	\$\$\$
High Volume Sampler	★ ★ ★	\$\$\$
Rotameter	★ ★	\$\$
Source: EPA's Lessons Learned Study		



Cost-Effective Repairs

Repair the Cost Effective Components			
Component	Value of Lost gas ¹ (\$)	Estimated Repair cost (\$)	Payback (Months)
Plug Valve: Valve Body	12,641	200	0.2
Union: Fuel Gas Line	12,155	100	0.1
Threaded Connection	10,446	10	0.0
Distance Piece: Rod Packing	7,649	2,000	3.1
Open-Ended Line	6,959	60	0.1
Compressor Seals	5,783	2,000	4.2
Gate Valve	4,729	60	0.2
Source: Hydrocarbon Processing, May 2002 ¹ Based on \$3/Mcf gas price			



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DI&M - Partner Experience

- **Partner A:** leaking cylinder head tightened, which reduced methane emissions from almost 64,000 Mcf/yr to 3,300 Mcf/yr
 - ◆ Repair required 9 man-hours labor and annualized gas savings were approximately 60,700 Mcf/yr. At \$3/Mcf, the estimated value of gas saved was \$182,100/yr
- **Partner B:** one-inch pressure relief valve emitted almost 36,774 Mcf/yr
 - ◆ Five man-hours labor and \$125 materials eliminated leak. The annualized value of gas saved was more than \$110,300 at \$3/Mcf



DI&M - Partner Experience

- Partner C: blowdown valve leaked almost 14,500 Mcf/yr
 - ◆ Rather than replace expensive valve, the Partner spent just \$720 on labor and materials to reduce emissions to ~100 Mcf/yr
 - ◆ Gas saved was approximately 14,400 Mcf/yr, worth \$43,200 at \$3/Mcf
- Partner D: tube fitting leaked 4,121 Mcf/yr
 - ◆ Very quick repair requiring only five minutes reduced leak rate to 10 Mcf/yr
 - ◆ Annualized value of gas saved was ~ \$12,300 at \$3/Mcf



Discussion Questions

- ❑ To what extent are you implementing these opportunities?
- ❑ Can you suggest other opportunities?
- ❑ How could these opportunities be improved upon or altered for use in your operation?
- ❑ What are the barriers (technological, economic, lack of information, regulatory, etc.) that are preventing you from implementing these practices?

