

Convert Gas Pneumatic Controls to Instrument Air

Lessons Learned
from Natural Gas STAR Partners



EPA's Natural Gas STAR Program,
Pioneer Natural Resources USA, Inc., and
The Gas Processors Association

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Air Pneumatic Devices

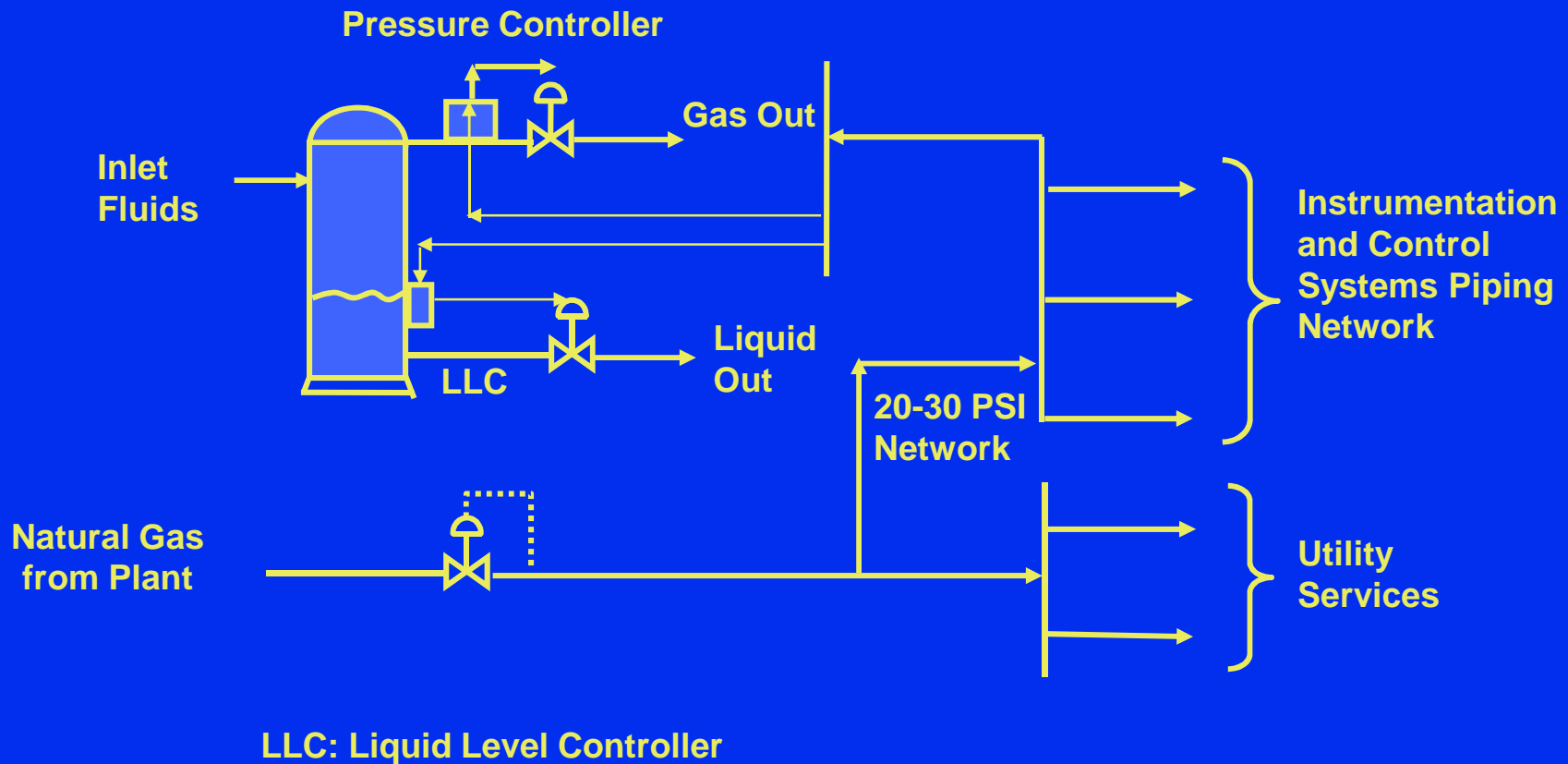
- ⌘ Methane Losses
- ⌘ Methane Recovery
- ⌘ Is Recovery Profitable?
- ⌘ Spreadsheet-based Analytical Tools
- ⌘ Industry Experience
- ⌘ Discussion Questions



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Natural Gas Pneumatic System



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Sources of Methane Losses

- ⌘ As part of normal operations, pneumatic devices release natural gas into the atmosphere
- ⌘ High-bleed devices bleed in excess of 6 scf per hour
 - ◆ Equates to >50 Mcf/ year
 - ◆ Typical high-bleed pneumatic devices bleed an average of 140 Mcf/year



Magnitude of Methane Losses

- ⌘ Major source of methane losses from the natural gas industry
- ⌘ Pneumatic devices are used throughout the natural gas industry
 - ◆ Over 13,000 in the processing sector
 - ◆ Estimated methane loss of 16 Bcf/year = \$48 million!



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Convert to Instrument Air devices

☞ Most applicable to:

- ◆ Large facility with high bleed pneumatic devices and has access to electricity

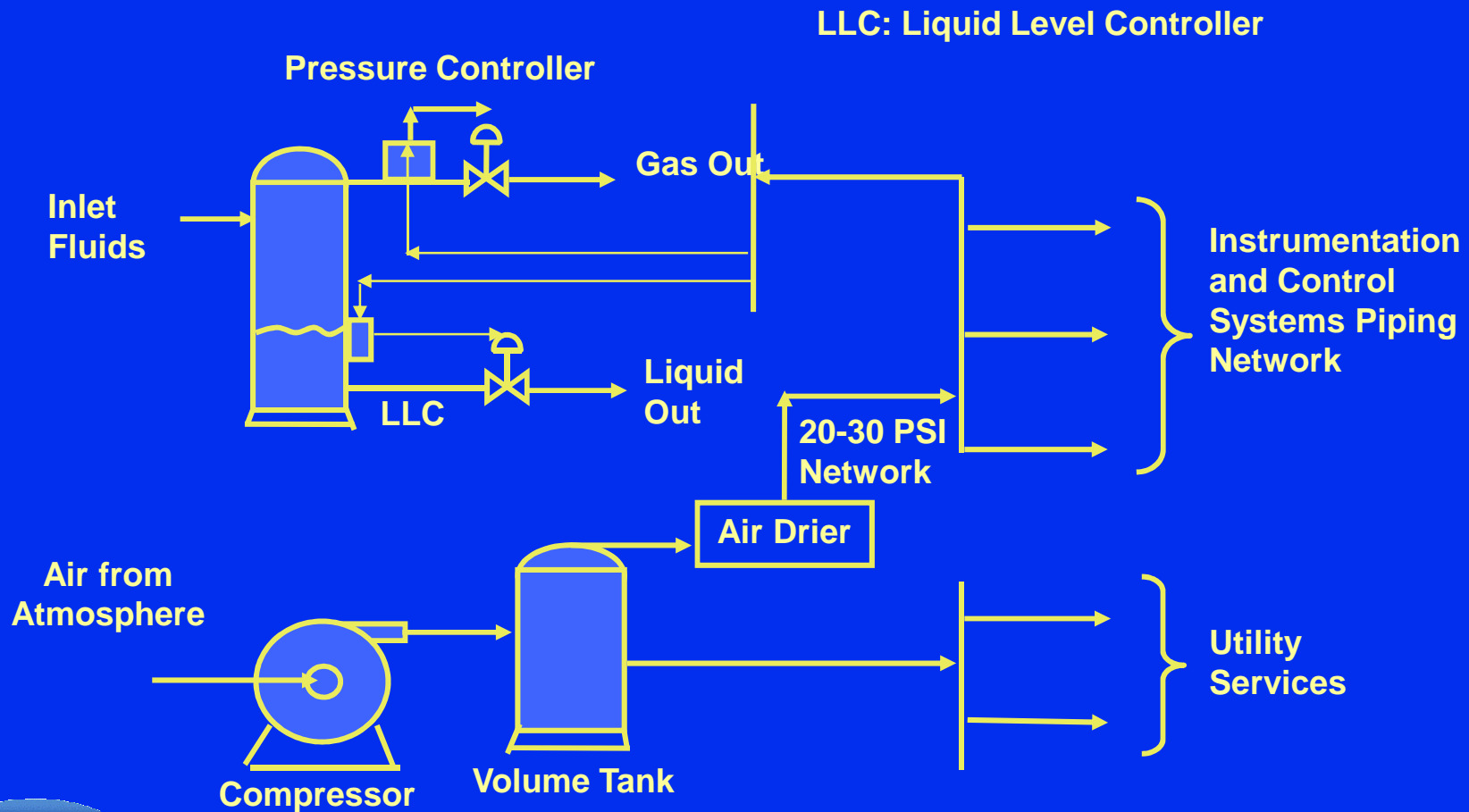
☞ Major components of instrument air system

- ◆ Compressor
- ◆ Power Source
- ◆ Air Drier
- ◆ Volume Tank

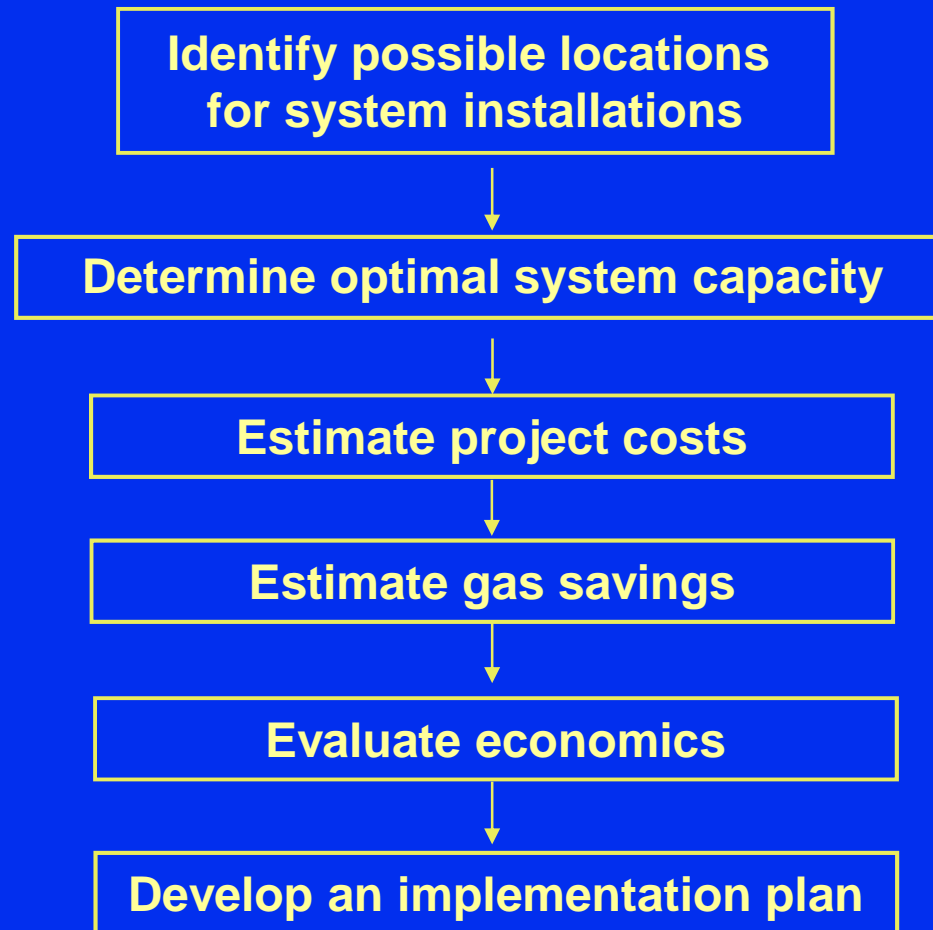


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Compressed Instrument Air System



Instrument Air Decision Process



Determine Optimal System Capacity

Instrument Air Requirements

- ◆ Volume of the compressed air
 - Meter pneumatic gas supply
 - Rule of Thumb: 1 cfm air/control loop
- ◆ Adjust for air losses
 - 17% of air input is bypassed in drier

Utility Air Requirements

- ◆ Rule of Thumb for pneumatic air systems:
 - 1/3 for instrument air
 - 2/3 for utility air



Calculate Gas Savings

☞ Determine the Gas Value Saved

◆ Value of Gas = $(IA_u + UA_u) * M * P / 1000$

- IA_u = Instrument Air Use: e.g. 35 control loops
- UA_u = Utility Air Use: e.g. assume 10 cfm utility gas
- M = Minutes in a year (525,600)
- P = Price of Gas: assume \$3.00/Mcf

◆ Value of Gas = $(35 * 1 + 10) * 525,600 * 3.00 / 1,000$

- Value of Gas Saved = \$ 71,000/year



Calculate Compressor Size

▣ Determine Air Compressor Capacity

◆ Air Compressor Capacity = $IA_S + UA_S$

- IA_S = Instrument Air Supply
= $IA_U / (100\% - \% \text{ air bypassed in drier})$
- UA_S = Utility Air Supply
= $IA_U * (\text{fraction of utility air use}) / (\text{fraction of instrument air use})$

◆ Air Compressor Capacity

$$= [(35 / (100\% - 17\%)) + ((35 * (2/3)) / (1/3))] = 112 \text{ cfm}$$



Determine Compressor Costs

Service Size	Air Volume	Compressor Type	Horsepower	Equipment Costs	Annual Service	Service Life
	(cfm)			(\$)	(\$/yr)	(yrs)
Small	30	Reciprocating	10	2,500 ¹	300	1
Medium	125	Screw	30	12,500	600	5-6 ²
Large	350	Screw	75	22,000	600	5-6 ²

¹ Cost included package compressor with a volume tank.

² Rebuilt compressor costs \$3,000 plus \$500 labor minus \$500 core exchange credit.



Determine Cost of Tank

Service Size	Air Volume (gallons)	Equipment Cost (\$)
Small	80	500
Medium	400	1,500
Large	1,000	3,000

Small reciprocating air compressors, 10 horsepower and less, are commonly supplied with a volume tank.



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Determine Cost of Drier

Service Size	Air Volume	Drier Type	Equipment Cost	Annual Service (\$/yr)
	(cfm)		(\$)	
Small	30	membrane	1,500	500
Medium	60 ¹	membrane	4,500	2,000
Large	350	alumina	10,000	3,000

¹ Largest membrane size; use multiple units larger volumes.



Calculate Capital and Operating Costs

☞ Determine Capital Cost

- ◆ Equipment Cost =
Compressors Cost (2)+Tank Cost (2)+Dryer Cost
 $= 2*\$12,500 + 2*\$500 + 1*\$4,500$
- ◆ Equipment Cost * Installation Cost Factor
Total Capital Cost = $\$30,500*1.5 = \$45,750$

☞ Determine Operating Cost

- ◆ Electrical Power = \$13,140
Engine Power * Operating Factor * Electricity Cost



Economics of Replacement

	Year 0	Year 1	Year 2	Year 3	Year 4	Year 5
Installation Cost (\$)	(45,750)					
O&M Cost (\$)	0	(13,140) ¹ (3,200) ²	(13,140) (3,200)	(13,140) (3,200)	(13,140) (3,200)	(13,140) (3,200)
Overhaul Cost (\$)	0	0	0	0	0	(4,800) ³
Total Cost (\$)	(45,750)	(16,340)	(16,340)	(16,340)	(16,340)	(21,140)
Gas Savings (\$)	0	71,000 ⁴	71,000	71,000	71,000	71,000
Annual Cash Flow (\$)	(45,750)	54,660	54,660	54,660	54,660	49,860
Cumulative Cash Flow (\$)	(45,750)	8,910	63,570	118,230	172,890	222,750
Payback Period (months)						10
IRR						117 %
NPV⁵						\$158,454



¹ Electrical Power at 7.5 cents/ kWh.

² Maintenance costs include \$1,200 compressor service and \$2,000 air drier membrane replacement

³ Compressor overhaul cost of \$3,000, inflated at 10% per year

⁴ Value of gas = \$3.00/Mcf

⁵ Net Present Value (NPV) based on 10% discount rate for 5 years

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Partner Experience: Spirit Energy '76

- ▣ Installed air compression system in its Fresh Water Bayou facility
- ▣ Project Cost = \$60,000
- ▣ Emissions Reductions = 69,350 Mcf/year
- ▣ Savings = \$208,050 /year
- ▣ Payback Period < 4 months



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Partner Experience : Texaco

- ✧ Installed compressed air system to drive pneumatic devices in 10 South Louisiana facilities
- ✧ Project Cost = \$40,000
- ✧ Emissions Reductions = 23,000 Mcf/year
- ✧ Savings = \$69,000 / year
- ✧ Payback Period ~ 7 months



Lessons Learned

- ⌘ Instrument air system has potential to increase revenue and cut methane emissions
- ⌘ It may extend the life of system equipment
- ⌘ Installing low-bleed devices in conjunction with switch to instrument air is economical
- ⌘ Existing infrastructure can be used
- ⌘ Rotary air compressors lubricated with oil must be filtered ahead of membrane dryer



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Other Technologies

- ⌘ Liquid nitrogen system
 - ◆ Expensive and potential safety hazard
- ⌘ Mechanical controls and instrumentation system
 - ◆ No power source needed
 - ◆ Limited application, frequent calibration required
- ⌘ Electric and electro-pneumatic devices



Discussion Questions

- ☞ To what extent are you implementing this BMP?
- ☞ How can this Lessons Learned study be improved upon or altered for use in your operation(s)?
- ☞ What are the barriers (technological, economic, lack of information, etc.) that are preventing you from implementing this technology?

