NEWFIELD

February 26, 2019

Claudia Smith Environmental Scientist Air Programs, Mail Code 8P-AR US Environmental Protection Agency Region 8 1595 Wynkoop Street Denver, Colorado 80202

### RE: Mamie 4-25-3-3WH Site-Specific Permit Application Revision 1

Dear Ms. Smith,

Newfield Production Company ("Newfield") is submitting the enclosed revision to the EPA Minor New Source Review permit application for a modification to the well pad Mamie 4-25-3-3WH. Newfield is proposing to add a well and associated tank battery equipment to the existing well pad which is located on Tribal land within the Uintah and Ouray Reservation in Duchesne County, Utah. Newfield submitted a Registration for New Sources (Form REG) for the existing well pad on October 30, 2013. The initial site-specific permit application for this project was submitted to EPA in January 2019. This revised permit application includes an Application for New Construction (Form NEW), a detailed project description, emission calculations and supporting documentation, an air quality review with dispersion modeling, and Endangered Species Act and National Historic Preservation Act compliance documentation. Changes from the initial permit application include revised oil production estimates and several updated/corrected emission calculations.

Please contact me (281-674-1588, jwoodall@newfield.com) with any questions or comments. We look forward to working with you to obtain a site-specific permit for this well pad.

Regards,

James Woodall Sr. Air Quality Specialist Newfield Production Company

Enclosure

Cc: Doug Jordan, Newfield Eric Farstad, Redhorse Corporation Bruce Pargeets, Uintah and Ouray Reservation Mike Natchees, Uintah and Ouray Reservation

# **Newfield Production Company**



# EPA Minor NSR, Application for New Construction MAMIE 4-25-3-3WH Revision 1

Submitted to:

Federal Minor NSR Permit Coordinator U.S. EPA, Region 8 1595 Wynkoop Street, 8P-AR Denver, CO 80202-1129

Submitted by:

Newfield Production Company 24 Waterway Avenue Suite 900 The Woodlands, Texas 77380

February 2019



Daga

### CONTENTS

### **SECTION**

		rage
1.0	INTRODUCTION	1
2.0	APPLICATION FOR CONSTRUCTION - Form NEW	2

## **ATTACHMENTS**

Attachment 1	Detailed Project Description
Attachment 2	Emission Calculations and Supporting Documentation
Attachment 3	Air Quality Review
Attachment 4	Endangered Species Act and National Historic Preservation Act Compliance Documentation



### **1.0 INTRODUCTION**

This document presents technical and regulatory information in support of an Application for New Construction to obtain a Federal Minor New Source Review (MNSR) permit from the United States (U.S.) Environmental Protection Agency (EPA) for a Newfield Production Company oil well production site. This permit application documentation is a revision to a permit application submitted to EPA in January 2019. This revision updates projected production values and corrects source emission calculations.

This NOI is submitted for: MAMIE 4-25-3-3WH

 Township:
 3S

 Range:
 3W

 Section:
 25

 County:
 DUCHESNE

 API #:
 4301351531

This document provides all required documentation supporting an Application for New Construction for the well site listed above pursuant to Federal Minor New Source Review Program in Indian Country 40 CFR 49.151. The completed application form (Form NEW) is provided in Section 2 of this document. Attachments are provided which contain required EPA associated documentation, as defined in the Form NEW instructions.



2.0 APPLICATION FOR CONSTRUCTION FEDERAL MINOR NSR, APPLICATION FOR NEW CONSTRUCTION

UNITED STATES ENVIRONMENTAL PROTECTION AGENCY FEDERAL MINOR NEW SOURCE REVIEW PROGRAM IN INDIAN COUNTRY 40 CFR 49.151 Application for New Construction (Form NEW)				
<ul> <li>Please check all that apply to show how you are using this form:</li> <li>□ Proposed Construction of a New Source</li> <li>□ Proposed Construction of New Equipment at an Existing Source</li> <li>☑ Proposed Modification of an Existing Source</li> <li>□ Other – Please Explain</li> </ul>				
Use of this information request form is voluntary and not approved by the Office of Management and Budget. The following is a check list of the type of information that Region 8 will use to process information on your proposed project. While submittal of this form is not required, it does offer details on the information we will use to complete your requested approval and providing the information requested may help expedite the process. An application form approved by the Office of Management and Budget can be found online at <a href="https://www.epa.gov/sites/production/files/2015-12/documents/new_source_general_application_rev2017.pdf">https://www.epa.gov/sites/production/files/2015-12/documents/new_source_general_application_rev2017.pdf</a> .				ement and Budget. The on your proposed project. o complete your requested form approved by the files/2015-
Federal Minor NSR Permit Coordinator U.S. EPA, Region 8 1595 Wynkoop Street, 8P-AR Denver, CO 80202-1129 <u>R8airpermitting@epa.gov</u> For more information, visit: <u>http://www.epa.gov/caa-permitting/tribal-nsr-permitting-region-8</u>		The rese If yo Trib cont <u>R8a</u>	The Tribal Environmental Contact for the specific reservation: If you need assistance in identifying the appropriate Tribal Environmental Contact and address, please contact: <u>R8airpermitting@epa.gov</u>	
<ul> <li>1. (a) Company Name (Who owns this facility?) Newfield Exploration</li> <li>(b) Operator Name (Is the company that operates this facility different than the company that owns this facility? What is the name of the company?)</li> </ul>		2. Facility Name Mamie 4-25-3-3WH		
<ul><li>3. Type of Operation Oil Wellpad</li><li>6. NAICS Code 21111</li></ul>		4. Portable Source?       □ Yes       ⊠ No         5. Temporary Source?       □ Yes       ⊠ No         7. SIC Code       1311		
8. Physical Address (Or, home base for portable sources)         NW ¼ of the NW ¼ Section 25, T.3S, R.3W, Utah				
9. Reservation*	10. County*	1 (d	1a. Latitude lecimal format)*	11b. Longitude (decimal format)*
Untah and Ouray 12a. Quarter Ouarter Section*	Duchesne 12b. Section*	40	0.19965 2c. Township*	-110.176876 12d. Range*
NWNW 25		3	S	3W
*Provide all proposed locations of op	eration for portable sour	rces		

# **B. PREVIOUS PERMIT ACTIONS** (Provide information in this format for each permit that has

been issued to this source. Provide as an attachment if additional space is necessary)

Facility Name on the Permit

The facility does not have a permit, but a FORM REG registration was submitted Permit Number (xx-xxx-xxxxx-xxxx)

Date of the Permit Action

FORM REG Submittal Date: October 30, 2013

Facility Name on the Permit

Permit Number (xx-xxx-xxxx.xx)

Date of the Permit Action

Facility Name on the Permit

Permit Number (xx-xxx-xxxx.xx)

Date of the Permit Action

Facility Name on the Permit

Permit Number (xx-xxx-xxxx.xx)

Date of the Permit Action

Facility Name on the Permit

Permit Number (xx-xxx-xxxxx-xxxx.xx)

Date of the Permit Action

## C. CONTACT INFORMATION

<b>Company Contact</b> (Who is the <u>primary contact</u> for the company that owns this facility?)			Title
Noel Putscher			Production Manager
Mailing Address 24 Waterway Avenue, Suite 900 The Woodlands, Texas 77380			
Email Address nputscher@newfield.com			
Telephone Number (281) 210-5100	Facsimile Number (281) 210-5101		
<b>Operator Contact</b> (Is the company that operates this facility company that owns this facility? Who is the <u>primary</u> contact operates this facility?) N/A	ity different than the t for the company that	Title	2
Mailing Address			
Email Address			
Telephone Number	Facsimile Number		
<b>Permitting Contact</b> (Who is the person <u>primarily</u> responsible for Clean Air Act permitting for the company? We are seeking one main contact for the company. Please do not list consultants.) James Woodall			e Air Quality Specialist
Mailing Address 24 Waterway Avenue, Suite 900 The Woodlands, Texas 77380			
Email Address jwoodall@newfield.com			
Telephone Number     (281) 674-1588	Facsimile Number (281) 210-5101		
Compliance Contact (Is the person responsible for Clean Air Act compliance for this company different than the person responsible for Clean Air Act permitting? Who is the person primarily responsible for Clean Air Act compliance for the company? We are seeking one main contact for the company. Please do not list consultants.)TitleJames WoodallSr. Air Quality Specialist			e Air Quality Specialist
Mailing Address 24 Waterway Avenue, Suite 900 The Woodlands, Texas 77380			
Email Address jwoodall@newfield.com			
Telephone NumberFacsimile Number(281) 674-1588(281) 210-5101			

### **D. ATTACHMENTS**

Include all of the following information (see the attached instructions)

\*Please do not send Part 71 Operating Permit Application Forms in lieu of the check list below.

□ **FORM SYNMIN -** New Source Review Synthetic Minor Limit Request Form, if synthetic minor limits are being requested.

 $\boxtimes$  Narrative description of the proposed production processes. This description should follow the flow of the process flow diagram to be submitted with this application.

⊠ Process flow chart identifying all proposed processing, combustion, handling, storage, and emission control equipment.

⊠ A list and descriptions of all proposed emission units and air pollution-generating activities.

⊠ Type and quantity of fuels, including sulfur content of fuels, proposed to be used on a daily, annual and maximum hourly basis.

If Type and quantity of raw materials used or final product produced proposed to be used on a daily, annual and maximum hourly basis.

⊠ Proposed operating schedule, including number of hours per day, number of days per week and number of weeks per year.

A list and description of all proposed emission controls, control efficiencies, emission limits, and monitoring for each emission unit and air pollution generating activity.

 $\boxtimes$  **Criteria Pollutant Emissions -** Estimates of Current Actual Emissions, Current Allowable Emissions, Post-Change Uncontrolled Emissions, and Post-Change Allowable Emissions for the following air pollutants: particulate matter, PM<sub>10</sub>, PM<sub>2.5</sub>, sulfur oxides (SOx), nitrogen oxides (NOx), carbon monoxide (CO), volatile organic compound (VOC), lead (Pb) and lead compounds, fluorides (gaseous and particulate), sulfuric acid mist (H<sub>2</sub>SO<sub>4</sub>), hydrogen sulfide (H<sub>2</sub>S), total reduced sulfur (TRS) and reduced sulfur compounds, including all calculations for the estimates.

These estimates are to be made for each emission unit, emission generating activity, and the project/source in total. Note, there are no insignificant emission units or activities in this permitting program, only exempted units and activities. Please see the regulation for a list of exempted units and activities.

☑ Air Quality Review

**ESA** (Endangered Species Act)

### ☑ NHPA (National Historic Preservation Act)

### E. TABLE OF ESTIMATED EMISSIONS

The following tables provide the total emissions in tons/year for all pollutants from the calculations required in Section D of this form, as appropriate for the use specified at the top of the form.

Pollutant	Potential Emissions (tpy)	Proposed Allowable Emissions (tny)	
PM	0.32	0.32	PM - Particulate Matter
PM10	0.32	0.32	than 10 microns in size
PM 2.5	0.32	0.32	PM <sub>2.5</sub> - Particulate Matter less than 2.5 microns in size
SO <sub>2</sub>	0.02	0.02	SO <sub>2</sub> - Sulfur Dioxide
NOx	6.35	6.35	CO - Carbon Monoxide
СО	12.31	12.31	Compound
VOC	8.81	8.81	Pb - Lead and lead compounds
Pb	0	0	particulates
Fluorides	0	0	$H_2SO_4$ - Sulfuric Acid Mist
H <sub>2</sub> SO <sub>4</sub>	0	0	TRS - Total Reduced Sulfur
H <sub>2</sub> S	negligible	negligible	RSC - Reduced Sulfur Compounds
TRS	0	0	<u>r</u>
RSC	0	0	

### E(i) – Proposed New Source

Emissions calculations must include fugitive emissions if the source is one the following listed sources, pursuant to CAA Section 302(j):

- (a) Coal cleaning plants (with thermal dryers);
- (b) Kraft pulp mills;
- (c) Portland cement plants;
- (d) Primary zinc smelters;
- (e) Iron and steel mills;
- (f) Primary aluminum ore reduction plants;
- (g) Primary copper smelters;
- (h) Municipal incinerators capable of charging more than 250 tons of refuse per day;
- (i) Hydrofluoric, sulfuric, or nitric acid plants;
- (j) Petroleum refineries;
- (k) Lime plants;
- (1) Phosphate rock processing plants;
- (m) Coke oven batteries;
- (n) Sulfur recovery plants;
- (o) Carbon black plants (furnace process);
- (p) Primary lead smelters;
- (q) Fuel conversion plants;

- (r) Sintering plants;
- (s) Secondary metal production plants;
- (t) Chemical process plants
- (u) Fossil-fuel boilers (or combination thereof) totaling more than 250 million British thermal units per hour heat input;
- (v) Petroleum storage and transfer units with a total storage capacity exceeding 300,000 barrels;
- (w) Taconite ore processing plants;
- (x) Glass fiber processing plants;
- (y) Charcoal production plants;
- (z) Fossil fuel-fired steam electric plants of more that 250 million British thermal units per hour heat input, and

(aa) Any other stationary source category which, as of August 7, 1980, is being regulated under section 111 or 112 of the Act.

Pollutant	Current	Current	Post-Change	Post-Change
	Actual	Allowable	Potential	Allowable
	Emissions	Emissions	Emissions	Emissions
	(tpy)	(tpy)	(tpy)	(tpy)
PM	0.11	N/A	0.19	0.19
PM <sub>10</sub>	0.11	N/A	0.19	0.19
PM 2.5	0.11	N/A	0.19	0.19
SO <sub>2</sub>	0.01	N/A	0.01	0.01
NO <sub>x</sub>	3.03	N/A	6.35	6.35
СО	5.43	N/A	12.31	12.31
VOC	4.45	N/A	11.64	11.64
Pb	0	N/A	0	0
Fluorides	0	N/A	0	0
H <sub>2</sub> SO <sub>4</sub>	0	N/A	0	0
$H_2S$	negligible	N/A	negligible	negligible
TRS	0	N/A	0	0
RSC	0	N/A	0	0

E(ii) – Proposed New Construction at an Existing Source or Modification of an Existing Source

PM - Particulate Matter

 $\begin{array}{l} PM_{10} & - Particulate Matter less than 10 microns in size \\ PM_{2.5} & - Particulate Matter less than 2.5 microns in size \\ SO_2 & - Sulfur Dioxide \\ NOx & - Nitrogen Oxides \\ CO & - Carbon Monoxide \\ VOC & - Volatile Organic Compound \\ Pb & - Lead and lead compounds \\ Fluorides & - Gaseous and particulates \\ H_2SO_4 & - Sulfuric Acid Mist \\ H_2S & - Hydrogen Sulfide \\ TRS & - Total Reduced Sulfur \\ RSC & - Reduced Sulfur Compounds \\ \end{array}$ 

[Disclaimers] The public reporting and recordkeeping burden for this collection of information is estimated to average 20 hours per response, unless a modeling analysis is required. If a modeling analysis is required, the public reporting and recordkeeping burden for this collection of information is estimated to average 60 hours per response. Send comments on the Agency's need for this information, the accuracy of the provided burden estimates, and any suggested methods for minimizing respondent burden, including through the use of automated collection techniques to the Director, Collection Strategies Division, U.S. Environmental Protection Agency (2822T), 1200 Pennsylvania Ave., NW, Washington, D.C. 20460. Include the OMB control number in any correspondence. Do not send the completed form to this address.

# Application for New Construction (Form NEW) REVISED FEBRUARY 2019 Newfield Exploration Mamie 4-25-3-3WH

### ATTACHMENTS

- 1. Narrative Description of the proposed production processes, process flow chart, list and description of proposed emission units and air pollution-generating activities
- 2. Emission Inventory, including fuels, raw materials, final product produced, operating schedules, and emission controls
- 3. Air Quality Review
- 4. Endangered Species Act and National Historic Preservation Act Documentation

Attachment 1

**Source Description** 

The Mamie 4-25-3-3WH facility is an existing oil well production facility for the extraction, storage, and separation of produced oil, gas, and water. A registration form (Form REG) was submitted for the facility in November 2013 in accordance with the Federal Minor New Source Review Program in Indian Country (40 CFR 49.151). The facility consists of a natural gas-fired generator, electric pumping units, oil storage tanks, a produced water storage tank, tank heaters, a heater treater/separator, and pneumatic devices. The proposed modification would add a new well to the facility along with additional equipment, including an electric pumping unit, three oil storage tanks, a produced water storage tank, tank heaters, a heater treater/separator, and pneumatic devices. Tank emissions are controlled with flares. A list of equipment proposed for the registered site after modification is given below:

### Emission units and air pollution generating activities:

### **Onsite Gas-Fired Engine:**

• Two natural gas-fired generator engines

### Heater Treaters and Tank Heaters:

- Two heater treaters
- Six tank heaters

### Storage Tanks:

- Six oil storage tanks (heated)
- Two produced water storage tanks

### Pneumatic Controllers:

• Pneumatic controllers

### **Storage Tank Unloading Operations:**

• Oil storage tank unloading operations to tanker trucks will utilize submerged loading. The proposed unloading rack will install vapor capture lines

### Fugitives:

• Fugitive emissions such as valves, connectors, open-ended lines, flanges, and other components

### Air pollution control equipment:

- One existing flare and one proposed flare will be utilized to control storage tank VOC emissions in accordance with NSPS OOOOa standards. The existing flare is a Steffes SFI and the proposed flare will be a Steffes SAA-2. Specifications are provided in Attachment 2.
- Vapor capture during tank unloading operations will be utilized for the new unloading rack. Captured vapors will be routed back through the system or sent to the flare.

Newfield will comply with all applicable federal regulations such as New Source Performance Standards (NSPS) and any other regulations required under the Minor NSR Program in Indian Country. Detailed description of the facility processes, a process flowchart, and site figures are given below.

Company:	Newfield Exploration
Facility:	MAMIE 4-25-3-3WH
Location:	Township: 3S, Range: 3W, Section: 25
API #:	4301351531

#### **Facility Description**

This is an example of common equipment at a well-head site. The equipment listed is not intended to be a specific representation of equipment at the site, but is an example of common equipment at a well pad for oil extraction. The well-head site is used for the extraction, storage, and separation of produced oil, gas, and water. For example, a well-head site could consist of pumping units, oil storage tanks, produced water storage tanks, tank heaters, heater treaters, dehydrators, and pneumatics. Details regarding the equipment listed in this document are presented below as this site description is representative of a typical well.

#### **Onsite Engines**

A well-site produces fluids from a well. The fluids are produced at the well-head by mechanically lifting the fluids out of the well using a pump. The mechanical action of the pump is generated by a co-located natural gas fired engine. The fluids produced at the well are piped to a heater treater, for separating oil, gas, and water. Information about the pumping unit at this site is presented below.

No. of engines:	2
List of engines:	ENG-1, ENG-2

Additional details are contained in individual associated emission estimate forms for each engine at this site.

#### **Heater Treaters**

Fluids from a well consist of oil, water, and gas. The fluids produced at the well are typically piped to a separator unit, referred to here as a heater treater, where it is separated into the oil, water, and gas components using pressure and heat. Heat for the separator is provided by combusting natural gas in a burner. Information about the heater treaters at this site is presented below.

No. of heater treaters:	2
List of heater treaters:	HTRTRTR-1, HTRTRTR-2

Additional details are contained in individual associated emission estimate forms for each heater treater at this site.

#### Tanks

Fluids produced by pumping units are typically stored on-site in vertical fixed-flat-roof tanks. The tanks at a site could be dedicated for production only from the well where it is located, a common tank battery fed by other well-sites, or a common tank battery fed by a well at that site in addition to other well-sites. Information about the tanks at this site is presented below.

No. of onsite oil tanks:	6
List of onsite oil tanks:	OILTK-1, OILTK-2, OILTK-3, OILTK-4, OILTK-5, OILTK-6
No. of onsite water tanks:	2
List of onsite water tanks:	PWTANK-1, PWTANK-2

Additional details are contained in individual associated emission estimate forms for each tank at this site.

#### Heaters

The temperature of the fluid in the tank can be controlled by using natural gas fired tank heaters. Tank heaters are typically small units used to keep the fluid viscous. Information about the heaters at this site is presented below.

No. of tank heaters:	6		
List of tank heaters:	TANKHTR1, TANKHTR2, TANKHTA, TANKHTANKHTA, TANKHTANKHTA, TANKHTANKHTA, TANKHTANKHTA, TANKHTANKHTA, TANKHTANKHTANKHTANKHTANKHTANKHTANKHTANKH	ANKHTR3, TANKHTR4,	TANKHTR5, TANKHTR6

Additional details are contained in individual associated emission estimate forms for each tank at this site.

Company:	Newfield Exploration
Facility:	MAMIE 4-25-3-3WH
Location:	Township: 3S, Range: 3W, Section: 25
API #:	4301351531

#### Pneumatic controllers

Pneumatic controllers are sometimes used to actuate functions using instrument natural gas at the well. The gas used to operate the pneumatic controllers is released to the atmosphere on an intermittent basis. Information concerning the pneumatic controllers at this site are contained in individual associated emission estimate forms for the pneumatic controllers.

#### **Tank Unloading**

Trucks are often used to remove the oil and produced water collected in tanks at a well. The oil is loaded into trucks and transported to a refinery. Oil tanks are isolated so that only one truck loading outlet is used. Produced water is loaded into trucks and transported to water treatment facilities. The act of loading the trucks generates emissions at the well site. Information about truck loading at this site is presented below:

No. of tanks loaded to trucks at this site:

6

Additional details are contained in individual associated emission estimate forms for the truck loading at this site.

#### Fugitives

Each well site includes piping used to move oil and gas products. The well site system contains numerous components such as valves, connectors, open-ended lines, flanges, and other components that have potential fugitive emissions associated with their operation. The type and quantity of components at well sites are assumed to be the same as the default average component count from Subpart W of Part 98 of the Code of Federal Regulations. Additional details are contained in individual associated emission estimate forms for well fugitives at this site.

#### Flares

Flares are used to control emissions from oil and water tanks at the site. The flares control VOC at a rate of 98%.

#### Small Tanks

Well pads may also include other small tanks containing miscellaneous chemicals with maximum tank capacity less than or equal to 500 gallons each. Typically, these liquids will be contained in 55 gallon drums and are listed for informational purposes only.









Attachment 2

**Emission Inventory** 

#### Criteria Pollutant Emission Summary

							Co	ntrolled PTE (T	PY)						
															Total
Туре	ID No.	Name	VOC	HAP	NOx	co	PM <sub>10</sub>	PM <sub>2.5</sub>	SO <sub>2</sub>	CO2	CH₄	CO <sub>2</sub> e	N <sub>2</sub> O <sup>**</sup>	CO <sub>2</sub> e	CO <sub>2</sub> e
							Existing Source	es							
Engine	1	ENG-1	1.54E+00	8.17E-02	2.20E+00	4.40E+00	4.91E-02	4.91E-02	1.49E-03	2.78E+02	5.82E-01	1.22E+01			2.90E+02
Treater Burner	2	HTRTRTR-1	2.36E-02	8.11E-03	4.29E-01	3.61E-01	3.26E-02	3.26E-02	2.58E-03	5.15E+02	9.88E-03	2.07E-01	9.45E-03	2.93E+00	5.18E+02
Oil Well Fugitives	3	FUG-1	5.42E-02	3.01E-03							6.02E-01	1.26E+01			1.26E+01
Oil Tank	4	OILTK-1	1.20E-01	2.80E-02	1.02E-02	5.57E-02				1.77E+01	1.96E-02	4.12E-01	3.24E-04	1.01E-01	1.82E+01
Oil Tank	5	OILTK-2	1.20E-01	2.80E-02	1.02E-02	5.57E-02				1.77E+01	1.96E-02	4.12E-01	3.24E-04	1.01E-01	1.82E+01
Oil Tank	6	OILTK-3	1.20E-01	2.80E-02	1.02E-02	5.57E-02				1.77E+01	1.96E-02	4.12E-01	3.24E-04	1.01E-01	1.82E+01
Oil Tank Unloading	7	OILTKLOAD-1	2.31E+00	4.17E-01							2.91E-01	6.11E+00			6.11E+00
Pneumatic Controllers	8	PCONT-1	8.85E-02								9.64E-01	2.02E+01			2.02E+01
Water Tank	9	PWTANK-1	5.48E-03	2.55E-04	2.65E-03	1.44E-02				4.58E+00	1.86E-02	3.91E-01	8.39E-05	2.60E-02	4.99E+00
Small Storage Tanks	10	SMTANKS-1	2.05E-02												
Heater	11	TANKHTR1	5.90E-03	2.03E-03	1.07E-01	9.02E-02	8.16E-03	8.16E-03	6.44E-04	1.29E+02	2.47E-03	5.19E-02	2.36E-03	7.32E-01	1.30E+02
Heater	12	TANKHTR2	5.90E-03	2.03E-03	1.07E-01	9.02E-02	8.16E-03	8.16E-03	6.44E-04	1.29E+02	2.47E-03	5.19E-02	2.36E-03	7.32E-01	1.30E+02
Heater	13	TANKHTR3	5.90E-03	2.03E-03	1.07E-01	9.02E-02	8.16E-03	8.16E-03	6.44E-04	1.29E+02	2.47E-03	5.19E-02	2.36E-03	7.32E-01	1.30E+02
Flare	14	FLARE-1	3.00E-02		3.93E-02	2.14E-01				6.80E+01	4.45E-02	1.38E+01	1.25E-03	3.87E-01	8.22E+01
						F	Proposed Sour	ces							
Engine	15	ENG-2	1.58E+00	2.66E-01	2.26E+00	4.52E+00	1.60E-01	1.60E-01	4.85E-03	9.07E+02	1.90E+00	3.98E+01			9.47E+02
Treater Burner	16	HTRTRTR-2	2.36E-02	8.11E-03	4.29E-01	3.61E-01	3.26E-02	3.26E-02	2.58E-03	5.15E+02	9.88E-03	2.07E-01	9.45E-03	2.93E+00	5.18E+02
Oil Well Fugitives	17	FUG-2	5.42E-02	3.01E-03							6.02E-01	1.26E+01			1.26E+01
Oil Tank	18	OILTK-4	5.40E-01	1.29E-01	4.77E-02	2.59E-01				8.25E+01	9.04E-02	1.90E+00	1.51E-03	4.69E-01	8.49E+01
Oil Tank	19	OILTK-5	5.40E-01	1.29E-01	4.77E-02	2.59E-01				8.25E+01	9.04E-02	1.90E+00	1.51E-03	4.69E-01	8.49E+01
Oil Tank	20	OILTK-6	5.40E-01	1.29E-01	4.77E-02	2.59E-01				8.25E+01	9.04E-02	1.90E+00	1.51E-03	4.69E-01	8.49E+01
Oil Tank Unloading	21	OILTKLOAD-2	7.97E-01	1.44E-01							1.00E-01	2.11E+00			2.11E+00
Pneumatic Controllers	22	PCONT-2	8.85E-02								9.64E-01	2.02E+01			2.02E+01
Water Tank	23	PWTANK-2	2.74E-02	1.28E-03	1.32E-02	7.20E-02				2.29E+01	9.31E-02	1.95E+00	4.20E-04	1.30E-01	2.50E+01
Small Storage Tanks	24	SMTANKS-2	2.05E-02												
Heater	25	TANKHTR4	5.90E-03	2.03E-03	1.07E-01	9.02E-02	8.16E-03	8.16E-03	6.44E-04	1.29E+02	2.47E-03	5.19E-02	2.36E-03	7.32E-01	1.30E+02
Heater	26	TANKHTR5	5.90E-03	2.03E-03	1.07E-01	9.02E-02	8.16E-03	8.16E-03	6.44E-04	1.29E+02	2.47E-03	5.19E-02	2.36E-03	7.32E-01	1.30E+02
Heater	27	TANKHTR6	5.90E-03	2.03E-03	1.07E-01	9.02E-02	8.16E-03	8.16E-03	6.44E-04	1.29E+02	2.47E-03	5.19E-02	2.36E-03	7.32E-01	1.30E+02
Flare	28	FLARE-2	1.23E-01		1.61E-01	8.78E-01				2.79E+02	1.83E-01	5.67E+01	5.12E-03	1.59E+00	3.37E+02
Totals	i (TPY)		8.81	1.42	6.35	12.31	0.32	0.32	0.02	3663.95	6.70	206.48	0.05	14.09	3884.52

 $^{**}N_2O$  emissions have not been estimated for engines due to the absence of an AP-42 emission factor (AP-42, Section 3.2.3.4).

#### Criteria Pollutant Emission Summary

							Unc	ontrolled PTE	(TPY)						
															Total
Туре	ID No.	Name	VOC	HAP	NOx	CO	PM <sub>10</sub>	PM <sub>2.5</sub>	SO <sub>2</sub>	CO2	CH₄	CO <sub>2</sub> e	N <sub>2</sub> O <sup>**</sup>	CO <sub>2</sub> e	CO <sub>2</sub> e
							Existing Source	ces							
Engine	1	ENG-1	1.54E+00	8.17E-02	2.20E+00	4.40E+00	4.91E-02	4.91E-02	1.49E-03	2.78E+02	5.82E-01	1.22E+01			2.90E+02
Treater Burner	2	HTRTRTR-1	2.36E-02	8.11E-03	4.29E-01	3.61E-01	3.26E-02	3.26E-02	2.58E-03	5.15E+02	9.88E-03	2.07E-01	9.45E-03	2.93E+00	5.18E+02
Oil Well Fugitives	3	FUG-1	5.42E-02	3.01E-03							6.02E-01	1.26E+01			1.26E+01
Oil Tank	4	OILTK-1	6.00E+00	1.40E+00							9.80E-01	2.06E+01			2.06E+01
Oil Tank	5	OILTK-2	6.00E+00	1.40E+00							9.80E-01	2.06E+01			2.06E+01
Oil Tank	6	OILTK-3	6.00E+00	1.40E+00							9.80E-01	2.06E+01			2.06E+01
Oil Tank Unloading	7	OILTKLOAD-1	2.31E+00	4.17E-01							2.91E-01	6.11E+00			6.11E+00
Pneumatic Controllers	8	PCONT-1	8.85E-02								9.64E-01	2.02E+01			2.02E+01
Water Tank	9	PWTANK-1	2.74E-01	1.28E-02							9.31E-01	1.95E+01			1.95E+01
Small Storage Tanks	10	SMTANKS-1	2.05E-02												
Heater	11	TANKHTR1	5.90E-03	2.03E-03	1.07E-01	9.02E-02	8.16E-03	8.16E-03	6.44E-04	1.29E+02	2.47E-03	5.19E-02	2.36E-03	7.32E-01	1.30E+02
Heater	12	TANKHTR2	5.90E-03	2.03E-03	1.07E-01	9.02E-02	8.16E-03	8.16E-03	6.44E-04	1.29E+02	2.47E-03	5.19E-02	2.36E-03	7.32E-01	1.30E+02
Heater	13	TANKHTR3	5.90E-03	2.03E-03	1.07E-01	9.02E-02	8.16E-03	8.16E-03	6.44E-04	1.29E+02	2.47E-03	5.19E-02	2.36E-03	7.32E-01	
Flare	14	FLARE-1	3.00E-02		3.93E-02	2.14E-01				6.80E+01	4.45E-02	1.38E+01	1.25E-03	3.87E-01	
						F	Proposed Sour	ces	<u> </u>	<u> </u>					
Engine	15	ENG-2	1.58E+00	2.66E-01	2.26E+00	4.52E+00	1.60E-01	1.60E-01	4.85E-03	9.07E+02	1.90E+00	3.98E+01			9.47E+02
Treater Burner	16	HTRTRTR-2	2.36E-02	8.11E-03	4.29E-01	3.61E-01	3.26E-02	3.26E-02	2.58E-03	5.15E+02	9.88E-03	2.07E-01	9.45E-03	2.93E+00	5.18E+02
Oil Well Fugitives	17	FUG-2	5.42E-02	3.01E-03							6.02E-01	1.26E+01			1.26E+01
Oil Tank	18	OILTK-4	2.70E+01	6.47E+00							4.52E+00	9.49E+01			9.49E+01
Oil Tank	19	OILTK-5	2.70E+01	6.47E+00							4.52E+00	9.49E+01			9.49E+01
Oil Tank	20	OILTK-6	2.70E+01	6.47E+00							4.52E+00	9.49E+01			9.49E+01
Oil Tank Unloading	21	OILTKLOAD-2	1.16E+01	2.08E+00							1.46E+00	3.06E+01			3.06E+01
Pneumatic Controllers	22	PCONT-2	8.85E-02								9.64E-01	2.02E+01			2.02E+01
Water Tank	23	PWTANK-2	1.37E+00	6.38E-02							4.65E+00	9.77E+01			9.77E+01
Small Storage Tanks	24	SMTANKS-2	2.05E-02												
Heater	25	TANKHTR4	5.90E-03	2.03E-03	1.07E-01	9.02E-02	8.16E-03	8.16E-03	6.44E-04	1.29E+02	2.47E-03	5.19E-02	2.36E-03	7.32E-01	1.30E+02
Heater	26	TANKHTR5	5.90E-03	2.03E-03	1.07E-01	9.02E-02	8.16E-03	8.16E-03	6.44E-04	1.29E+02	2.47E-03	5.19E-02	2.36E-03	7.32E-01	1.30E+02
Heater	27	TANKHTR6	5.90E-03	2.03E-03	1.07E-01	9.02E-02	8.16E-03	8.16E-03	6.44E-04	1.29E+02	2.47E-03	5.19E-02	2.36E-03	7.32E-01	
Flare	28	FLARE-2	1.23E-01		1.61E-01	8.78E-01				2.79E+02	1.83E-01	5.67E+01	5.12E-03	1.59E+00	
Totals	(TPY)		1.18E+02	2.66E+01	6.16E+00	1.13E+01	3.23E-01	3.23E-01	1.54E-02	3.34E+03	2.97E+01	6.89E+02	3.94E-02	1.22E+01	3.36E+03

 $**N_2O$  emissions have not been estimated for engines due to the absence of an AP-42 emission factor (AP-42, Section 3.2.3.4).

#### Criteria Pollutant Emission Summary

							Cor	ntrolled PTE (It	o/hr)						
Туре	ID No.	Name	VOC	HAP	NOx	CO	PM <sub>10</sub>	PM <sub>2.5</sub>	SO <sub>2</sub>	CO <sub>2</sub>	CH₄	CO <sub>2</sub> e	N <sub>2</sub> O <sup>m</sup>	CO <sub>2</sub> e	CO <sub>2</sub> e
							Existing Source	es							
Engine	1	ENG-1	3.52E-01	1.87E-02	5.03E-01	1.01E+00	1.12E-02	1.12E-02	3.40E-04	6.35E+01	1.33E-01	2.79E+00			6.63E+01
Treater Burner	2	HTRTRTR-1	5.39E-03	1.85E-03	9.80E-02	8.24E-02	7.45E-03	7.45E-03	5.88E-04	1.18E+02	2.25E-03	4.74E-02	2.16E-03	6.69E-01	1.18E+02
Oil Well Fugitives	3	FUG-1	1.24E-02	6.87E-04							1.37E-01	2.89E+00			2.89E+00
Oil Tank	4	OILTK-1	2.74E-02	6.40E-03	2.34E-03	1.27E-02				4.04E+00	4.47E-03	9.40E-02	7.41E-05	2.30E-02	4.16E+00
Oil Tank	5	OILTK-2	2.74E-02	6.40E-03	2.34E-03	1.27E-02				4.04E+00	4.47E-03	9.40E-02	7.41E-05	2.30E-02	4.16E+00
Oil Tank	6	OILTK-3	2.74E-02	6.40E-03	2.34E-03	1.27E-02				4.04E+00	4.47E-03	9.40E-02	7.41E-05	2.30E-02	4.16E+00
Oil Tank Unloading	7	OILTKLOAD-1	1.94E+01	3.50E+00							2.45E+00	6.11E+01			6.11E+01
Pneumatic Controllers	8	PCONT-1	2.02E-02								2.20E-01	4.62E+00			4.62E+00
Water Tank	9	PWTANK-1	1.25E-03	5.83E-05	6.04E-04	3.29E-03				1.05E+00	4.25E-03	8.93E-02	1.92E-05	5.94E-03	1.14E+00
Small Storage Tanks	10	SMTANKS-1	4.69E-03												
Heater	11	TANKHTR1	1.35E-03	4.63E-04	2.45E-02	2.06E-02	1.86E-03	1.86E-03	1.47E-04	2.94E+01	5.64E-04	1.18E-02	5.39E-04	1.67E-01	
Heater	12	TANKHTR2	1.35E-03	4.63E-04	2.45E-02	2.06E-02	1.86E-03	1.86E-03	1.47E-04	2.94E+01	5.64E-04	1.18E-02	5.39E-04	1.67E-01	
Heater	13	TANKHTR3	1.35E-03	4.63E-04	2.45E-02	2.06E-02	1.86E-03	1.86E-03	1.47E-04	2.94E+01	5.64E-04	1.18E-02	5.39E-04	1.67E-01	
Flare	14	FLARE-1	6.84E-03		8.98E-03	4.89E-02				1.55E+01	1.02E-02	3.15E+00	2.85E-04	8.83E-02	
						F	Proposed Sour	ces							
Engine	15	ENG-2	3.61E-01	6.08E-02	5.16E-01	1.03E+00	3.65E-02	3.65E-02	1.11E-03	2.07E+02	4.33E-01	9.09E+00			2.16E+02
Treater Burner	16	HTRTRTR-2	5.39E-03	1.85E-03	9.80E-02	8.24E-02	7.45E-03	7.45E-03	5.88E-04	1.18E+02	2.25E-03	4.74E-02	2.16E-03	6.69E-01	1.18E+02
Oil Well Fugitives	17	FUG-2	1.24E-02	6.87E-04							1.37E-01	2.89E+00			2.89E+00
Oil Tank	18	OILTK-4	1.23E-01	2.95E-02	1.09E-02	5.92E-02				1.88E+01	2.06E-02	4.33E-01	3.45E-04	1.07E-01	1.94E+01
Oil Tank	19	OILTK-5	1.23E-01	2.95E-02	1.09E-02	5.92E-02				1.88E+01	2.06E-02	4.33E-01	3.45E-04	1.07E-01	1.94E+01
Oil Tank	20	OILTK-6	1.23E-01	2.95E-02	1.09E-02	5.92E-02				1.88E+01	2.06E-02	4.33E-01	3.45E-04	1.07E-01	1.94E+01
Oil Tank Unloading	21	OILTKLOAD-2	1.34E+00	2.42E-01							1.69E-01	6.11E+01			6.11E+01
Pneumatic Controllers	22	PCONT-2	2.02E-02								2.20E-01	4.62E+00			4.62E+00
Water Tank	23	PWTANK-2	6.25E-03	2.91E-04	3.02E-03	1.64E-02				5.23E+00	2.13E-02	4.46E-01	9.58E-05	2.97E-02	5.70E+00
Small Storage Tanks	24	SMTANKS-2	4.69E-03												
Heater	25	TANKHTR4	1.35E-03	4.63E-04	2.45E-02	2.06E-02	1.86E-03	1.86E-03	1.47E-04	2.94E+01	5.64E-04	1.18E-02	5.39E-04	1.67E-01	
Heater	26	TANKHTR5	1.35E-03	4.63E-04	2.45E-02	2.06E-02	1.86E-03	1.86E-03	1.47E-04	2.94E+01	5.64E-04	1.18E-02	5.39E-04	1.67E-01	
Heater	27	TANKHTR6	1.35E-03	4.63E-04	2.45E-02	2.06E-02	1.86E-03	1.86E-03	1.47E-04	2.94E+01	5.64E-04	1.18E-02	5.39E-04	1.67E-01	
Flare	28	FLARE-2	2.81E-02		3.68E-02	2.00E-01				6.37E+01	4.17E-02	1.29E+01	1.17E-03	3.62E-01	
Totals	s (lb/hr)		2.21E+01	3.94E+00	1.45E+00	2.81E+00	7.38E-02	7.38E-02	3.51E-03	8.37E+02	4.06E+00	1.68E+02	1.04E-02	3.22E+00	7.34E+02

 $**N_2O$  emissions have not been estimated for engines due to the absence of an AP-42 emission factor (AP-42, Section 3.2.3.4).

#### Criteria Pollutant Emission Summary

							Unco	ontrolled PTE (	lb/hr)						
															Total
Туре	ID No.	Name	VOC	HAP	NOx	CO	PM <sub>10</sub>	PM <sub>2.5</sub>	SO <sub>2</sub>	CO2	CH₄	CO <sub>2</sub> e	N <sub>2</sub> O	CO <sub>2</sub> e	CO <sub>2</sub> e
							Existing Source	es			- i				_
Engine	1	ENG-1	3.52E-01	1.87E-02	5.03E-01	1.01E+00	1.12E-02	1.12E-02	3.40E-04	6.35E+01	1.33E-01	2.79E+00	_		6.63E+01
Treater Burner	2	HTRTRTR-1	5.39E-03	1.85E-03	9.80E-02	8.24E-02	7.45E-03	7.45E-03	5.88E-04	1.18E+02	2.25E-03	4.74E-02	2.16E-03	6.69E-01	1.18E+02
Oil Well Fugitives	3	FUG-1	1.24E-02	6.87E-04							1.37E-01	2.89E+00	_		2.89E+00
Oil Tank	4	OILTK-1	1.37E+00	3.20E-01							2.24E-01	4.70E+00			4.70E+00
Oil Tank	5	OILTK-2	1.37E+00	3.20E-01							2.24E-01	4.70E+00			4.70E+00
Oil Tank	6	OILTK-3	1.37E+00	3.20E-01							2.24E-01	4.70E+00			4.70E+00
Oil Tank Unloading	7	OILTKLOAD-1	1.94E+01	3.50E+00							2.45E+00	6.11E+01			6.11E+01
Pneumatic Controllers	8	PCONT-1	2.02E-02								2.20E-01	4.62E+00			4.62E+00
Water Tank	9	PWTANK-1	6.25E-02	2.91E-03							2.13E-01	4.46E+00			4.46E+00
Small Storage Tanks	10	SMTANKS-1	4.69E-03												
Heater	11	TANKHTR1	1.35E-03	4.63E-04	2.45E-02	2.06E-02	1.86E-03	1.86E-03	1.47E-04	2.94E+01	5.64E-04	1.18E-02	5.39E-04	1.67E-01	
Heater	12	TANKHTR2	1.35E-03	4.63E-04	2.45E-02	2.06E-02	1.86E-03	1.86E-03	1.47E-04	2.94E+01	5.64E-04	1.18E-02	5.39E-04	1.67E-01	
Heater	13	TANKHTR3	1.35E-03	4.63E-04	2.45E-02	2.06E-02	1.86E-03	1.86E-03	1.47E-04	2.94E+01	5.64E-04	1.18E-02	5.39E-04	1.67E-01	
Flare	14	FLARE-1	6.84E-03		8.98E-03	4.89E-02				1.55E+01	1.02E-02	3.15E+00	2.85E-04	8.83E-02	
						F	Proposed Sour	ces							
Engine	15	ENG-2	3.61E-01	6.08E-02	5.16E-01	1.03E+00	3.65E-02	3.65E-02	1.11E-03	2.07E+02	4.33E-01	9.09E+00			2.16E+02
Treater Burner	16	HTRTRTR-2	5.39E-03	1.85E-03	9.80E-02	8.24E-02	7.45E-03	7.45E-03	5.88E-04	1.18E+02	2.25E-03	4.74E-02	2.16E-03	6.69E-01	1.18E+02
Oil Well Fugitives	17	FUG-2	1.24E-02	6.87E-04							1.37E-01	2.89E+00			2.89E+00
Oil Tank	18	OILTK-4	6.16E+00	1.48E+00							1.03E+00	2.17E+01			2.17E+01
Oil Tank	19	OILTK-5	6.16E+00	1.48E+00							1.03E+00	2.17E+01			2.17E+01
Oil Tank	20	OILTK-6	6.16E+00	1.48E+00							1.03E+00	2.17E+01			2.17E+01
Oil Tank Unloading	21	OILTKLOAD-2	1.94E+01	3.50E+00							2.45E+00	6.11E+01			6.11E+01
Pneumatic Controllers	22	PCONT-2	2.02E-02								2.20E-01	4.62E+00			4.62E+00
Water Tank	23	PWTANK-2	3.13E-01	1.46E-02							1.06E+00	2.23E+01			2.23E+01
Small Storage Tanks	24	SMTANKS-2	4.69E-03												
Heater	25	TANKHTR4	1.35E-03	4.63E-04	2.45E-02	2.06E-02	1.86E-03	1.86E-03	1.47E-04	2.94E+01	5.64E-04	1.18E-02	5.39E-04	1.67E-01	
Heater	26	TANKHTR5	1.35E-03	4.63E-04	2.45E-02	2.06E-02	1.86E-03	1.86E-03	1.47E-04	2.94E+01	5.64E-04	1.18E-02	5.39E-04	1.67E-01	
Heater	27	TANKHTR6	1.35E-03	4.63E-04	2.45E-02	2.06E-02	1.86E-03	1.86E-03	1.47E-04	2.94E+01	5.64E-04	1.18E-02	5.39E-04	1.67E-01	
Flare	28	FLARE-2	2.81E-02		3.68E-02	2.00E-01				6.37E+01	4.17E-02	1.29E+01	1.17E-03	3.62E-01	
		·													
			6.26E+01	1.25E+01	1.41E+00	2.57E+00	7.38E-02	7.38E-02	3.51E-03	7.62E+02	1.13E+01	2.71E+02	9.00E-03	2.79E+00	7.62E+02

\*\*N<sub>2</sub>O emissions have not been estimated for engines due to the absence of an AP-42 emission factor (AP-42, Section 3.2.3.4).

#### Criteria Pollutant Emission Summary

							Cont	rolled Actuals	(TPY)						
									`				1		Total
Туре	ID No.	Name	voc	HAP	NOx	со	PM10	PM <sub>2.5</sub>	SO <sub>2</sub>	CO <sub>2</sub>	CH₄	CO <sub>2</sub> e	N <sub>2</sub> O"	CO <sub>2</sub> e	CO <sub>2</sub> e
						- <b>L</b> L	Existing Source	es	- <b>L L</b>						
Engine	1	ENG-1	1.54E+00	8.17E-02	2.20E+00	4.40E+00	4.91E-02	4.91E-02	1.49E-03	2.78E+02	5.82E-01	1.22E+01			2.90E+02
Treater Burner	2	HTRTRTR-1	2.36E-02	8.11E-03	4.29E-01	3.61E-01	3.26E-02	3.26E-02	2.58E-03	5.15E+02	9.88E-03	2.07E-01	9.45E-03	2.93E+00	5.18E+02
Oil Well Fugitives	3	FUG-1	5.42E-02	1.01E-02							6.02E-01	1.26E+01			1.26E+01
Oil Tank	4	OILTK-1	1.20E-01	2.80E-02	1.02E-02	5.57E-02				1.77E+01	1.96E-02	4.12E-01	3.24E-04	1.01E-01	1.82E+01
Oil Tank	5	OILTK-2	1.20E-01	2.80E-02	1.02E-02	5.57E-02				1.77E+01	1.96E-02	4.12E-01	3.24E-04	1.01E-01	1.82E+01
Oil Tank	6	OILTK-3	1.20E-01	2.80E-02	1.02E-02	5.57E-02				1.77E+01	1.96E-02	4.12E-01	3.24E-04	1.01E-01	1.82E+01
Oil Tank Unloading	7	OILTKLOAD-1	2.31E+00	4.17E-01							2.91E-01	7.28E+00			7.28E+00
Pneumatic Controllers	8	PCONT-1	8.85E-02								9.64E-01	2.02E+01			2.02E+01
Water Tank	9	PWTANK-1	5.48E-03	2.55E-04	2.65E-03	1.44E-02				4.58E+00	1.86E-02	3.91E-01	8.39E-05	2.60E-02	4.99E+00
Small Storage Tanks	10	SMTANKS-1	2.05E-02												
Heater	11	TANKHTR1	5.90E-03	2.03E-03	1.07E-01	9.02E-02	8.16E-03	8.16E-03	6.44E-04	1.29E+02	2.47E-03	5.19E-02	2.36E-03	7.32E-01	
Heater	12	TANKHTR2	5.90E-03	2.03E-03	1.07E-01	9.02E-02	8.16E-03	8.16E-03	6.44E-04	1.29E+02	2.47E-03	5.19E-02	2.36E-03	7.32E-01	
Heater	13	TANKHTR3	5.90E-03	2.03E-03	1.07E-01	9.02E-02	8.16E-03	8.16E-03	6.44E-04	1.29E+02	2.47E-03	5.19E-02	2.36E-03	7.32E-01	
Flare	14	FLARE-1	3.00E-02		3.93E-02	2.14E-01				6.80E+01	4.45E-02	1.38E+01	1.25E-03	3.87E-01	
						F	Proposed Sour	ces	- <b>L L</b>						
Engine	15	ENG-2													
Treater Burner	16	HTRTRTR-2													
Oil Well Fugitives	17	FUG-2													
Oil Tank	18	OILTK-4													
Oil Tank	19	OILTK-5													
Oil Tank	20	OILTK-6													
Oil Tank Unloading	21	OILTKLOAD-2													
Pneumatic Controllers	22	PCONT-2													
Water Tank	23	PWTANK-2													
Small Storage Tanks	24	SMTANKS-2													
Heater	25	TANKHTR4													
Heater	26	TANKHTR5													
Heater	27	TANKHTR6													
Flare	28	FLARE-2													
			L				L								
	I	L	H	H			<b>—</b>								
L	I	L		L			L				L		L		
			4.45E+00	6.07E-01	3.03E+00	5.43E+00	1.06E-01	1.06E-01	6.00E-03	1.31E+03	2.58E+00	6.82E+01	1.88E-02	5.84E+00	9.09E+02

#### Criteria Pollutant Emission Summary

							Uncor	trolled Actuals	s (TPY)						
															Total
Туре	ID No.	Name	VOC	HAP	NOx	CO	PM <sub>10</sub>	PM <sub>2.5</sub>	SO <sub>2</sub>	CO <sub>2</sub>	CH₄	CO <sub>2</sub> e	N <sub>2</sub> O	CO <sub>2</sub> e	CO <sub>2</sub> e
				· · ·		<u> </u>	Existing Source	es							
Engine	1	ENG-1	1.54E+00	8.17E-02	2.20E+00	4.40E+00	4.91E-02	4.91E-02	1.49E-03	2.78E+02	5.82E-01	1.22E+01			2.90E+02
Treater Burner	2	HTRTRTR-1	2.36E-02	8.11E-03	4.29E-01	3.61E-01	3.26E-02	3.26E-02	2.58E-03	5.15E+02	9.88E-03	2.07E-01	9.45E-03	2.93E+00	5.18E+02
Oil Well Fugitives	3	FUG-1	5.42E-02	1.01E-02							6.02E-01	1.26E+01			1.26E+01
Oil Tank	4	OILTK-1	6.00E+00	1.40E+00							9.80E-01	2.06E+01			2.06E+01
Oil Tank	5	OILTK-2	6.00E+00	1.40E+00							9.80E-01	2.06E+01			2.06E+01
Oil Tank	6	OILTK-3	6.00E+00	1.40E+00							9.80E-01	2.06E+01			2.06E+01
Oil Tank Unloading	7	OILTKLOAD-1	2.31E+00	4.17E-01							2.91E-01	7.28E+00			7.28E+00
Pneumatic Controllers	8	PCONT-1	8.85E-02								9.64E-01	2.02E+01			2.02E+01
Water Tank	9	PWTANK-1	2.74E-01	1.28E-02							9.31E-01	1.95E+01			
Small Storage Tanks	10	SMTANKS-1	2.05E-02												
Heater	11	TANKHTR1	5.90E-03	2.03E-03	1.07E-01	9.02E-02	8.16E-03	8.16E-03	6.44E-04	1.29E+02	2.47E-03	5.19E-02	2.36E-03	7.32E-01	
Heater	12	TANKHTR2	5.90E-03	2.03E-03	1.07E-01	9.02E-02	8.16E-03	8.16E-03	6.44E-04	1.29E+02	2.47E-03	5.19E-02	2.36E-03	7.32E-01	
Heater	13	TANKHTR3	5.90E-03	2.03E-03	1.07E-01	9.02E-02	8.16E-03	8.16E-03	6.44E-04	1.29E+02	2.47E-03	5.19E-02	2.36E-03	7.32E-01	
Flare	14	FLARE-1	3.00E-02		3.93E-02	2.14E-01				6.80E+01	4.45E-02	1.38E+01	1.25E-03	3.87E-01	
						F	Proposed Sour	ces							
Engine	15	ENG-2													
Treater Burner	16	HTRTRTR-2													
Oil Well Fugitives	17	FUG-2													
Oil Tank	18	OILTK-4													
Oil Tank	19	OILTK-5													
Oil Tank	20	OILTK-6													
Oil Tank Unloading	21	OILTKLOAD-2													
Pneumatic Controllers	22	PCONT-2													
Water Tank	23	PWTANK-2													
Small Storage Tanks	24	SMTANKS-2													
Heater	25	TANKHTR4													
Heater	26	TANKHTR5													
Heater	27	TANKHTR6													
Flare	28	FLARE-2													
												· · · · · · · · · · · · · · · · · · ·	<b></b>		
I			2.24E+01	4.74E+00	2.99E+00	5.25E+00	1.06E-01	1.06E-01	6.00E-03	1.25E+03	6.37E+00	1.48E+02	1.78E-02	5.51E+00	9.11E+02

							Co	ontrolled PTE (T	PY)				
Туре	ID No.	Name	Benzene	Toluene	Ethyl- benzene	Xylene	2,2,4-Tri- methylpentane	Acrolien	Acetal- dehyde	n-Hexane	Methanol	1,3- Butadiene	Formal- dehyde
			<u> </u>	<u> </u>	· · · ·	Existing	Sources		<u> </u>				
Engine	1	ENG-1	4.00E-03	1.41E-03	6.27E-05	4.93E-04		6.65E-03	7.06E-03		7.74E-03	1.68E-03	5.19E-02
Treater Burner	2	HTRTRTR-1	9.02E-06	1.46E-05						7.73E-03			3.22E-04
Oil Well Fugitives	3	FUG-1	1.30E-03	1.25E-03	6.22E-05	2.41E-04	1.56E-04						
Oil Tank	4	OILTK-1	6.23E-04	1.42E-03	1.63E-04	2.84E-04	3.28E-04			2.52E-02			
Oil Tank	5	OILTK-2	6.23E-04	1.42E-03	1.63E-04	2.84E-04	3.28E-04			2.52E-02			
Oil Tank	6	OILTK-3	6.23E-04	1.42E-03	1.63E-04	2.84E-04	3.28E-04			2.52E-02			
Oil Tank Unloading	7	OILTKLOAD-1	9.26E-03	2.11E-02	2.42E-03	4.21E-03	4.88E-03			3.75E-01			
Pneumatic Controllers	8	PCONT-1	2.12E-03	2.05E-03	1.02E-04	3.94E-04	2.54E-04						
Water Tank	9	PWTANK-1	5.48E-05	1.64E-04	3.29E-06	3.29E-05							
Small Storage Tanks	10	SMTANKS-1									2.05E-02		
Heater	11	TANKHTR1	2.25E-06	3.65E-06						1.93E-03			8.05E-05
Heater	12	TANKHTR2	2.25E-06	3.65E-06						1.93E-03			8.05E-05
Heater	13	TANKHTR3	2.25E-06	3.65E-06						1.93E-03			8.05E-05
Flare	14	FLARE-1											
	1				1	Proposed	d Sources		-				
Engine	15	ENG-2	1.30E-02	4.60E-03	2.04E-04	1.61E-03		2.17E-02	2.30E-02		2.52E-02	5.47E-03	1.69E-01
Treater Burner	16	HTRTRTR-2	9.02E-06	1.46E-05						7.73E-03			3.22E-04
Oil Well Fugitives	17	FUG-2	1.30E-03	1.25E-03	6.22E-05	2.41E-04	1.56E-04						
Oil Tank	18	OILTK-4	2.87E-03	6.56E-03	7.50E-04	1.31E-03	1.51E-03			1.16E-01			
Oil Tank	19	OILTK-5	2.87E-03	6.56E-03	7.50E-04	1.31E-03	1.51E-03			1.16E-01			
Oil Tank	20	OILTK-6	2.87E-03	6.56E-03	7.50E-04	1.31E-03	1.51E-03			1.16E-01			
Oil Tank Unloading	21	OIL TKL OAD-2	3 19E-03	7 29E-03	8.34E-04	1.45E-03	1.68E-03			1.29E-01			
Pneumatic Controllers	22	PCONT-2	2.12E-03	2.05E-03	1.02E-04	3.94E-04	2.54E-04			1.202 01			
Water Tank	23	PWTANK-2	2 74E-04	8 21E-04	1.64E-05	1.64E-04							
Small Storage Tanks	24	SMTANKS-2									2.05E-02		
Heater	25	TANKHTR4	2.25E-06	3.65E-06						1.93E-03	2.002.02		8.05E-05
Heater	26	TANKHTR5	2.25E-06	3.65E-06						1.93E-03			8.05E-05
Heater	27	TANKHTR6	2.25E-06	3.65E-06						1.93E-03			8.05E-05
Flare	28	FLARE-2	2.202 00	5.002.00									5.002 00
		<u> </u>											
L		· J		·]	·	·	L]	·	· I	·	·	L	· · · · · ·
Total	s (TPY)		4.72E-02	6.60E-02	6.60E-03	1.40E-02	1.29E-02	2.83E-02	3.01E-02	9.56E-01	7.40E-02	7.14E-03	2.22E-01
ц.							· · · · ·			<u>.</u>		· · · · · · · · ·	

							Unc	ontrolled PTE (	TPY)				
Туре	ID No.	Name	Benzene	Toluene	Ethyl- benzene	Xylene	2,2,4-Tri- methylpentane	Acrolien	Acetal- dehyde	n-Hexane	Methanol	1,3- Butadiene	Formal- dehyde
		· ·				Existing	Sources						-
Engine	1	ENG-1	4.00E-03	1.41E-03	6.27E-05	4.93E-04		6.65E-03	7.06E-03		7.74E-03	1.68E-03	5.19E-02
Treater Burner	2	HTRTRTR-1	9.02E-06	1.46E-05						7.73E-03			3.22E-04
Oil Well Fugitives	3	FUG-1	1.30E-03	1.25E-03	6.22E-05	2.41E-04	1.56E-04						
Oil Tank	4	OILTK-1	3.12E-02	7.11E-02	8.13E-03	1.42E-02	1.64E-02			1.26E+00			
Oil Tank	5	OILTK-2	3.12E-02	7.11E-02	8.13E-03	1.42E-02	1.64E-02			1.26E+00			
Oil Tank	6	OILTK-3	3.12E-02	7.11E-02	8.13E-03	1.42E-02	1.64E-02			1.26E+00			
Oil Tank Unloading	7	OILTKLOAD-1	9.26E-03	2.11E-02	2.42E-03	4.21E-03	4.88E-03			3.75E-01			
Pneumatic Controllers	8	PCONT-1	2.12E-03	2.05E-03	1.02E-04	3.94E-04	2.54E-04						
Water Tank	9	PWTANK-1	2.74E-03	8.21E-03	1.64E-04	1.64E-03							
Small Storage Tanks	10	SMTANKS-1									2.05E-02		
Heater	11	TANKHTR1	2.25E-06	3.65E-06						1.93E-03			8.05E-05
Heater	12	TANKHTR2	2.25E-06	3.65E-06						1.93E-03			8.05E-05
Heater	13	TANKHTR3	2.25E-06	3.65E-06						1.93E-03			8.05E-05
Flare	14	FLARE-1											
		J I.				Propose	d Sources						
Engine	15	ENG-2	1.30E-02	4.60E-03	2.04E-04	1.61E-03		2.17E-02	2.30E-02		2.52E-02	5.47E-03	1.69E-01
Treater Burner	16	HTRTRTR-2	9.02E-06	1.46E-05						7.73E-03			3.22E-04
Oil Well Fugitives	17	FUG-2	1.30E-03	1.25E-03	6.22E-05	2.41E-04	1.56E-04						
Oil Tank	18	OILTK-4	1.44E-01	3.28E-01	3.75E-02	6.54E-02	7.57E-02			5.82E+00			
Oil Tank	19	OIL TK-5	1.44E-01	3.28E-01	3.75E-02	6.54E-02	7.57E-02			5.82E+00			
Oil Tank	20	OILTK-6	1.44E-01	3.28E-01	3.75E-02	6.54E-02	7.57E-02			5.82E+00			
Oil Tank Unloading	21	OII TKI OAD-2	4.63E-02	1.06E-01	1.21E-02	2.11E-02	2.44E-02			1.87E+00			
Pneumatic Controllers	22	PCONT-2	2.12E-03	2.05E-03	1.02E-04	3.94E-04	2.54E-04						
Water Tank	23	PWTANK-2	1.37E-02	4.11E-02	8.21E-04	8.21E-03							
Small Storage Tanks	24	SMTANKS-2									2.05E-02		
Heater	25	TANKHTR4	2 25E-06	3.65E-06						1 93E-03			8.05E-05
Heater	26	TANKHTR5	2.25E-06	3.65E-06						1.93E-03			8.05E-05
Heater	27	TANKHTRG	2.25E-06	3.65E-06						1.00E-00			8.05E-05
Flare	28	FLARE-2	2.202-00	0.002-00						1.002-00			0.00E-00
	20	I LANC-Z											$\vdash$
	+	<u> </u>						H					
	-							H					
L		+I	·	· · · · · · · · · · · · · · · · · · ·	l	· · · · · · · · · · · · · · · · · · ·		· · · · · · · · · · · · · · · · · · ·	·	·	·	·	<u>ا</u>
Tota	s (TPY)		6.21E-01	1.39E+00	1.53E-01	2.77E-01	3.07E-01	2.83E-02	3.01E-02	2.35E+01	7.40E-02	7.14E-03	2.22E-01

							Co	ntrolled PTE (lb	/hr)				
Туре	ID No.	Name	Benzene	Toluene	Ethyl- benzene	Xylene	2,2,4-Tri- methylpentane	Acrolien	Acetal- dehyde	n-Hexane	Methanol	1,3- Butadiene	Formal- dehyde
						Existing	Sources						
Engine	1	ENG-1	9.12E-04	3.22E-04	1.43E-05	1.13E-04		1.52E-03	1.61E-03		1.77E-03	3.83E-04	1.18E-02
Treater Burner	2	HTRTRTR-1	2.06E-06	3.33E-06						1.76E-03			7.35E-05
Oil Well Fugitives	3	FUG-1	2.96E-04	2.86E-04	1.42E-05	5.50E-05	3.55E-05						
Oil Tank	4	OILTK-1	1.42E-04	3.25E-04	3.71E-05	6.48E-05	7.50E-05			5.76E-03			
Oil Tank	5	OILTK-2	1.42E-04	3.25E-04	3.71E-05	6.48E-05	7.50E-05			5.76E-03			
Oil Tank	6	OILTK-3	1.42E-04	3.25E-04	3.71E-05	6.48E-05	7.50E-05			5.76E-03			
Oil Tank Unloading	7	OILTKLOAD-1	7.78E-02	1.78E-01	2.03E-02	3.54E-02	4.10E-02			3.15E+00			
Pneumatic Controllers	8	PCONT-1	4.85E-04	4.67E-04	2.32E-05	8.99E-05	5.80E-05						
Water Tank	9	PWTANK-1	1.25E-05	3.75E-05	7.50E-07	7.50E-06							
Small Storage Tanks	10	SMTANKS-1									4.68E-03		
Heater	11	TANKHTR1	5.10E-07	8.30E-07						4.41E-04			1.84E-05
Heater	12	TANKHTR2	5.10E-07	8.30E-07						4.41E-04			1.84E-05
Heater	13	TANKHTR3	5.10E-07	8.30E-07						4.41E-04			1.84E-05
Flare	14	FLARE-1											
						Proposed	d Sources						
Engine	15	ENG-2	2.97E-03	1.05E-03	4.67E-05	3.67E-04		4.95E-03	5.25E-03		5.76E-03	1.25E-03	3.86E-02
Treater Burner	16	HTRTRTR-2	2.06E-06	3.33E-06						1.76E-03			7.35E-05
Oil Well Fugitives	17	FUG-2	2.96E-04	2.86E-04	1.42E-05	5.50E-05	3.55E-05						
Oil Tank	18	OILTK-4	6.56E-04	1.50E-03	1.71E-04	2.99E-04	3.46E-04			2.66E-02			
Oil Tank	19	OILTK-5	6.56E-04	1.50E-03	1.71E-04	2.99E-04	3.46E-04			2.66E-02			
Oil Tank	20	OILTK-6	6.56E-04	1.50E-03	1.71E-04	2.99E-04	3.46E-04			2.66E-02			
Oil Tank Unloading	21	OILTKLOAD-2	5.37E-03	1.22E-02	1.40E-03	2.44E-03	2.83E-03			2.17E-01			
Pneumatic Controllers	22	PCONT-2	4.85E-04	4.67E-04	2.32E-05	8.99E-05	5.80E-05						
Water Tank	23	PWTANK-2	6.25E-05	1.88E-04	3.75E-06	3.75E-05							
Small Storage Tanks	24	SMTANKS-2									4.68E-03		
Heater	25	TANKHTR4	5.10E-07	8.30E-07						4.41E-04			1.84E-05
Heater	26	TANKHTR5	5.10E-07	8.30E-07						4.41E-04			1.84E-05
Heater	27	TANKHTR6	5.10E-07	8.30E-07						4.41E-04			1.84E-05
Flare	28	FLARE-2											
		• • • •			·		,		·+	, ,		, , , , , , , , , , , , , , , , , , , ,	, ,
Total	s (lb/hr)		9.11E-02	1.98E-01	2.25E-02	3.98E-02	4.53E-02	6.47E-03	6.86E-03	3.47E+00	1.69E-02	1.63E-03	5.07E-02

							Unc	ontrolled PTE (I	b/hr)				
Туре	ID No.	Name	Benzene	Toluene	Ethyl- benzene	Xylene	2,2,4-Tri- methylpentane	Acrolien	Acetal- dehyde	n-Hexane	Methanol	1,3- Butadiene	Formal- dehyde
						Existing	Sources						
Engine	1	ENG-1	9.12E-04	3.22E-04	1.43E-05	1.13E-04		1.52E-03	1.61E-03		1.77E-03	3.83E-04	1.18E-02
Treater Burner	2	HTRTRTR-1	2.06E-06	3.33E-06						1.76E-03			7.35E-05
Oil Well Fugitives	3	FUG-1	2.96E-04	2.86E-04	1.42E-05	5.50E-05	3.55E-05						
Oil Tank	4	OILTK-1	7.12E-03	1.62E-02	1.86E-03	3.24E-03	3.75E-03			2.88E-01			
Oil Tank	5	OILTK-2	7.12E-03	1.62E-02	1.86E-03	3.24E-03	3.75E-03			2.88E-01			
Oil Tank	6	OILTK-3	7.12E-03	1.62E-02	1.86E-03	3.24E-03	3.75E-03			2.88E-01			
Oil Tank Unloading	7	OILTKLOAD-1	7.78E-02	1.78E-01	2.03E-02	3.54E-02	4.10E-02			3.15E+00			
Pneumatic Controllers	8	PCONT-1	4.85E-04	4.67E-04	2.32E-05	8.99E-05	5.80E-05						
Water Tank	9	PWTANK-1	6.25E-04	1.88E-03	3.75E-05	3.75E-04							
Small Storage Tanks	10	SMTANKS-1									4.68E-03		
Heater	11	TANKHTR1	5.10E-07	8.30E-07						4.41E-04			1.84E-05
Heater	12	TANKHTR2	5.10E-07	8.30E-07						4.41E-04			1.84E-05
Heater	13	TANKHTR3	5.10E-07	8.30E-07						4.41E-04			1.84E-05
Flare	14	FLARE-1											
						Proposed	d Sources			- J J.			
Engine	15	ENG-2	2.97E-03	1.05E-03	4.67E-05	3.67E-04		4.95E-03	5.25E-03		5.76E-03	1.25E-03	3.86E-02
Treater Burner	16	HTRTRTR-2	2.06E-06	3.33E-06						1.76E-03			7.35E-05
Oil Well Fugitives	17	FUG-2	2.96E-04	2.86E-04	1.42E-05	5.50E-05	3.55E-05						
Oil Tank	18	OILTK-4	3.28E-02	7.49E-02	8.56E-03	1.49E-02	1.73E-02			1.33E+00			
Oil Tank	19	OILTK-5	3.28E-02	7.49E-02	8.56E-03	1.49E-02	1.73E-02			1.33E+00			
Oil Tank	20	OILTK-6	3.28E-02	7.49E-02	8.56E-03	1.49E-02	1.73E-02			1.33E+00			
Oil Tank Unloading	21	OILTKLOAD-2	7.78E-02	1.78E-01	2.03E-02	3.54E-02	4.10E-02			3.15E+00			
Pneumatic Controllers	22	PCONT-2	4.85E-04	4.67E-04	2.32E-05	8.99E-05	5.80E-05						
Water Tank	23	PWTANK-2	3.13E-03	9.38E-03	1.88E-04	1.88E-03							
Small Storage Tanks	24	SMTANKS-2									4.68E-03		
Heater	25	TANKHTR4	5.10E-07	8.30E-07						4.41E-04			1.84E-05
Heater	26	TANKHTR5	5.10E-07	8.30E-07						4.41E-04			1.84E-05
Heater	27	TANKHTR6	5.10E-07	8.30E-07						4.41E-04			1.84E-05
Flare	28	FLARE-2											
L					,I	·	,i		·	·	,I	++	,I
Total	s (lb/hr)		2.85E-01	6.43E-01	7.22E-02	1.28E-01	1.45E-01	6.47E-03	6.86E-03	1.12E+01	1.69E-02	1.63E-03	5.07E-02

1. Company:	Newfield Exploration		Р	Potential Emission	S
2. Site/Source:	MAMIE 4-25-3-3WH		3. Date: 2/7/2019		
4. Type of Operatio	n: Oil and Gas	Production Engine	)		
5. Emission Point:	ID Number	Name	7. Identification and Description of	of Control Equipment	
	1	ENG-1			
6. Description of Eq	uipment:		None		
Baldor 170 kW	/ Gen, NG, 277/480 V				
8. Fuel Consumptio	n: 22.18	MMscf/yr	9. Operating Schedule:	8,760	Hours/yr

Pollutant	Uncontrolled Emissions	Controlled Emissions	
	(TPY)	(TPY)	
PM	4.91E-02	4.91E-02	PM Particulate Matter
PM <sub>10</sub>	4.91E-02	4.91E-02	$PM_{12} = PM$ less than 10 microns in size
PM <sub>2.5</sub>	4.91E-02	4.91E-02	$PM_{0.5}$ - PM less than 2.5 microns in size
SO <sub>X</sub>	1.49E-03	1.49E-03	$SO_{\rm y}$ - Sulfur Oxides
NO <sub>X</sub>	2.20E+00	2.20E+00	NO <sub>x</sub> - Nitrogen Oxides
CO	4.40E+00	4.40E+00	CO - Carbon Monoxide
VOC	1.54E+00	1.54E+00	VOC - Volatile Organic Compound
Pb			Pb - Lead and lead compounds
Fluorides			Fluorides - Gaseous and particulates
$H_2SO_4$			H <sub>2</sub> SO <sub>4</sub> - Sulfuric Acid Mist
H <sub>2</sub> S			H <sub>2</sub> S - Hydrogen Sulfide
TRS			TRS - Total Reduced Sulfur
RSC			RSC - Reduced Sulfur Compounds

Potential Emissions Attachment 1 of 14

1. Company:	Newfield Exploration			Actual Emissions	
2. Site/Source:	MAMIE 4-25-3-3WH		3. Date: 2/7/2019		
4. Type of Operatio	n: Oil and Gas	Production Engine	)		
5. Emission Point:	ID Number	Name	7. Identification and Description	of Control Equipment	
	1	ENG-1			
6. Description of Equipment:			None		
Baldor 170 kV	/ Gen, NG, 277/480 V				
8. Fuel Consumptio	on: 22.18	MMscf/yr	.9. Operating Schedule:	8,760	Hours/yr

Pollutant	Uncontrolled Emissions	Controlled Emissions	
	(TPY)	(TPY)	
PM	4.91E-02	4.91E-02	DM Derticulate Matter
PM <sub>10</sub>	4.91E-02	4.91E-02	PM - PM less than 10 microns in size
PM <sub>2.5</sub>	4.91E-02	4.91E-02	$PM_{0.5}$ - PM less than 2.5 microns in size
SO <sub>X</sub>	1.49E-03	1.49E-03	$SO_{\rm v}$ - Sulfur Oxides
NO <sub>X</sub>	2.20E+00	2.20E+00	NO <sub>v</sub> - Nitrogen Oxides
CO	4.40E+00	4.40E+00	CO - Carbon Monoxide
VOC	1.54E+00	1.54E+00	VOC - Volatile Organic Compound
Pb			Pb - Lead and lead compounds
Fluorides			Fluorides - Gaseous and particulates
$H_2SO_4$			H <sub>2</sub> SO <sub>4</sub> - Sulfuric Acid Mist
H <sub>2</sub> S			H <sub>2</sub> S - Hydrogen Sulfide
TRS			TRS - Total Reduced Sulfur
RSC			RSC - Reduced Sulfur Compounds

Actual Emissions Attachment 1 of 14 Newfield MAMIE 4-25-3-3WH

ENG-1



NOx, CO & VOC Emission Factors are from manufacturer's data. SO2, PM, & PM2.5 & HAPs Emission Factors are from AP-42 Table 3.2-1, Table 3.2-2, or Table 3.2-3.

ENG-1 Calculation Page 1 of 1

1. Company:	Newfield Exploration			Potential Emissions	
2. Site/Source:	Site/Source: MAMIE 4-25-3-3WH		3. Date: 2/7/2019		
4. Type of Operation	n: Oil and Gas	Production Treate	er Burner		
5. Emission Point:	ID Number 2	Name HTRTRTR-1	7. Identification and Descripti	on of Control Equipment	
6. Description of Equipment: Oil/Water Separation Unit		None			
8. Type of Fuel Use	d: Na	tural Gas	9. Amount of Fuel Used:	8,760,000,000	Btu/year
10. Burner Rating:	1,000,000	BTU/hr	11. Operating Schedule:	8,760	Hours/yr

Pollutant	Uncontrolled Emissions	Controlled Emissions	
	(TPY)	(TPY)	
PM	3.26E-02	3.26E-02	DM Barticulate Matter
PM <sub>10</sub>	3.26E-02	3.26E-02	PM = PM less than 10 microns in size
PM <sub>2.5</sub>	3.26E-02	3.26E-02	$PM_{}$ PM less than 2.5 microns in size
SO <sub>X</sub>	2.58E-03	2.58E-03	$SO_{\rm X}$ - Sulfur Oxides
NO <sub>X</sub>	4.29E-01	4.29E-01	NO <sub>×</sub> - Nitrogen Oxides
CO	3.61E-01	3.61E-01	CO - Carbon Monoxide
VOC	2.36E-02	2.36E-02	VOC - Volatile Organic Compound
Pb			Pb - Lead and lead compounds
Fluorides			Fluorides - Gaseous and particulates
$H_2SO_4$			H <sub>2</sub> SO <sub>4</sub> - Sulfuric Acid Mist
H <sub>2</sub> S			H <sub>2</sub> S - Hydrogen Sulfide
TRS			TRS - Total Reduced Sulfur
RSC			RSC - Reduced Sulfur Compounds

Potential Emissions Attachment 2 of 14

1. Company: Ne	ewfield Exploration			Actual Emissions	
2. Site/Source: MAMIE 4-25-3-3WH			3. Date: 2/7/2019		
4. Type of Operation: Oil and Gas Production Treate			er Burner		
5. Emission Point:	ID Number Name	•	7. Identification and Description of Control Equipment		
	2 HTRT	RTR-1			
6. Description of Equip	ment:		None		
Oil/Water Separa	tion Unit				
8. Type of Fuel Used:	Natural Ga	Natural Gas		8,760,000,000	Btu/year
10. Burner Rating:	1,000,000	BTU/hr	11. Operating Schedule:	8,760 I	Hours/yr
Dollutont	Lincontrolled Emissions		entrolled Emissions		
Pollulani	(TPY)		(TPY)		
PM	3.26E-02		3.26E-02		
PM <sub>10</sub>	3.26E-02	3.26E-02		<ul> <li>PM - Particulate Matter</li> <li>PM<sub>10</sub> - PM less than 10 microns in size</li> <li>PM<sub>22</sub> - PM less than 2.5 microns in size</li> </ul>	
PM <sub>2.5</sub>	3.26E-02	3.26E-02			
SO <sub>X</sub>	2.58E-03		2.58E-03	$SO_{v}$ - Sulfur Oxides	

SO<sub>X</sub> - Sulfur Oxides NO<sub>X</sub> - Nitrogen Oxides NO<sub>X</sub> 4.29E-01 4.29E-01 3.61E-01 CO 3.61E-01 CO - Carbon Monoxide VOC - Volatile Organic Compound Pb - Lead and lead compounds VOC 2.36E-02 2.36E-02 Pb Fluorides - Gaseous and particulates  $H_2SO_4$  - Sulfuric Acid Mist  $H_2S$  - Hydrogen Sulfide Fluorides  $H_2SO_4$  $H_2S$ TRS TRS - Total Reduced Sulfur RSC - Reduced Sulfur Compounds RSC

Actual Emissions Attachment 2 of 14
Newfield MAMIE 4-25-3-3WH						
Burner Rating 1,000,000 Btu/hr						
NOx: 0.10 lb/MMBtu x 1.00 MMBtu/hr = 9.80E-02 lb/hr   9.80E-02 lb/hr x 8,760 hr/yr x 1 ton / 2000 lb = 4.29E-01 TPY						
CO: 0.082 lb/MMBtu x 1.00 MMBtu/hr = 8.24E-02 lb/hr   8.24E-02 lb/hr x 8,760 hr/yr x 1 ton / 2000 lb = 3.61E-01 TPY						
VOC: 0.0054 lb/MMBtu x 1.00 MMBtu/hr = 5.39E-03 lb/hr   5.39E-03 lb/hr x 8,760 hr/yr x 1 ton / 2000 lb = 2.36E-02 TPY						
SO2: 0.0006 lb/MMBtu x 1.00 MMBtu/hr = 5.88E-04 lb/hr   5.88E-04 lb/hr x 8,760 hr/yr x 1 ton / 2000 lb = 2.58E-03 TPY						
PM: 0.0075 lb/MMBtu x 1.00 MMBtu/hr = 7.45E-03 lb/hr   T.45E-03 lb/hr x 8,760 hr/yr x 1 ton / 2000 lb = 3.26E-02 TPY						

Emission Factors are from AP-42 Table 1.4-1, 1.4-2, 1.4-3, & 1.4-4.

HTRTRTR-1 Calculation Page 1 of 2

			Newfield MAMIE 4-25	5-3-3WH		
			HTRTRTR	-1		
	Burner Rating	1,000,000	Btu/hr			
Benzene:	2.06E-06 lb/MMBtu 2.06E-06 lb/hr	x x	1.00 MMBtu/hr 8,760 hr/yr x	= 1 ton / 2000 lb =	<b>2.06E-06</b> lb/hr <b>9.02E-06</b> TPY	
Toluene:	3.33E-06 lb/MMBtu 3.33E-06 lb/hr	x x	1.00 MMBtu/hr 8,760 hr/yr x	= 1 ton / 2000 lb =	3.33E-06 lb/hr 1.46E-05 TPY	
n-Hexane:	1.76E-03 lb/MMBtu 1.76E-03 lb/hr	] x ] x	1.00 MMBtu/hr 8,760 hr/yr x	= 1 ton / 2000 lb =	<b>1.76E-03</b> lb/hr <b>7.73E-03</b> TPY	
Formaldehyde:	7.35E-05 lb/MMBtu 7.35E-05 lb/hr	x x	1.00 MMBtu/hr 8,760 hr/yr x	= 1 ton / 2000 lb =	7.35E-05   lb/hr     3.22E-04   TPY	

Emission Factors are from AP-42 Table 1.4-1, 1.4-2, 1.4-3, & 1.4-4.

HTRTRTR-1 Calculation Page 2 of 2

1. Company: N	ewfield Exploration		Potential Emissions
2. Site/Source: MAMIE 4-25-3-3WH			3. Date: 2/7/2019
4. Type of Operation:	Oil and Ga	s Production Well	Fugitives
5. Emission Point:	ID Number	Name	7. Identification and Description of Control Equipment
	3	FUG-1	N/A
6. Description of Equip	oment:		
Oil Well Fugitive	Emissions		

Pollutant	Uncontrolled Emissions (TPY)	Controlled Emissions (TPY)	
PM			PM - Particulato Mattor
PM <sub>10</sub>			$PM_{in} = PM$ less than 10 microns in size
PM <sub>2.5</sub>			$PM_{10}$ - PM less than 2.5 microns in size
SO <sub>X</sub>			SO <sub>2.5</sub> - Sulfur Oxides
NO <sub>X</sub>			NO Nitrogen Oxides
CO			CO - Carbon Monoxide
VOC	5.42E-02	5.42E-02	VOC - Volatile Organic Compound
Pb			Pb - Lead and lead compounds
Fluorides			Fluorides - Gaseous and particulates
$H_2SO_4$			H <sub>2</sub> SO <sub>4</sub> - Sulfuric Acid Mist
H <sub>2</sub> S			H <sub>2</sub> S - Hydrogen Sulfide
TRS			TRS - Total Reduced Sulfur
RSC			RSC - Reduced Sulfur Compounds

Potential Emissions Attachment 3 of 14

1. Company: N	Newfield Exploration		Actual Emissions
2. Site/Source:	/AMIE 4-25-3-3WH		3. Date: 2/7/2019
4. Type of Operation:	Oil and Ga	as Production Wel	Il Fugitives
5. Emission Point:	ID Number	Name	7. Identification and Description of Control Equipment
	3	FUG-1	N/A
6. Description of Equi	pment:		
Oil Well Fugitive	Emissions		

Pollutant	Uncontrolled Emissions (TPY)	Controlled Emissions (TPY)	
PM		· · ·	DM Darticulate Matter
PM <sub>10</sub>			PM - PARticulate Matter
PM <sub>2.5</sub>			$PM_{10} = PM$ less than 2.5 microns in size
SO <sub>X</sub>			$SO_{\rm v}$ - Sulfur Oxides
NO <sub>X</sub>			$NO_{\rm X}$ - Nitrogen Oxides
CO			CO - Carbon Monoxide
VOC	5.42E-02	5.42E-02	VOC - Volatile Organic Compound
Pb			Pb - Lead and lead compounds
Fluorides			Fluorides - Gaseous and particulates
$H_2SO_4$			H <sub>2</sub> SO <sub>4</sub> - Sulfuric Acid Mist
H <sub>2</sub> S			H <sub>2</sub> S - Hydrogen Sulfide
TRS			TRS - Total Reduced Sulfur
RSC			RSC - Reduced Sulfur Compounds

Actual Emissions Attachment 3 of 14

## OIL PRODUCTION WELL FUGITIVES 1 Newfield MAMIE 4-25-3-3WH

EQUIPMENT TYPE	NUMBER	HOURS OF	VOC	CH₄	EMISSION	EMISSION	VOC	CH₄
AND SERVICE	OF	OPERATION	WEIGHT	WEIGHT	FACTOR <sup>3</sup>	FACTOR	EMISSIONS	EMISSIONS
		(hours/yr)	FRACTION <sup>2</sup>	FRACTION <sup>2</sup>	(kg/hr-unit)	(lb/hr-unit)	(tons/yr)	(tons/yr)
Wellhead								
Valves	5	8760	0.070	0.775	0.0025	0.005525	8.43E-03	9.37E-02
Connectors	4	8760	0.070	0.775	0.00021	0.0004641	5.66E-04	6.30E-03
Open-Ended Lines	0	8760	0.070	0.775	0.0014	0.003094	0.00E+00	0.00E+00
Flanges	10	8760	0.070	0.775	0.00011	0.0002431	7.42E-04	8.25E-03
Other	1	8760	0.070	0.775	0.0075	0.016575	5.06E-03	5.62E-02
Separator								
Valves	6	8760	0.070	0.775	0.0025	0.005525	1.01E-02	1.12E-01
Connectors	10	8760	0.070	0.775	0.00021	0.0004641	1.42E-03	1.57E-02
Open-Ended Lines	0	8760	0.070	0.775	0.0014	0.003094	0.00E+00	0.00E+00
Flanges	12	8760	0.070	0.775	0.00011	0.0002431	8.90E-04	9.90E-03
Other	0	8760	0.070	0.775	0.0075	0.016575	0.00E+00	0.00E+00
Heater Treater								
Valves	8	8760	0.070	0.775	0.0025	0.005525	1.35E-02	1.50E-01
Connectors	20	8760	0.070	0.775	0.00021	0.0004641	2.83E-03	3.15E-02
Open-Ended Lines	0	8760	0.070	0.775	0.0014	0.003094	0.00E+00	0.00E+00
Flanges	12	8760	0.070	0.775	0.00011	0.0002431	8.90E-04	9.90E-03
Other	0	8760	0.070	0.775	0.0075	0.016575	0.00E+00	0.00E+00
Header								
Valves	5	8760	0.070	0.775	0.0025	0.005525	8.43E-03	9.37E-02
Connectors	4	8760	0.070	0.775	0.00021	0.0004641	5.66E-04	6.30E-03
Open-Ended Lines	0	8760	0.070	0.775	0.0014	0.003094	0.00E+00	0.00E+00
Flanges	10	8760	0.070	0.775	0.00011	0.0002431	7.42E-04	8.25E-03
Other	0	8760	0.070	0.775	0.0075	0.016575	0.00E+00	0.00E+00
TOTAL EMISSIONS (tons/y	OTAL EMISSIONS (tons/yr) 5.42E-02 6.02E-01							

Pollutant	Weight Fraction <sup>2</sup>	HAP Emissions (tons/yr)	HAP Emissions (lb/hr)
n-Hexane	0.00000	0.00E+00	0.00E+00
Benzene	0.00167	1.30E-03	2.96E-04
2,2,4 Trimethylpentane	0.00020	1.55E-04	3.55E-05
Toluene	0.00161	1.25E-03	2.86E-04
Ethylbenzene	0.00008	6.22E-05	1.42E-05
M&P XylenesO-Xylenes	0.00031	2.41E-04	5.50E-05
Total HAPs		3.01E-03	6.87E-04

<sup>1</sup>Average component count from Table W-1C to Subpart W of Part 98-Default Average Component Counts For Major Crude Oil Production Equipment. <sup>2</sup>Based on gas composition and properties from samples collected at the KM Bar F fuel tap. HAPs values from samples collected at 12 different Newfield sites.

<sup>3</sup>"Protocol for Equipment Leak Emission Estimates," EPA-453/R-95-017, Table 2-4, Light Oil

1. Company:	Newfield Exploration		Potential Emissions	
2. Site/Source:	MAMIE 4-25-3-3WH		3. Date: 2/7/2019	
4. Type of Operation:	Oil and Gas	Production Tanks		
5. Emission Point:	ID Number 4	Name OILTK-1	7. Identification and Descrip	tion of Control Equipment
6. Description of Equi 400 Barrel Ve	pment: rtical Fixed Roof Steel Oil	Tank		Flare
8. Throughput:	18,250	barrels/year	. 9. Operating Schedule:	Not Applicable

Pollutant	Uncontrolled Emissions	Controlled Emissions	
	(TPY)	(TPY)	
PM			DM Dortioulate Matter
PM <sub>10</sub>			PM - PM loss than 10 microns in size
PM <sub>2.5</sub>			PM PM less than 10 microns in size
SOx			PM <sub>2.5</sub> - PM less than 2.5 microns in size
NO <sub>X</sub>		1.02E-02	$_{X}$ = SO <sub>X</sub> - Sulful Oxides
CO		5.57E-02	CO - Carbon Monoxide
VOC	6.00E+00	1.20E-01	VOC - Volatile Organic Compound
Pb			Pb - Lead and lead compounds
Fluorides			Fluorides - Gaseous and particulates
$H_2SO_4$			H₂SO₄ - Sulfuric Acid Mist
$H_2S$	Negligible	Negligible	H <sub>2</sub> S - Hydrogen Sulfide
TRS			TRS - Total Reduced Sulfur
RSC			RSC - Reduced Sulfur Compounds

Potential Emissions Attachment 4 of 14

1. Company:	Newfield Explora	tion		A	ctual Emissions
2. Site/Source:	MAMIE 4-25-3-3	WH		3. Date: 2/7/2019	
4. Type of Operation:	Oil a	nd Gas Produ	ction Tanks	•	
5. Emission Point:	ID Number	Name		7. Identification and Descript	ion of Control Equipment
		4	OILTK-1		
6. Description of Equip	oment:			Flare	
400 Barrel Ve	rtical Fixed Roof S	teel Oil Tank			
8. Throughput:	18,250		barrels/year	9. Operating Schedule:	Not Applicable

Pollutant	Uncontrolled Emissions (TPY)	Controlled Emissions (TPY)	
PM			DM Destinuted Method
PM <sub>10</sub>			PIM - PARTICULATE MATTER
PM <sub>2.5</sub>			$PM_{0.5} - PM$ less than 2.5 microns in size
SO <sub>X</sub>			$SO_{\rm Y}$ - Sulfur Oxides
NO <sub>X</sub>		1.02E-02	NO <sub>x</sub> - Nitrogen Oxides
CO		5.57E-02	CO - Carbon Monoxide
VOC	6.00E+00	1.20E-01	VOC - Volatile Organic Compound
Pb			Pb - Lead and lead compounds
Fluorides			Fluorides - Gaseous and particulates
$H_2SO_4$			H <sub>2</sub> SO <sub>4</sub> - Sulfuric Acid Mist
H <sub>2</sub> S	Negligible	Negligible	H <sub>2</sub> S - Hydrogen Sulfide
TRS			TRS - Total Reduced Sulfur
RSC			RSC - Reduced Sulfur Compounds

Actual Emissions Attachment 4 of 14

## FLASH LIBERATION OF HYDROCARBON LIQUID FROM CENTRAL BASIN OIL STORAGE TANKS MAMIE 4-25-3-3WH

#### CB UB SXL

OILTK-1	PTE	
GOR from analysis	6.64	scf/bbl
Throughput (bbls/yr)	18,250	bbls/yr
Throughput (bbls/day)	50.00	bbls/day
Gas Flash Rate (SCFD):	332.0	scfd
Gas Flash Rate (lbs./day):	37.49	lb/day
Lb./Day = gas (ft <sup>3</sup> /day)x(Mwgas - lb/lb-mole) / (379.49 ft3/lb-mole)		

Gas oil ratio and mole percent of flash gas are representative of tanks in this region.

Component	Mole percent	Molecular Weight	Mole Frac x Mole <b>Stream MW</b>	Weight Percent	Weight Fraction	PTE Uncontrolled Emissions (lb/hr)	PTE Uncontrolled Emissions (tpy)
Hydrogen Sufide	0.000%	34.080	0.0000	0.000%	0.0000	0.00E+00	0.00E+00
Nitrogen	3.093%	28.013	0.8664	2.022%	0.0202	3.16E-02	1.38E-01
Carbon Dioxide	0.751%	44.010	0.3307	0.772%	0.0077	1.21E-02	5.28E-02
Methane	33.643%	16.043	5.3974	12.595%	0.1260	1.97E-01	8.62E-01
Ethane	15.073%	30.070	4.5325	1 <b>0.577%</b>	0.1058	1.65E-01	7.24E-01
Propane	13.269%	44.097	5.8513	13.654%	0.1365	2.13E-01	9.34E-01
Iso-Butane	3.081%	58.123	1.7909	4.179%	0.0418	6.53E-02	2.86E-01
n-Butane	7.803%	58.123	4.5352	1 <b>0.583%</b>	0.1058	1.65E-01	7.24E-01
2,2 Dimethylpropane	0.000%	72.140	0.0000	0.000%	0.0000	0.00E+00	0.00E+00
Iso-Pentane	2.905%	72.150	2.0957	4.890%	0.0489	7.64E-02	3.35E-01
n-Pentane	4.186%	72.150	3.0205	7.048%	0.0705	1.10E-01	4.82E-01
2,2 Dimethylbutane	0.158%	86.178	0.1363	0.318%	0.0032	4.97E-03	2.18E-02
Cyclopentane	1.187%	70.100	0.8324	<b>1.942%</b>	0.0194	3.03E-02	1.33E-01
2,3 Dimethylbutane	0.237%	86.178	0.2046	0.477%	0.0048	7.46E-03	3.27E-02
2 Methylpentane	0.481%	86.178	0.4145	0.967%	0.0097	1.51E-02	6.62E-02
3 Methylpentane	0.283%	86.178	0.2441	0.570%	0.0057	8.90E-03	3.90E-02
n-Hexane	8.062%	86.178	6.9478	16.213%	0.1621	2.53E-01	1.11E+00
Methylcyclopentane	0.953%	84.160	0.8020	<b>1.872%</b>	0.0187	2.92E-02	1.28E-01
Benzene	0.220%	78.114	0.1717	0.401%	0.0040	6.26E-03	2.74E-02
Cyclohexane	0.225%	84.160	0.1890	0.441%	0.0044	6.89E-03	3.02E-02
2-Methylhexane	0.056%	100.200	0.0563	0.131%	0.0013	2.05E-03	8.99E-03
3-Methylhexane	0.080%	100.200	0.0806	0.188%	0.0019	2.94E-03	1.29E-02
2,2,4 Trimethylpentane	0.079%	114.230	0.0905	0.211%	0.0021	3.30E-03	1.44E-02

OILTK-1 Calculation Page 1 of 4

## FLASH LIBERATION OF HYDROCARBON LIQUID FROM CENTRAL BASIN OIL STORAGE TANKS MAMIE 4-25-3-3WH

#### CB UB SXL

OILTK-1	PTE	
GOR from analysis	6.64	scf/bbl
Throughput (bbls/yr)	18,250	bbls/yr
Throughput (bbls/day)	50.00	bbls/day
Gas Flash Rate (SCFD):	332.0	scfd
Gas Flash Rate (lbs./day):	37.49	lb/day
Lb./Day = gas (ft <sup>3</sup> /day)x(Mwgas - lb/lb-mole) / (379.49 ft3/lb-mole)		

Gas oil ratio and mole percent of flash gas are representative of tanks in this region.

Component	Mole percent	Molecular Weight	Mole Frac x Mole <b>Stream MW</b>	Weight Percent	Weight Fraction	PTE Uncontrolled Emissions (lb/hr)	PTE Uncontrolled Emissions (tpy)
Other C7's	1.588%	100.272	1.5925	3.716%	0.0372	5.81E-02	2.54E-01
n-Heptane	0.635%	100.272	0.6367	1.486%	0.0149	2.32E-02	1.02E-01
Mehtylcyclohexane	0.712%	98.190	0.6995	1.632%	0.0163	2.55E-02	1.12E-01
Toluene	0.425%	92.140	0.3918	0.914%	0.0091	1.43E-02	6.26E-02
Other C8's	0.367%	114.230	0.4192	0.978%	0.0098	1.53E-02	6.69E-02
n-Octane	0.198%	114.230	0.2257	0.527%	0.0053	8.23E-03	3.60E-02
Ethylbenzene	0.042%	106.170	0.0448	0.105%	0.0010	1.63E-03	7.15E-03
M&P Xylenes	0.061%	106.170	0.0652	0.152%	0.0015	2.38E-03	1.04E-02
O-Xylenes	0.012%	106.170	0.0130	0.030%	0.0003	4.72E-04	2.07E-03
Other C9's	0.063%	128.258	0.0811	0.189%	0.0019	2.95E-03	1.29E-02
n-Nonane	0.034%	128.258	0.0434	0.101%	0.0010	1.58E-03	6.92E-03
Other C10's	0.024%	142.280	0.0347	0.081%	0.0008	1.27E-03	5.54E-03
n-Decane	0.007%	142.280	0.0097	0.023%	0.0002	3.53E-04	1.54E-03
Undecanes+	0.004%	156.310	0.0056	0.013%	0.0001	2.05E-04	8.98E-04
Total	100.000%		42.853	100.000%			
					Total:	1.5621E+00	6.8419E+00

VOC INFO	
Mole % VOCs	47.44%
Total NM/NE Stream MW VOCs	31.726
lb Voc / mmscf	83602.308
MMSCF/YR	0.121

	Uncontrolled	Uncontrolled
	Emissions, (lb/hr)	Emissions, (tpy)
Total VOC:	1.16E+00	5.07E+00
Total Me/Eth	3.62E-01	1.59E+00

OILTK-1 Calculation Page 2 of 4

AP-42 TANK WORKING and BREATHING EMISSIO DILTK-1 Newfie	NS Id MAMIE 4-	25-3-3WH		
INPUT DA	TA			]
	Symbol	PTE	Units	
Molecular Weight	NA.	50	l h/lh mole	4
Tank design data	IVIV	50	LD/ID-MOle	
Shell height	Hs	20.00	ft	4
Diameter	D	12.00	ft	4
Liquid height	Н	20.00	ft	
Ava, Liquid height	HI	10.00	ft	1
vapor space outage	Hvo	10.00	ft	
Tank volume		16,921	gallons	
Turnovers	Ν	45		
Net throughput	Q	18250.00	bbl/yr	
Tunover factor	KN	0.829	)	
Working loss product factor	Кр	0.75	i	From AP-42, 11/06 Section 7 Equ. 1-31, page 7.1-19
leteorological data				<b>_</b>
Daily ave. ambient temp.	TAA	51.9625	°F	From TANKS
Daily max. ambient temp.	TAX	63.641667	۴	for Salt Lake
Daily min. ambient temp.	IAN	40.283333	ĭ⊢ Io⊑	
Daily ambient temp. range	DIA	23.36	2	
nank paint solar absorptance (see adjacent table)	α	0.68	Duv/40 dave	From TANKS for Sold Jake City LT
Daily total insolation factor	-	1,452.11835	Btu/ft2-day	From TANKS for Salt Lake City, UT
	DA	4,102		
Autospheric pressure	FA	12.044		
Liquid bulk temperature	TB	61 /0	٥F	Tank is heated and temperature varies + 2°E
Daily vapor temp, range	DTv	4 00	٩	Tank is heated and temperature varies ± 2°F
Daily vapor temp. range	511	4.00		
Daily ave, liquid surface temp.	TLA	65.10	°F	
Daily max. liquid surface temp.	TLX	66.10	°F	1
Daily min. liquid surface temp.	TIN	64.10	°F	1
VP @ daily ave. liquid surf. temp.	PvA	165.19	mm Hg	Equation from AP-42, 11/06 Section 7 Figure 7.1-13b
VP @ daily max. liquid surf. temp.	PvX	168.39	mm Hg	Equation from AP-42, 11/06 Section 7 Figure 7.1-13b
VP @ daily min. liquid surf. temp.	PvN	162.03	mm Hg	Equation from AP-42, 11/06 Section 7 Figure 7.1-13b
Daily vapor pressure range	DPv	6.36	mm Hg	
Breather vent pressure setting range	DPB	0.06	psia	Value from AP-42, 11/06 Section 7 page 7.1-13 Note
Breather vent pressure setting range	DPB	3.10	mm Hg	4
CALCULATIONS				
CALCULATIONS	Cumhal		Unito	4
	Symbol		Units	
Breathing Losses				
Tank vanor space volume	Vv	1 130 98	ft3	4
Vanor density	Wy	2 834E-02	lh/ft3	4
Vapor space expansion factor	KE	0.01427	15/110	
Vented vapor saturation factor	Ks	0.3713	ft2	1
				1
Breathing losses	LB	62.02	lb/yr	
Vorking losses	Lw	1,812.02	lb/yr	
OTAL LOSSES	LT	0.21	lb/hr	
		1,874.04	lb/yr	
		0.9370	tpy	4
		38.97	scfd	<u>_</u>
IAP Emissions <sup>2</sup>	Wt%			1
n-Hexane	16.21%	0.15	tpy	1
Benzene	0.40%	0.00	tpy	4
2,2,4-Trimethylpentane	0.21%	0.00	tpy	4
Toluene	0.91%	0.01	tpy	4
Ethylbenzene	0.10%	0.00	tpy	4
Xylenes	0.18%	0.00	tpy	

<sup>1</sup>Calculations performed on this spreadsheet are taken from the USEPA AP-42- Section 7.1 Organic Liquid Storage Tanks - November 2006. <sup>2</sup>HAP Emissions (tpy) = HAP Wt% \* Total Losses (tpy)

Paint Color	Paint Shade or Type	Good	Poor
Aluminum	Specular	0.39	0.49
Aluminum	Diffuse	0.6	0.68
Aluminum	Mill finish, unpainted	0.1	0.15
Beige/Cream		0.35	0.49
Black		0.97	0.97
Brown		0.58	0.67
Gray	Light	0.54	0.63
Gray	Medium	0.68	0.74
Green	Dark	0.89	0.91
Red	Primer	0.89	0.91
Rust	Red iron oxide	0.38	0.5
Tan		0.43	0.55
White	NA	0.17	0.34

From AP-42, 11/06 Section 7 Table 7.1-6, page 7.1-69

OILTK-1 Calculation Page 3 of 4

Newfield MAMIE 4-25-3-3WH	
OILTK-1	

Potential to Emit Emission Calculations

Maximum Tank Vapor 15.5 scf/hr Lower Heating Value 2,222 Btu/scf	Controlled emissions are calculated based on a 98% destruction efficiency of the VOC gas.
VOC:   1.37E+00   lb/hr   x   100% -   98%     6.00E+00   TPY   x   100% -   98%	= <b>2.74E-02</b> lb/hr = <b>1.20E-01</b> TPY
Benzene:   7.12E-03   lb/hr   x   100% -   98%     3.12E-02   TPY   x   100% -   98%	= <b>1.42E-04</b> lb/hr = <b>6.23E-04</b> TPY
Toluene:   1.62E-02   lb/hr   x   100% -   98%     7.11E-02   TPY   x   100% -   98%	= <b>3.25E-04</b> lb/hr = <b>1.42E-03</b> TPY
Ethylbenzene:   1.86E-03   lb/hr   x   100% -   98%     8.13E-03   TPY   x   100% -   98%	= <b>3.71E-05</b> lb/hr = <b>1.63E-04</b> TPY
Xylenes:   3.24E-03   lb/hr   x   100% -   98%     1.42E-02   TPY   x   100% -   98%	= <b>6.48E-05</b> lb/hr = <b>2.84E-04</b> TPY
n-Hexane: 2.88E-01 lb/hr x 100% - 98% 1.26E+00 TPY x 100% - 98%	= <b>5.76E-03</b> lb/hr = <b>2.52E-02</b> TPY
2,2,4-Trimethyl- pentane:   3.75E-03   lb/hr   x   100% -   98%     1.64E-02   TPY   x   100% -   98%	= <b>7.50E-05</b> lb/hr = <b>3.28E-04</b> TPY

1. Company:	Newfield Exploration		Р	otential Emissions
2. Site/Source:	MAMIE 4-25-3-3WH		3. Date: 2/7/2019	
4. Type of Operation:	Oil and Gas	Production Tanks		
5. Emission Point:	ID Number 5	Name OILTK-2	7. Identification and Descrip	tion of Control Equipment
6. Description of Equi 400 Barrel Ve	pment: rtical Fixed Roof Steel Oil	Tank		Flare
8. Throughput:	18,250	barrels/year	. 9. Operating Schedule:	Not Applicable

Pollutant	Uncontrolled Emissions	Controlled Emissions	
	(TPY)	(TPY)	
PM			DM Dortioulate Matter
PM <sub>10</sub>			PM - PM loss than 10 microns in size
PM <sub>2.5</sub>			PM PM less than 10 microns in size
SOx			PM <sub>2.5</sub> - PM less than 2.5 microns in size
NO <sub>X</sub>		1.02E-02	$_{X}$ = SO <sub>X</sub> - Sulful Oxides
CO		5.57E-02	CO - Carbon Monoxide
VOC	6.00E+00	1.20E-01	VOC - Volatile Organic Compound
Pb			Pb - Lead and lead compounds
Fluorides			Fluorides - Gaseous and particulates
$H_2SO_4$			H₂SO₄ - Sulfuric Acid Mist
$H_2S$	Negligible	Negligible	H <sub>2</sub> S - Hydrogen Sulfide
TRS			TRS - Total Reduced Sulfur
RSC			RSC - Reduced Sulfur Compounds

Potential Emissions Attachment 5 of 14

1. Company:	Newfield Exploration	วท		Ad	ctual Emissions
2. Site/Source:	MAMIE 4-25-3-3W	Ή		3. Date: 2/7/2019	
4. Type of Operation:	Oil and	I Gas Produ	ction Tanks	•	
5. Emission Point:	ID Number	Name		7. Identification and Descripti	ion of Control Equipment
	5		OILTK-2		
6. Description of Equip	oment:			Flare	
400 Barrel Ver	tical Fixed Roof Ste	el Oil Tank			
8. Throughput:	18,250		barrels/year	9. Operating Schedule:	Not Applicable

Pollutant	Uncontrolled Emissions (TPY)	Controlled Emissions (TPY)	
PM		· · ·	
PM <sub>10</sub>			PM - Particulate Matter
PM <sub>2.5</sub>			$PM_{10} = PM$ less than 2.5 microns in size
SO <sub>X</sub>			$SO_{v}$ - Sulfur Oxides
NO <sub>X</sub>		1.02E-02	$NO_{\rm x}$ - Nitrogen Oxides
CO		5.57E-02	CO - Carbon Monoxide
VOC	6.00E+00	1.20E-01	VOC - Volatile Organic Compound
Pb			Pb - Lead and lead compounds
Fluorides			Fluorides - Gaseous and particulates
$H_2SO_4$			H <sub>2</sub> SO <sub>4</sub> - Sulfuric Acid Mist
H <sub>2</sub> S	Negligible	Negligible	H <sub>2</sub> S - Hydrogen Sulfide
TRS			TRS - Total Reduced Sulfur
RSC			RSC - Reduced Sulfur Compounds

Actual			
Emissions			
Attachment	5	of	14

## FLASH LIBERATION OF HYDROCARBON LIQUID FROM CENTRAL BASIN OIL STORAGE TANKS MAMIE 4-25-3-3WH

#### CB UB SXL

OILTK-2	PTE	
GOR from analysis	6.64	scf/bbl
Throughput (bbls/yr)	18,250	bbls/yr
Throughput (bbls/day)	50.00	bbls/day
Gas Flash Rate (SCFD):	332.0	scfd
Gas Flash Rate (lbs./day):	37.49	lb/day
Lb./Day = gas (ft <sup>3</sup> /day)x(Mwgas - lb/lb-mole) / (379.49 ft3/lb-mole)		

Gas oil ratio and mole percent of flash gas are representative of tanks in this region.

Component	Mole percent	Molecular Weight	Mole Frac x Mole <b>Stream MW</b>	Weight Percent	Weight Fraction	PTE Uncontrolled Emissions (lb/hr)	PTE Uncontrolled Emissions (tpy)
Hydrogen Sufide	0.000%	34.080	0.0000	0.000%	0.0000	0.00E+00	0.00E+00
Nitrogen	3.093%	28.013	0.8664	2.022%	0.0202	3.16E-02	1.38E-01
Carbon Dioxide	0.751%	44.010	0.3307	0.772%	0.0077	1.21E-02	5.28E-02
Methane	33.643%	16.043	5.3974	12.595%	0.1260	1.97E-01	8.62E-01
Ethane	15.073%	30.070	4.5325	10.577%	0.1058	1.65E-01	7.24E-01
Propane	1 <b>3.269%</b>	44.097	5.8513	13.654%	0.1365	2.13E-01	9.34E-01
Iso-Butane	<b>3.081%</b>	58.123	1.7909	4.179%	0.0418	6.53E-02	2.86E-01
n-Butane	7.803%	58.123	4.5352	10.583%	0.1058	1.65E-01	7.24E-01
2,2 Dimethylpropane	0.000%	72.140	0.0000	0.000%	0.0000	0.00E+00	0.00E+00
Iso-Pentane	<b>2.905%</b>	72.150	2.0957	4.890%	0.0489	7.64E-02	3.35E-01
n-Pentane	4.186%	72.150	3.0205	7.048%	0.0705	1.10E-01	4.82E-01
2,2 Dimethylbutane	0.158%	86.178	0.1363	0.318%	0.0032	4.97E-03	2.18E-02
Cyclopentane	1.187%	70.100	0.8324	1.942%	0.0194	3.03E-02	1.33E-01
2,3 Dimethylbutane	0.237%	86.178	0.2046	0.477%	0.0048	7.46E-03	3.27E-02
2 Methylpentane	0.481%	86.178	0.4145	0.967%	0.0097	1.51E-02	6.62E-02
3 Methylpentane	0.283%	86.178	0.2441	0.570%	0.0057	8.90E-03	3.90E-02
n-Hexane	8.062%	86.178	6.9478	16.213%	0.1621	2.53E-01	1.11E+00
Methylcyclopentane	0.953%	84.160	0.8020	1.872%	0.0187	2.92E-02	1.28E-01
Benzene	0.220%	78.114	0.1717	0.401%	0.0040	6.26E-03	2.74E-02
Cyclohexane	0.225%	84.160	0.1890	0.441%	0.0044	6.89E-03	3.02E-02
2-Methylhexane	0.056%	100.200	0.0563	0.131%	0.0013	2.05E-03	8.99E-03
3-Methylhexane	0.080%	100.200	0.0806	0.188%	0.0019	2.94E-03	1.29E-02
2,2,4 Trimethylpentane	0.079%	114.230	0.0905	0.211%	0.0021	3.30E-03	1.44E-02

OILTK-2 Calculation Page 1 of 4

## FLASH LIBERATION OF HYDROCARBON LIQUID FROM CENTRAL BASIN OIL STORAGE TANKS MAMIE 4-25-3-3WH

#### CB UB SXL

OILTK-2	PTE	
GOR from analysis	6.64	scf/bbl
Throughput (bbls/yr)	18,250	bbls/yr
Throughput (bbls/day)	50.00	bbls/day
Gas Flash Rate (SCFD):	332.0	scfd
Gas Flash Rate (lbs./day):	37.49	lb/day
Lb./Day = gas (ft <sup>3</sup> /day)x(Mwgas - lb/lb-mole) / (379.49 ft3/lb-mole)		

Gas oil ratio and mole percent of flash gas are representative of tanks in this region.

Component	Mole percent	Molecular Weight	Mole Frac x Mole <b>Stream MW</b>	Weight Percent	Weight Fraction	PTE Uncontrolled Emissions (lb/hr)	PTE Uncontrolled Emissions (tpy)
Other C7's	1.588%	100.272	1.5925	3.716%	0.0372	5.81E-02	2.54E-01
n-Heptane	0.635%	100.272	0.6367	1.486%	0.0149	2.32E-02	1.02E-01
Mehtylcyclohexane	0.712%	98.190	0.6995	1.632%	0.0163	2.55E-02	1.12E-01
Toluene	0.425%	92.140	0.3918	0.914%	0.0091	1.43E-02	6.26E-02
Other C8's	0.367%	114.230	0.4192	0.978%	0.0098	1.53E-02	6.69E-02
n-Octane	0.198%	114.230	0.2257	0.527%	0.0053	8.23E-03	3.60E-02
Ethylbenzene	0.042%	106.170	0.0448	0.105%	0.0010	1.63E-03	7.15E-03
M&P Xylenes	0.061%	106.170	0.0652	0.152%	0.0015	2.38E-03	1.04E-02
O-Xylenes	0.012%	106.170	0.0130	0.030%	0.0003	4.72E-04	2.07E-03
Other C9's	0.063%	128.258	0.0811	0.189%	0.0019	2.95E-03	1.29E-02
n-Nonane	0.034%	128.258	0.0434	0.101%	0.0010	1.58E-03	6.92E-03
Other C10's	0.024%	142.280	0.0347	0.081%	0.0008	1.27E-03	5.54E-03
n-Decane	0.007%	142.280	0.0097	0.023%	0.0002	3.53E-04	1.54E-03
Undecanes+	0.004%	156.310	0.0056	0.013%	0.0001	2.05E-04	8.98E-04
Total	100.000%		42.853	100.000%			
					Total:	1.5621E+00	6.8419E+00

VOC INFO	
Mole % VOCs	47.44%
Total NM/NE Stream MW VOCs	31.726
lb Voc / mmscf	83602.308
MMSCF/YR	0.121

	Uncontrolled	Uncontrolled
	Emissions, (lb/hr)	Emissions, (tpy)
Total VOC:	1.16E+00	5.07E+00
Total Me/Eth	3.62E-01	1.59E+00

OILTK-2 Calculation Page 2 of 4

OILTK-2 Newfiel	d MAMIE 4-	25-3-3WH		=
INPUT DA	TA			
Aclosular Weight	Symbol	PTE	Units	4
Molecular weight	My	50	l b/lb-mole	
ank design data	IVIV		LD/ID-IIIOle	4
Shell height	Hs	20.00	ft	
Diameter	D	12.00	ft	1
Liquid height	HI	20.00	ft	1
Avg. Liquid height	HI	10.00	ft	
vapor space outage	Hvo	10.00	ft	
Tank volume		16,921	gallons	
Turnovers	N	45		
Net throughput	Q	18250.00	bbl/yr	
Tunover factor	KN	0.829		
Working loss product factor	Кр	0.75		From AP-42, 11/06 Section 7 Equ. 1-31, page 7.1-19
leteorological data				<b>_</b>
Daily ave. ambient temp.	TAA	51.9625	°F	From TANKS
Daily max. ambient temp.	TAX	63.641667	۴F	for Salt Lake
Daily min. ambient temp.	IAN	40.283333	°F	City, UT
Daily ambient temp. range	DIA	23.36	°F 2	
rank paint solar absorptance (see adjacent table)	α	0.68	Dtu/ft0 dou:	From TANKS for Sold Jako City LIT
Daily total Insolation factor	1	1,452.11835	Btu/ft2-day	From TAINKS for Salt Lake City, UT
Sile elevation (leet)	DA	4,102		
	FA.	12.044		-
Liquid bulk temperature	TB	61 49	°F	Tank is heated and temperature varies + 2°F
Daily vapor temp range	DTv	4 00	°F	Tank is heated and temperature varies + 2°F
	5			
Daily ave, liquid surface temp.	TLA	65.10	°F	
Daily max, liquid surface temp.	TLX	66.10	°F	1
Daily min. liquid surface temp.	TIN	64.10	°F	
VP @ daily ave. liquid surf. temp.	PvA	165.19	mm Hg	Equation from AP-42, 11/06 Section 7 Figure 7.1-13b
VP @ daily max. liquid surf. temp.	PvX	168.39	mm Hg	Equation from AP-42, 11/06 Section 7 Figure 7.1-13
VP @ daily min. liquid surf. temp.	PvN	162.03	mm Hg	Equation from AP-42, 11/06 Section 7 Figure 7.1-13
Daily vapor pressure range	DPv	6.36	mm Hg	
Breather vent pressure setting range	DPB	0.06	psia	Value from AP-42, 11/06 Section 7 page 7.1-13 Note
Breather vent pressure setting range	DPB	3.10	mm Hg	4
CALCUL ATIONS				4
CALCULATIONS	Ourseland		Unite	4
	Symbol		Units	
Prosthing lossos	-			
Tank vanor space volume	Vv	1 130 08	ft3	1
Vanor density	Wv	2 834E-02	lb/ft3	1
Vapor space expansion factor	KF	0 01427	10/110	1
Vented vapor saturation factor	Ks	0.3713	ft2	
Tomod Vapor oddaradon laotor	110	0.07.10		1
Breathing losses	LB	62.02	lb/vr	1
Vorking losses	Lw	1,812.02	lb/yr	
OTAL LOSSES	LT	0.21	lb/hr	
		1,874.04	lb/yr	
		0.9370	tpy	4
		38.97	scfd	<u>_</u>
IAP Emissions <sup>2</sup>	Wt%			<u>_</u>
n-Hexane	16.21%	0.15	tpy	1
Benzene	0.40%	0.00	tpy	4
2,2,4-Trimethylpentane	0.21%	0.00	tpy	4
Toluene	0.91%	0.01	tpy	4
Ethylbenzene	0.10%	0.00	tpy	4
Xylenes	0.18%	0.00	ιψγ	

<sup>1</sup>Calculations performed on this spreadsheet are taken from the USEPA AP-42- Section 7.1 Organic Liquid Storage Tanks - November 2006. <sup>2</sup>HAP Emissions (tpy) = HAP Wt% \* Total Losses (tpy)

Paint Color	Paint Shade or Type	Good	Poor
Aluminum	Specular	0.39	0.49
Aluminum	Diffuse	0.6	0.68
Aluminum	Mill finish, unpainted	0.1	0.15
Beige/Cream		0.35	0.49
Black		0.97	0.97
Brown		0.58	0.67
Gray	Light	0.54	0.63
Gray	Medium	0.68	0.74
Green	Dark	0.89	0.91
Red	Primer	0.89	0.91
Rust	Red iron oxide	0.38	0.5
Tan		0.43	0.55
White	NA	0.17	0.34

From AP-42, 11/06 Section 7 Table 7.1-6, page 7.1-69

OILTK-2 Calculation Page 3 of 4

Newfield MAMIE 4-25-3-3WH	
OILTK-2	

Potential to Emit Emission Calculations

Maximum Tank Vapor 15.5 scf/hr Lower Heating Value 2,222 Btu/scf	Controlled emissions are calculated based on a 98% destruction efficiency of the VOC gas.
VOC:   1.37E+00   lb/hr   x   100% -   98%     6.00E+00   TPY   x   100% -   98%	= <b>2.74E-02</b> lb/hr = <b>1.20E-01</b> TPY
Benzene:   7.12E-03   lb/hr   x   100% -   98%     3.12E-02   TPY   x   100% -   98%	= <b>1.42E-04</b> lb/hr = <b>6.23E-04</b> TPY
Toluene:   1.62E-02   lb/hr   x   100% -   98%     7.11E-02   TPY   x   100% -   98%	= <b>3.25E-04</b> lb/hr = <b>1.42E-03</b> TPY
Ethylbenzene:   1.86E-03   lb/hr   x   100% -   98%     8.13E-03   TPY   x   100% -   98%	= <b>3.71E-05</b> lb/hr = <b>1.63E-04</b> TPY
Xylenes:   3.24E-03   lb/hr   x   100% -   98%     1.42E-02   TPY   x   100% -   98%	= <b>6.48E-05</b> lb/hr = <b>2.84E-04</b> TPY
n-Hexane: 2.88E-01 lb/hr x 100% - 98% 1.26E+00 TPY x 100% - 98%	= <b>5.76E-03</b> lb/hr = <b>2.52E-02</b> TPY
2,2,4-Trimethyl- pentane:   3.75E-03   lb/hr   x   100% -   98%     1.64E-02   TPY   x   100% -   98%	= <b>7.50E-05</b> lb/hr = <b>3.28E-04</b> TPY

1. Company:	Newfield Exploration		Р	otential Emissions
2. Site/Source:	MAMIE 4-25-3-3WH		3. Date: 2/7/2019	
4. Type of Operation:	Oil and Gas	Production Tanks		
5. Emission Point:	ID Number 6	Name OILTK-3	7. Identification and Descrip	tion of Control Equipment
6. Description of Equi 400 Barrel Ve	pment: rtical Fixed Roof Steel Oil	Tank		Flare
8. Throughput:	18,250	barrels/year	. 9. Operating Schedule:	Not Applicable

Pollutant	Uncontrolled Emissions	Controlled Emissions	
	(TPY)	(TPY)	
PM			DM Dortioulate Matter
PM <sub>10</sub>			PM - PM loss than 10 microns in size
PM <sub>2.5</sub>			PM PM less than 10 microns in size
SOx			PM <sub>2.5</sub> - PM less than 2.5 microns in size
NO <sub>X</sub>		1.02E-02	$_{X}$ = SO <sub>X</sub> - Sulful Oxides
CO		5.57E-02	CO - Carbon Monoxide
VOC	6.00E+00	1.20E-01	VOC - Volatile Organic Compound
Pb			Pb - Lead and lead compounds
Fluorides			Fluorides - Gaseous and particulates
$H_2SO_4$			H₂SO₄ - Sulfuric Acid Mist
$H_2S$	Negligible	Negligible	H <sub>2</sub> S - Hydrogen Sulfide
TRS			TRS - Total Reduced Sulfur
RSC			RSC - Reduced Sulfur Compounds

Potential Emissions Attachment 6 of 14

1. Company:	Newfield Explorat	on		Α	ctual Emissions
2. Site/Source:	MAMIE 4-25-3-3V	/H		3. Date: 2/7/2019	
4. Type of Operation:	Oil an	d Gas Produ	ction Tanks	•	
5. Emission Point:	ID Number	Name		7. Identification and Descript	ion of Control Equipment
	6		OILTK-3		
6. Description of Equip	oment:			Flare	
400 Barrel Ver	tical Fixed Roof Ste	el Oil Tank			
8. Throughput:	18,250		barrels/year	9. Operating Schedule:	Not Applicable

Pollutant	Uncontrolled Emissions (TPY)	Controlled Emissions (TPY)	
PM			
PM <sub>10</sub>			PM - Particulate Matter
PM <sub>2.5</sub>			$PM_{10} = PM$ less than 2.5 microns in size
SO <sub>X</sub>			$SO_{v}$ - Sulfur Oxides
NO <sub>X</sub>		1.02E-02	$NO_{\rm x}$ - Nitrogen Oxides
CO		5.57E-02	CO - Carbon Monoxide
VOC	6.00E+00	1.20E-01	VOC - Volatile Organic Compound
Pb			Pb - Lead and lead compounds
Fluorides			Fluorides - Gaseous and particulates
$H_2SO_4$			H <sub>2</sub> SO <sub>4</sub> - Sulfuric Acid Mist
H <sub>2</sub> S	Negligible	Negligible	H <sub>2</sub> S - Hydrogen Sulfide
TRS			TRS - Total Reduced Sulfur
RSC			RSC - Reduced Sulfur Compounds

Actual Emissions Attachment 6 of 14

## FLASH LIBERATION OF HYDROCARBON LIQUID FROM CENTRAL BASIN OIL STORAGE TANKS MAMIE 4-25-3-3WH

#### CB UB SXL

OILTK-3	PTE	
GOR from analysis	6.64	scf/bbl
Throughput (bbls/yr)	18,250	bbls/yr
Throughput (bbls/day)	50.00	bbls/day
Gas Flash Rate (SCFD):	332.0	scfd
Gas Flash Rate (lbs./day):	37.49	lb/day
Lb./Day = gas (ft <sup>3</sup> /day)x(Mwgas - lb/lb-mole) / (379.49 ft3/lb-mole)		

Gas oil ratio and mole percent of flash gas are representative of tanks in this region.

Component	Mole percent	Molecular Weight	Mole Frac x Mole <b>Stream MW</b>	Weight Percent	Weight Fraction	PTE Uncontrolled Emissions (lb/hr)	PTE Uncontrolled Emissions (tpy)
Hydrogen Sufide	0.000%	34.080	0.0000	0.000%	0.0000	0.00E+00	0.00E+00
Nitrogen	3.093%	28.013	0.8664	2.022%	0.0202	3.16E-02	1.38E-01
Carbon Dioxide	0.751%	44.010	0.3307	0.772%	0.0077	1.21E-02	5.28E-02
Methane	33.643%	16.043	5.3974	12.595%	0.1260	1.97E-01	8.62E-01
Ethane	15.073%	30.070	4.5325	10.577%	0.1058	1.65E-01	7.24E-01
Propane	1 <b>3.269%</b>	44.097	5.8513	13.654%	0.1365	2.13E-01	9.34E-01
Iso-Butane	<b>3.081%</b>	58.123	1.7909	4.179%	0.0418	6.53E-02	2.86E-01
n-Butane	7.803%	58.123	4.5352	10.583%	0.1058	1.65E-01	7.24E-01
2,2 Dimethylpropane	0.000%	72.140	0.0000	0.000%	0.0000	0.00E+00	0.00E+00
Iso-Pentane	<b>2.905%</b>	72.150	2.0957	4.890%	0.0489	7.64E-02	3.35E-01
n-Pentane	4.186%	72.150	3.0205	7.048%	0.0705	1.10E-01	4.82E-01
2,2 Dimethylbutane	0.158%	86.178	0.1363	0.318%	0.0032	4.97E-03	2.18E-02
Cyclopentane	1.187%	70.100	0.8324	1.942%	0.0194	3.03E-02	1.33E-01
2,3 Dimethylbutane	0.237%	86.178	0.2046	0.477%	0.0048	7.46E-03	3.27E-02
2 Methylpentane	0.481%	86.178	0.4145	0.967%	0.0097	1.51E-02	6.62E-02
3 Methylpentane	0.283%	86.178	0.2441	0.570%	0.0057	8.90E-03	3.90E-02
n-Hexane	8.062%	86.178	6.9478	16.213%	0.1621	2.53E-01	1.11E+00
Methylcyclopentane	0.953%	84.160	0.8020	1.872%	0.0187	2.92E-02	1.28E-01
Benzene	0.220%	78.114	0.1717	0.401%	0.0040	6.26E-03	2.74E-02
Cyclohexane	0.225%	84.160	0.1890	0.441%	0.0044	6.89E-03	3.02E-02
2-Methylhexane	0.056%	100.200	0.0563	0.131%	0.0013	2.05E-03	8.99E-03
3-Methylhexane	0.080%	100.200	0.0806	0.188%	0.0019	2.94E-03	1.29E-02
2,2,4 Trimethylpentane	0.079%	114.230	0.0905	0.211%	0.0021	3.30E-03	1.44E-02

OILTK-3 Calculation Page 1 of 4

## FLASH LIBERATION OF HYDROCARBON LIQUID FROM CENTRAL BASIN OIL STORAGE TANKS MAMIE 4-25-3-3WH

#### CB UB SXL

OILTK-3	PTE	
GOR from analysis	6.64	scf/bbl
Throughput (bbls/yr)	18,250	bbls/yr
Throughput (bbls/day)	50.00	bbls/day
Gas Flash Rate (SCFD):	332.0	scfd
Gas Flash Rate (lbs./day):	37.49	lb/day
Lb./Day = gas (ft <sup>3</sup> /day)x(Mwgas - lb/lb-mole) / (379.49 ft3/lb-mole)		

Gas oil ratio and mole percent of flash gas are representative of tanks in this region.

Component	Mole percent	Molecular Weight	Mole Frac x Mole <b>Stream MW</b>	Weight Percent	Weight Fraction	PTE Uncontrolled Emissions (lb/hr)	PTE Uncontrolled Emissions (tpy)
Other C7's	1.588%	100.272	1.5925	3.716%	0.0372	5.81E-02	2.54E-01
n-Heptane	0.635%	100.272	0.6367	1.486%	0.0149	2.32E-02	1.02E-01
Mehtylcyclohexane	0.712%	98.190	0.6995	1.632%	0.0163	2.55E-02	1.12E-01
Toluene	0.425%	92.140	0.3918	0.914%	0.0091	1.43E-02	6.26E-02
Other C8's	0.367%	114.230	0.4192	0.978%	0.0098	1.53E-02	6.69E-02
n-Octane	0.198%	114.230	0.2257	0.527%	0.0053	8.23E-03	3.60E-02
Ethylbenzene	0.042%	106.170	0.0448	0.105%	0.0010	1.63E-03	7.15E-03
M&P Xylenes	0.061%	106.170	0.0652	0.152%	0.0015	2.38E-03	1.04E-02
O-Xylenes	0.012%	106.170	0.0130	0.030%	0.0003	4.72E-04	2.07E-03
Other C9's	0.063%	128.258	0.0811	0.189%	0.0019	2.95E-03	1.29E-02
n-Nonane	0.034%	128.258	0.0434	0.101%	0.0010	1.58E-03	6.92E-03
Other C10's	0.024%	142.280	0.0347	0.081%	0.0008	1.27E-03	5.54E-03
n-Decane	0.007%	142.280	0.0097	0.023%	0.0002	3.53E-04	1.54E-03
Undecanes+	0.004%	156.310	0.0056	0.013%	0.0001	2.05E-04	8.98E-04
Total	100.000%		42.853	100.000%			
Total: 1.5621E+00 6.8419E+00							

VOC INFO	
Mole % VOCs	47.44%
Total NM/NE Stream MW VOCs	31.726
lb Voc / mmscf	83602.308
MMSCF/YR	0.121

	Uncontrolled	Uncontrolled	
	Emissions, (lb/hr)	Emissions, (tpy)	
Total VOC:	1.16E+00	5.07E+00	
Total Me/Eth	3.62E-01	1.59E+00	

OILTK-3 Calculation Page 2 of 4

DILTK-3 Newfiel	d MAMIE 4-2	25-3-3WH		_
INPUT DA	ΓA			
Acless Joy Weight	Symbol	PTE	Units	-
Molecular weight	Mv	50	l h/lh-molo	-
ank design data	IVIV	50	LD/ID-III0le	-
Shell height	Hs	20.00	ft	-
Diameter	D	12.00	ft	-
Liquid height	Н	20.00	ft	
Ava. Liquid height	HI	10.00	ft	
vapor space outage	Hvo	10.00	ft	
Tank volume		16,921	gallons	
Turnovers	N	45		
Net throughput	Q	18250.00	bbl/yr	
Tunover factor	KN	0.829		
Working loss product factor	Кр	0.75		From AP-42, 11/06 Section 7 Equ. 1-31, page 7.1-19
leteorological data				
Daily ave. ambient temp.	TAA	51.9625	°F	From TANKS
Daily max. ambient temp.	TAX	63.641667	°F	for Salt Lake
Daily min. ambient temp.	TAN	40.283333	°F	City, UT
Daily ambient temp. range	DTA	23.36	°F	<u></u>
Tank paint solar absorptance (see adjacent table)	α	0.68	-	Tank color gray, condition good
Daily total insolation factor	I	1,452.11835	Btu/ft2-day	From TANKS for Salt Lake City, UT
Site elevation (feet)	-	4,162		
Atmospheric pressure	PA	12.644		_
	75	04.40		
Liquid bulk temperature	IB	61.49	°F	Tank is heated and temperature varies ± 2°F
Dally vapor temp. range	DIV	4.00		Tank is neated and temperature varies ± 2°F
Deily ave liquid autoes temp		CE 10	or	-
Daily ave. liquid surface temp.	TLA	66.10	°F	-
Daily max. liquid surface tomp		64.10	PE	-
Daily min. liquid surface temp.		04.10	1	-
VP @ daily ave liquid suff temp	ΡνΑ	165 19	mm Ha	Equation from AP-42 11/06 Section 7 Figure 7 1-13h
VP @ daily max_liquid surf_temp	PvX	168 39	mm Ha	Equation from AP-42 11/06 Section 7 Figure 7 1-13
VP @ daily min_liquid surf_temp	PvN	162.03	mm Ha	Equation from AP-42, 11/06 Section 7 Figure 7.1-13
		102.00	g	
Daily vapor pressure range	DPv	6.36	mm Ha	
Breather vent pressure setting range	DPB	0.06	psia	Value from AP-42, 11/06 Section 7 page 7.1-13 Note
Breather vent pressure setting range	DPB	3.10	mm Hg	
CALCULATIONS				
	Symbol		Units	
sreathing losses			110	
I ank vapor space volume	Vv	1,130.98	tt3	4
Vapor density	Wv	2.834E-02	lb/ft3	4
Vapor space expansion factor	KE	0.01427	40	
Vented vapor saturation factor	Ks	0.3713	ft2	-
× 417 1		00.00	u /	-
areathing losses	LB	62.02	id/yr	-
Norking lossos	1.14	1 010 00	lbár	-
vorking losses	LW	1,012.02	iD/yi	-
OTAL LOSSES	IT	0.24	llb/br	4
UTAL LUGGES		1 874 04	lb/rr	-
		0.9270	tov	1
		38.97	scfd	1
IAP Emissions <sup>2</sup>	\ <b>\/</b> +9/_	00.07		1
n-Hevana	16 21%	0.15	tov	1
Benzene	0.40%	0.15	tov	-
2 2 4-Trimethylpentane	0.40%	0.00	tov	1
Toluene	0.91%	0.00	tov	1
Ethylhonzono	0.10%	0.00	tpy	1
	0.10//			

<sup>1</sup>Calculations performed on this spreadsheet are taken from the USEPA AP-42- Section 7.1 Organic Liquid Storage Tanks - November 2006. <sup>2</sup>HAP Emissions (tpy) = HAP Wt% \* Total Losses (tpy)

Paint Color	Paint Shade or Type	Good	Poor
Aluminum	Specular	0.39	0.49
Aluminum	Diffuse	0.6	0.68
Aluminum	Mill finish, unpainted	0.1	0.15
Beige/Cream		0.35	0.49
Black		0.97	0.97
Brown		0.58	0.67
Gray	Light	0.54	0.63
Gray	Medium	0.68	0.74
Green	Dark	0.89	0.91
Red	Primer	0.89	0.91
Rust	Red iron oxide	0.38	0.5
Tan		0.43	0.55
White	NA	0.17	0.34

From AP-42, 11/06 Section 7 Table 7.1-6, page 7.1-69

OILTK-3 Calculation Page 3 of 4

	Newfield MAMIE 4-25-3-3WH	
	1	
	OILTK-3	
μ		

Potential to Emit Emission Calculations

Maximum Tank Vapor 15.5 scf/hr Lower Heating Value 2,222 Btu/scf	Controlled emissions are calculated based on a 98% destruction efficiency of the VOC gas.
VOC: 1.37E+00 lb/hr x 100% - 98% 6.00E+00 TPY x 100% - 98%	= <b>2.74E-02</b> lb/hr = <b>1.20E-01</b> TPY
Benzene:   7.12E-03   lb/hr   x   100% -   98%     3.12E-02   TPY   x   100% -   98%	= <b>1.42E-04</b> lb/hr = <b>6.23E-04</b> TPY
Toluene:   1.62E-02   lb/hr   x   100% -   98%     7.11E-02   TPY   x   100% -   98%	= <b>3.25E-04</b> lb/hr = <b>1.42E-03</b> TPY
Ethylbenzene:   1.86E-03   lb/hr   x   100% -   98%     8.13E-03   TPY   x   100% -   98%	= <b>3.71E-05</b> lb/hr = <b>1.63E-04</b> TPY
Xylenes:   3.24E-03   lb/hr   x   100% -   98%     1.42E-02   TPY   x   100% -   98%	= <b>6.48E-05</b> lb/hr = <b>2.84E-04</b> TPY
n-Hexane: 2.88E-01 lb/hr x 100% - 98% 1.26E+00 TPY x 100% - 98%	= <b>5.76E-03</b> lb/hr = <b>2.52E-02</b> TPY
2,2,4-Trimethyl- pentane:   3.75E-03   lb/hr   x   100% -   98%     1.64E-02   TPY   x   100% -   98%	= <b>7.50E-05</b> lb/hr = <b>3.28E-04</b> TPY

1. Company:	Newfield Exploration		Potential Emissions
2. Site/Source:	MAMIE 4-25-3-3WH		3. Date: 2/7/2019
4. Type of Operatio	n: Oil and Gas	Production Tank l	Jnloading
5. Emission Point:	ID Number 7	Name OILTKLOAD-1	7. Identification and Description of Control Equipment
6. Description of Eq	uipment:		Not Applicable
Emissions rela	ted to unloading of oil ta	ank via truck	
8. Load Quantity:	54,750	barrels/yr	

Pollutant	Uncontrolled Emissions	Controlled Emissions	
	(TPY)	(TPY)	
PM			DNA Dortiouloto Mottor
PM <sub>10</sub>			PM - PM less than 10 microns in size
PM <sub>2.5</sub>			$1 \text{ M}_{10} = 1 \text{ M}_{10} \text{ so } 1 \text{ M}_{10} \text{ so } 1 \text{ merons in size}$
<u> </u>			PM <sub>2.5</sub> - PM less than 2.5 microns in size
30 <sub>X</sub>			SO <sub>X</sub> - Sulfur Oxides
NO <sub>X</sub>			NO <sub>x</sub> - Nitrogen Oxides
CO			CO - Carbon Monoxide
VOC	2.31E+00	2.31E+00	VOC - Volatile Organic Compound
Pb			Pb - Lead and lead compounds
Fluorides			Fluorides - Gaseous and particulates
$H_2SO_4$			H <sub>2</sub> SO <sub>4</sub> - Sulfuric Acid Mist
H <sub>2</sub> S			H <sub>2</sub> S - Hydrogen Sulfide
TRS			TRS - Total Reduced Sulfur
RSC			RSC - Reduced Sulfur Compounds

Potential Emissions Attachment 7 of 14

1. Company:	Newfield Exploration		Actual Emissions
2. Site/Source:	MAMIE 4-25-3-3WH		3. Date: 2/7/2019
4. Type of Operatio	n: Oil and Gas	Production Tank L	Inloading
5. Emission Point:	ID Number	Name	7. Identification and Description of Control Equipment
	7	OILTKLOAD-1	
6. Description of Eq	quipment:		Not Applicable
Emissions rela	ated to unloading of oil t	ank via truck	
8. Load Quantity:	54,750	barrels/yr	

Pollutant	Uncontrolled Emissions (TPY)	Controlled Emissions (TPY)	
PM			
PM <sub>10</sub>			PM - Particulate Matter
PM <sub>2.5</sub>			$PM_{10} = PM$ less than 2.5 microns in size
SO <sub>X</sub>			$SO_{\rm v}$ - Sulfur Oxides
NO <sub>X</sub>			NO <sub>v</sub> - Nitrogen Oxides
CO			CO - Carbon Monoxide
VOC	2.31E+00	2.31E+00	VOC - Volatile Organic Compound
Pb			Pb - Lead and lead compounds
Fluorides			Fluorides - Gaseous and particulates
$H_2SO_4$			H <sub>2</sub> SO <sub>4</sub> - Sulfuric Acid Mist
H <sub>2</sub> S			H <sub>2</sub> S - Hydrogen Sulfide
TRS			TRS - Total Reduced Sulfur
RSC			RSC - Reduced Sulfur Compounds

Actual Emissions Attachment 7 of 14



OILTKLOAD-1 Calculation Page 1 of 2



Calculation basis: AP-42 Section 5.2. Defaults assume submerged loading: dedicated normal service.

OILTKLOAD-1 Calculation Page 2 of 2

1. Company:	Newfield Exploration	I		Potential Emissions	
2. Site/Source:	MAMIE 4-25-3-3WH		3. Date: 2/7/2019		
4. Type of Operation	n: Oil and Ga	as Production Pneu	matic Controllers		
5. Emission Point:	ID Number 8	Name PCONT-1	7. Identification and Description	n of Control Equipment	
6. Description of Ec Low Pneuma	quipment: tic Controllers		None		
8. Controller Bleed	Rate:	1 scf/	hr 9. Operating Schedule:	8,760	Hours/year
10. Number of Pne	umatic Controllers:	6			

Pollutant	Uncontrolled Emissions	Controlled Emissions	
	(TPY)	(TPY)	
PM			DM Dorticulate Matter
PM <sub>10</sub>			DM DM loss than 10 microns in size
PM <sub>2.5</sub>			PM <sub>10</sub> - PM less than 10 microns in size
SOx			PIN2.5 - FIN less than 2.5 microns in size
NOv			SO <sub>X</sub> - Sullur Oxides
			NO <sub>X</sub> - Nitrogen Oxides
00	0.075.00		CO - Carbon Monoxide
VOC	8.85E-02	8.85E-02	VOC - Volatile Organic Compound
Pb			Pb - Lead and lead compounds
Fluorides			Fluorides - Gaseous and particulates
$H_2SO_4$			H <sub>2</sub> SO <sub>4</sub> - Sulfuric Acid Mist
H <sub>2</sub> S			H <sub>2</sub> S - Hydrogen Sulfide
TRS			TRS - Total Reduced Sulfur
RSC			RSC - Reduced Sulfur Compounds

Potential Emissions Attachment 8 of 14

1. Company: Newfield Exploration				Actual Emissions	
2. Site/Source: MAMIE 4-25-3-3WH			3. Date: 2/7/2019		
4. Type of Operation: Oil and Gas Production Pneum			natic Controllers		
5. Emission Point:	ID Number	Name	7. Identification and Desc	cription of Control Equipment	
	8	PCONT-1			
6. Description of Equipme	ent:		None		
Low Pneumatic Cor	ntrollers				
8. Controller Bleed Rate:		1 scf/hr	. 9. Operating Schedule:	8,760	Hours/year
10. Number of Pneumatic	c Controllers:	6			
Pollutant	Uncontrolled Em	issions Co	ontrolled Emissions (TPY)		

	(TPY)	(TPY)	
PM			
PM <sub>10</sub>			PM - Particulate Matter
PM <sub>2.5</sub>			PM <sub>10</sub> - PM less than 10 microns in size
SO <sub>X</sub>			PM <sub>2.5</sub> - PM less than 2.5 microns in size
NO <sub>X</sub>			NO <sub>v</sub> - Nitrogen Oxides
CO			CO - Carbon Monoxide
VOC	8.85E-02	8.85E-02	VOC - Volatile Organic Compound
Pb			Pb - Lead and lead compounds
Fluorides			Fluorides - Gaseous and particulates
$H_2SO_4$			H <sub>2</sub> SO <sub>4</sub> - Sulfuric Acid Mist
H <sub>2</sub> S			H <sub>2</sub> S - Hydrogen Sulfide
TRS			TRS - Total Reduced Sulfur
RSC			RSC - Reduced Sulfur Compounds

Actual Emissions Attachment 8 of 14



UINTA CENTRAL BASIN

Emissions (lb/hr) = PSCR (scf/hr) x (1/379 scf/lb-mole) x (VOC wt. Fraction) Emissions (TPY) = (lb/hr VOC) x (8760 hr/yr) x (1 ton/2000)



Molecular weight and weight percent of gas constituents are from an extend gas analysis representative of this region.

PCONT-1 Calculation Page 1 of 2



UINTA CENTRAL BASIN

Emissions (lb/hr) = PSCR (scf/hr) x (1/379 scf/lb-mole) x (VOC wt. Fraction) Emissions (TPY) = (lb/hr VOC) x (8760 hr/yr) x (1 ton/2000)



Molecular weight and weight percent of gas constituents are from an extended gas analysis representative of this region.

PCONT-1 Calculation Page 2 of 2

1. Company:	Newfield Exploration		Potential Emissions	
2. Site/Source:	MAMIE 4-25-3-3WH		3. Date: 2/7/2019	
4. Type of Operation:	Oil and Gas	Production Tanks		
5. Emission Point:	ID Number 9	Name PWTANK-1	7. Identification and Descript	tion of Control Equipment
6. Description of Equip 400 Barrel Ver	oment: tical Fixed Roof Steel Pro	oduced Water Tank		Flare
8. Throughput:	54,750	barrels/year	9. Operating Schedule:	Not Applicable

Pollutant	Uncontrolled Emissions	Controlled Emissions	
	(TPY)	(TPY)	
PM			DM Dortiouloto Mottor
PM <sub>10</sub>			PM - PM loss than 10 microns in size
PM <sub>2.5</sub>			PM $PM$ loss than 2.5 microns in size
SO <sub>X</sub>			= FW <sub>2.5</sub> - FW less that 2.5 microns in size
NO <sub>X</sub>		2.65E-03	$NO_{x}$ - Nitrogen Oxides
CO		1.44E-02	CO - Carbon Monoxide
VOC	2.74E-01	5.48E-03	VOC - Volatile Organic Compound
Pb			Pb - Lead and lead compounds
Fluorides			Fluorides - Gaseous and particulates
$H_2SO_4$			$H_2SO_4$ - Sulfuric Acid Mist
H <sub>2</sub> S	Negligible	Negligible	H <sub>2</sub> S - Hydrogen Sulfide
TRS			TRS - Total Reduced Sulfur
RSC			RSC - Reduced Sulfur Compounds

Potential Emissions Attachment 9 of 14

1. Company: Newfield Exploration			Actual Emissions		
2. Site/Source: MAMIE 4-25-3-3WH			3. Date: 2/7/2019		
4. Type of Operation:	Oil ar	nd Gas Proc	luction Tanks	•	
5. Emission Point:	ID Number	Name		7. Identification and Descript	ion of Control Equipment
	g	)	PWTANK-1		
6. Description of Equipment:				Flare	
400 Barrel Vertical Fixed Roof Steel Produced Water Tank			ed Water Tank		
8. Throughput:	54,750		barrels/year	9. Operating Schedule:	Not Applicable

Pollutant	Uncontrolled Emissions (TPY)	Controlled Emissions (TPY)	
PM			
PM <sub>10</sub>			PM - Particulate Matter
PM <sub>2.5</sub>			$PM_{0.5}$ - PM less than 2.5 microns in size
SO <sub>X</sub>			$SO_{x}$ - Sulfur Oxides
NO <sub>X</sub>		2.65E-03	NO <sub>x</sub> - Nitrogen Oxides
CO		1.44E-02	CO - Carbon Monoxide
VOC	2.74E-01	5.48E-03	VOC - Volatile Organic Compound
Pb			Pb - Lead and lead compounds
Fluorides			Fluorides - Gaseous and particulates
$H_2SO_4$			H <sub>2</sub> SO <sub>4</sub> - Sulfuric Acid Mist
H <sub>2</sub> S	Negligible	Negligible	H <sub>2</sub> S - Hydrogen Sulfide
TRS			TRS - Total Reduced Sulfur
RSC			RSC - Reduced Sulfur Compounds

Actual Emissions Attachment 9 of 14 Newfield MAMIE 4-25-3-3WH

# PWTANK-1

## Potential to Emit Emission Calculations

Maximum Water Tank Throughput 54,750 bbl/yr	Environ Emission Factors for Produced Water Tanks Environ Project No. 06-17477T, TCEQ Project 2010-29 Prepared for Texas Commission on Environmental Quality.			
Flash Factor 1.90 scf/bbl	Given in pounds of emissions per barrel of produced water.			
Maximum Tank Vapor 11.9 scf/hr	Methane Emission and Flash Factors were not provided in this report as such it was calculated from the data available within the report.			
Lower Heating Value 748 Btu/scf	Maximum Tank Vapor (scf/hr) =			
VOC 0.01 lb/bbl				
Benzene 0.0001 lb/bbl				
Toluene 0.0003 lb/bbl				
Ethylbenzene 0.000006 lb/bbl				
Xylenes 0.00006 lb/bbl	Controlled emissions are calculated based on a			
	<u>9676</u> destruction enciency of the VOC gas.			
	v 0.010.lb/bbl v 100% - 98% - 1 <b>255-03</b> lb/br			
54,750 bbl/m × 0.01 lb/bbl				
Benzene: 262.5 gai/nr x 1/42 barrei/galion	X = 0.0001  ib/bb $X = 1.25E-05  ib/nr$			
54,750 bbl/yr x 0.0001 lb/bbl	x 1/2,000 ton/lb x 100% - 98% = 5.48E-05 IPY			
Toluene: 262.5 gal/hr x 1/42 barrel/gallon	x 0.0003 lb/bbl x 100% - 98% = 3.75E-05 lb/hr			
54,750 bbl/yr x 0.0003 lb/bbl	x 1/2,000 ton/lb x 100% - 98% = 1.64E-04 TPY			
Ethylbenzene: 262.5 gal/hr x 1/42 barrel/gallon	x 0.000006 lb/bbl x 100% - 98% = <b>7.50E-07</b> lb/hr			
54,750 bbl/yr x 0.000006 lb/bbl	x 1/2,000 ton/lb x 100% - 98% = 3.29E-06 TPY			

Newfield MAMIE 4-25-3-3WH				
PWTANK-1				
Xylenes:	<b>262.5</b> gal/hr x 1/42 barrel/gallon x 0.00006 lb/bbl x 100% - 98% = <b>7.50E-06</b> lb/hr			
Xylenes:	262.5 gal/hr x 1/42 barrel/gallon x 0.00006 lb/bbl x 100% - 98% = 7.50E-06 lb/hr   54,750 bbl/yr x 0.00006 lb/bbl x 1/2,000 ton/lb x 100% - 98% = 3.29E-05 TPY			

NOx & CO emission factors are from AP-42 Table 13.5-1 (Emission Factors for Flare Operations).  $CO_2 \& N_2O$  emission factors are from AP-42 Table 1.4-2 (Emission Factors for Natural Gas Combustion).

PWTANK Calculation Page 2 of 2

1. Company:	Newfield Exploration		Po	tential Emissions
2. Site/Source: MAMIE 4-25-3-3WH			3. Date: 2/07/2019	
4. Type of Operation:	Miscellaneou	is Tanks		
5. Emission Point:	ID Number 10	Name SMTANKS-1	7. Identification and Description	on of Control Equipment
6. Description of Equip Small Storage	oment: Tanks			
8. Throughput:	Not Applicable	barrels/yea	9. Operating Schedule:	Not Applicable

Pollutant	Uncontrolled Emissions (TPY)	Controlled Emissions (TPY)	
PM			DNA Deutieulete Metteu
PM <sub>10</sub>			PM - Particulate Matter
DM.			- FIVI <sub>10</sub> - FIVI less that TO Inicions in size
1 1012.5			PM <sub>2.5</sub> - PM less than 2.5 microns in size
SO <sub>X</sub>			SO <sub>x</sub> - Sulfur Oxides
NO <sub>X</sub>			NO <sub>x</sub> - Nitrogen Oxides
CO			CO - Carbon Monoxide
VOC	2.05E-02	2.05E-02	VOC - Volatile Organic Compound
Pb			Pb - Lead and lead compounds
Fluorides			Fluorides - Gaseous and particulates
H <sub>2</sub> SO <sub>4</sub>			$H_2SO_4$ - Sulfuric Acid Mist
H <sub>2</sub> S			H <sub>2</sub> S - Hydrogen Sulfide
TRS			TRS - Total Reduced Sulfur
RSC			RSC - Reduced Sulfur Compounds

Potential Emissions Attachment 10 of 15
1. Company:	Newfield Exploration		Ac	tual Emissions
2. Site/Source:	MAMIE 4-25-3-3WH		3. Date: 2/07/2019	
4. Type of Operation:	Miscellaneou	is Tanks		
5. Emission Point:	ID Number 10	Name SMTANKS-1	7. Identification and Description	on of Control Equipment
6. Description of Equip Small Storage	oment: Tanks		_	
8. Throughput:	Not Applicable	barrels/yea	. 9. Operating Schedule:	Not Applicable

Pollutant	Uncontrolled Emissions (TPY)	Controlled Emissions (TPY)	
PM			DNA Deutievilete Metter
PM <sub>10</sub>			PM - Particulate Matter
DM.			- FIVI <sub>10</sub> - FIVI less that TO Inicions in size
1 1012.5			PM <sub>2.5</sub> - PM less than 2.5 microns in size
SO <sub>X</sub>			SO <sub>x</sub> - Sulfur Oxides
NO <sub>X</sub>			NO <sub>x</sub> - Nitrogen Oxides
CO			CO - Carbon Monoxide
VOC	2.05E-02	2.05E-02	VOC - Volatile Organic Compound
Pb			Pb - I ead and lead compounds
Fluorides			Fluorides - Gaseous and particulates
H <sub>2</sub> SO <sub>4</sub>			$H_2SO_4$ - Sulfuric Acid Mist
H <sub>2</sub> S			H <sub>2</sub> S - Hydrogen Sulfide
TRS			TRS - Total Reduced Sulfur
RSC			RSC - Reduced Sulfur Compounds

Actual Emissions Attachment 10 of 15

#### Newfield Mamie 4-25-3-3WH

SMALL STORAGE TANKS -1			
	Emission Factor	Units	
Annual Storage Quantity			
Methanol	8,600	gallons/yr	
Ethylene glycol	1,000	gallons/yr	_
Breathing losses Emission Factors			-
Methanol	3.70E+00	lb VOC/1000 gal	Value from "http://cfpub.epa.gov/webfire"
Ethylene glycol	5.20E-02	lb VOC/1000 gal	Value from "http://cfpub.epa.gov/webfire"
Breathing Emissions			-
Methanol	3.63E-03	VOC lb/hr	= 3.7 lb/1000 gal * 8600 gal/yr * 1 yr/365 days * 1 day/24 hrs
Ethylene glycol	5.94E-06	VOC lb/hr	= 0.052 lb/1000 gal * 1000 gal/yr * 1 yr/365 days * 1 day/24 hrs
Manhimula and Emission Eastern			
Working losses Emission Factors	4.075.00		
Methanol	1.07E+00	Ib VOC/1000 gai	Value from "http://cfpub.epa.gov/webfire"
Ethylene glycol	2.00E-03	Ib VOC/1000 gai	Value from "http://cfpub.epa.gov/webfire"
Working Emissions			
Methanol	1.05E-03	VOC lb/hr	= 1.07 lb/1000 gal * 8600 gal/yr * 1 yr/365 days * 1 day/24 hrs
Ethylene glycol	2.28E-07	VOC lb/hr	= 0.002 lb/1000 gal * 1000 gal/yr * 1 yr/365 days * 1 day/24 hrs
Total Working & Breathing Emissions			_
Methanol	4 68E-03	VOC lb/hr	—
Methanol	2.05E-02	VOC ton/yr	
		Í	
Ethylene glycol	6.16E-06	VOC lb/hr	—
Ethylene glycol	2.70E-05	VOC ton/yr	
Totals	4.69E-03	VOC lb/hr	
Totals	2.05E-02	VOC ton/yr	

SMTANKS-1 Calculation Page 1 of 1

1. Company:	Newfield Exploration			Potential Emissions	
2. Site/Source:	MAMIE 4-25-3-3WH		3. Date: 2/7/2019		
4. Type of Operation:	Oil and Gas	Production Tank	Heater		
5. Emission Point:	ID Number 11	Name TANKHTR1	7. Identification and Description	n of Control Equipment	
<ol> <li>Description of Equ Tank Heater</li> </ol>	pment:		None		
8. Hours of Operation	<sup>1:</sup> 8,760	Hours/Year	9. Burner Rating:	250,000	BTU/hr
10. Type of Fuel Use	d: Nat	ural Gas	11. Amount of Fuel Used:	2,190,000,000	BTU/yr

Pollutant	Uncontrolled Emissions	Controlled Emissions	
	(TPY)	(TPY)	
PM	8.16E-03	8.16E-03	PM Porticulate Matter
PM <sub>10</sub>	8.16E-03	8.16E-03	$PM_{co}$ - PM less than 10 microns in size
PM <sub>2.5</sub>	8.16E-03	8.16E-03	$PM_{10}$ - PM less than 2.5 microns in size
SO <sub>X</sub>	6.44E-04	6.44E-04	$SO_{\rm v}$ - Sulfur Oxides
NO <sub>X</sub>	1.07E-01	1.07E-01	NO <sub>v</sub> - Nitrogen Oxides
CO	9.02E-02	9.02E-02	CO - Carbon Monoxide
VOC	5.90E-03	5.90E-03	VOC - Volatile Organic Compound
Pb			Pb - Lead and lead compounds
Fluorides			Fluorides - Gaseous and particulates
$H_2SO_4$			$H_2SO_4$ - Sulfuric Acid Mist
H <sub>2</sub> S			H <sub>2</sub> S - Hydrogen Sulfide
TRS			TRS - Total Reduced Sulfur
RSC			RSC - Reduced Sulfur Compounds

Potential Emissions Attachment 11 of 14

1. Company: N	Newfield Exploration			Actual Emissions	
2. Site/Source:	/IAMIE 4-25-3-3WH		3. Date: 2/7/2019		
4. Type of Operation:	Oil and Gas	Production Tank	Heater		
5. Emission Point:	ID Number	Name	7. Identification and Description	n of Control Equipment	
	11	TANKHTR1			
6. Description of Equi	pment:		None		
Tank Heater					
8. Hours of Operation	: 8,760	Hours/Year	9. Burner Rating:	250,000	BTU/hr
10. Type of Fuel Used	d: Na	tural Gas	11. Amount of Fuel Used:	2,190,000,000	BTU/yr
			· · · · · · · · · · · · · · · · · · ·		

Pollutant	Uncontrolled Emissions	Controlled Emissions	
	(TPY)	(TPY)	
PM	8.16E-03	8.16E-03	DNA Desticulate Matter
PM <sub>10</sub>	8.16E-03	8.16E-03	PM - Particulate Matter PM - PM less than 10 microns in size
PM <sub>2.5</sub>	8.16E-03	8.16E-03	$PM_{0.5}$ - PM less than 2.5 microns in size
SO <sub>X</sub>	6.44E-04	6.44E-04	$SO_{\rm v}$ - Sulfur Oxides
NO <sub>X</sub>	1.07E-01	1.07E-01	NO <sub>v</sub> - Nitrogen Oxides
CO	9.02E-02	9.02E-02	CO - Carbon Monoxide
VOC	5.90E-03	5.90E-03	VOC - Volatile Organic Compound
Pb			Pb - Lead and lead compounds
Fluorides			Fluorides - Gaseous and particulates
$H_2SO_4$			H <sub>2</sub> SO <sub>4</sub> - Sulfuric Acid Mist
H <sub>2</sub> S			H <sub>2</sub> S - Hydrogen Sulfide
TRS			TRS - Total Reduced Sulfur
RSC			RSC - Reduced Sulfur Compounds

Actual Emissions Attachment 11 of 14

### Newfield MAMIE 4-25-3-3WH

# TANKHTR1



Emission Factors are from AP-42 Table 1.4-1, 1.4-2, 1.4-3, & 1.4-4.

TANKHTR1 Calculation Page 1 of 1

1. Company:	Newfield Exploration			Potential Emissions	
2. Site/Source:	MAMIE 4-25-3-3WH		3. Date: 2/7/2019		
4. Type of Operation:	Oil and Gas	Production Tank	Heater		
5. Emission Point:	ID Number 12	Name TANKHTR2	7. Identification and Description	n of Control Equipment	
<ol> <li>Description of Equ Tank Heater</li> </ol>	ipment:		None		
8. Hours of Operation	n: 8,760	Hours/Year	9. Burner Rating:	250,000	BTU/hr
10. Type of Fuel Use	d: Nat	ural Gas	11. Amount of Fuel Used:	2,190,000,000	BTU/yr

Pollutant	Uncontrolled Emissions	Controlled Emissions	
	(TPY)	(TPY)	
PM	8.16E-03	8.16E-03	DM Dortiouloto Mottor
PM <sub>10</sub>	8.16E-03	8.16E-03	$PM_{co} - PM$ less than 10 microns in size
PM <sub>2.5</sub>	8.16E-03	8.16E-03	$PM_{0.5}$ - PM less than 2.5 microns in size
SO <sub>X</sub>	6.44E-04	6.44E-04	$SO_{\rm v}$ - Sulfur Oxides
NO <sub>X</sub>	1.07E-01	1.07E-01	NO <sub>v</sub> - Nitrogen Oxides
CO	9.02E-02	9.02E-02	CO - Carbon Monoxide
VOC	5.90E-03	5.90E-03	VOC - Volatile Organic Compound
Pb			Pb - Lead and lead compounds
Fluorides			Fluorides - Gaseous and particulates
$H_2SO_4$			$H_2SO_4$ - Sulfuric Acid Mist
H <sub>2</sub> S			H <sub>2</sub> S - Hydrogen Sulfide
TRS			TRS - Total Reduced Sulfur
RSC			RSC - Reduced Sulfur Compounds

Potential Emissions Attachment 12 of 14

	3. Date: 2/7/2019		
oduction Tank	Heater		
Name TANKHTR2	7. Identification and Description	of Control Equipment	
	None		
Hours/Year	9. Burner Rating:	250,000	BTU/hr
al Gas	11. Amount of Fuel Used:	2,190,000,000	BTU/yr
	oduction Tank Name TANKHTR2 Hours/Year al Gas	oduction Tank Heater         Name         TANKHTR2         7. Identification and Description         None         Hours/Year         9. Burner Rating:         al Gas	oduction Tank Heater         Name         TANKHTR2         7. Identification and Description of Control Equipment         None         Hours/Year         9. Burner Rating:       250,000         al Gas       11. Amount of Fuel Used:       2,190,000,000

Pollutant	Uncontrolled Emissions	Controlled Emissions	
	(TPY)	(TPY)	
PM	8.16E-03	8.16E-03	DM Derticulate Metter
PM <sub>10</sub>	8.16E-03	8.16E-03	PM - Particulate Matter
PM <sub>2.5</sub>	8.16E-03	8.16E-03	$PM_{0,r}$ - PM less than 2.5 microns in size
SO <sub>X</sub>	6.44E-04	6.44E-04	$SO_{\rm v}$ - Sulfur Oxides
NO <sub>X</sub>	1.07E-01	1.07E-01	NO <sub>x</sub> - Nitrogen Oxides
CO	9.02E-02	9.02E-02	CO - Carbon Monoxide
VOC	5.90E-03	5.90E-03	VOC - Volatile Organic Compound
Pb			Pb - Lead and lead compounds
Fluorides			Fluorides - Gaseous and particulates
$H_2SO_4$			H <sub>2</sub> SO <sub>4</sub> - Sulfuric Acid Mist
H <sub>2</sub> S			H <sub>2</sub> S - Hydrogen Sulfide
TRS			TRS - Total Reduced Sulfur
RSC			RSC - Reduced Sulfur Compounds

Actual Emissions Attachment 12 of 14

### Newfield MAMIE 4-25-3-3WH

# TANKHTR2



Emission Factors are from AP-42 Table 1.4-1, 1.4-2, 1.4-3, & 1.4-4.

TANKHTR2 Calculation Page 1 of 1

1. Company:	Newfield Exploration			Potential Emissions	
2. Site/Source:	MAMIE 4-25-3-3WH		3. Date: 2/7/2019		
4. Type of Operation:	Oil and Gas	Production Tank	Heater		
5. Emission Point:	ID Number 13	Name TANKHTR3	7. Identification and Descriptio	n of Control Equipment	
<ol> <li>Description of Equ Tank Heater</li> </ol>	ipment:		None		
8. Hours of Operation	n: 8,760	Hours/Year	9. Burner Rating:	250,000	BTU/hr
10. Type of Fuel Use	d: Nat	ural Gas	11. Amount of Fuel Used:	2,190,000,000	BTU/yr

Pollutant	Uncontrolled Emissions	Controlled Emissions	
	(TPY)	(TPY)	
PM	8.16E-03	8.16E-03	DM Particulate Matter
PM <sub>10</sub>	8.16E-03	8.16E-03	$PM_{12} = PM$ less than 10 microns in size
PM <sub>2.5</sub>	8.16E-03	8.16E-03	$PM_{0.5}$ - PM less than 2.5 microns in size
SO <sub>X</sub>	6.44E-04	6.44E-04	$SO_{\rm v}$ - Sulfur Oxides
NO <sub>X</sub>	1.07E-01	1.07E-01	NO <sub>v</sub> - Nitrogen Oxides
CO	9.02E-02	9.02E-02	CO - Carbon Monoxide
VOC	5.90E-03	5.90E-03	VOC - Volatile Organic Compound
Pb			Pb - Lead and lead compounds
Fluorides			Fluorides - Gaseous and particulates
$H_2SO_4$			H <sub>2</sub> SO <sub>4</sub> - Sulfuric Acid Mist
H <sub>2</sub> S			H <sub>2</sub> S - Hydrogen Sulfide
TRS			TRS - Total Reduced Sulfur
RSC			RSC - Reduced Sulfur Compounds

Potential Emissions Attachment 13 of 14

1. Company: Nev	wfield Exploration			Actual Emissions	
2. Site/Source: MA	MIE 4-25-3-3WH		3. Date: 2/7/2019		
4. Type of Operation:	Oil and Gas	Production Tank	Heater		
5. Emission Point:	ID Number	Name	7. Identification and Description	n of Control Equipment	
	13	TANKHTR3			
6. Description of Equipm	nent:		None		
Tank Heater					
8. Hours of Operation:	8,760	Hours/Year	9. Burner Rating:	250,000	BTU/hr
10. Type of Fuel Used:	Na	tural Gas	11. Amount of Fuel Used:	2,190,000,000	BTU/yr

Pollutant	Uncontrolled Emissions	Controlled Emissions	
	(TPY)	(TPY)	
PM	8.16E-03	8.16E-03	DM Dortiouloto Mottor
PM <sub>10</sub>	8.16E-03	8.16E-03	PM - Particulate Matter
PM <sub>2.5</sub>	8.16E-03	8.16E-03	$PM_{o,c}$ - PM less than 2.5 microns in size
SO <sub>X</sub>	6.44E-04	6.44E-04	$SO_{v}$ - Sulfur Oxides
NO <sub>X</sub>	1.07E-01	1.07E-01	NO <sub>v</sub> - Nitrogen Oxides
CO	9.02E-02	9.02E-02	CO - Carbon Monoxide
VOC	5.90E-03	5.90E-03	VOC - Volatile Organic Compound
Pb			Pb - Lead and lead compounds
Fluorides			Fluorides - Gaseous and particulates
$H_2SO_4$			H <sub>2</sub> SO <sub>4</sub> - Sulfuric Acid Mist
H <sub>2</sub> S			H <sub>2</sub> S - Hydrogen Sulfide
TRS			TRS - Total Reduced Sulfur
RSC			RSC - Reduced Sulfur Compounds

Actual Emissions Attachment 13 of 14

### Newfield MAMIE 4-25-3-3WH

# TANKHTR3



Emission Factors are from AP-42 Table 1.4-1, 1.4-2, 1.4-3, & 1.4-4.

TANKHTR3 Calculation Page 1 of 1

1. Company:	Newfield Exploration		Po	tential Emissions
2. Site/Source:	MAMIE 4-25-3-3WH		3. Date: 2/01/2019	
4. Type of Operation:	Flare			
5. Emission Point:	ID Number 14	Name FLARE-1	7. Identification and Description	on of Control Equipment
6. Description of Equip Flare	oment:			Flare
8. Throughput:	78	scf/hr	9. Operating Schedule:	Not Applicable

	1	1	
Pollutant	Uncontrolled Emissions	Controlled Emissions	
	(1F1)	(IFT)	
PM			DM Derticulate Matter
PM			Pini - Particulate Matter
1 1110			PM <sub>10</sub> - PM less than 10 microns in size
PM <sub>2.5</sub>			PM <sub>es</sub> - PM less than 2.5 microns in size
SO <sub>X</sub>			$SO_{\rm Y}$ - Sulfur Oxides
NO <sub>x</sub>		3.93E-02	NO Nitrogen Oxides
0.0		2 140E-01	
200		2.1402 01	CO - Carbon Monoxide
VOC		3.00E-02	VOC - Volatile Organic Compound
Pb			Pb - Lead and lead compounds
Fluorides			Fluorides - Gaseous and particulates
H <sub>2</sub> SO <sub>4</sub>			$H_2SO_4$ - Sulfuric Acid Mist
HaS		Negligible	H.S. Hydrogen Sulfide
1120		Itegligible	H <sub>2</sub> S - Hydrogen Sunde
TRS			TRS - Total Reduced Sulfur
RSC			RSC - Reduced Sulfur Compounds

Potential Emissions Attachment 14 of 14

1. Company:	Newfield Exploration		Ac	tual Emissions
2. Site/Source:	MAMIE 4-25-3-3WH		3. Date: 2/07/2019	
4. Type of Operation:	Flare			
5. Emission Point:	ID Number 14	Name FLARE-1	7. Identification and Description	on of Control Equipment
6. Description of Equip Flare	oment:			Flare
8. Throughput:	78	scf/hr	9. Operating Schedule:	Not Applicable

Pollutant	Uncontrolled Emissions	Controlled Emissions	
	(TPY)	(TPY)	
PM			
PM			PM - Particulate Matter
1 10110			PM <sub>10</sub> - PM less than 10 microns in size
PM <sub>2.5</sub>			PM <sub>25</sub> - PM less than 2.5 microns in size
SO <sub>X</sub>			SO <sub>v</sub> - Sulfur Oxides
NO <sub>X</sub>		3.93E-02	NO <sub>x</sub> - Nitrogen Oxides
CO		2.140E-01	CO - Carbon Monoxide
VOC		3.00E-02	VOC - Volatile Organic Compound
Pb			Pb - Lead and lead compounds
Fluorides			Fluorides - Gaseous and particulates
H <sub>2</sub> SO <sub>4</sub>			$H_2SO_4$ - Sulfuric Acid Mist
H <sub>2</sub> S		Negligible	H <sub>2</sub> S - Hydrogen Sulfide
TRS			TRS - Total Reduced Sulfur
RSC			RSC - Reduced Sulfur Compounds

Actual Emissions Attachment 14 of 14



Combustor Calculation Page 1 of 2



CO <sub>2</sub> : 78 scf/hr x 1,682 Btu/scf x 1 Mmbtu/1,000,000 Btu x 117.65 lb/MMBtu 1.55E+01 lb/hr x 8760 hr/yr x 1 ton/2000 lb	= <b>1.55E+01</b> lb/hr = <b>6.80E+01</b> TPY
CH4: 78 scf/hr x 1,682 Btu/scf x 1 Mmbtu/1,000,000 Btu x 0.077 lb/MMBtu 1.02E-02 lb/hr x 8760 hr/yr x 1 ton/2000 lb	CH <sub>4</sub> as CO <sub>2</sub> e: = 1.02E-02 lb/hr 3.15E+00 lb/hr = 4.45E-02 TPY 1.38E+01 TPY
N <sub>2</sub> O: 78 scf/hr x 1,682 Btu/scf x 1 Mmbtu/1,000,000 Btu x 0.002 lb/MMBtu 2.85E-04 lb/hr x 8760 hr/yr x 1 ton/2000 lb	N2O as CO2e:         2.85E-04       lb/hr         8.83E-02       lb/hr         =       1.25E-03       TPY         3.87E-01       TPY

NOx, CO, VOC, & CH<sub>4</sub> emission factors are from AP-42 Table 13.5-1 & 13.5-2

(Emission Factors for Flare Operations).

CO<sub>2</sub> & N<sub>2</sub>O emission factors are from AP-42 Table 1.4-2

(Emission Factors for Natural Gas Combustion).

Combustor Calculation Page 2 of 2

1. Company:	Newfield Exploration		P	otential Emission	s
2. Site/Source:	MAMIE 4-25-3-3WH		3. Date: 2/22/2019		
4. Type of Operatio	n: Oil and Gas	Production Engine	9		
5. Emission Point:	ID Number	Name	7. Identification and Description	of Control Equipment	
	15	ENG-2			
6. Description of Eq	juipment:		None		
Blue Star 480	V, 175 kW				
8. Fuel Consumptio	n: 16.22	MMscf/yr	.9. Operating Schedule:	8,760	Hours/yr

Pollutant	Uncontrolled Emissions	Controlled Emissions	
	(TPY)	(TPY)	
PM	1.60E-01	1.60E-01	PM Dortioulate Matter
PM <sub>10</sub>	1.60E-01	1.60E-01	PM - PM less than 10 microns in size
PM <sub>2.5</sub>	1.60E-01	1.60E-01	$PM_{0.5}$ - PM less than 2.5 microns in size
SO <sub>X</sub>	4.85E-03	4.85E-03	$SO_{\rm v}$ - Sulfur Oxides
NO <sub>X</sub>	2.26E+00	2.26E+00	NO <sub>v</sub> - Nitrogen Oxides
CO	4.52E+00	4.52E+00	CO - Carbon Monoxide
VOC	1.58E+00	1.58E+00	VOC - Volatile Organic Compound
Pb			Pb - Lead and lead compounds
Fluorides			Fluorides - Gaseous and particulates
$H_2SO_4$			H <sub>2</sub> SO <sub>4</sub> - Sulfuric Acid Mist
H <sub>2</sub> S			H <sub>2</sub> S - Hydrogen Sulfide
TRS			TRS - Total Reduced Sulfur
RSC			RSC - Reduced Sulfur Compounds

Potential Emissions Attachment 1 of 14

1. Company:	Newfield Exploration			Actual Emissions	
2. Site/Source:	MAMIE 4-25-3-3WH		3. Date: 2/22/2019		
4. Type of Operatio	n: Oil and Gas	Production Engine	)		
5. Emission Point:	ID Number	Name	7. Identification and Description	of Control Equipment	
	15	ENG-2			
6. Description of Eq	uipment:		None		
Blue Star 480	V, 175 kW				
8. Fuel Consumptio	n: 16.22	MMscf/yr	9. Operating Schedule:	8,760	Hours/yr

Pollutant	Uncontrolled Emissions	Controlled Emissions	
	(TPY)	(TPY)	
PM	1.60E-01	1.60E-01	DM Dortioulote Motter
PM <sub>10</sub>	1.60E-01	1.60E-01	PM - PM less than 10 microns in size
PM <sub>2.5</sub>	1.60E-01	1.60E-01	$PM_{0.5}$ - PM less than 2.5 microns in size
SO <sub>X</sub>	4.85E-03	4.85E-03	$SO_{\rm v}$ - Sulfur Oxides
NO <sub>X</sub>	2.26E+00	2.26E+00	NO <sub>v</sub> - Nitrogen Oxides
CO	4.52E+00	4.52E+00	CO - Carbon Monoxide
VOC	1.58E+00	1.58E+00	VOC - Volatile Organic Compound
Pb			Pb - Lead and lead compounds
Fluorides			Fluorides - Gaseous and particulates
$H_2SO_4$			H <sub>2</sub> SO <sub>4</sub> - Sulfuric Acid Mist
H <sub>2</sub> S			H <sub>2</sub> S - Hydrogen Sulfide
TRS			TRS - Total Reduced Sulfur
RSC			RSC - Reduced Sulfur Compounds

Actual Emissions Attachment 1 of 14 Newfield MAMIE 4-25-3-3WH

ENG-2



NOx, CO & VOC Emission Factors are from manufacturer's data. SO2, PM, & PM2.5 & HAPs Emission Factors are from AP-42 Table 3.2-1, Table 3.2-2, or Table 3.2-3.

ENG-2 Calculation Page 1 of 1

	Newfield MAMIE 4-25-3-3V HTRTRTR-2	VH
Burner Rating	<b>1,000,000</b> Btu/hr	
NO <sub>x</sub> : 0.10 lb/MMBtu	x 1.00 MMBtu/hr	= <b>9.80E-02</b> lb/hr
9.80E-02 lb/hr	x 8,760 hr/yr x 1 ton / 2	2000 lb = <b>4.29E-01</b> TPY
CO: 0.082 lb/MMBtu	x 1.00 MMBtu/hr	= <b>8.24E-02</b> lb/hr
8.24E-02 lb/hr	x 8,760 hr/yr x 1 ton / 2	2000 lb = <b>3.61E-01</b> TPY
VOC: 0.0054 lb/MMBtu	x 1.00 MMBtu/hr	= <b>5.39E-03</b> lb/hr
5.39E-03 lb/hr	x 8,760 hr/yr x 1 ton / 2	2000 lb = <b>2.36E-02</b> TPY
<b>SO</b> <sub>2</sub> : 0.0006 lb/MMBtu	x 1.00 MMBtu/hr	= <b>5.88E-04</b> lb/hr
5.88E-04 lb/hr	x 8,760 hr/yr x 1 ton / 2	2000 lb = <b>2.58E-03</b> TPY
PM: 0.0075 lb/MMBtu	x 1.00 MMBtu/hr	= <b>7.45E-03</b> lb/hr
7.45E-03 lb/hr	x 8,760 hr/yr x 1 ton / 2	2000 lb = <b>3.26E-02</b> TPY

Emission Factors are from AP-42 Table 1.4-1, 1.4-2, 1.4-3, & 1.4-4.

HTRTRTR-2 Calculation Page 1 of 2

			Newfield MAMIE 4-25-3	3-3WH		
HTRTRTR-2						
	Burner Rating	1,000,000	Btu/hr			
Benzene:	2.06E-06 lb/MMBtu 2.06E-06 lb/hr	ı x	1.00 MMBtu/hr 8,760 hr/yr x 1 to	= <b>2.06E-06</b> lb/hr on / 2000 lb = <b>9.02E-06</b> TPY		
Toluene:	3.33E-06 lb/MMBtu 3.33E-06 lb/hr	- x x	1.00 MMBtu/hr 8,760 hr/yr x 1 to	= <b>3.33E-06</b> lb/hr on / 2000 lb = <b>1.46E-05</b> TPY		
n-Hexane:	1.76E-03 lb/MMBtu 1.76E-03 lb/hr	x x	1.00 MMBtu/hr 8,760 hr/yr x 1 to	= <b>1.76E-03</b> lb/hr on / 2000 lb = <b>7.73E-03</b> TPY		
Formaldehyde:	7.35E-05 lb/MMBtu 7.35E-05 lb/hr	× ×	1.00 MMBtu/hr 8,760 hr/yr x 1 to	= <b>7.35E-05</b> lb/hr on / 2000 lb = <b>3.22E-04</b> TPY		

Emission Factors are from AP-42 Table 1.4-1, 1.4-2, 1.4-3, & 1.4-4.

HTRTRTR-2 Calculation Page 2 of 2

1. Company:	Newfield Exploration		Potential Emissions
2. Site/Source: MAMIE 4-25-3-3WH			3. Date: 2/22/2019
4. Type of Operation:	Oil and Ga	s Production Wel	l Fugitives
5. Emission Point:	ID Number	Name	7. Identification and Description of Control Equipment
	17	FUG-2	N/A
6. Description of Equ	ipment:		
Oil Well Fugitive	e Emissions		

Pollutant	Uncontrolled Emissions (TPY)	Controlled Emissions (TPY)	
PM			PM Particulate Matter
PM <sub>10</sub>			$PM_{in} = PM$ less than 10 microns in size
PM <sub>2.5</sub>			$PM_{10} = PM$ less than 2.5 microns in size
SO <sub>X</sub>			$SO_{12}$ - Sulfur Oxides
NO <sub>X</sub>			NO <sub>x</sub> - Nitrogen Oxides
CO			CO - Carbon Monoxide
VOC	5.42E-02	5.42E-02	VOC - Volatile Organic Compound
Pb			Pb - Lead and lead compounds
Fluorides			Fluorides - Gaseous and particulates
$H_2SO_4$			$H_2SO_4$ - Sulfuric Acid Mist
H <sub>2</sub> S			H <sub>2</sub> S - Hydrogen Sulfide
TRS			TRS - Total Reduced Sulfur
RSC			RSC - Reduced Sulfur Compounds

Potential Emissions Attachment 3 of 14

### OIL PRODUCTION WELL FUGITIVES 2 Newfield MAMIE 4-25-3-3WH

EQUIPMENT TYPE	NUMBER	HOURS OF	VOC	CH₄	EMISSION	EMISSION	VOC	CH₄
AND SERVICE	OF	OPERATION	WEIGHT	WEIGHT	FACTOR <sup>3</sup>	FACTOR	EMISSIONS	EMISSIONS
		(hours/yr)	FRACTION <sup>2</sup>	FRACTION <sup>2</sup>	(kg/hr-unit)	(lb/hr-unit)	(tons/yr)	(tons/yr)
Wellhead								
Valves	5	8760	0.070	0.775	0.0025	0.005525	8.43E-03	9.37E-02
Connectors	4	8760	0.070	0.775	0.00021	0.0004641	5.66E-04	6.30E-03
Open-Ended Lines	0	8760	0.070	0.775	0.0014	0.003094	0.00E+00	0.00E+00
Flanges	10	8760	0.070	0.775	0.00011	0.0002431	7.42E-04	8.25E-03
Other	1	8760	0.070	0.775	0.0075	0.016575	5.06E-03	5.62E-02
Separator								
Valves	6	8760	0.070	0.775	0.0025	0.005525	1.01E-02	1.12E-01
Connectors	10	8760	0.070	0.775	0.00021	0.0004641	1.42E-03	1.57E-02
Open-Ended Lines	0	8760	0.070	0.775	0.0014	0.003094	0.00E+00	0.00E+00
Flanges	12	8760	0.070	0.775	0.00011	0.0002431	8.90E-04	9.90E-03
Other	0	8760	0.070	0.775	0.0075	0.016575	0.00E+00	0.00E+00
Heater Treater								
Valves	8	8760	0.070	0.775	0.0025	0.005525	1.35E-02	1.50E-01
Connectors	20	8760	0.070	0.775	0.00021	0.0004641	2.83E-03	3.15E-02
Open-Ended Lines	0	8760	0.070	0.775	0.0014	0.003094	0.00E+00	0.00E+00
Flanges	12	8760	0.070	0.775	0.00011	0.0002431	8.90E-04	9.90E-03
Other	0	8760	0.070	0.775	0.0075	0.016575	0.00E+00	0.00E+00
Header								
Valves	5	8760	0.070	0.775	0.0025	0.005525	8.43E-03	9.37E-02
Connectors	4	8760	0.070	0.775	0.00021	0.0004641	5.66E-04	6.30E-03
Open-Ended Lines	0	8760	0.070	0.775	0.0014	0.003094	0.00E+00	0.00E+00
Flanges	10	8760	0.070	0.775	0.00011	0.0002431	7.42E-04	8.25E-03
Other	0	8760	0.070	0.775	0.0075	0.016575	0.00E+00	0.00E+00
TOTAL EMISSIONS (tons/y	r)						5.42E-02	6.02E-01

Pollutant	Weight Fraction <sup>2</sup>	HAP Emissions (tons/yr)	HAP Emissions (lb/hr)	
n-Hexane	0.00000	0.00E+00	0.00E+00	
Benzene	0.00167	1.30E-03	2.96E-04	
2,2,4 Trimethylpentane	0.00020	1.55E-04	3.55E-05	
Toluene	0.00161	1.25E-03	2.86E-04	
Ethylbenzene	0.00008	6.22E-05	1.42E-05	
M&P XylenesO-Xylenes	0.00031	2.41E-04	5.50E-05	
Total HAPs		3.01E-03	6.87E-04	

<sup>1</sup>Average component count from Table W-1C to Subpart W of Part 98-Default Average Component Counts For Major Crude Oil Production Equipment. <sup>2</sup>Based on gas composition and properties from samples collected at the KM Bar F fuel tap. HAPs values from samples collected at 12 different Newfield sites.

<sup>3</sup>"Protocol for Equipment Leak Emission Estimates," EPA-453/R-95-017, Table 2-4, Light Oil

1. Company:	Newfield Exploration		Potential Emissions		
2. Site/Source:	MAMIE 4-25-3-3WH		3. Date: 2/7/2019		
4. Type of Operation:	Oil and Gas	Production Tanks			
5. Emission Point:	ID Number 18	Name OILTK-4	7. Identification and Descrip	tion of Control Equipment	
6. Description of Equi 400 Barrel Ve	pment: rtical Fixed Roof Steel Oil	Tank		Flare	
8. Throughput:	91,250	barrels/year	. 9. Operating Schedule:	Not Applicable	

Pollutant	Uncontrolled Emissions (TPY)	Controlled Emissions	
PM	(11.1)	(11.1)	
PM <sub>10</sub>			PM - Particulate Matter
PM <sub>2.5</sub>			$PM_{0.5}$ - PM less than 2.5 microns in size
SOX			$SO_{\rm Y}$ - Sulfur Oxides
NO <sub>X</sub>		4.77E-02	NO <sub>x</sub> - Nitrogen Oxides
CO		2.59E-01	CO - Carbon Monoxide
VOC	2.70E+01	5.40E-01	VOC - Volatile Organic Compound
Pb			Pb - Lead and lead compounds
Fluorides			Fluorides - Gaseous and particulates
$H_2SO_4$			$H_2SO_4$ - Sulfuric Acid Mist
H <sub>2</sub> S	Negligible	Negligible	H <sub>2</sub> S - Hydrogen Sulfide
TRS			TRS - Total Reduced Sulfur
RSC			RSC - Reduced Sulfur Compounds

Potential Emissions Attachment 4 of 14

# FLASH LIBERATION OF HYDROCARBON LIQUID

### FROM CENTRAL BASIN OIL STORAGE TANKS

### MAMIE 4-25-3-3WH

CB UB SXL

OILTK-4	PTE	
GOR from analysis	6.64	scf/bbl
Throughput (bbls/yr)	91,250	bbls/yr
Throughput (bbls/day)	250.00	bbls/day
Gas Flash Rate (SCFD):	1,660.0	scfd
Gas Flash Rate (lbs./day):	187.452	lb/day
Lb./Day = gas (ft <sup>3</sup> /day)x(Mwgas - lb/lb-mole) / (379.49 ft3/lb-mole)		

Gas oil ratio and mole percent of flash gas are representative of tanks in this region.

Component	Mole percent	Molecular Weight	Mole Frac x Mole <b>Stream MW</b>	Weight Percent	Weight Fraction	PTE Uncontrolled Emissions (lb/hr)	PTE Uncontrolled Emissions (tpy)
Hydrogen Sufide	0.000%	34.080	0.0000	0.000%	0.0000	0.00E+00	0.00E+00
Nitrogen	3.093%	28.013	0.8664	2.022%	0.0202	1.58E-01	6.92E-01
Carbon Dioxide	0.751%	44.010	0.3307	0.772%	0.0077	6.03E-02	2.64E-01
Methane	33.643%	16.043	5.3974	12.595%	0.1260	9.84E-01	4.31E+00
Ethane	15.073%	30.070	4.5325	1 <b>0.577%</b>	0.1058	8.26E-01	3.62E+00
Propane	13.269%	44.097	5.8513	13.654%	0.1365	1.07E+00	4.67E+00
Iso-Butane	3.081%	58.123	1.7909	4.179%	0.0418	3.26E-01	1.43E+00
n-Butane	7.803%	58.123	4.5352	10.583%	0.1058	8.27E-01	3.62E+00
2,2 Dimethylpropane	0.000%	72.140	0.0000	0.000%	0.0000	0.00E+00	0.00E+00
Iso-Pentane	2.905%	72.150	2.0957	4.890%	0.0489	3.82E-01	1.67E+00
n-Pentane	4.186%	72.150	3.0205	7.048%	0.0705	5.51E-01	2.41E+00
2,2 Dimethylbutane	0.158%	86.178	0.1363	0.318%	0.0032	2.48E-02	1.09E-01
Cyclopentane	1.187%	70.100	0.8324	1.942%	0.0194	1.52E-01	6.64E-01
2,3 Dimethylbutane	0.237%	86.178	0.2046	0.477%	0.0048	3.73E-02	1.63E-01
2 Methylpentane	0.481%	86.178	0.4145	0.967%	0.0097	7.56E-02	3.31E-01
3 Methylpentane	0.283%	86.178	0.2441	0.570%	0.0057	4.45E-02	1.95E-01
n-Hexane	8.062%	86.178	6.9478	16.213%	0.1621	1.27E+00	5.55E+00
Methylcyclopentane	0.953%	84.160	0.8020	1.872%	0.0187	1.46E-01	6.40E-01
Benzene	0.220%	78.114	0.1717	0.401%	0.0040	3.13E-02	1.37E-01
Cyclohexane	0.225%	84.160	0.1890	0.441%	0.0044	3.45E-02	1.51E-01
2-Methylhexane	0.056%	100.200	0.0563	0.131%	0.0013	1.03E-02	4.50E-02
3-Methylhexane	0.080%	100.200	0.0806	0.188%	0.0019	1.47E-02	6.43E-02
2,2,4 Trimethylpentane	0.079%	114.230	0.0905	0.211%	0.0021	1.65E-02	7.22E-02

OILTK-4 Calculation Page 1 of 4

# FLASH LIBERATION OF HYDROCARBON LIQUID

### FROM CENTRAL BASIN OIL STORAGE TANKS

### MAMIE 4-25-3-3WH

#### CB UB SXL

OILTK-4	PTE	
GOR from analysis	6.64	scf/bbl
Throughput (bbls/yr)	91,250	bbls/yr
Throughput (bbls/day)	250.00	bbls/day
Gas Flash Rate (SCFD):	1,660.0	scfd
Gas Flash Rate (lbs./day):	187.452	lb/day
Lb./Day = gas (ft <sup>3</sup> /day)x(Mwgas - lb/lb-mole) / (379.49 ft3/lb-mole)		

Gas oil ratio and mole percent of flash gas are representative of tanks in this region.

Component	Mole percent	Molecular Weight	Mole Frac x Mole <b>Stream MW</b>	Weight Percent	Weight Fraction	PTE Uncontrolled Emissions (lb/hr)	PTE Uncontrolled Emissions (tpy)		
Other C7's	1.588%	100.272	1.5925	3.716%	0.0372	2.90E-01	1.27E+00		
n-Heptane	0.635%	100.272	0.6367	1.486%	0.0149	1.16E-01	5.08E-01		
Mehtylcyclohexane	0.712%	98.190	0.6995	1.632%	0.0163	1.27E-01	5.58E-01		
Toluene	0.425%	92.140	0.3918	0.914%	0.0091	7.14E-02	3.13E-01		
Other C8's	0.367%	114.230	0.4192	0.978%	0.0098	7.64E-02	3.35E-01		
n-Octane	0.198%	114.230	0.2257	0.527%	0.0053	4.11E-02	1.80E-01		
Ethylbenzene	0.042%	106.170	0.0448	0.105%	0.0010	8.17E-03	3.58E-02		
M&P Xylenes	0.061%	106.170	0.0652	0.152%	0.0015	1.19E-02	5.20E-02		
O-Xylenes	0.012%	106.170	0.0130	0.030%	0.0003	2.36E-03	1.03E-02		
Other C9's	0.063%	128.258	0.0811	0.189%	0.0019	1.48E-02	6.47E-02		
n-Nonane	0.034%	128.258	0.0434	0.101%	0.0010	7.90E-03	3.46E-02		
Other C10's	0.024%	142.280	0.0347	0.081%	0.0008	6.33E-03	2.77E-02		
n-Decane	0.007%	142.280	0.0097	0.023%	0.0002	1.76E-03	7.72E-03		
Undecanes+	0.004%	156.310	0.0056	0.013%	0.0001	1.03E-03	4.49E-03		
Total	100.000%		42.853	100.000%					
	Total: 7.8105E+00 3.4210E+01								

VOC INFO	
Mole % VOCs	47.44%
Total NM/NE Stream MW VOCs	31.726
lb Voc / mmscf	83602.308
MMSCF/YR	0.606

	Uncontrolled	Uncontrolled
	Emissions, (lb/hr)	Emissions, (tpy)
Total VOC:	5.78E+00	2.53E+01
Total Me/Eth	1.81E+00	7.93E+00

OILTK-4 Calculation Page 2 of 4

AP-42 TANK WORKING and BREATHING EMISSIO OILTK-4 Newfie	NS Id MAMIE 4-	25-3-3WH		
INPUT DA	TA			
	Symbol	PTE	Units	
Molecular Weight	Mir	50	l h/lh mode	-
Tank design data	IVIV	50	LD/ID-MOle	-
Shell height	Hs	20.00	ft	
Diameter	D	12.00	ft	
Liquid height	HI	20.00	ft	
Ava, Liquid height	HI	10.00	ft	
vapor space outage	Hvo	10.00	ft	
Tank volume		16,921	gallons	
Turnovers	N	226		
Net throughput	Q	91250.00	bbl/yr	
Tunover factor	KN	0.299	1	
Working loss product factor	Кр	0.75		From AP-42, 11/06 Section 7 Equ. 1-31, page 7.1-19
leteorological data				
Daily ave. ambient temp.	TAA	51.9625	°F	From TANKS
Daily max. ambient temp.	TAX	63.641667	°F	for Salt Lake
Daily min. ambient temp.	TAN	40.283333	°F	City, UT
Daily ambient temp. range	DTA	23.36	°F	
I ank paint solar absorptance (see adjacent table)	α	0.68	-	I ank color gray, condition good
Daily total insolation factor	-	1,452.11835	Btu/ft2-day	From TANKS for Salt Lake City, UT
Site elevation (feet)	DA	4,162		-
Atmospheric pressure	PA	12.644		-
Liquid bulk tomporature	TP	61.40	٥E	Took is booted and temperature veries + 2°F
Daily yapor tomp, range	DTy	4.00	PE	Tank is heated and temperature varies $\pm 2$ F
Daily vapor temp. range	DIV	4.00		
Daily ave liquid surface temp	TLA	65 10	°F	
Daily max_liquid surface temp	TLX	66 10	°F	
Daily min. liquid surface temp.	TIN	64.10	°F	
Baily miningala banabb tempi		00		
VP @ daily ave. liquid surf. temp.	PvA	165.19	mm Hg	Equation from AP-42, 11/06 Section 7 Figure 7.1-13b
VP @ daily max. liquid surf. temp.	PvX	168.39	mm Hg	Equation from AP-42, 11/06 Section 7 Figure 7.1-13t
VP @ daily min. liquid surf. temp.	PvN	162.03	mm Hg	Equation from AP-42, 11/06 Section 7 Figure 7.1-13t
Daily vapor pressure range	DPv	6.36	mm Hg	
Breather vent pressure setting range	DPB	0.06	psia	Value from AP-42, 11/06 Section 7 page 7.1-13 Note
Breather vent pressure setting range	DPB	3.10	mm Hg	
CALCULATIONS		1		
	Symbol		Units	-
Prosthing Jacoba				-
Tank vanor snaco volumo	Mar (	1 130 08	#3	-
Vapor dopsity	VV \\\\\	2 834E-02	lb/#2	-
Vapor space expansion factor	KE	0.01/27	10/113	
Vented vapor saturation factor	Ks	0.01427	ft2	
Vented vapor saturation factor	113	0.0710	112	
Breathing losses	IB	62.02	lb/vr	
			, j :	
Vorking losses	Lw	3,269.36	lb/yr	
0			,	
TOTAL LOSSES	LT	0.38	lb/hr	
		3,331.38	lb/yr	
		1.6657	tpy	<u>_</u>
		69.27	scfd	<u>_</u>
IAP Emissions <sup>2</sup>	Wt%			
n-Hexane	16.21%	0.27	tpy	
Benzene	0.40%	0.01	tpy	
2,2,4-Trimethylpentane	0.21%	0.00	tpy	<u>_</u>
Toluene	0.91%	0.02	tpy	<u>_</u>
Ethylbenzene	0.10%	0.00	tpy	4
Xylenes	0.18%	0.00	tpy	

<sup>1</sup>Calculations performed on this spreadsheet are taken from the USEPA AP-42- Section 7.1 Organic Liquid Storage Tanks - November 2006. <sup>2</sup>HAP Emissions (tpy) = HAP Wt% \* Total Losses (tpy)

Paint Color	Paint Shade or Type	Good	Poor
Aluminum	Specular	0.39	0.49
Aluminum	Diffuse	0.6	0.68
Aluminum	Mill finish, unpainted	0.1	0.15
Beige/Cream		0.35	0.49
Black		0.97	0.97
Brown		0.58	0.67
Gray	Light	0.54	0.63
Gray	Medium	0.68	0.74
Green	Dark	0.89	0.91
Red	Primer	0.89	0.91
Rust	Red iron oxide	0.38	0.5
Tan		0.43	0.55
White	NA	0.17	0.34

From AP-42, 11/06 Section 7 Table 7.1-6, page 7.1-69

OILTK-4 Calculation Page 3 of 4



Potential to Emit Emission Calculations

Maximum Tank Vapor 72.1 scf/hr Lower Heating Value 2,222 Btu/scf	Controlled emissions are calculated based on a 98% destruction efficiency of the VOC gas.
VOC: 6.16E+00 lb/hr x 100% - 98% 2.70E+01 TPY x 100% - 98%	= 1.23E-01 ib/hr = 5.40E-01 TPY
Benzene: 3.28E-02 lb/hr x 100% - 98%	= 6.56E-04 lb/hr = 2.87E-03 TPY
Toluene:         7.49E-02         lb/hr         x         100% -         98%           3.28E-01         TPY         x         100% -         98%	= 1.50E-03 lb/hr = 6.56E-03 TPY
Ethylbenzene: 8.56E-03 lb/hr x 100% - 98%	= 1.71E-04 lb/hr
0.102-02 111 1 100//* 30//	= 7.502-04 111
Xylenes:         1.49E-02         lb/hr         x         100% -         98%           6.54E-02         TPY         x         100% -         98%	= 2.99E-04 lb/hr = 1.31E-03 TPY
Xylenes:         1.49E-02         ib/hr         x         100% -         98%           6.54E-02         TPY         x         100% -         98%           n-Hexane:         1.33E+00         lb/hr         x         100% -         98%           5.82E+00         TPY         x         100% -         98%	= 2.99E-04 ib/hr = 1.31E-03 TPY = 2.66E-02 ib/hr = 1.16E-01 TPY

Maximum Tank Vapor is a sum of the gas flash rate (scfd) plus the total losses rate (scfd) converted to scf/hr.

OILTK-4 Calculation Page 4 of 4

1. Company:	Newfield Exploration		Potential Emissions		
2. Site/Source:	MAMIE 4-25-3-3WH		3. Date: 2/7/2019		
4. Type of Operation:	Oil and Gas	Production Tanks			
5. Emission Point:	ID Number 19	Name OILTK-5	7. Identification and Descripti	on of Control Equipment	
6. Description of Equi 400 Barrel Ve	pment: rtical Fixed Roof Steel Oil	Tank		Flare	
8. Throughput:	91,250	barrels/year	. 9. Operating Schedule:	Not Applicable	

Pollutant	Uncontrolled Emissions (TPY)	Controlled Emissions	
PM	(11.1)	(11-1)	
PM <sub>10</sub>			PM - Particulate Matter
PM <sub>2.5</sub>			$PM_{0.5}$ - PM less than 2.5 microns in size
SOX			$SO_{\rm Y}$ - Sulfur Oxides
NO <sub>X</sub>		4.77E-02	NO <sub>x</sub> - Nitrogen Oxides
CO		2.59E-01	CO - Carbon Monoxide
VOC	2.70E+01	5.40E-01	VOC - Volatile Organic Compound
Pb			Pb - Lead and lead compounds
Fluorides			Fluorides - Gaseous and particulates
$H_2SO_4$			$H_2SO_4$ - Sulfuric Acid Mist
H <sub>2</sub> S	Negligible	Negligible	H <sub>2</sub> S - Hydrogen Sulfide
TRS			TRS - Total Reduced Sulfur
RSC			RSC - Reduced Sulfur Compounds

Potential Emissions Attachment 5 of 14

# FLASH LIBERATION OF HYDROCARBON LIQUID

### FROM CENTRAL BASIN OIL STORAGE TANKS

### MAMIE 4-25-3-3WH

CB UB SXL

OILTK-5	PTE	
GOR from analysis	6.64	scf/bbl
Throughput (bbls/yr)	91,250	bbls/yr
Throughput (bbls/day)	250.00	bbls/day
Gas Flash Rate (SCFD):	1,660.0	scfd
Gas Flash Rate (lbs./day):	187.452	lb/day
Lb./Day = gas (ft <sup>3</sup> /day)x(Mwgas - lb/lb-mole) / (379.49 ft3/lb-mole)		

Gas oil ratio and mole percent of flash gas are representative of tanks in this region.

Component	Mole percent	Molecular Weight	Mole Frac x Mole <b>Stream MW</b>	Weight Percent	Weight Fraction	PTE Uncontrolled Emissions (lb/hr)	PTE Uncontrolled Emissions (tpy)
Hydrogen Sufide	0.000%	34.080	0.0000	0.000%	0.0000	0.00E+00	0.00E+00
Nitrogen	3.093%	28.013	0.8664	2.022%	0.0202	1.58E-01	6.92E-01
Carbon Dioxide	0.751%	44.010	0.3307	0.772%	0.0077	6.03E-02	2.64E-01
Methane	33.643%	16.043	5.3974	12.595%	0.1260	9.84E-01	4.31E+00
Ethane	15.073%	30.070	4.5325	10.577%	0.1058	8.26E-01	3.62E+00
Propane	13.269%	44.097	5.8513	13.654%	0.1365	1.07E+00	4.67E+00
Iso-Butane	3.081%	58.123	1.7909	4.179%	0.0418	3.26E-01	1.43E+00
n-Butane	7.803%	58.123	4.5352	10.583%	0.1058	8.27E-01	3.62E+00
2,2 Dimethylpropane	0.000%	72.140	0.0000	0.000%	0.0000	0.00E+00	0.00E+00
Iso-Pentane	2.905%	72.150	2.0957	4.890%	0.0489	3.82E-01	1.67E+00
n-Pentane	4.186%	72.150	3.0205	7.048%	0.0705	5.51E-01	2.41E+00
2,2 Dimethylbutane	0.158%	86.178	0.1363	0.318%	0.0032	2.48E-02	1.09E-01
Cyclopentane	1.187%	70.100	0.8324	1.942%	0.0194	1.52E-01	6.64E-01
2,3 Dimethylbutane	0.237%	86.178	0.2046	0.477%	0.0048	3.73E-02	1.63E-01
2 Methylpentane	0.481%	86.178	0.4145	0.967%	0.0097	7.56E-02	3.31E-01
3 Methylpentane	0.283%	86.178	0.2441	0.570%	0.0057	4.45E-02	1.95E-01
n-Hexane	8.062%	86.178	6.9478	16.213%	0.1621	1.27E+00	5.55E+00
Methylcyclopentane	0.953%	84.160	0.8020	1.872%	0.0187	1.46E-01	6.40E-01
Benzene	0.220%	78.114	0.1717	0.401%	0.0040	3.13E-02	1.37E-01
Cyclohexane	0.225%	84.160	0.1890	0.441%	0.0044	3.45E-02	1.51E-01
2-Methylhexane	0.056%	100.200	0.0563	0.131%	0.0013	1.03E-02	4.50E-02
3-Methylhexane	0.080%	100.200	0.0806	0.188%	0.0019	1.47E-02	6.43E-02
2,2,4 Trimethylpentane	0.079%	114.230	0.0905	0.211%	0.0021	1.65E-02	7.22E-02

OILTK-5 Calculation Page 1 of 4

# FLASH LIBERATION OF HYDROCARBON LIQUID

### FROM CENTRAL BASIN OIL STORAGE TANKS

### MAMIE 4-25-3-3WH

CB UB SXL

OILTK-5	PTE	
GOR from analysis	6.64	scf/bbl
Throughput (bbls/yr)	91,250	bbls/yr
Throughput (bbls/day)	250.00	bbls/day
Gas Flash Rate (SCFD):	1,660.0	scfd
Gas Flash Rate (lbs./day):	187.452	lb/day
Lb./Day = gas (ft <sup>3</sup> /day)x(Mwgas - lb/lb-mole) / (379.49 ft3/lb-mole)		

Gas oil ratio and mole percent of flash gas are representative of tanks in this region.

Component	Mole percent	Molecular Weight	Mole Frac x Mole <b>Stream MW</b>	Weight Percent	Weight Fraction	PTE Uncontrolled Emissions (lb/hr)	PTE Uncontrolled Emissions (tpy)
Other C7's	1.588%	100.272	1.5925	3.716%	0.0372	2.90E-01	1.27E+00
n-Heptane	0.635%	100.272	0.6367	1.486%	0.0149	1.16E-01	5.08E-01
Mehtylcyclohexane	0.712%	98.190	0.6995	1.632%	0.0163	1.27E-01	5.58E-01
Toluene	0.425%	92.140	0.3918	0.914%	0.0091	7.14E-02	3.13E-01
Other C8's	0.367%	114.230	0.4192	0.978%	0.0098	7.64E-02	3.35E-01
n-Octane	0.198%	114.230	0.2257	0.527%	0.0053	4.11E-02	1.80E-01
Ethylbenzene	0.042%	106.170	0.0448	0.105%	0.0010	8.17E-03	3.58E-02
M&P Xylenes	0.061%	106.170	0.0652	0.152%	0.0015	1.19E-02	5.20E-02
O-Xylenes	0.012%	106.170	0.0130	0.030%	0.0003	2.36E-03	1.03E-02
Other C9's	0.063%	128.258	0.0811	0.189%	0.0019	1.48E-02	6.47E-02
n-Nonane	0.034%	128.258	0.0434	0.101%	0.0010	7.90E-03	3.46E-02
Other C10's	0.024%	142.280	0.0347	0.081%	0.0008	6.33E-03	2.77E-02
n-Decane	0.007%	142.280	0.0097	0.023%	0.0002	1.76E-03	7.72E-03
Undecanes+	0.004%	156.310	0.0056	0.013%	0.0001	1.03E-03	4.49E-03
Total	100.000%		42.853	100.000%			
Total: 7.8105E+00 3.4210E+01							

VOC INFO	
Mole % VOCs	47.44%
Total NM/NE Stream MW VOCs	31.726
lb Voc / mmscf	83602.308
MMSCF/YR	0.606

	Uncontrolled	Uncontrolled
	Emissions, (lb/hr)	Emissions, (tpy)
Total VOC:	5.78E+00	2.53E+01
Total Me/Eth	1.81E+00	7.93E+00

OILTK-5 Calculation Page 2 of 4

OILTK-5 Newfiel	d MAMIE 4-	25-3-3WH		
INPUT DA				
Molocular Weight	Symbol	PTE	Units	4
Molecular weight	Mv	50	l b/lb-mole	4
Tank design data	1010	00		
Shell height	Hs	20.00	ft	1
Diameter	D	12.00	ft	
Liquid height	HI	20.00	ft	
Avg. Liquid height	HI	10.00	ft	
vapor space outage	Hvo	10.00	ft	
Tank volume		16,921	gallons	
Turnovers	N	226		
Net throughput	Q	91250.00	bbl/yr	4
Tunover factor	KN	0.299		
Working loss product factor	Кр	0.75		From AP-42, 11/06 Section 7 Equ. 1-31, page 7.1-19
Neteorological data	<b>T</b> A A	54 0005	٥ <b>-</b>	
Daily ave. ambient temp.		51.9625	*F	FIOTI TAINS
Daily max. ambient temp.		40 202222	*F	
Daily ambient temp, range		40.203333	1 <sup>-</sup>	
Tank naint solar absorntance (see adjacent table)		23.30	2	Tank color gray, condition good
Daily total insolation factor	μ Ι	1 452 11825	Btu/ft2-day	From TANKS for Salt Lake City LIT
Site elevation (feet)	1	<u>1,452.11055</u> <u>4</u> 162	Did/112-uay	I TOTT TANKS TO Sail Lake Oily, OT
Atmospheric pressure	PA	12 644		
		12.011		1
Liquid bulk temperature	ТВ	61.49	°F	Tank is heated and temperature varies ± 2°F
Daily vapor temp. range	DTv	4.00	°F	Tank is heated and temperature varies ± 2°F
				1 '
Daily ave. liquid surface temp.	TLA	65.10	°F	
Daily max. liquid surface temp.	TLX	66.10	°F	
Daily min. liquid surface temp.	TIN	64.10	°F	
VP @ daily ave. liquid surf. temp.	PvA	165.19	mm Hg	Equation from AP-42, 11/06 Section 7 Figure 7.1-13b
VP @ daily max. liquid surf. temp.	PvX	168.39	mm Hg	Equation from AP-42, 11/06 Section 7 Figure 7.1-13t
VP @ daily min. liquid surf. temp.	PvN	162.03	mm Hg	Equation from AP-42, 11/06 Section 7 Figure 7.1-13b
D.1	20	0.00		4
Daily vapor pressure range	DPv	6.36	mm Hg	
Breather vent pressure setting range	DDB	0.06	psia	Value from AP-42, 11/06 Section 7 page 7.1-13 Note
Breather vent pressure setting range	DPD	3.10	mm Hg	
CALCULATIONS				4
	Symbol		Units	1
	Cynibol		Onico	
Breathing losses				1
Tank vapor space volume	Vv	1,130.98	ft3	1
Vapor density	Wv	2.834E-02	lb/ft3	1
Vapor space expansion factor	KE	0.01427		]
Vented vapor saturation factor	Ks	0.3713	ft2	
Breathing losses	LB	62.02	lb/yr	
Norking losses	Lw	3,269.36	lb/yr	
OTAL LOSSES	LT	0.38	lb/hr	4
		3,331.38	ib/yr	4
		1.6657	tpy sofd	4
IAD Emissions <sup>2</sup>	14/60/	69.27	SUIU	4
	Wt%		4	4
n-Hexañe	16.21%	0.27	tpy	4
Benzene	0.40%	0.01	tpy	4
	0.21%	0.00	tov	
Fthylbonzono	0.91%	0.02	tov	
Luiyibelizelle	0.10%	0.00	ιψy	4

<sup>1</sup>Calculations performed on this spreadsheet are taken from the USEPA AP-42- Section 7.1 Organic Liquid Storage Tanks - November 2006. <sup>2</sup>HAP Emissions (tpy) = HAP Wt% \* Total Losses (tpy)

Paint Color	Paint Shade or Type	Good	Poor
Aluminum	Specular	0.39	0.49
Aluminum	Diffuse	0.6	0.68
Aluminum	Mill finish, unpainted	0.1	0.15
Beige/Cream		0.35	0.49
Black		0.97	0.97
Brown		0.58	0.67
Gray	Light	0.54	0.63
Gray	Medium	0.68	0.74
Green	Dark	0.89	0.91
Red	Primer	0.89	0.91
Rust	Red iron oxide	0.38	0.5
Tan		0.43	0.55
White	NA	0.17	0.34

From AP-42, 11/06 Section 7 Table 7.1-6, page 7.1-69

OILTK-5 Calculation Page 3 of 4



Potential to Emit Emission Calculations

Maximum Tank Vapor 72.1 scf/hr Lower Heating Value 2,222 Btu/scf	Controlled emissions are calculated based on a 98% destruction efficiency of the VOC gas.
VOC: 6.16E+00 lb/hr x 100% - 98% 2.70E+01 TPY x 100% - 98%	= 1.23E-01 lb/hr = 5.40E-01 TPY
Benzene:         3.28E-02         lb/hr         x         100% -         98%           1.44E-01         TPY         x         100% -         98%	= 6.56E-04 lb/hr = 2.87E-03 TPY
Toluene:         7.49E-02         lb/hr         x         100% -         98%           3.28E-01         TPY         x         100% -         98%	= 1.50E-03 lb/hr = 6.56E-03 TPY
Ethylbenzene: 8.56E-03 lb/hr x 100% - 98%	= <b>1.71E-04</b> lb/hr = <b>7.50E-04</b> TPY
Xylenes:         1.49E-02         lb/hr         x         100% -         98%           6.54E-02         TPY         x         100% -         98%	= <b>2.99E-04</b> lb/hr = <b>1.31E-03</b> TPY
n-Hexane: 1.33E+00 lb/hr x 100% - 98% 5.82E+00 TPY x 100% - 98%	= 2.66E-02 lb/hr = 1.16E-01 TPY

Maximum Tank Vapor is a sum of the gas flash rate (scfd) plus the total losses rate (scfd) converted to scf/hr.

OILTK-5 Calculation Page 4 of 4

1. Company:	Newfield Exploration		Potential Emissions	
2. Site/Source:	MAMIE 4-25-3-3WH		3. Date: 2/7/2019	
4. Type of Operation:	Oil and Gas	Production Tanks		
5. Emission Point:	ID Number 20	Name OILTK-6	7. Identification and Descrip	tion of Control Equipment
6. Description of Equi 400 Barrel Ve	pment: rtical Fixed Roof Steel Oil	Tank		Flare
8. Throughput:	91,250	barrels/year	. 9. Operating Schedule:	Not Applicable

Pollutant	Uncontrolled Emissions	Controlled Emissions	
	(TPY)	(TPY)	
PM			DM Dortioulate Matter
PM <sub>10</sub>			PM – PM loss than 10 microns in size
PM <sub>2.5</sub>			Pivi <sub>10</sub> - Piviless than 10 microns in size
SO <sub>x</sub>			PM <sub>2.5</sub> - PM less than 2.5 microns in size
NO <sub>X</sub>		4.77E-02	$_{\rm NO_{\rm X}}$ - Sullul Oxides
CO		2.59E-01	CO - Carbon Monoxide
VOC	2.70E+01	5.40E-01	VOC - Volatile Organic Compound
Pb			Pb - I ead and lead compounds
Fluorides			Fluorides - Gaseous and particulates
$H_2SO_4$			$H_2SO_4$ - Sulfuric Acid Mist
H <sub>2</sub> S	Negligible	Negligible	H <sub>2</sub> S - Hydrogen Sulfide
TRS			TRS - Total Reduced Sulfur
RSC			RSC - Reduced Sulfur Compounds

Potential Emissions Attachment 6 of 14

# FLASH LIBERATION OF HYDROCARBON LIQUID

### FROM CENTRAL BASIN OIL STORAGE TANKS

### MAMIE 4-25-3-3WH

CB UB SXL

OILTK-6	PTE	
GOR from analysis	6.64	scf/bbl
Throughput (bbls/yr)	91,250	bbls/yr
Throughput (bbls/day)	250.00	bbls/day
Gas Flash Rate (SCFD):	1,660.0	scfd
Gas Flash Rate (lbs./day):	187.452	lb/day
Lb./Day = gas (ft <sup>3</sup> /day)x(Mwgas - lb/lb-mole) / (379.49 ft3/lb-mole)		

Gas oil ratio and mole percent of flash gas are representative of tanks in this region.

Component	Mole percent	Molecular Weight	Mole Frac x Mole <b>Stream MW</b>	Weight Percent	Weight Fraction	PTE Uncontrolled Emissions (lb/hr)	PTE Uncontrolled Emissions (tpy)
Hydrogen Sufide	0.000%	34.080	0.0000	0.000%	0.0000	0.00E+00	0.00E+00
Nitrogen	3.093%	28.013	0.8664	2.022%	0.0202	1.58E-01	6.92E-01
Carbon Dioxide	0.751%	44.010	0.3307	0.772%	0.0077	6.03E-02	2.64E-01
Methane	33.643%	16.043	5.3974	12.595%	0.1260	9.84E-01	4.31E+00
Ethane	15.073%	30.070	4.5325	10.577%	0.1058	8.26E-01	3.62E+00
Propane	13.269%	44.097	5.8513	13.654%	0.1365	1.07E+00	4.67E+00
Iso-Butane	3.081%	58.123	1.7909	4.179%	0.0418	3.26E-01	1.43E+00
n-Butane	7.803%	58.123	4.5352	10.583%	0.1058	8.27E-01	3.62E+00
2,2 Dimethylpropane	0.000%	72.140	0.0000	0.000%	0.0000	0.00E+00	0.00E+00
Iso-Pentane	2.905%	72.150	2.0957	4.890%	0.0489	3.82E-01	1.67E+00
n-Pentane	4.186%	72.150	3.0205	7.048%	0.0705	5.51E-01	2.41E+00
2,2 Dimethylbutane	0.158%	86.178	0.1363	0.318%	0.0032	2.48E-02	1.09E-01
Cyclopentane	1.187%	70.100	0.8324	1.942%	0.0194	1.52E-01	6.64E-01
2,3 Dimethylbutane	0.237%	86.178	0.2046	0.477%	0.0048	3.73E-02	1.63E-01
2 Methylpentane	0.481%	86.178	0.4145	0.967%	0.0097	7.56E-02	3.31E-01
3 Methylpentane	0.283%	86.178	0.2441	0.570%	0.0057	4.45E-02	1.95E-01
n-Hexane	8.062%	86.178	6.9478	16.213%	0.1621	1.27E+00	5.55E+00
Methylcyclopentane	0.953%	84.160	0.8020	1.872%	0.0187	1.46E-01	6.40E-01
Benzene	0.220%	78.114	0.1717	0.401%	0.0040	3.13E-02	1.37E-01
Cyclohexane	0.225%	84.160	0.1890	0.441%	0.0044	3.45E-02	1.51E-01
2-Methylhexane	0.056%	100.200	0.0563	0.131%	0.0013	1.03E-02	4.50E-02
3-Methylhexane	0.080%	100.200	0.0806	0.188%	0.0019	1.47E-02	6.43E-02
2,2,4 Trimethylpentane	0.079%	114.230	0.0905	0.211%	0.0021	1.65E-02	7.22E-02

OILTK-6 Calculation Page 1 of 4

# FLASH LIBERATION OF HYDROCARBON LIQUID

### FROM CENTRAL BASIN OIL STORAGE TANKS

### MAMIE 4-25-3-3WH

CB UB SXL

OILTK-6	PTE	
GOR from analysis	6.64	scf/bbl
Throughput (bbls/yr)	91,250	bbls/yr
Throughput (bbls/day)	250.00	bbls/day
Gas Flash Rate (SCFD):	1,660.0	scfd
Gas Flash Rate (lbs./day):	187.452	lb/day
Lb./Day = gas (ft³/day)x(Mwgas - lb/lb-mole) / (379.49 ft3/lb-mole)		

Gas oil ratio and mole percent of flash gas are representative of tanks in this region.

Component	Mole percent	Molecular Weight	Mole Frac x Mole <b>Stream MW</b>	Weight Percent	Weight Fraction	PTE Uncontrolled Emissions (lb/hr)	PTE Uncontrolled Emissions (tpy)
Other C7's	1.588%	100.272	1.5925	3.716%	0.0372	2.90E-01	1.27E+00
n-Heptane	0.635%	100.272	0.6367	1.486%	0.0149	1.16E-01	5.08E-01
Mehtylcyclohexane	0.712%	98.190	0.6995	1.632%	0.0163	1.27E-01	5.58E-01
Toluene	0.425%	92.140	0.3918	0.914%	0.0091	7.14E-02	3.13E-01
Other C8's	0.367%	114.230	0.4192	0.978%	0.0098	7.64E-02	3.35E-01
n-Octane	0.198%	114.230	0.2257	0.527%	0.0053	4.11E-02	1.80E-01
Ethylbenzene	0.042%	106.170	0.0448	0.105%	0.0010	8.17E-03	3.58E-02
M&P Xylenes	0.061%	106.170	0.0652	0.152%	0.0015	1.19E-02	5.20E-02
O-Xylenes	0.012%	106.170	0.0130	0.030%	0.0003	2.36E-03	1.03E-02
Other C9's	0.063%	128.258	0.0811	0.189%	0.0019	1.48E-02	6.47E-02
n-Nonane	0.034%	128.258	0.0434	0.101%	0.0010	7.90E-03	3.46E-02
Other C10's	0.024%	142.280	0.0347	0.081%	0.0008	6.33E-03	2.77E-02
n-Decane	0.007%	142.280	0.0097	0.023%	0.0002	1.76E-03	7.72E-03
Undecanes+	0.004%	156.310	0.0056	0.013%	0.0001	1.03E-03	4.49E-03
Total	100.000%		42.853	100.000%			
					Total:	7.8105E+00	3.4210E+01

VOC INFO	
Mole % VOCs	47.44%
Total NM/NE Stream MW VOCs	31.726
lb Voc / mmscf	83602.308
MMSCF/YR	0.606

	Uncontrolled	Uncontrolled
	Emissions, (lb/hr)	Emissions, (tpy)
Total VOC:	5.78E+00	2.53E+01
Total Me/Eth	1.81E+00	7.93E+00

OILTK-6 Calculation Page 2 of 4

UILIK-6 Newfie	3			
INPUT DA				
Aclosular Weight	Symbol	PTE	Units	4
Molecular weight	Mv	50	l b/lb-mole	4
Tank design data		00		
Shell height	Hs	20.00	ft	1
Diameter	D	12.00	ft	
Liquid height	HI	20.00	ft	
Avg. Liquid height	HI	10.00	ft	
vapor space outage	Hvo	10.00	ft	4
Tank volume	N	16,921	gallons	-
Net throughout		91250.00	bbl/vr	
Tunover factor	KN	0 299	bbi/yi	4
Working loss product factor	Kp	0.200		From AP-42, 11/06 Section 7 Equ. 1-31, page 7,1-19
leteorological data	. 4			
Daily ave. ambient temp.	TAA	51.9625	°F	From TANKS
Daily max. ambient temp.	TAX	63.641667	°F	for Salt Lake
Daily min. ambient temp.	TAN	40.283333	°F	City, UT
Daily ambient temp. range	DTA	23.36	°F	
I ank paint solar absorptance (see adjacent table)	α	0.68	- -	I ank color gray, condition good
Daily total insolation factor	1	1,452.11835	Btu/ft2-day	From TANKS for Salt Lake City, UT
Site elevation (feet)	DA	4,162		
Atmospheric pressure	PA	12.044		
Liquid bulk temperature	TB	61 49	°F	Tank is heated and temperature varies + 2°F
Daily vapor temp, range	DTv	4.00	°F	Tank is heated and temperature varies ± 2°F
Daily ave. liquid surface temp.	TLA	65.10	°F	
Daily max. liquid surface temp.	TLX	66.10	°F	
Daily min. liquid surface temp.	TIN	64.10	°F	
VP @ daily ave. liquid surf. temp.	PvA	165.19	mm Hg	Equation from AP-42, 11/06 Section 7 Figure 7.1-13b
VP @ daily max. liquid surf. temp.	PvX	168.39	mm Hg	Equation from AP-42, 11/06 Section 7 Figure 7.1-13b
VP @ daily min. liquid surf. temp.	PVN	162.03	mm Hg	Equation from AP-42, 11/06 Section 7 Figure 7.1-13t
	DPv	6 36	mm Ha	
Breather vent pressure setting range	DPB	0.00	nsia	Value from AP-42 11/06 Section 7 page 7 1-13 Note
Breather vent pressure setting range	DPB	3.10	mm Ha	
			J	1
CALCULATIONS				
	Symbol		Units	
				4
Breathing losses	14.	4 400 00	40	4
lank vapor space volume	VV M(r)	1,130.98	II.3	-
Vapor space expansion factor		2.034E-02	10/113	
Vented vapor saturation factor	Ke	0.01427	ft2	
Vented vapor saturation factor	113	0.0710	112	4
Breathing losses	LB	62.02	lb/vr	
			, j :	1
Norking losses	Lw	3,269.36	lb/yr	
OTAL LOSSES	LT	0.38	lb/hr	
		3,331.38	lb/yr	4
		1.6657	tpy	4
	Muc:	69.27	SCIO	4
	Wt%		4	4
n-Hexane Ronzono	16.21%	0.27	tpy	
2 2 1-Trimethylpentane	0.40%	0.01	tov	1
Toluene	0.21%	0.00	tov	1
Ethylbenzene	0.10%	0.00	tov	1
Vulanaa	0.18%	0.00	tov	1

<sup>1</sup>Calculations performed on this spreadsheet are taken from the USEPA AP-42- Section 7.1 Organic Liquid Storage Tanks - November 2006. <sup>2</sup>HAP Emissions (tpy) = HAP Wt% \* Total Losses (tpy)

Paint Color	Paint Shade or Type	Good	Poor
Aluminum	Specular	0.39	0.49
Aluminum	Diffuse	0.6	0.68
Aluminum	Mill finish, unpainted	0.1	0.15
Beige/Cream		0.35	0.49
Black		0.97	0.97
Brown		0.58	0.67
Gray	Light	0.54	0.63
Gray	Medium	0.68	0.74
Green	Dark	0.89	0.91
Red	Primer	0.89	0.91
Rust	Red iron oxide	0.38	0.5
Tan		0.43	0.55
White	NA	0.17	0.34

From AP-42, 11/06 Section 7 Table 7.1-6, page 7.1-69

OILTK-6 Calculation Page 3 of 4


Potential to Emit Emission Calculations

Maximum Tank Vapor 72.1 scf/hr Lower Heating Value 2,222 Btu/scf	Controlled emissions are calculated based on a 98% destruction efficiency of the VOC gas.
VOC: 6.16E+00 lb/hr x 100% - 98% 2.70E+01 TPY x 100% - 98%	= 1.23E-01 lb/hr = 5.40E-01 TPY
Benzene:         3.28E-02         ib/hr         x         100% -         98%           1.44E-01         TPY         x         100% -         98%	= 6.56E-04 lb/hr = 2.87E-03 TPY
Toluene:         7.49E-02         lb/hr         x         100% -         98%           3.28E-01         TPY         x         100% -         98%	= 1.50E-03 lb/hr = 6.56E-03 TPY
Ethylbenzene: 8.56E-03 lb/hr x 100% - 98%	= 1.71E-04 lb/hr = 7.50E-04 TPY
Xylenes:         1.49E-02         lb/hr         x         100% -         98%           6.54E-02         TPY         x         100% -         98%	= 2.99E-04 lb/hr = 1.31E-03 TPY
n-Hexane: 1.33E+00 lb/hr x 100% - 98% 5.82E+00 TPY x 100% - 98%	= 2.66E-02 lb/hr = 1.16E-01 TPY
2,2,4-Trimethyl- pentane: 1.73E-02 lb/hr x 100% - 98% 7.57E-02 TPY x 100% - 98%	= 3.46E-04 lb/hr = 1.51E-03 TPY

Maximum Tank Vapor is a sum of the gas flash rate (scfd) plus the total losses rate (scfd) converted to scf/hr.

OILTK-6 Calculation Page 4 of 4

1. Company:	Newfield Exploration		Potential Emissions
2. Site/Source: MAMIE 4-25-3-3WH			3. Date: 2/22/2019
4. Type of Operatio	n: Oil and Gas	Production Tank I	Jnloading
5. Emission Point:	ID Number 21	Name OILTKLOAD-2	7. Identification and Description of Control Equipment
6. Description of Ec	uipment:		Not Applicable
Emissions rela	ited to unloading of oil ta	ank via truck	
8. Load Quantity:	273,750	barrels/yr	

Pollutant	Uncontrolled Emissions	Controlled Emissions	
	(191)	(191)	
PM			DM Dartiquiata Mattar
PM <sub>10</sub>			PM - PM less than 10 microns in size
PM <sub>2 6</sub>			= 1 M <sub>10</sub> 1 M less than 10 microns in size
2:5			PM <sub>2.5</sub> - PM less than 2.5 microns in size
SUX			SO <sub>x</sub> - Sulfur Oxides
NO <sub>X</sub>			NO <sub>x</sub> - Nitrogen Oxides
CO			CO - Carbon Monoxide
VOC	1.16E+01	7.97E-01	VOC - Volatile Organic Compound
Pb			Pb - Lead and lead compounds
Fluorides			Fluorides - Gaseous and particulates
$H_2SO_4$			$H_2SO_4$ - Sulfuric Acid Mist
H <sub>2</sub> S			H <sub>2</sub> S - Hydrogen Sulfide
TRS			TRS - Total Reduced Sulfur
RSC			RSC - Reduced Sulfur Compounds

Potential Emissions Attachment 7 of 14



OILTKLOAD-2 Calculation Page 1 of 2



Calculation basis: AP-42 Section 5.2. Defaults assume submerged loading: dedicated normal service.

OILTKLOAD-2 Calculation Page 2 of 2

1. Company:	Newfield Exploration	ı			Potential Emissions	
2. Site/Source: MAMIE 4-25-3-3WH		3. Date: 2/7/2019				
4. Type of Operatio	n: Oil and G	as Producti	on Pneum	atic Controllers		
5. Emission Point:	ID Number 22	Name PCO	ame 7. Identification and Description of Control Equipment PCONT-2			
6. Description of Ec Low Pneumat	uipment: tic Controllers			None		
8. Controller Bleed	Rate:	1	scf/hr	9. Operating Schedule:	8,760	Hours/year
10. Number of Pne	umatic Controllers:		6			

Pollutant	Uncontrolled Emissions	Controlled Emissions	
	(TPY)	(TPY)	
PM			DM Particulate Matter
PM <sub>10</sub>			PM = PM loss than 10 microns in size
PM <sub>2.5</sub>			- Finitess than 10 microns in size
<u> </u>			- PM <sub>2.5</sub> - PM less than 2.5 microns in size
30 <sub>x</sub>			SO <sub>X</sub> - Sulfur Oxides
NO <sub>X</sub>			NO <sub>x</sub> - Nitrogen Oxides
CO			CO - Carbon Monoxide
VOC	8.85E-02	8.85E-02	VOC - Volatile Organic Compound
Pb			Pb - Lead and lead compounds
Fluorides			Fluorides - Gaseous and particulates
$H_2SO_4$			$H_2SO_4$ - Sulfuric Acid Mist
H <sub>2</sub> S			H <sub>2</sub> S - Hydrogen Sulfide
TRS			TRS - Total Reduced Sulfur
RSC			RSC - Reduced Sulfur Compounds

Potential Emissions Attachment 8 of 14



## PCONT-2

UINTA CENTRAL BASIN

Emissions (lb/hr) = PSCR (scf/hr) x (1/379 scf/lb-mole) x (VOC wt. Fraction) Emissions (TPY) = (lb/hr VOC) x (8760 hr/yr) x (1 ton/2000)



Molecular weight and weight percent of gas constituents are from an extend gas analysis representative of this region.

PCONT-2 Calculation Page 1 of 2



UINTA CENTRAL BASIN

Emissions (lb/hr) = PSCR (scf/hr) x (1/379 scf/lb-mole) x (VOC wt. Fraction) Emissions (TPY) = (lb/hr VOC) x (8760 hr/yr) x (1 ton/2000)



Molecular weight and weight percent of gas constituents are from an extended gas analysis representative of this region.

PCONT-2 Calculation Page 2 of 2

1. Company:	Newfield Exploration		Potential Emissions	
2. Site/Source: MAMIE 4-25-3-3WH		3. Date: 2/7/2019		
4. Type of Operation:	Oil and Gas	Production Tanks		
5. Emission Point:	ID Number 23	Name PWTANK-2	7. Identification and Descripti	on of Control Equipment
6. Description of Equipment: 400 Barrel Vertical Fixed Roof Steel Produced Water Tank			Flare	
8. Throughput:	273,750	barrels/year	9. Operating Schedule:	Not Applicable

Pollutant	Uncontrolled Emissions	Controlled Emissions	
DM	(11.1)	(11-1)	
PIVI			PM - Particulate Matter
PM <sub>10</sub>			PM PM less than 10 microns in size
PM <sub>2.5</sub>			$\mathbf{D}\mathbf{M}$ $\mathbf{D}\mathbf{M}$ less than 0.5 microns in size
<u> </u>			- PM <sub>2.5</sub> - PM less than 2.5 microns in size
30 <sub>X</sub>			SO <sub>x</sub> - Sulfur Oxides
NO <sub>X</sub>		1.32E-02	NO <sub>x</sub> - Nitrogen Oxides
CO		7.20E-02	CO - Carbon Monoxide
VOC	1.37E+00	2.74E-02	VOC - Volatile Organic Compound
Pb			Pb - I ead and lead compounds
Fluorides			Fluorides - Gaseous and particulates
H <sub>2</sub> SO <sub>4</sub>			$H_2SO_4$ - Sulfuric Acid Mist
H <sub>2</sub> S	Negligible	Negligible	$H_2S$ - Hydrogen Sulfide
TRS			TRS - Total Reduced Sulfur
RSC			RSC - Reduced Sulfur Compounds

Potential Emissions Attachment 9 of 14 Newfield MAMIE 4-25-3-3WH

## PWTANK-2

#### Potential to Emit Emission Calculations

Maximum Water Tank Throughput       273,750       bbl/yr         Flash Factor       1.90       scf/bbl         Maximum Tank Vapor       59.4       scf/hr         Lower Heating Value       748       Btu/scf         VOC       0.01       lb/bbl         Benzene       0.0001       lb/bbl         Toluene       0.0003       lb/bbl	Environ Emission Factors for Produced Water Tanks Environ Project No. 06-17477T, TCEQ Project 2010-29 Prepared for Texas Commission on Environmental Quality. Given in pounds of emissions per barrel of produced water. Methane Emission and Flash Factors were not provided in this report as such it was calculated from the data available within the report. Maximum Tank Vapor (scf/hr) = Flash Factor (scf/bbl) * Maximum Water Tank Throughput (bbl/yr) ÷ 8,760 (hr/yr)
Ethylbenzene 0.000006 lb/bbl Xylenes 0.00006 lb/bbl	Controlled emissions are calculated based on a 98% destruction efficiency of the VOC gas.
VOC:         1,312.5         gal/hr         x         1/42 barrel/gallon           273,750         bbl/yr         x         0.01 lb/bbl	x       0.010 lb/bbl       x       100% - 98%       =       6.25E-03       lb/hr         x       1/2,000 ton/lb       x       100% - 98%       =       2.74E-02       TPY
Benzene:         1,312.5         gal/hr         x         1/42 barrel/gallon           273,750         bbl/yr         x         0.0001 lb/bbl	x       0.0001 lb/bbl       x       100% - 98%       =       6.25E-05       lb/hr         x       1/2,000 ton/lb       x       100% - 98%       =       2.74E-04       TPY
Toluene:         1,312.5         gal/hr         x         1/42 barrel/gallon           273,750         bbl/yr         x         0.0003 lb/bbl	x       0.0003 lb/bbl       x       100% - 98%       = <b>1.88E-04</b> lb/hr         x       1/2,000 ton/lb       x       100% - 98%       = <b>8.21E-04</b> TPY
Ethylbenzene:         1,312.5         gal/hr         x         1/42 barrel/gallon           273,750         bbl/yr         x         0.000006 lb/bbl	x       0.000006 lb/bbl       x       100% - 98%       =       3.75E-06       lb/hr         x       1/2,000 ton/lb       x       100% - 98%       =       1.64E-05       TPY

	Newfield MAMIE 4-25-3-3WH				
	PWTANK-2				
Xylenes:	<b>1,312.5</b> gal/hr x 1/42 barrel/gallon x 0.00006 lb/bbl x 100% - 98% = <b>3.75E-05</b> lb/hr				
	<b>273,750</b> bbl/yr x 0.00006 lb/bbl x 1/2,000 ton/lb x 100% - 98% = <b>1.64E-04</b> TPY				

NOx & CO emission factors are from AP-42 Table 13.5-1 (Emission Factors for Flare Operations).  $CO_2 \& N_2O$  emission factors are from AP-42 Table 1.4-2 (Emission Factors for Natural Gas Combustion).

PWTANK-2- Calculation Page 2 of 2

1. Company:	Newfield Exploration		Potential Emissions	
2. Site/Source:	MAMIE 4-25-3-3WH		3. Date: 2/07/2019	
4. Type of Operation:	Miscellaneous	s Tanks		
5. Emission Point:	ID Number 24	Name SMTANKS-2	7. Identification and Description of Control Equ	ipment
6. Description of Equip Small Storage	ment: Tanks			
8. Throughput:	Not Applicable	barrels/year	. 9. Operating Schedule: Not App	licable

	÷		
Pollutant	Uncontrolled Emissions	Controlled Emissions	
	(11-1)	(11.1)	
PM			DM Dortioulate Matter
PM <sub>10</sub>			
			PM <sub>10</sub> - PM less than 10 microns in size
PM <sub>2.5</sub>			PM <sub>2.5</sub> - PM less than 2.5 microns in size
SO <sub>X</sub>			SO <sub>x</sub> - Sulfur Oxides
NO <sub>x</sub>			NO Nitrogen Oxides
00			
00			CO - Carbon Monoxide
VOC	2.05E-02	2.05E-02	VOC - Volatile Organic Compound
Pb			Pb - Lead and lead compounds
Fluorides			Fluorides - Gaseous and particulates
$H_2SO_4$			H <sub>2</sub> SO <sub>4</sub> - Sulfuric Acid Mist
11.0			
H <sub>2</sub> S			H <sub>2</sub> S - Hydrogen Sulfide
TRS			TRS - Total Reduced Sulfur
RSC			RSC - Reduced Sulfur Compounds

Potential Emissions Attachment 10 of 15

#### Newfield Mamie 4-25-3-3WH

SMALL STORAGE TANKS 2			
	<b>Emission Factor</b>	Units	
Annual Storage Quantity			
Methanol	8,600	gallons/yr	
Ethylene glycol	1,000	gallons/yr	_
Breathing losses Emission Factors			-
Methanol	3.70E+00	lb VOC/1000 gal	Value from "http://cfpub.epa.gov/webfire"
Ethylene glycol	5.20E-02	lb VOC/1000 gal	Value from "http://cfpub.epa.gov/webfire"
Breathing Emissions			-
Methanol	3.63E-03	VOC lb/hr	= 3.7 lb/1000 gal * 8600 gal/yr * 1 yr/365 days * 1 day/24 hrs
Ethylene glycol	5.94E-06	VOC lb/hr	= 0.052 lb/1000 gal * 1000 gal/yr * 1 yr/365 days * 1 day/24 hrs
Working lossos Emission Factors			_
Mothanal	1.075±00		Value from "http://cfpub.epa.gov/webfire"
Ethylene alvcol	2.00E-03	lb VOC/1000 gal	Value from "http://cipub.epa.gov/webfire"
Working Emissions			
Methanol	1.05E-03	VOC lb/hr	= 1.07 lb/1000 gal * 8600 gal/yr * 1 yr/365 days * 1 day/24 hrs
Ethylene glycol	2.28E-07	VOC lb/hr	= 0.002 lb/1000 gal * 1000 gal/yr * 1 yr/365 days * 1 day/24 hrs
Total Working & Prosthing Emissions			_
Methanol	4 68E-03	VOC lb/br	
Methanol	2.05E-03	VOC ton/vr	-
moularior		100 (01.8)	
Ethylene glycol	6.16E-06	VOC lb/hr	
Ethylene glycol	2.70E-05	VOC ton/yr	
Totals	4.69E-03	VOC lb/hr	
Totals	2.05E-02	VOC ton/yr	

SMTANKS-2 Calculation Page 1 of 1

1. Company:	Newfield Exploration			Potential Emissions	
2. Site/Source:	/AMIE 4-25-3-3WH		3. Date: 2/7/2019		
4. Type of Operation:	Oil and Gas	Production Tank	Heater		
5. Emission Point:	ID Number 25	Name TANKHTR4	7. Identification and Description of Control Equipment		
<ol> <li>Description of Equi Tank Heater</li> </ol>	pment:		None		
8. Hours of Operation	: 8,760	Hours/Year	9. Burner Rating:	250,000	BTU/hr
10. Type of Fuel Use	d: Nat	ural Gas	11. Amount of Fuel Used:	2,190,000,000	BTU/yr

Pollutant	Uncontrolled Emissions	Controlled Emissions	
	(TPY)	(TPY)	
PM	8.16E-03	8.16E-03	DM Darticulate Matter
PM <sub>10</sub>	8.16E-03	8.16E-03	$PM_{r} = PM$ less than 10 microns in size
PM <sub>2.5</sub>	8.16E-03	8.16E-03	$PM_{a,c}$ - PM less than 2.5 microns in size
SO <sub>X</sub>	6.44E-04	6.44E-04	$SO_{\rm x}$ - Sulfur Oxides
NO <sub>X</sub>	1.07E-01	1.07E-01	NO <sub>v</sub> - Nitrogen Oxides
CO	9.02E-02	9.02E-02	CO - Carbon Monoxide
VOC	5.90E-03	5.90E-03	VOC - Volatile Organic Compound
Pb			Pb - Lead and lead compounds
Fluorides			Fluorides - Gaseous and particulates
$H_2SO_4$			H <sub>2</sub> SO <sub>4</sub> - Sulfuric Acid Mist
H <sub>2</sub> S			H <sub>2</sub> S - Hydrogen Sulfide
TRS			TRS - Total Reduced Sulfur
RSC			RSC - Reduced Sulfur Compounds

Potential Emissions Attachment 11 of 14

#### Newfield MAMIE 4-25-3-3WH

### TANKHTR4



Emission Factors are from AP-42 Table 1.4-1, 1.4-2, 1.4-3, & 1.4-4.

TANKHTR4 Calculation Page 1 of 1

1. Company:	Newfield Exploration	Potential Emissions			
2. Site/Source:	/AMIE 4-25-3-3WH		3. Date: 2/7/2019		
4. Type of Operation:	Oil and Gas	Production Tank	Heater		
5. Emission Point:	ID Number 26	Name TANKHTR5	7. Identification and Description of Control Equipment		
<ol> <li>Description of Equi Tank Heater</li> </ol>	pment:		None		
8. Hours of Operation	: 8,760	Hours/Year	9. Burner Rating:	250,000	BTU/hr
10. Type of Fuel Use	d: Nat	ural Gas	11. Amount of Fuel Used:	2,190,000,000	BTU/yr

Pollutant	Uncontrolled Emissions	Controlled Emissions	
	(TPY)	(TPY)	
PM	8.16E-03	8.16E-03	DM Darticulate Matter
PM <sub>10</sub>	8.16E-03	8.16E-03	$PM_{r} = PM$ less than 10 microns in size
PM <sub>2.5</sub>	8.16E-03	8.16E-03	$PM_{a,c}$ - PM less than 2.5 microns in size
SO <sub>X</sub>	6.44E-04	6.44E-04	$SO_{\rm x}$ - Sulfur Oxides
NO <sub>X</sub>	1.07E-01	1.07E-01	NO <sub>v</sub> - Nitrogen Oxides
CO	9.02E-02	9.02E-02	CO - Carbon Monoxide
VOC	5.90E-03	5.90E-03	VOC - Volatile Organic Compound
Pb			Pb - Lead and lead compounds
Fluorides			Fluorides - Gaseous and particulates
$H_2SO_4$			H <sub>2</sub> SO <sub>4</sub> - Sulfuric Acid Mist
H <sub>2</sub> S			H <sub>2</sub> S - Hydrogen Sulfide
TRS			TRS - Total Reduced Sulfur
RSC			RSC - Reduced Sulfur Compounds

Potential Emissions Attachment 12 of 14

#### Newfield MAMIE 4-25-3-3WH

### **TANKHTR5**



Emission Factors are from AP-42 Table 1.4-1, 1.4-2, 1.4-3, & 1.4-4.

TANKHTR5 Calculation Page 1 of 1

1. Company:	Newfield Exploration	Potential Emissions			
2. Site/Source:	MAMIE 4-25-3-3WH		3. Date: 2/7/2019		
4. Type of Operation:	Oil and Gas	Production Tank	Heater		
5. Emission Point:	ID Number 27	Name TANKHTR6	7. Identification and Descriptio	n of Control Equipment	
<ol> <li>Description of Equ Tank Heater</li> </ol>	pment:		None		
8. Hours of Operation	<sup>1:</sup> 8,760	Hours/Year	9. Burner Rating:	250,000	BTU/hr
10. Type of Fuel Use	d: Nat	ural Gas	11. Amount of Fuel Used:	2,190,000,000	BTU/yr

Pollutant	Uncontrolled Emissions	Controlled Emissions	
	(TPY)	(TPY)	
PM	8.16E-03	8.16E-03	DM Particulate Matter
PM <sub>10</sub>	8.16E-03	8.16E-03	$PM_{r} = PM$ less than 10 microns in size
PM <sub>2.5</sub>	8.16E-03	8.16E-03	$PM_{o,c}$ - PM less than 2.5 microns in size
SO <sub>X</sub>	6.44E-04	6.44E-04	$SO_{\rm v}$ - Sulfur Oxides
NO <sub>X</sub>	1.07E-01	1.07E-01	$NO_{x}$ - Nitrogen Oxides
CO	9.02E-02	9.02E-02	CO - Carbon Monoxide
VOC	5.90E-03	5.90E-03	VOC - Volatile Organic Compound
Pb			Pb - Lead and lead compounds
Fluorides			Fluorides - Gaseous and particulates
$H_2SO_4$			H <sub>2</sub> SO <sub>4</sub> - Sulfuric Acid Mist
H <sub>2</sub> S			H <sub>2</sub> S - Hydrogen Sulfide
TRS			TRS - Total Reduced Sulfur
RSC			RSC - Reduced Sulfur Compounds

Potential Emissions Attachment 13 of 14

#### Newfield MAMIE 4-25-3-3WH

### **TANKHTR6**



Emission Factors are from AP-42 Table 1.4-1, 1.4-2, 1.4-3, & 1.4-4.

TANKHTR6 Calculation Page 1 of 1

1. Co	ompany:	Newfield Exploration		Po	otential Emissions
2. Sit	te/Source:	MAMIE 4-25-3-3WH		3. Date: 2/07/2019	
4. Ty	pe of Operation:	Flare			
5. Er	mission Point:	ID Number 28	Name FLARE-2	7. Identification and Descript	ion of Control Equipment
6. De	escription of Equip Flare	ment:			Flare
8. Th	nroughput:	296	scf/hr	9. Operating Schedule:	Not Applicable

Pollutant	Uncontrolled Emissions	Controlled Emissions	
	(TDV)		
		(161)	
PM			DM Dortioulate Matter
PM <sub>40</sub>			
			PM <sub>10</sub> - PM less than 10 microns in size
PM <sub>2.5</sub>			PM <sub>25</sub> - PM less than 2.5 microns in size
SO <sub>X</sub>			SO <sub>v</sub> - Sulfur Oxides
NO <sub>x</sub>		1.61E-01	
00		0 70E 01	NO <sub>X</sub> - Millogen Oxides
		0.70E-01	CO - Carbon Monoxide
VOC		1.23E-01	VOC - Volatile Organic Compound
Pb			Pb - Lead and lead compounds
Fluorides			Fluorides - Gaseous and particulates
H₂SO₄			H SO - Sulfuric Acid Mist
2 4		N. 19 11 1	
H <sub>2</sub> S		Negligible	H <sub>2</sub> S - Hydrogen Sulfide
TRS			TRS - Total Reduced Sulfur
RSC			RSC - Reduced Sulfur Compounds

Potential Emissions Attachment 14 of 14



Combustor Calculation Page 1 of 2



CO <sub>2</sub> : 296 scf/hr x 1,832 Btu/scf x 1 Mmbtu/1,000,000 Btu x 117. 6.37E+01 lb/hr x 8760 hr/yr x 1 ton/2000 ll	65 lb/MMBtu = <b>6.37E+01</b> lb/hr
CH <sub>4</sub> : 296 scf/hr x 1,832 Btu/scf x 1 Mmbtu/1,000,000 Btu x 0.0 4.17E-02 lb/hr x 8760 hr/yr x 1 ton/2000 ll	$CH_4 \text{ as } CO_2e:$ 77 lb/MMBtu = 4.17E-02 lb/hr 1.29E+01 lb/hr $= 1.83E-01 \text{ TPY} 5.67E+01 \text{ TPY}$
N <sub>2</sub> O: 296 scf/hr x 1,832 Btu/scf x 1 Mmbtu/1,000,000 Btu x 0.0 1.17E-03 lb/hr x 8760 hr/yr x 1 ton/2000 lb	N2O as CO2e:         02 lb/MMBtu       =       1.17E-03 lb/hr         02 lb/MMBtu       =       5.12E-03 TPY         1.59E+00 TPY

NOx, CO, VOC, & CH<sub>4</sub> emission factors are from AP-42 Table 13.5-1 & 13.5-2

(Emission Factors for Flare Operations).

CO<sub>2</sub> & N<sub>2</sub>O emission factors are from AP-42 Table 1.4-2

(Emission Factors for Natural Gas Combustion).

Combustor Calculation Page 2 of 2



**Detailed Information on Equipment Controls** 



The Steffes Variable Orifice Flare offers optimum system performance with its ability to self-adjust to accommodate high, low or various gas flow rates. Its patented variable annular orifice design efficiently mixes air with gas prior to combustion for smokeless, efficient operation and a clean consistent burn.

**FLARES** 

Our experienced team of professionals can help you configure assemblies to meet a wide range of pressures, including designs for multiple pressures. The continuous running stable pilot ensures the flare remains lit and running, even in some of the harshest conditions. With its smokeless operation and ability to accommodate multiple pressures, the Steffes Variable Orifice Flare has become the industry standard.

#### FEATURES:

- · Various flow rates for high and low pressures
- Single, combo, and dual flare tip combinations
- Stainless steel construction
- Patent pending technology
- Field proven 98% destruction efficiency .
- Designed to meet EPA 40 CFR §60.18 requirement .

#### BENEFITS:

- High, low, and combination pressure systems
- Continuous running stable pilot .
- Smokeless operation
- Thermocouple for monitoring pilot with datalogger and . temperature transmitter
- . Reliable and complete solution



High Pressure		Low Pressure				
Model: SHP-6 Rated Flow Capacity:" 1.1 MMSCFD Max Flow Capacity:" 2.2 MMSCFD <sup>3</sup> Weight: 200 lbs	Model: SHC-6 Rated Flow Capacity: 3.0 MMSCFD Max Flow Capacity: <sup>9</sup> 6.0 MMSCFD <sup>13</sup> Weight: 230 lbs	Model: SVG-3B4 Rated Flow Capacity:" 106 MSCFD Max Flow Capacity: 750 MSCFD" Weight: 70 lbs	Model: SVG-3D4 Rated Flow Capacity: 106 MSCFD Max Flow Capacity: 750 MSCFD <sup>®</sup> Weight: 20 lbs	Model: SVG-3D8 Rated Flow Capacity: 120 MSCFD Max Flow Capacity: 750 MSCFD <sup>**</sup> Weight: 22 lbs		
Model: SPL-1 Gas Flow Rate: Pilot orifice is a #70   Propane at 8 PSI is 1 Propane at 10 PSI is Weight: 15 lbs Multiply flow by 1.6 f	MTD 1 Cu. Ft./Hr. 13 Cu. Ft./Hr. for Natural Gas	SHP-6 SHC	All data is fu Call Factory J	pr reference only. for more specifics.		







Steffes is committed to working with our customers to provide the simplest, most efficient, and most reliable solutions for flaring requirements. Our flares are designed to help operators meet the EPA 40 CFR §60.18 requirements, including our patent pending variable orifice design.

Flare Tip		Technology	Back	Rated Flow <sup>*1</sup>	Max Flow	Power	Pipe	Typical Installations	
Ν	/lodel	rechnology	Pressure*	Meeting 40 CFR 60.18	Capacity	Required	Connections	Produced Gas	Tank Gas
gh sure	SHP-6		5.5 - 10 PSI	1.1 MMSCFD	2.2 MMSCFD* <sup>2</sup>	No	4"	Х	
High	SHC-6		4 - 6 PSI	3.0 MMSCFD	6.0 MMSCFD*2	No	4"	Х	
	SVG-3B4	Variable	3 - 5 OSI	106 MSCFD	750 MSCFD* <sup>3</sup>	No	3"		Х
ure	SVG-3D4	Office	4 - 6 OSI	106 MSCFD	750 MSCFD* <sup>3</sup>	No	3″		Х
Press	SVG-3D8		7 - 10 OSI	120 MSCFD	750 MSCFD* <sup>3</sup>	No	3″		Х
Low	SAA-2	Air Accist	0 - 3 OSI	200 MSCFD	See chart 4	120 v	3"		Х
	SAA-4	AII ASSISL	0 - 1 OSI	600 MSCFD	See chart 5	480 V 3 Phase	4"		Х
Pilot*4	SPL-1	Pilot	8 PSI	264 SCFD	N/A	Spark System Required	3/8" Compression	X or Propane	

Data is for reference only. Call Steffes Technical support for more specific information.

\*Measured at flare tip. \*1 "Rated Flow" is the flow rate used by independent third parties to confirm Steffes' flare compliance with the perspective provisions of 40 CFR 60.18. Gas flow rates that do not exceed these values can be assumed to comply with all relevant EPA flare performance requirements. \*2 "Max Flow Capacity" is the highest flow rate allowed by Steffes for use in each specified flare. Flow rates above the "Max Flow Rate" may void warranties. \*3 All low pressure flares can meet requirements of 40 CFR 60.18 if smokeless operation is confirmed by Method 22. Also will need to be evaluated for flame stability, re-light capability, and radiation. \*4 Pilot can run at 6 - 10 PSI, Flow Rate will vary by pressure and gas composition.



#### VARIABLE ORIFICE FLARES

The Steffes Variable Orifice Flares give optimum system performance over a wide range of gas flows for both high pressure and low pressure gases. Configure your flare system



SVG-3D4

SVG-3D8

with singular or multiple flare tips to maximize performance. Models SHP - 6, SHC - 6, SVG - 3B4, SVG - 3D4, and SVG - 3D8.

**FLARE SOLUTIONS Specifications** 



#### **AIR ASSIST FLARES**

SHC-6

SHP-6

The Steffes Air Assist Flares burn low pressure gas over a wide range of flow rates. Low pressure gas is mixed with air from a variable speed fan to provide a clean burn. Model 2 (SAA - 2) and Model 4 (SAA - 4).

SVG-3B4



Page 1

#### VARIABLE ORIFICE FLARES





Phone: 888.783.3337 <u>www.steffes.com</u> oilfieldproducts@steffes.com



#### SHP-6

Maximum Rate Tested by 3 <sup>rd</sup> Party	1.1 MMSCFD
Minimum Rate Tested	0.05 MMSCFD

#### SHC-6

Maximum Rate Tested by 3 <sup>rd</sup> Party	3.0 MMSCFD		
Minimum Rate Tested	0.05 MMSCFD		

#### GAS CHARACTERISTICS (SEPARATOR GAS) DURING 3RD PARTY TESTING

Specific Gravity at 40 psig and 100F	0.89*			
Gross Heating Value	1550* BTU/SCF			

\*Pressure was measured at the test port on tip during third party testing.

\*Data is from third party test report. Flare is designed to operate with 1100 to 2500 BTU/SCF gas. Performance can be affected by specific gas composition.

\*Flares are able to handle more flow than the current ratings allow, however "Max Flow Capacity" is the highest flow rate allowed by Steffes for use in each specified flare. Flow rates above the "Max Flow Rate" may void warranties.

\*Data is for reference only.

\*Smokeless operation is achieved by building pressure in the flare, and the Minimum Rate is defined as typical flow required to begin building pressure in flare barrel. Minimum Rate can be affected by conditions restricting the proper seating of the translating tip and the barrel resulting in lower operating pressures. Flares operating at pressures less than those shown on chart can still meet the requirements of 40 CFR 60.18 if verification of smokeless operation is confirmed by Method 22.



#### CHART 3



Page 4





LOW PRESSURE FLARES	Rated Flow	Minimum Flow Rate	Gross Heating Value During Testing
Maximum Rate Tested by 3 <sup>rd</sup> Party - SVG-3B4	106 MSCFD	18,000 SCFD	1750 BTU/SCF (on-site gas)
Maximum Rate Tested by 3 <sup>rd</sup> Party - SVG-3D4	106 MSCFD	18,000 SCFD	2479 BTU/SCF (propane)
Maximum Rate Tested by 3 <sup>rd</sup> Party - SVG-3D8	120 MSCFD	18,000 SCFD	2479 BTU/SCF (propane)
Maximum Rate Tested by 3 <sup>rd</sup> Party - SAA-2	200 MSCFD	0	2479 BTU/SCF (propane)
Maximum Rate Tested by 3 <sup>rd</sup> Party - SAA-4	600 MSCFD	0	2479 BTU/SCF (propane)

\*Low Pressure curves represent testing data done with air as a medium, and pressure was measured at the test port on tip.

\*Low Pressure Flares (SVG-3B4, SVG-3D4, and SVG-3D8) meet requirements of 40 CFR 60.18 up to flow rates of 750 mscfd if verification of smokeless operation is confirmed by method 22.

\*Flares are designed to operate with 1100 to 2500 BTU/SCF gas. Performance can be affected by specific gas composition.

\*Low Pressure curves represent the nominal to max pressure.

\*Data is for reference only.

\*Smokeless operation is achieved by building pressure in the flare, and the Minimum Rate is defined as typical flow required to begin building pressure in flare barrel. Minimum Rate can be effected by conditions restricting the proper seating of the translating tip and the barrel resulting in lower operating pressures. Flares operating at pressures less than those shown on chart can still meet the requirements of 40 CFR 60.18 if verification of smokeless operation is confirmed by Method 22.

# Third Party has also confirmed the presence of a standing pilot flame monitored by a thermocouple on all Steffes flares in compliance with EPA 40 CFR 60.18.













The Gas Assist is used to reduce smoke from low pressure flares, in cases when the BTU of gas is too high, the flow rate is too low or the flow rate is too high. Intended to fit low pressure models of the Variable Orifice Flares: SVG-3B4, SVG-3D4 and SVG-3D8.

Test data based on propane.

Data is reference only. Call factory for more specifics.



# **Gaseous Fuel**

#### **Ratings Range – 60 Hertz Operation**

Liquid Propane:	kW kVA	123 - 175 123 - 219
Natural Gas:	kW kVA	123 - 264 123 - 330

Baldor generators are available in a variety of power ratings and installation styles to meet the energy needs of the smallest businesses and the largest manufacturing facilities. All generator sets are designed to meet the specifications to ensure the fastest startup and dependable long-term operation. Rely on Baldor generators to provide the clean, quiet and environmentally friendly electrical power when you need it most. Emergency backup, standby, peak shaving or for any of your day or night electrical power needs, you can count on a dependable Baldor generator to provide the peace of mind and security you desire.

#### **Standby Power Features**

- ✓ Heavy-duty industrial gaseous fuel engine that meets the latest EPA emissions levels
- ✓ Brushless synchronous alternators with dynamic balancing and four pole construction
- ✓ Fully featured microprocessor based controller that's easy to use and field programmable for customized installations
- ✓ Generator sets are prototype tested and production tested to ensure easy startup
- ✓ Gen-set accepts rated load in one step
- ✓ Heavy duty construction that's designed for use in standby applications
- Manufactured in a dedicated and secure ISO-9001 certified facility
- Generator sets are backed by a world wide network of parts and service centers
- ✓ Optional agency approvals available including UL2200 and NFPA110
- Optional environmental enclosures available including weather resistant, sound attenuated, containerized, and walk-in models
- ✓ Full range of genset accessories and factory installed options available

Genset		Voltero			150°C Rise Alternator		150°C Rise Alternator		125°C Rise Alternator	
Model	Alternator	Voitage	Phase	Hertz	Standby Rating – LP Fuel		Standby Rating – Natural Gas		Prime Rating –	Natural Gas
Number					kW / kVA	Amps	kW / kVA	Amps	kW / kVA	Amps
IGLC280-2N	UCI274G-311	208 / 120	3	60	170 / 213	591	170 / 213	591	164 / 205	570
		220 / 127	3	60	173 / 216	568	183 / 229	601	174 / 218	571
		240 / 120 (1)	3	60	170 / 213	512	170 / 213	512	164 / 205	494
		240 / 120 (1)	1	60	123 / 123	513	123 / 123	513	123 / 123	513
		240 / 139	3	60	173 / 216	521	200 / 250	602	185 / 231	557
		380 / 220	3	60	154 / 193	293	154 / 193	293	149 / 186	283
		416 / 240	3	60	170 / 213	295	170 / 213	295	164 / 205	285
		440 / 254	3	60	173 / 216	284	183 / 229	301	174 / 218	286
		480 / 277	3	60	173 / 216	260	200 / 250	301	185 / 231	278
	UCI274G-17	600 / 347	3	60	173 / 216	208	192 / 240	231	180 / 225	217
	UCI274H-311	208 / 120	3	60	174 / 218	604	200 / 250	695	190 / 238	660
		220 / 127	3	60	174 / 218	571	207 / 259	680	196 / 245	644
		240 / 120 (1)	3	60	174 / 218	524	200 / 250	602	190 / 238	572
		240 / 120 (1)	1	60	142 / 142	592	142 / 142	592	142 / 142	592
		240 / 139	3	60	175 / 219	527	207 / 259	623	204 / 255	614
		380 / 220	3	60	171 / 214	325	182 / 228	346	170 / 213	323
		416 / 240	3	60	174 / 218	302	200 / 250	347	190 / 238	330
		440 / 254	3	60	174 / 218	286	207 / 259	340	196 / 245	322
		480 / 277	3	60	175 / 219	100	220 / 275	331	204 / 255	307
	HCI444D-311	208 / 120	3	60	173 / 216	601	262 / 328	910	236 / 295	820
		220 / 127	3	60	173 / 216	568	263 / 329	864	236 / 295	775
		240 / 120 (1)	3	60	173 / 216	521	262 / 328	789	236 / 295	711
		240 / 120 (1)	1	60	170 / 170	708	170 / 170	708	170 / 170	708
		240 / 139	3	60	174 / 218	524	264 / 330	795	237 / 296	714
		380 / 220	3	60	171 / 214	325	260 / 325	494	235 / 294	447
		416 / 240	3	60	173 / 216	300	262 / 328	455	236 / 295	410
		440 / 254	3	60	173 / 216	284	263 / 329	432	236 / 295	388
		480 / 277	3	60	174 / 218	100	264 / 330	397	237 / 296	357
	HCI444C-17	600 / 347	3	60	174 / 218	210	263 / 329	317	237 / 296	285
NOTES: (1) Alte	<b>IOTES:</b> (1) Alternator connections have two circuits available for low voltage.									
Availat	Available current in each low voltage circuit is equal to high voltage current listed in table.									
FOR Rat Stand	ungs and voitages by ratings do not h	not listed above re	ier to the anability b	ut can be	selector.	iration of the ut	ility failure per ISO-3	3046 DIN6271 :	and BS5514	
Baldor	Baldor reserves the right to implement specifications or design changes without notice.									

#### **Genset Ratings**

#### **Engine Application Data**

#### **Engine Specifications**

Manufacturer Engine Model # Engine Type Induction System

Displacement, L (in<sup>3</sup>) EPA Emissions Certification

HP at Rated Speed BHP (kWm) NG HP at Rated Speed BHP (kWm) Propane 269 (201) Rated RPM Bore and Stroke in (mm)

Compression Ratio Air Filter Type Governor Type / Model Governor Manufacturer Freq Req NL to FL Freq Reg Steady State

#### **Engine Lubrication System**

Oil Pan Capacity gal (L) Oil Capacity w/Filter gal (L) **Oil Filter Quantity** Oil Filter Type Oil Cooler Recommended Oil Oil Press psi (kPa)

#### **Engine Cooling System**

Genset Max Ambient Temp °F (°C) Engine Coolant Cap qt (L) Engine + Radiator System Cap qt (L) Water Pump Type Coolant Flow gpm (Lpm) Charge Air Cooler Flow cfm (cmm) Heat Rejected to Charge Air Cooler @ Rated kW; Btu/min (kW) Heat Rejected to Radiator @ Rated kW; Btu/min(kW) Max Restriction of Cooling Air in H<sub>2</sub>O (kPa)

#### Engine Exhaust System

Exhaust Manifold Type Exhaust Flow @ Rated kW cfm (cmm) Exhaust Temp (dry manifold) °F (°C) Min Back Pressure in H<sub>2</sub>O (kPa) Max Back Pressure in H<sub>2</sub>O (kPa) Exhaust Outlet Diameter in (mm) Exhaust Outlet Type Exhaust Catalyst

ALDOR GENERATORS NG Engine D146TIC 4 Cycle, 8 Cylinder Turbocharged/ Charge Air Cooled 14.62 (892) 40 CFR Part 60 & 1048 402 (300) 1800 5.04x5.59 (128x142) 10.5:1 Dry Electronic **EControls** Isochronous +/-0.5%

8.2 (31.0) 10.1 (38.1) 2 Cartridge Water Cooled 15W-40 Low Ash 43.5 (299)

122 (50) 38 (43.2) 200 (227.0) Centrifugal 180 (680) 809 (22.9) 1430 (25.1) 16189 (284.7) 0.5 (0.124)

Wet 1895 (53.7) 1382 (750) 0 (0) 20.4 (5.1) 3.5 (88.9) Flange Included

Engine Electrical System	
Charging Alternator Volts dc	24
Charging Alternator Amps	45
Grounding Polarity	Negative
Starter Motor Volts dc	24
Battery Recommendations	
Battery Volts dc	24
Min Cold Cranking Amps	900
Quantity Required	2
Ventilation Requirements	
Cooling Airflow, scfm (cmm)	30000 (850)
Combustion Airflow, cfm (cmm)	532 (15.1)
Heat Rejected to Ambient	
From Engine, Btu/min (kW)	2389 (42)
From Alternator, Btu/min (KVV)	1115 (19.6)
Recommended Free Area Intake	
Louver Size, ft <sup>2</sup> (m <sup>2</sup> )	62.0 (5.76)
Engine Fuel System	
	1015
Natural Gas min HHV (Btu/ft°)	1015
	2000
	7-11(1.7-2.7)
Supply Line, npt	2
Pronane Fuel Consumption - Sta	undby Bating
100% Load cfph (m <sup>3</sup> ph)	926 (26.2)
75% Load cfph ( $m^3$ ph)	789 (22.3)
50% Load cfph ( $m^3$ ph)	532 (15.1)
25% Load cfph (m <sup>3</sup> ph)	335 (9.5)
NG Fuel Consumption – Standby	Rating
100% Load cfph (m <sup>3</sup> ph)	2782 (78.8)
75% Load cfph (m <sup>3</sup> ph)	2168 (61.4)
50% Load cfph (m³ph)	1522 (43.1)
25% Load cfph (m <sup>3</sup> ph)	928 (26.3)
NG Fuel Consumption – Standby	Rating
100% Load cfph (m <sup>3</sup> ph)	2532 (71.7)
75% Load cfph (m <sup>3</sup> ph)	1973 (55.9)
50% Load cfph (m <sup>3</sup> ph)	1385 (39.2)
25% Load cfph (m <sup>3</sup> ph)	844 (23.9)
Engine Output Deratings - Stand	lby
Rated Temp	77°F
Rated Altitude	325 ft
Max Altitude	10.000 ft
Temperature Derate	-1% / 8º F
Altitude Derate	-3% / 1000 #
	0707 10001

#### **Alternator Specifications**

Alternator Type4Exciter TypeEExcitation System5Shunt Connection5PMG0Insulation0Material0Standby Temp Rise1Lead Connection1Stator Pitch2Amortisseur Winding5Drive Coupling6Unbalanced Load2

4-Pole, Rotating Field Brushless

Standard Optional per NEMA MG1 Class H 150°C 12 Lead, Reconnectable 2/3 Full Single, Double Shielded Flexible Disk 20% of Standby Rating

#### Automatic Voltage Regulator

Wound FieldSX460, SX440 for HCI444DPMGMX341, MX321Voltage RegulationNo Load to Full LoadStd Regulator+/- 1.5%, +/- 1%PMG Regulator+/- 1%, +/- 0.5%Load Acceptance100% of Rating, One Step

#### Subtransient Reactance

 480V, Per Unit
 11%, 13%

 TIF (1960 Weighting)
 <50</td>

 Line Harmonics
 5% Maximum

 Motor Starting kVA
 30% Max Voltage Dip

 Alt @ 480V SkVA
 UCI274H-311
 730 kVA

 Alt @ 480V SkVA
 HCI444D-311
 780 kVA

#### **Genset Controller Specifications**

#### **Baldor InteliLite NT Features**

- Large back-lit graphical LCD Display 64x128 pixel resolution
- 6 LED Genset Status Indicators Alarm Red LED Not In Auto Red LED Warning Yellow LED Running Green LED Ready / Auto Green LED Supplying Load Green LED

Supplying Load Sealed Membrane Panel to IP65 Push Buttons for Simple Control Start, Stop, Fault Reset, Horn Reset, Mode, Page, and Enter Keys **Display Metering and Protection** Oil Pressure Warning / Shutdown High / Low Coolant Temperature Warning High Coolant Temperature Shutdown Low Coolant Level Shutdown **Over Speed Protection** Battery Voltage Over / Under Warning **Running Hour Meter** Generator Under / Over Volts Warn / Shutdown Generator Under / Over Freq Warn / Shutdown Generator Over Current Shutdown Generator Output Metering for V1-V3, I1-I3, Hz, kW, kWh, kVAr, kVAh




## Additional Standard Genset Features

- ✓ Structural Steel Sub-Base
- ✓ Sub-Base Lifting Eyes
- ✓ Unit Mounted Radiator
- ✓ Engine Mounted Fan
- ✓ Radiator Fan Guard
- ✓ Battery Charging Alternator
- ✓ Battery Rack and Cables
- Unit Mounted Control Panel
- ✓ Spin-On Oil Filter
- Enamel Finish
- ✓ One Set Operation / Maintenance Manual
- ✓ Factory Tested Prior to Shipment
- ✓ Limited Warranty

# **Optional Agency Approvals**

- UL2200 (Review Option Availability)
- NFPA110 (Request Remote Annunciator)

## Weight and Dimensions (Open Unit)

Weight – Wet Ib (kg) Overall Dimensions inches mm 8030 (3642) Length x Width x Height 137 x 72 x 79 3479 x 1828 x 2006

**Note:** Drawing is provided for reference only. Use engineering outline for installation planning.



# Available Accessories and Options

### Open Unit

- Industrial SilencerCritical Silencer
- Residential Silencer
- Hospital Grade Silencer
- Exhaust Flex Pipe
- Rain Cap

# Radiator Duct Flange Enclosed Units

- Weather Resistant Enclosure
- □ Sound Attenuated w/Internal Critical Silencer
- □ ISO Container □ Walk-In Enclosure

### Alternator Accessories

- PMG Exciter and AVR Upgrade
- Alternator Space Heater
- □ Exciter Field Circuit Breaker
- □ Alternator Drip Shield

### **Genset Accessories**

- Voltage Adjust Potentiometer
- □ Starting Battery

Battery Charger D Auto/Float

Auto/ Float Equalize Timer D Manual D Automatic

- Battery Heater
- □ Engine Coolant Heater
- □ Oil & Coolant Drain Valves (Engine/Radiator)
- □ Oil & Coolant Drain Extended to Base

### Main Output Breaker

Wall Mount

Manual

🗖 Unit Mount

- Transfer Switch
  - Automatic

### Control Panel

- Remote Annunciator
- □ Remote Communications
- □ Remote E-Stop

### **Fuel System**

- Fuel Strainer
- Dual Fuel Automatic Changeover

### **Vibration Isolators**

- Elastomer Isolator
- Standard Spring
- □ Seismic Spring



Baldor Electric Company • P. O. Box 2400 • Fort Smith, AR 72902-2400 U.S.A.

Phone (479) 646-4711 • Fax (479) 648-5792 • International Fax (479) 648-5895 www.baldor.com

e**m** Biner



# Gaseous Product Line

#### 208-600 Volt

#### NG200-01 / NG200-01P

# 60 Hz / 1800 RPM

#### 190 - 200 kWe / 175 kWe

### Standby UL 2200 / Non-UL 2200 / Prime UL 2200

# Ratings

	240V	208V	240V	480V	600V
Phase	1	3	3	3	3
PF	1.0	0.8	0.8	0.8	0.8
Hz	60	60	60	60	60
Generator Model	432CSL6210	431CSL6206	431CSL6206	431CSL6206	431PSL6243
Connection	12 LEAD ZIG-ZAG	12 LEAD WYE	12 LEAD DELTA	12 LEAD WYE	4 LEAD WYE
Standby UL 2200					
kWe Nat (LP)	190 (130)	190 (130)	190 (130)	190 (130)	190 (130)
AMPS Nat (LP)	792 (542)	660 (452)	572 (391)	286 (196)	229 (157)
Temp Rise	130°C / 27°C	130°C / 27°C	130°C / 27°C	130°C / 27°C	130°C / 27°C
Standby Non-UL 220	00 [This rating not avail	able with UL 2200 Listing	or CSA Certification]		
kWe Nat (LP)	200 (130)	200 (130)	200 (130)	200 (130)	200 (130)
AMPS Nat (LP)	833 (542)	695 (452)	602 (391)	301 (196)	241 (157)
Temp Rise	130°C / 27°C	130°C / 27°C	130°C / 27°C	130°C / 27°C	130°C / 27°C
Prime					
kWe Nat (LP)	175 (NA)	175 (NA)	175 (NA)	175 (NA)	175 (NA)
AMPS Nat (LP)	729 (NA)	608 (NA)	527 (NA)	263 (NA)	211 (NA)
Temp Rise	105°C / 40°C	105°C / 40°C	105°C / 40°C	105°C / 40°C	105°C / 40°C

# Standard Equipment

#### Engine

- Radiator Cooled Unit Mounted (50°C)
- Blower Fan & Fan Drive
- Starter & Alternator
- Oil Pump & Filter
- ► Oil Drain Extension w/Valve
- Governor Electronic Isochronous
- ► 24V Battery System & Cables
- Air Cleaner (Dry Single Stage)
- Flexible Fuel Connector
- ► EPA Certified
- MasterTrak Remote Monitoring System

#### Listing Certifications

- ▶ UL 2200 Listed
- ▶ cUL Listed
- CSA Certified
- Seismic Certified to IBC 2012

#### NG200-01 / NG200-01P

#### Generator

- Brushless Single Bearing
- Automatic Voltage Regulator
- ► ± 1% Voltage Regulation
- ► 4 Pole, Rotating Field
- ► 130°C Standby Temperature Rise
- ▶ 105°C Prime Temperature Rise
- ▶ 100% of Rated Load One Step
- ▶ 5% Maximum Harmonic Content
- ► NEMA MG 1, IEEE and ANSI Standards Compliance for Temperature Rise

#### Additional

- Microprocessor Based Digital Control
- Interface Connection Box
- ▶ Control Panel Mounted in NEMA 12 Enclosure
- Base Formed Steel
- ► Main Line Circuit Breaker Mounted & Wired
- ► Catalyst / Silencer Mounted
- Battery Charger 24V 5 Amp
- Jacket Water Heater -20°F 3000W 240V w/Isolation Valves
- Vibration Isolation Mounts
- Radiator Duct Flange (OPU Only)
- ► Single Source Supplier
- > 2YR / 2000HR Standby Warranty
- ▶ 1YR / 1500HR Prime Warranty
- ► Standard Colors White / Tan / Gray

# Gaseous Product Line

### 190 - 200 kWe / 175 kWe

# BLUE ST R Power Systems Inc.

# Application Data

Engine			
Manufacturer:	Power Solutions International	Displacement - Cu. In. (lit):	673 (11.1)
Model:	lodel: D111TIC		4.84 (12.3) x 6.1 (15.5)
Туре:	4-Cycle	Compression Ratio:	10.5 : 1
Aspiration:	Turbo Charged, CAC	Rated RPM:	1800
Cylinder Arrangement:	6 Cylinder Inline	Max HP Stby (kWm):	302 (225)
Exhaust System		Standby	Prime
Gas Temp. (Stack): °F (°C)		1,350 (732)	1,350 (732)
Gas Volume at Stack Temp: CFM (	m³/min)	1,247 (35.3)	1,247 (35.3)
Maximum Allowable Exhaust Restr	iction: in. H2O (kPa)	40.8 (10.2)	40.8 (10.2)
Cooling System			
Ambient Capacity of Radiator: °F (°	°C)	122 (50.0)	122 (50.0)
Maximum Allowable Static Pressure	e on Rad. Exhaust: in. H2O (kPa)	0.50 (0.12)	0.50 (0.12)
Water Pump Flow Rate: GPM (lit/m	nin)	81.9 (310)	81.9 (310)
Heat Rejection to Coolant: BTUM (	kW)	9,687 (170)	9,687 (170)
Heat Rejection to CAC: BTUM (kW	)	1,278 (22.4)	1,278 (22.4)
Heat Radiated to Ambient: BTUM (	(kW)	1,893 (33.1)	1,893 (33.1)
Air Requirements			
Aspirating: CFM (m³/min)		392 (11.1)	392 (11.1)
Air Flow Required for Rad. Cooled	Unit: CFM (m³/min)	18,000 (509)	18,000 (509)

Consult Factory For Remote Cooled Applications

	Standby		Prime	
Fuel Consumption	Natural Gas	LP	Natural Gas	LP
At 100% of Power Rating: ft3/hr (m3/hr)	2,115 (59.9)	704 (19.9)	1,851 (52.4)	N/A
At 75% of Power Rating: ft3/hr (m3/hr)	1,648 (46.7)	549 (15.5)	1,442 (40.8)	N/A
At 50% of Power Rating: ft3/hr (m3/hr)	1,157 (32.8)	463 (13.1)	1,012 (28.7)	N/A
Fuel Inlet Size: NPT	2.0	0"	2.00	)"
Fuel Pressure Required: in. H <sub>2</sub> O (kPa)	7.00 - 11.0 (1	.75 - 2.75)	7.00 - 11.0 (1	.75 - 2.75)
Fluids Capacity				
Total Oil System: gal (lit)				6.60 (25.0)
Engine Jacket Water Capacity: gal (lit)				6.60 (25.0)
System Coolant Capacity: gal (lit)				27.7 (105)

All calculations based on natural gas fuel.

Air Flow Required for Heat Exchanger/Rem. Rad. CFM (m³/min)

Deration Factors: Temperature: Derate 1.5% Per 10°F Over 77°F Air Inlet Temperature | Altitude: Derate 2.5% Per 1,000 ft Over 1,200 ft

# Gaseous Product Line

### 190 - 200 kWe / 175 kWe

# BLUE ST R Power Systems Inc.

# DGC-2020 Control Panel

#### Standard Features

- Digital Metering
- ▶ Engine Parameters
- ► Generator Protection Functions
- ► Engine Protection
- CAN Bus ECU Communications
- ► Windows-Based Software
- Multilingual Capability
- ▶ Remote Communications to RDP-110 Remote Annunciator
- ▶ 16 Programmable Contact Inputs
- ▶ Up to 15 Contact Outputs (7 standard)
- ▶ UL Recognized, CSA Certified, CE Approved
- ► Event Recording
- ▶ IP 54 Front Panel Rating with Integrated Gasket
- ► NFPA 110 Level 1 Compatible



# Weights / Dimensions / Sound Data

	L x W x H	Weight lbs
OPU	120 x 66 x 80 in	6,475
Level 1	156 x 66 x 94 in	7,725
Level 2	156 x 66 x 94 in	7,775
Level 3	196 x 66 x 94 in	8,100

Please allow 6-12 inches of height of exhaust stack.

	No Load	Full Load
OPU	82 dBA	84 dBA
Level 1	80 dBA	82 dBA
Level 2	75 dBA	77 dBA
Level 3	69 dBA	71 dBA









Drawings based on standard open power 480 volt standby generator. Lengths may vary with other voltages. Subject to change without notice. Sound data as measured at 23 feet (7 meters) in accordance with ISO 8528-10 at standby rating.

### 190 - 200 kWe / 175 kWe

# BLUE ST R Power Systems Inc.

# Enclosures







All enclosures are 150 MPH Wind Rated.

Level 2 & 3 enclosures include sound attenuation foam. Level 3 enclosure includes frontal sound & exhaust hood. \*Enclosure height does not include exhaust stack.

American Owned



Blue Star Power Systems, Inc.

52146 Ember Road Lake Crystal, Minnesota 56055 Phone + 1 507 726 2508 bluestarps.com quote.bluestarps.com sales@bluestarps.com

All specification sheet dimensions are represented in inches. Materials and specifications subject to change without notice.

Distributed By:

Attachment 3

**Air Quality Review** 

# Introduction

The Mamie 4-25-3-3WH well pad is located in Duchesne County, Utah, approximately 5.5 miles west of Myton and 4 miles northeast of Bridgeland. The land use surrounding the well pad location consists of a mixture of open land, agriculture and oil and gas operations. The nearest residence (and associated farm) is located approximately 1 mile northeast of the well pad. Air quality in the region is generally good but does have elevated ozone concentrations. Table 3-1 shows measured criteria pollutant concentrations at the closest ambient monitors to the proposed well pad. All monitored values shown in Table 2 are below the respective National Ambient Air Quality Standard (NAAQS) except for ozone. Parts of the Uintah Basin are designated as marginal nonattainment for ozone, including the area surrounding the Mamie 4-25-3-3WH well pad. The 24-hour 2.5-micron particulate matter ( $PM_{2.5}$ ) monitored value of 24 µg/m<sup>3</sup> is 69 percent of the 35 µg/m<sup>3</sup> NAAQS value.

The proposed well pad will increase pollutant emissions by less than 100 tons per year (tpy) for each pollutant, making it a minor source of criteria pollutant emissions. The largest criteria pollutant emissions from the site will be volatile organic compounds (VOC) [8.81 tpy], carbon monoxide (CO) [12.3 tpy], and nitrogen oxides (NO<sub>x</sub>) [6.35 tpy]. VOC and NO<sub>x</sub> emissions are precursors to ozone formation. The minor emissions of these precursor pollutants would not significantly change ozone concentrations in the region. Likewise, CO emissions would not be expected to significantly affect CO concentrations in the area.

Increased NO<sub>x</sub> emissions from the well pad would result in an increase in Nitrogen dioxide (NO<sub>2</sub>) concentrations, but the increases would be highly localized to the well pad and will not affect compliance with the NAAQS. NO<sub>x</sub> emissions from the source will be 6.35 tpy, well below EPA's Significant Emission Rate (SER) of 40 tpy. The primary contributor of NO<sub>x</sub> emissions at the site will be two natural gas-fired generator engines. One engine is an existing source at the site and the second engine is proposed. The engines have 9.3-foot stack heights which allow plumes to disperse and thereby reduce ground-level NO<sub>2</sub> concentrations.

Pollutant	Monitor	City	County	Averaging Period	Form	3-Year Average Value	NAAQS	Units
	490130002	Roosevelt	Duchesne	1 hours ORthor		29.0	100	nnh
NO	490137011	near Myton	Duchesne	1-nour	98 %	21.3	100	hhp
NO <sub>2</sub>	490130002	Roosevelt	Duchesne	Annual	Maan	Mean 4.7 53	F 2	ppb
	490137011	near Myton	Duchesne	Annual	Mean		55	
PM <sub>2.5</sub>	490130002	Roosevelt	Duchesne	24-hour	98 <sup>th</sup> %	24.0	35	µg/m³
	490130002	Roosevelt	Duchesne	Annual	Mean	6.0	12	µg/m³
Ozone	490130002	Roosevelt	Duchesne	<sup>8</sup> hour	4 <sup>th</sup> bigb	73.0	70	nnh
	490137011	near Myton	Duchesne	8-110UI	4 <sup></sup> nign	77.3	70	hhn

 Table 3-1

 2015-2017 Ambient Monitor Values\*

\* Data from https://www.epa.gov/outdoor-air-quality-data/monitor-values-report

# **Dispersion Modeling**

To verify that the NAAQS will be protected during operation of the modified well pad, a dispersion modeling analysis was completed for the site. A summary of the modeling methodology, model input data, and model results is provided in the following sections.

The technical approach to completing the dispersion modeling followed the guidance outlined in EPA's Guideline on Air Quality Models (Revised) (EPA 2017). The EPA guidance includes elements that only apply to major PSD sources, however the general modeling methodologies described in this document applies to all regulatory modeling. Based on the projected emissions from the project and modeling procedures set forth by EPA, the pollutants and averaging periods that were modeled include the following:

- 24-hour PM<sub>10</sub>
- 24-hour and annual PM<sub>2.5</sub>
- 1-hour and 3-hour SO<sub>2</sub>
- 1-hour and Annual NO2
- 1-hour and 8-hour CO

The air quality impact analysis involved characterizing the release parameters for the emission sources, selection of appropriate meteorological data, developing model receptors, identifying appropriate background concentrations, and processing these data in the dispersion model. Model inputs such as meteorological data, model receptors, and background pollutant concentrations were developed following guidance and recommendations from the EPA.

Modeling was completed by evaluating criteria pollutant emissions resulting from well pad emission sources, including tanks, tank heaters, heater-treaters, generator engines, and the flare. Modeled concentrations were added to background concentrations to estimate the cumulative impacts to air quality in the vicinity of the well pad. These cumulative concentrations were compared to the NAAQS to evaluate compliance with the standards.

## **Dispersion Model Selection**

Dispersion modeling was completed using the American Meteorological Society/ EPA Regulatory Model Improvement Committee Dispersion Model named "AERMOD." AERMOD is EPA's preferred regulatory model for near-field dispersion modeling (EPA 2017). The most recent approved version of AERMOD (Version 18081) was used for this analysis. AERMOD is a Gaussian plume dispersion model based on planetary boundary layer principles for characterizing atmospheric stability. The model evaluates the non-Gaussian vertical behavior of plumes during convective conditions based on the probability density function and the superposition of several Gaussian plumes. The AERMOD modeling system has three components: (1) AERMAP, the terrain preprocessor program; (2) AERMET, the meteorological data preprocessor; and (3) AERMOD, which includes the dispersion modeling algorithms.

AERMOD was developed to handle simple and complex terrain issues using improved algorithms. As with the Complex Terrain Dispersion Model, AERMOD uses the dividing streamline concept to address interactions of the plume with elevated terrain. AERMOD was run using the regulatory default options, including use of elevated terrain algorithms, stack-tip downwash, calms processing routines, and use of missing data processing routines.

The latest versions of AERMOD incorporate new model options that were developed to address model performance issues during stable, low wind conditions. Recent studies have shown large model over-predictions during stable, low wind conditions, especially for low-level sources and ground-level fugitive sources such as those at the Mamie 4-25-3-3WH well pad (Paine and others 2012). The new model options are designed to reduce the amount of model over-prediction and produce more realistic model results. One new option has been accepted as a regulatory option by EPA and has been incorporated into this modeling analysis. This model option is referred to as the surface friction velocity adjustment and is briefly described below:

 AERMET Surface Friction Velocity Adjustment (STABLEBL ADJ\_U\*) – This model option is included in the AERMET pre-processor and addresses problems with modeled concentrations during stable, low wind conditions. During hours with a stable, low wind atmosphere, the surface friction velocity is adjusted to increase turbulence for that hour. Because most of the emission sources at the well pad will be low-level sources, this model option is appropriate for the use in the modeling analysis.

### Nitrogen Dioxide Conversion Options

AERMOD includes several options for calculating the conversion of  $NO_X$  emissions to  $NO_2$  in the atmosphere. EPA has identified a tiering approach for addressing  $NO_2$  conversion, with each tier requiring a more technical approach and typically resulting in a less conservative result (EPA 2016). Three tiers are available for modeling. A summary of each tier is given below:

- Tier 1: All of the NO<sub>x</sub> emissions released from the source are assumed to convert to NO<sub>2</sub>. This is the most conservative option and likely will result in an overestimate of NO<sub>2</sub> concentrations in the ambient air.
- Tier 2: Modeled NO<sub>x</sub> concentrations are converted to NO<sub>2</sub> by multiplying empirically-derived scaling factors. Two methods are available, the Ambient Ratio Method (ARM) and the Ambient Ratio Method 2 (ARM2).
- Tier 3: NO<sub>2</sub> concentrations are calculated from NO<sub>x</sub> within AERMOD using screening algorithms that estimate the amount of NO<sub>2</sub> conversion based on ambient ozone concentrations and other environmental factors. Two options are available in AERMOD, the Ozone Limiting Method (OLM) and the Plume Volume Molar Ratio Method (PVMRM2). Both Tier 3 methods are considered regulatory options by EPA and are generally considered acceptable for use in a regulatory context (EPA 2016).

The modeling option used for this analysis is the Tier 2 ARM2 method for calculating NO<sub>2</sub> chemical conversion. Use of the ARM2 method requires input of the upper and lower limits of the ambient ratio of NO<sub>2</sub>/NO<sub>x</sub>. The default values of 0.9 and 0.5, respectively, were used for the modeling.

### Meteorological Data

UDEQ has processed several datasets through the AERMET meteorological data pre-processor and has made these datasets available on its website. Meteorological data from the closest available station is the Vernal, Utah dataset. Vernal is located approximately 38 miles northeast of the project site. The elevation of the Vernal station and the project site are similar, and both locations are located on the southern side of the Uinta Mountains. A review of wind data from nearby Roosevelt, UT shows that the vicinity of the project site is dominated by westering wind directions, which is similar to Vernal, UT. As a result, the Vernal meteorological dataset has been deemed representative of conditions at the project site. The dataset consists of five years of data (2008-2012) from the Vernal National Weather Service (NWS) station, combined with upper air data from the Grand Junction, CO NWS station and processed by UDEQ into model-ready format using the AERMET pre-processor software. This meteorological dataset was used for the modeling analysis. Figure 3-1 shows the wind rose diagram meteorological data used in the modeling analysis.

## Receptor Grid

A grid of model receptor points was defined for the modeling. The receptor points define where the model will calculate pollutant concentrations. Receptor points were developed using a dense grid of model receptors surrounding the well pad ambient boundary. Multiple receptor grid tiers were used to ensure that the maximum estimated impacts are identified. Following EPA guidelines, receptor locations were identified with sufficient density and spatial coverage to isolate the area with the highest impacts. To accomplish this goal, the following nested receptor grid was used for the modeling assessments:

- 25-meter spaced receptors located along the entire ambient boundary
- 1 km by 1 km receptor grid with 50 m spacing, centered on the well pad
- 4 km by 4 km receptor grid with 100 m spacing, centered on the well pad

A total of 2,020 receptors were processed in the modeling. All model receptors were preprocessed using the AERMAP software (Version 18081) that is associated with AERMOD. The AERMAP software establishes a base elevation and a height scale for each receptor location. The height scale is a measure of the receptor's location and base elevation and its relation to the terrain feature that has the greatest influence on dispersion for that receptor.

AERMAP was run using digital terrain from the U.S. Geological Survey (USGS) National Elevation Dataset (NED). Use of NED terrain data in AERMAP is recommended by EPA for characterizing the terrain throughout the model domain. Output from AERMAP was used as input to the AERMOD runstream file for each model run. Model receptors are presented in the UTM coordinate system, NAD83. Figure 3-2 shows the model receptors used for the analysis.

### **Emission Sources**

The emissions incorporated into the modeling were all characterized as point sources. Effluent parameters were obtained from manufacturer specification, site drawings, and engineering judgement. Table 3-2 summarizes the stack parameters used in the modeling for each emission source. Emission rates are from the detailed emission inventory for the well pad. Figure 3-3 illustrates the locations of the emission sources at the well pad relative to the ambient boundary.

### **Building Wake Effects**

The modeling analysis includes evaluation of building dimensions to assess potential downwash effects on stack emissions from nearby structures. Direction-specific downwash parameters were calculated for the facility's buildings using facility plot-plan maps and EPA's Building Profile Input Program PRIME (BPIPPRM) software. The primary structures at the well pad are associated with the tank batteries. Output from BPIPPRM produced building dimension data that was incorporated into AERMOD to calculate building downwash from emission sources.







Source ID	Source Description	UTM Location (m)	Stack Height (m)	Stack Temperature (K)	Exit Velocity (m/s)	Stack Diameter (m)	
ENG1	Gen Engine 1	570079.6/4450259.9	2.85	1023.15	58.21	0.102	
ENG2	Gen Engine 2	570101.4/4450231.0	2.85	1023.15	58.21	0.102	
HTRTRTR1	Heater-Treater 1	570070.4/4450274.9	5.49	675.00	15.88	0.102	
HTRTRTR2	Heater-Treater 2	570109.3/4450230.0	5.49	675.00	15.88	0.102	
HTR1	Heater 1	570092.6/4450269.1	1.52	588.71	11.55	0.102	
HTR2	Heater 2	570097.2/4450269.1	1.52	588.71	11.55	0.102	
HTR3	Heater 3	570101.6/4450269.1	1.52	588.71	11.55	0.102	
HTR4	Heater 4	570106.7/4450256.0	1.52	588.71	11.55	0.102	
HTR5	Heater 5	570106.8/4450251.0	1.52	588.71	11.55	0.102	
HTR6	Heater 6	570106.8/4450246.0	1.52	588.71	11.55	0.102	
Flare1	Flare	570106.8/4450283.9	3.66	962.59	41.20	0.300	
Flare2	Flare	570112.0/4450217.0	3.66	962.59	41.20	0.300	

Table 3-2 Mamie 4-25-3-3WH Modeled Sources

### Air Quality Background Data

Ambient background concentrations represent the contribution of pollutant sources not included in the modeling analysis, including naturally occurring sources. The background concentration for each criteria pollutant is added to the maximum modeled concentration to calculate the total estimated pollutant concentration. Monitored pollutant data has been collected in the region and is available on EPA's outdoor-air-quality-data website. Nearby monitored pollutant data summarized in Table 3-1 has been used as background concentrations for this modeling analysis.

### Summary of Model Results

Results of the modeling indicate that operating the Mamie 4-25-3-3WH well pad after the proposed modification would comply with ambient air quality standards. Table 3-3 shows the modeled impacts, background concentrations, and total concentrations for the site. The highest modeled concentrations for all pollutants occurred on the northern and eastern edge of the ambient boundary, directly downwind of the operations. As expected with low-level emission sources, the modeled concentrations decrease quickly with distance from the well pad.

Modeled concentrations for  $PM_{10}$ , CO, and  $SO_2$  were all less than the respective significant impact levels (SILs). Therefore, the impacts for these pollutants are considered insignificant and there is no need to evaluate total impacts with background concentrations added in.

The air quality impact evaluation involved development of the proposed emission inventory followed by detailed dispersion modeling analyses to assess compliance with the NAAQS. Based on the projected emissions, Mamie 4-25-3-3WH will be considered a minor air emission source for permitting purposes.

Pollutant	Averaging Period	Maximum Modeled Concentration (µg/m <sup>3</sup> ) <sup>(a)</sup>	Significant Impact Level (μg/m <sup>3</sup> ) <sup>(a)</sup>	Measured Background Concentration (μg/m <sup>3</sup> ) <sup>(a)</sup>	Total Concentration (µg/m³) <sup>(a)</sup>	NAAQS (μg/m³) <sup>(a)</sup>
NO <sub>2</sub>	Annual	15.47 <sup>(b)</sup>	1	7.9	23.4	100 <sup>(b)</sup>
	1-hour	83.05 <sup>(c)</sup>	7.5 <sup>(d)</sup>	40.0	123.1	188 <sup>(c)</sup>
PM <sub>10</sub>	24-hour	2.67 <sup>(e)</sup>	5	N/A	N/A	150 <sup>(f)</sup>
PM <sub>2.5</sub>	Annual	1.08 <sup>(g)</sup>	0.3	6.0	7.1	12 <sup>(g)</sup>
	24-hour	1.84 <sup>(h)</sup>	1.2	24.0	25.8	35 <sup>(h)</sup>
CO	8-hour	129.78 <sup>(e)</sup>	10,000	N/A	N/A	10,000 <sup>(f)</sup>
	1-hour	241.63 <sup>(e)</sup>	40,000	N/A	N/A	40,000 <sup>(f)</sup>
SO <sub>2</sub>	3-hour	0.42 <sup>(e)</sup>	25	N/A	N/A	1,300 <sup>(f)</sup>
	1-hour	0.60 <sup>(e)</sup>	7.9 <sup>(d)</sup>	N/A	N/A	196.5 <sup>(i)</sup>

 Table 3-3

 Mamie 4-25-3-3WH Dispersion Modeling Results

Notes: (a)  $\mu g/m^3$  = micrograms per cubic meter

(b) Annual mean

(c) 98th percentile value, averaged over 3 years

(d) Interim value

(e) Overall maximum modeled value

(f) Not to be exceeded more than once in a calendar year

(g) Annual mean, averaged over 3 years

(h) 98<sup>th</sup> percentile value, averaged over 3 years

(i) 99<sup>th</sup> percentile value, averaged over 3 years

#### REFERENCES

- Paine, B., J. Connors, C. Szembek, and S. Hanna. 2012. AERMOD Low Wind Speed Evaluation Study. Presented at the 10th EPA Modeling Conference. March.
- EPA. 2017. Revision to the Guideline on Air Quality Models: Enhancements to the AERMOD Dispersion Modeling System and Incorporation of Approaches to Address Ozone and Fine Particulate Matter. Fed. Reg./Vol. 82, No. 10/Tuesday, January 17, 2017, Rules and Regulations, pp. 5182-5235. 40 CFR Part 51, FRL-9956-23-OAR. RIN 2060-AS54.
- EPA. 2016. User's Guide for the AMS/EPA Regulatory Model (AERMOD). EPA-454/B-16-011. Office of Air Quality Planning and Standards, Air Quality Assessment Division. Research Triangle Park, North Carolina. December.

# Attachment 4

# **Endangered Species Act and**

# **National Historic Preservation Act Documentation**

The Mamie 4-25-4-4WH facility is located on a previously developed wellpad. The previously developed site will not require a change to the site's disturbed footprint. The well pad is part of the Rocky Point Exploration and Development plan. Enclosed is as copy of the Final Biological Opinion for the Rocky Point EDA. Newfield received an Administrative Modification approval for adding the new well with no additional disturbance from Bureau of Indian Affairs (BIA).

As a result, Newfield concludes that there is no potential to cause effects on federally-listed or endangered species or designated critical habitats.

In addition, no historic properties will be affected resulting from the proposed modification. BIA and the Uintah and Ouray Agency rendered a finding that the new construction would not impact archaeological or cultural resources. See the enclosed supporting documentation.



United States Department of the Interior BUREAU OF INDIAN AFFAIRS Uintah and Ouray Agency P. O. Box 130 Fort Duchesne, Utah 84026



OCT 3 0 2018

Jerry Kenczka Bureau of Land Management Vernal Field Office 170 South 500 East Vernal, UT 84078

## Re: Application for Permit to Drill Concurrence for **NEWFIELD PRODUCTION** COMPANY

Dear Mr. Kenczka:

This letter is to inform you that the Bureau of Indian Affairs, Uintah and Ouray Agency recommends the approval of the Applications for Permit to Drill for the below mentioned well sites along and associated access roads and pipelines, with required stipulations:

ROW No.	Well Name	Qtr/Qtr	Sec.	Twn.	Rng.	<b>ROW Type</b>
H62-2013-27	0 MAMIE UT 4-25-3-3WH	NWNW	25	3S	3W	WELLSITE

Based on available information received during the site specific inspection the proposed locations were cleared in the following areas of environmental impact:

YES	NO	X	Listed Threatened/Endangered Species
YES	NO	X	Critical Wildlife Habitat
YES	NO	X	Archaeological/Cultural Resources
YES	NO	X	Air Quality Aspects (to be used only if the project is in or
			adjacent to a Class I area)

Attached is a copy of the Grant of Easement for Right-of-way, as well as a copy of the Environmental Assessment.

If you have any questions, or if you require any additional information, please contact Karen Austin, Realty Specialist at 435-722-4326 or karen.austin@bia.gov

Sincerely,

Acting Superintendent

cc: Ute Indian Tribe Energy and Minerals Agency/Branch Chrono



# United States Department of the Interior

BUREAU OF INDIAN AFFAIRS UINTAH AND OURAY AGENCY P.O. Box 130 1400 South 7002 East Fort Duchesne, Utah 84026 Phone (435) 722-4300 Fax (435) 722-2323



IN REPLY REFER TO: Real Estate Services – MS 420

OCT 2 8 2018

Corie Miller, Regulatory Specialist Newfield Production Company 10530 South County Road #33 Myton, Utah 84052

Re: Letter for an Administrative Modification

Dear Mr. Miller:

The following Administrative Modification has been completed for approved wellsite.

ROW No.	Well Name/No.	Modification Type
H62-2013-270	Mamie UT 4-25-3-3WH	Additional well bore Mamie UT 4-25-3-3- 25-36-46H. No additional disturbance

Attached is an original copy of the Administrative Modification form that reflects the authorized modification to the original Grant of Easement. Please adhere to all original regulations and stipulations cited in the original site specific Environmental Assessment.

Retain this letter as your permit to begin construction on Tribal lands. Please remind your field personnel of the firearm restrictions on the Uintah and Ouray Reservation.

If you have any questions, or if you require any additional information, please contact Karen Austin, Realty Specialist, at (435) 722-4326 or <u>karen.austin@bia.gov</u>.

Sincerely.

Superintendent

cc: Ute Indian Tribe Energy and Minerals Agency/Branch Chrono 420:KA/SG:10/24/2018:TR4616-P5

RECEIVED

# UNITED STATES DEPARTMENT OF THE INTERIOR ULT 1 1 2018 BUREAU OF INDIAN AFFAIRS

#### **ADMINISTRATIVE MODIFICATION**

AGENCY AP 426-19 Superintendent

TRACT NO.:\_\_\_\_\_

The United States of America, acting by and through the Bureau of Indian Affairs, Department of the Interior, <u>Uintah & Ouray Agency</u> for, and on behalf, of: <u>Ute Indian Tribe</u> (the GRANTOR), it is hereby agreed by and between, <u>Newfield Production Company</u>, that the Grant of Right-of-Way Easement No. <u>H62 2013-270</u>, approved on <u>March 15, 2013</u>, is hereby modified to correct the following clerical error:

Add Mamie UT 4-25 3-3-25-36-46H well bore to existing Mamie 4-25-3-3WH wellsite. No additional disturbance or change in acreage is proposed. Mamie wellsite is located in the NWNW Sec 25 T3S R3W USB&M.

This modification does not change any of the terms, conditions, or stipulations except as specifically set forth herein.

The within modification is hereby approved and declared to be made in accordance with the law and the rules and regulations prescribed by the Secretary of the Interior thereunder, and now in force.

DATE: 10/10/2018

(Grantee)

Newfield Regulatory Specialist

IN WITNESS WHEREOF, GRANTOR, pursuant to authority delegated to the Assistant Secretary – Indian Affairs by 209 DM 8, to the Director of BIA by 230 DM 1 and to the Western Regional Director by 3 IAM 4 and to the Superintendent by historic Phoenix Area Re-Delegation Documents in 10 BIAM is granting and executing this Modification of Grant of Easement on this \_\_\_\_\_\_\_ 26\_\_\_\_ day of  $\mathcal{L}_{Hbec}$ , 2018.

BY:

Acting Superintendent U.S. Department of the Interior Bureau of Indian Affairs

## ACKNOWLEDGEMENT

STATE OF: Utah		
: SS		
COUNTY OF: Uintah		
Subscribed and sworn to before me this day o	<b>October</b> f	, 20 <mark></mark> .
Signature of Notary Public		
My commission expires on	_, 20	
Notary Public SHAWNEE GUZMAN Commission #887153 My Commission Expires January 26, 2020 State of Utah		



IN REPLY REFER TO: Natural Resources – MS 460

# United States Department of the Interior

BUREAU OF INDIAN AFFAIRS UINTAH AND OURAY AGENCY P.O. Box 130 988 South 7500 East Fort Duchesne, Utah 84026 Phone (435) 722-4300 Fax (435) 722-2323



Decision Record and Finding of No Significant Impact Environmental Assessment and Biological Assessment No. U&O-FY13-Q1-020

### Newfield Exploration Company's Ten (10)Well Central Basin Exploratory Environmental Assessment and Biological Assessment

## DECISION

I have reviewed the final Environmental Assessment and Biological Assessment (EA & BA) of Newfield Exploration Company's (Newfield) proposed *Ten (10) Well Central Basin Exploratory EA & BA*, BIA NEPA No. U&O-FY13-Q1-020.

Based upon my review of this information, and information contained in the EA's Administrative Record, I have decided to approve and implement the portions of the Proposed Action, together with general Bureau of Indian Affairs (BIA) generated mitigation measures (See Chapter 4 of the EA) and Applicant-committed Environmental Protection Measures (ACEPMs) (See Chapter 2.1.8 of the EA). Site specific mitigations and stipulations have been determined during the site-specific environmental assessment process, as well as ACEPMs and cited mitigation measures contained in the programmatic *Rocky Point Exploration and Development Agreement Leasing and Exploratory Drilling Environmental Assessment and Biological Assessment*, BIA NEPA No. U&O-FY12-Q1-040.

The Proposed Action analyzed the construction, drilling, completion and production of the following ten (10) well bores and pads, including their associated rights-of-way and support infrastructure, which would occur in the Central Basin area of the Rocky Point Exploration and Development Agreement (Rocky Point EDA) project area:

- 1. Rhea 2-9-3-1W, located in Section 9
- 2. Chegar 1-10-3-1WH, located in Section 10
- 3. Oscar 1-19-3-1WH, located in Section 19
- 4. Tuck 1-20-3-1WH, located in Section 20
- 5. Jack Johnson 3-20-3-1WH, located in Section 20
- 6. Pekev 2-29-3-1WH, located in Section 29 Township 3 South, Range 1 West;
- 7. Poker Jack 4-13-3-2WH, located in Section 18

Decision Record/ Finding of No Significant Impact EA No. U&O-FY13-Q1-020

Page 2

Township 3 South, Range 2 West;

- 8. Ute Tribal 4-21-3-3WH, located in Section 21
- 9. Mamie 4-25-3-3WH, located in Section 25
- Ute Tribal 7-26-3-3W, located in Section 26 Township 3 South, Range 3 West, Uintah Special Base and Meridian, Duchesne County, Utah.

Approval and implementation of the modified Proposed Action would include the following primary components, which would occur on lands owned privately and by the Ute Indian Tribe (Tribe/Tribal):

- Issuance of BIA Grants of Easement for right-of-way for ten (10) oil and gas well rightsof-way, also issue an Application for Permit to Drill concurrence for each well bore to the Bureau of Land Management, which would consist of approximately 47.331 acres, more or less, on both Tribal lands;
- Construction of ten (10) access roads, which would be approximately 40-foot width and 18,109-feet in length, being approximately 16.635 acres, more or less, on both Tribal and private lands;
- Construction of ten (10) pipeline corridors, which would be approximately 60-foot width and 26,035.78-feet in length, being approximately 40.292 acres, more or less, on both Tribal and private lands;

### REASONS FOR THE DECISION

I have decided to implement the Proposed Action and concur with the *Ten (10) Well Central Basin Exploratory EA & BA* because of the following:

- 1. It meets the intent of the Indian Mineral Development Act (25 United States Code [U.S.C.] Section 2102).
- 2. BIA, Tribal, and other federal entity input were obtained and the environmental issues related to the Proposed Action were identified and analyzed.
- 3. The EA disclosed the environmental consequences of the Proposed Action and No Action alternatives.
- 4. Compliance will be met with all relevant federal, state, and local laws, as well as county and Tribal regulations and policies. Newfield will follow strict procedures during construction, operation and maintenance activities.
- 5. The EA provides for protection of affected resources before, during, and after the planned construction, operation, and reclamation activities associated with the Proposed Action.
- 6. The Proposed Action allows for the continued exploration and production of natural gas and oil activities in the Rocky Point EDA project area, which in turn keeps Newfield, the Tribe, and BIA in compliance with their approved EDA and associated Tribal leases.

Decision Record/ Finding of No Significant Impact EA No. U&O-FY13-Q1-020

#### Page 3

- 7. The project will contribute to the economic development of Indian land and will assist in the self-determination objectives of the Tribe through job opportunities, lease revenue, and fees.
- 8. The project will contribute to the economy of the Uintah Basin through the purchase of goods and services.

### SCOPING AND PUBLIC INVOLVEMENT

Due to the small scale of this project and exploratory nature of the proposed wells, no external public scoping was conducted for this project. Internal scoping meetings were conducted by the BIA, Tribe, BLM and Newfield and their contractors during onsite meetings conducted on May 1, 2012, and a determination of potential impacts to individual resources was conducted at that time.

Name	Representing	Responsibility
Audie Appawoo	Ute Tribe, Energy & Minerals Department	Compliance Officer
Bucky Secakuku	Bureau of Indian Affairs, Uintah & Ouray Agency	Environmental Protection Specialist
Sherri Wysong	Bureau of Land Management, Vernal Field Office	Natural Resource Specialist
Tim Eaton	Newfield Exploration Company	Regulatory Technician
Corie Miller	Newfield Exploration Company	Regulatory Technician
Zander McIntyre	Newfield Exploration Company	Production Foreman
Forest Bird	Newfield Exploration Company	Construction Foreman
Dennis Petty	Tri-State Surveying & Consulting, Inc. (TSLSC)	Surveyor
McCoy Anderson	Uinta Engineering & Land Surveying, Inc. (UELS)	Surveyor
Jodie Eisil	Outlaw Engineering, Inc.	Botanist
Randy Freston	Outlaw Engineering, Inc.	Biologist
Bridget Atkin	Outlaw Engineering, Inc.	Botanist
Todd Sherman	Outlaw Engineering, Inc.	Biologist
Amy Ackman	Montgomery Archaeological Consultants, Inc. (MOAC)	Archaeologist
Lindsey Kester	SWCA Environmental Consultants, Inc. (SWCA)	Archaeologist
Justin Strauss	SWCA	Paleontologist
Don Hamilton	Star Point Enterprises, Inc.	Regulatory Specialist
Jean Sinclear	Kleinfelder (KLF)	NEPA Specialist

List of Participants at the May 1, 2012 Onsite Meeting

## PLAN CONFORMANCE AND CONSISTENCY

**Rocky Point Exploration and Development Agreement Leasing and Exploratory Drilling Environmental Assessment and Biological Assessment, BIA NEPA No. U&O-FY12-Q1-040** The Proposed Action would be in compliance with the approved *Rocky Point Exploration and Development Agreement Leasing and Exploratory Drilling Environmental Assessment and Biological Assessment*, which allows for the Newfield Production Company and Ute Energy the right to conduct oil and gas operations on approximately 19,035 acres of Tribal and individual Allotted surfaces and minerals west of the project area. The proposed action would be used to transport product to either side of the Duchesne River, thereby reducing the need to construct

Decision Record/ Finding of No Significant Impact EA No. U&O-FY13-Q1-020

#### Page 4

additional pipelines across the river. The continued oil and gas development of the Rocky Point field would continue operations, thereby developing Tribal and Allotted natural resources and generating revenue from those resources.

### OTHER ALTERNATIVES CONSIDERED IN DETAIL

#### No Action Alternative

Under the No Action Alternative, the contract lands would not be leased to Newfield, and the ten (10) proposed well pads and ten (10) exploratory wells with their supporting infrastructure, including the installation and operation of production supporting gathering pipelines would not be authorized. Lacking federal approval, neither the BIA's purpose and need, nor the operator's purpose and need for the project would be realized. The No Action Alternative effectively constitutes denial of the Proposed Action as set out in this document. Other surface land uses in the project area would continue at their current trends. Newfield would continue to exercise and comply with their contractual rights and obligations to explore, and develop Tribal mineral resources as set forth in the Rocky Point EDA document. All such future exploration and/or development activities in the project area would be considered on a case-by-case basis and would be subject to separate NEPA analysis.

#### FINDING OF NO SIGNIFICANT IMPACT (FONSI)

I have considered both the beneficial and potential adverse effects of concurring with the approval of the modified Proposed Action. Based on experience and the results of the conceptual analyses contained in the *Ten (10) Well Central Basin Exploratory EA & BA*, I have determined that the effect of implementation will be limited in scope and intensity. Any effect that may occur will be within an acceptable range and, in and of themselves or by using the mitigation measures described in the Proposed Action of the *Ten (10) Well Central Basin Exploratory EA & BA*, and the ACEPMs and citied mitigation in Chapter 4 of the Proposed Action, if applicable, will result in no significant adverse environmental impact(s) either individually or cumulatively, to the physical or biological components of the environment, as defined in 40 *Code of Federal Regulations* (C.F.R.) 1508.27. My finding is based on the following determination:

- 1. Both beneficial and adverse effects were considered, and this action will not have a significant effect on the quality of the human environment.
- 2. The project will not adversely affect any unique characteristics of the geographic area (historic, heritage resources, prime farm lands, wetlands, etc.).
- 3. Based on the lack of information received from public participation, the scientific, social, and economic effects on the quality of the human environment are not likely to be highly controversial by implementing the Proposed Action.

#### Page 5

- 4. There are no known effects on the human environment that are highly uncertain, involve unique or unknown risks.
- 5. The actions in this decision will not establish a precedent for future actions with significant effects, nor do they represent a decision in principle about a future consideration.
- 6. There are no known significant local cumulative effects from this project and other projects implemented or planned on areas separated from the affected area of this project.
- 7. The actions planned will not adversely affect any sites listed in, or eligible for listing on, the National Register of Historic Places, nor will they cause the loss or destruction of any other significant scientific, cultural, heritage, historic, or prehistoric resources. This finding is based upon the commitment to survey all areas and to satisfactorily complete the Section 106 Consultation process prior to surface disturbance in all areas to be disturbed.
- 8. The decided actions are not likely to adversely affect any listed or proposed endangered, threatened, or sensitive plant or animal species, critical habitats, or unique natural communities.
- 9. The actions do not constitute, nor will they lead to, a violation of any federal, state, or local law, ordinance, or requirement imposed for the protection of the environment.

Authority: This finding and decision is made in accordance with section 1503.1 of the Council on Environmental Quality Regulations (40 CFR Parts 1500 through 1508) implementing the procedural requirements of the National Environmental Policy Act of 1969, as amended (42 U.S.C. 4321 et seq.), and the Department of the Interior Manual (516 DM 1-6), and is in the exercise of authority delegated to the Assistant Secretary-Indian Affairs (209 DM 8) to the Director of Indian Affairs (230 DM 1) to Regional Directors (3 IAM 4) to Agency Superintendents (10 BIAM).

Any questions regarding this Decision Record and Finding of No Significant Impact, please contact Bucky Secakuku, Environmental Protection Specialist, at (435) 722-4331 or bucky.secakuku@bia.gov.

**Responsible Official:** 

ACTING uperintendent Uintah and Ouray Agency



# United States Department of the Interior FISH AND WILDLIFE SERVICE

2369 WEST ORTON CIRCLE, SUITE 50 WEST VALLEY CITY, UTAH 84119

March 20, 2012

In Reply Refer To: FWS/R6 ES/UT 12-F-0085 6-UT-12-F-019

Memorandum

To:

Superintendent, Bureau of Indian Affairs, Uintah and Ouray Agency, Fort Duchesne, Utah

From: Utah Field Supervisor, Ecological Services, U.S. Fish and Wildlife Service, West Valley City, Utah

Subject:Final Biological Opinion for Newfield Exploration Company and Ute<br/>Energy, LLC's proposed Rocky Point Exploration and Development

In accordance with section 7 of the Endangered Species Act (ESA) of 1973, as amended (16 U.S.C. 1531 et seq.), and the Interagency Cooperation Regulations (50 CFR 402), this transmits our final biological opinion for impacts to the endangered Colorado pikeminnow (*Ptychocheilus lucius*), razorback sucker (*Xyrauchen texanus*), humpback chub (*Gila cypha*), and bonytail (*Gila elegans*); including their designated critical habitat. We refer to your correspondence and final environmental assessment/biological assessment (EA/BA) that we received on March 9, 2012, in which you requested formal consultation for this project.

Spiranthes diluvialis, Sclerocactus brevispinus, and S. wetlandicus were also analyzed within the EA/BA. We concur with that this project may affect, but is not likely to adversely affect these species based on the applicant-committed conservation measures included in the final EA/BA. In particular, our concurrence is based on the fact that initiation of formal section 7 consultation will be sought on a site-specific basis for well locations that are unable to avoid occupied listed plant habitat by 300 feet (see applicant-committed conservation measures in the EA/BA beginning on page 26).

#### **Consultation History**

This section summarizes significant steps in the consultation process:

#### Colorado River Fish Recovery Program

On January 21-22, 1988, the Secretary of the Department of the Interior; the Governors of Wyoming, Colorado, and Utah; and the Administrator of the Western Area Power Administration were cosigners of a Cooperative Agreement to implement the "Recovery Implementation Program for Endangered Fish Species in the Upper Colorado River Basin" (Recovery Program; Service 1987). The Recovery Program has been extended until September 30, 2013. An objective of the Recovery Program is to recover the listed species while providing for new water development in the Upper Colorado River Basin.

In order to further define and clarify processes outlined in sections 4.1.5, 4.1.6, and 5.3.4 of the Recovery Program, a section 7 Agreement (Agreement) and a Recovery Implementation Program Recovery Action Plan (RIPRAP) was developed. The Agreement establishes a framework for conducting all future section 7 consultations on depletion impacts related to new projects and all impacts associated with historic (defined as being initiated prior to January 1988) projects in the Upper Basin. Procedures outlined in the Agreement are used to determine if sufficient progress is being accomplished in the recovery of the endangered fishes to enable the Recovery Program to serve as a reasonable and prudent alternative to avoid jeopardy. The RIPRAP was finalized on October 15, 1993, and has been reviewed and updated annually.

In accordance with the 1993 Agreement, we assess the impacts of projects that require section 7 consultation and determine if progress toward recovery has been sufficient for the Recovery Program to serve as the reasonable and prudent alternative. As long as the Recovery Program achieves sufficient progress, biological opinions are written to identify activities and accomplishments of the Recovery Program that support it being used as the reasonable and prudent alternative. If sufficient progress in the recovery of the endangered fishes is not achieved by the Recovery Program, additional actions from the RIPRAP are identified for the project proponent to implement in order to avoid jeopardy to the endangered fishes. For historic projects, the Recovery Program serves as the reasonable and prudent alternative as long as recovery actions are completed according to the schedule identified in the RIPRAP. For new projects, the Recovery Program and/or addition actions identified from the RIPRAP serve as the reasonable and prudent alternative as long to the project being implemented.

After many years of successful implementation of the Recovery Program and Agreement, Federal action agencies anticipate recovery activities that must be included in their project planning to avoid jeopardy to listed species. Thus, our reasonable and prudent alternative is essentially part of the proposed action. The Recovery Program now serves as a conservation measure within the proposed action and in many cases minimizes adverse effects to listed species or critical habitat. The following excerpts summarize portions of the Recovery Program that address depletion impacts, section 7 consultation, and project proponent responsibilities:

"All future section 7 consultations completed after approval and implementation of this program (establishment of the Implementation Committee, provision of congressional funding, and initiation of the elements) will result in a one-time contribution to be paid to the Service by water project proponents in the amount of \$10.00 per acre-foot based on the average annual depletion of the project ... This figure will be adjusted annually for inflation [the current figure is \$19.21 per acre-foot] ... Concurrently with the completion of the Federal action which initiated the consultation, e.g., ... issuance of a 404 permit, 10 percent of the total contribution will be provided. The balance ... will be ... due at the time the construction commences ....."

It is important to note that these provisions of the Recovery Program were based on appropriate legal protection of the instream flow needs of the endangered Colorado River fishes. The Recovery Program further states:

"... it is necessary to protect and manage sufficient habitat to support self-sustaining populations of these species. One way to accomplish this is to provide long term protection of the habitat by acquiring or appropriating water rights to ensure instream flows. Since this program sets in place a mechanism and a commitment to assure that the instream flows are protected under State law, the [U.S. Fish and Wildlife] Service (Service) will consider these elements under section 7 consultation as offsetting project depletion impacts."

On July 8, 1997, we issued an intra-Service biological opinion determining that the depletion fee for average annual depletions of 100 acre-feet or less are no longer required because the Recovery Program has made sufficient progress to be the reasonable and prudent alternative to avoid the likelihood of jeopardy to the endangered fishes and to avoid destruction or adverse modification of their critical habitat by these small depletions. The intra-Service biological opinion has been reinitiated several times since 1997 to account for additional water depletions. The most recent update occurred on June 4, 2010 and increased the cap for small water depletions to 12,000 acre-feet. This increase will allow us to continue to exempt small depletions of 100 acre-feet or less.

<u>Chronology of recent events and past consultations between the Bureau of Indian Affairs</u> (BIA) and US Fish and Wildlife Service (Service) with regard to this section 7 consultation:

• 03/19/2012; we received clarification from Newfield and Ute Energy regarding pumping activities and water withdrawals from the Green River

- 03/09/2012; we received the final EA/BA and an addendum with updated applicant-committed conservation measures.
- 02/06/2012; we met with the BIA, Ute Tribe, Newfield, and biological consultants to discuss *Spiranthes diluvialis* mitigation measures.
- 02/02/2012; we sent comments to your office on the draft EA/BA.
- 01/26/2012; we received a scoping notice and a draft EA/BA from your office.
- 11/29/2011; we attended onsites with the BIA, Ute Tribe, Newfield, and Rana, Inc.

A complete administrative record for this project is on file in our office.

## **Biological Opinion**

#### I. DESCRIPTION OF PROPOSED ACTION

The project area is approximately 92,098 acres located mostly within Duchesne County (83,296 acres) and a small portion within Uintah County (8,802 acres). Surface ownership is 22,376 acres of Tribal surface administered by the BIA, 69,454 acres of Indian allottee or private land, and 268 acres of state lands. Under the proposed action (agency-preferred Alternative C of the EA/BA), Newfield and Ute Energy propose to construct, drill, complete, and produce 81 wells and build associated access roads and pipelines. Newfield intends to drill 55 exploratory oil and gas wells, and Ute Energy intends to drill 26 exploratory oil and gas wells over a two-year period. This alternative assumes that 4 wells from the original proposed action will not be developed because of overlap with occupied *Sclerocactus* habitat. The expected amount of new surface disturbance associated with this project is 1,539.3 acres. The life of the project is expected to be 20 to 30 years.

#### Action Area

The action area is defined in 50 CFR 402 to mean "all areas to be affected directly or indirectly by the Federal action and not merely the immediate area involved in the action." For the purposes of this consultation, we define the action area to encompass all of the project area proposed for well development including a 300 foot buffer surrounding these areas, and waterways downstream of the project area including the Duchesne and Green Rivers within and outside of the project area.

#### Applicant Committed Conservation Measures

Conservation measures are actions that the action agency and applicant agree to implement to further the recovery of the species under review. The beneficial effects of conservation measures are taken into consideration for determining both jeopardy and incidental take analyses.

#### Colorado River Endangered Fish Species

The following applicant-committed conservation measures will help minimize the impacts of the Proposed Action to the four Colorado River endangered fish species:

- Newfield will not pump surface water from the Green River. Specifically, for Newfield's development, water collection wells will be connected to a centralized pumping station via underground waterlines. The water wells will be developed using conventional drilling methods. Each well will extend to a depth of approximately 100 feet below the surface.
- Ute Energy will not withdraw water directly from the Green River.

In addition, Newfield and Ute Energy agreed to have the Upper Colorado River Recovery Program (Recovery Program) serve as a conservation measure within the proposed action. A portion of the water needed for this project may be acquired from the Newfield Green River Collector Well (water right numbers 47-1802 and 47-1804). Approximately 2,081 acre-feet of water depletion per year was consulted on during formal section 7 consultation completed for the Castle Peak Eight Mile Flat Oil and Gas Expansion Project (6-UT-05-012). However, additional consultation is needed for depletion through the Newfield Green River Collector Well for this leasing and exploratory drilling project and to account for additional freshwater needs to support Newfield's waterflood program in the nearby Greater Monument Butte Unit. While not part of the Rocky Point Proposed Action, Newfield, the BIA, and the Service have agreed to use this EA/BA as the mechanism for the programmatic section 7 consultation on additional water depletion for the waterflood program for the life of the Greater Monument Butte Development (approximately 20 to 30 years).

It is expected that approximately 2,823 acre-feet will be used annually for Newfield's waterflood program. Approximately 742 acre-feet that have not yet been consulted on (2823 acre-feet – 2,081 acre-feet = 742 acre-feet) will be withdrawn from the Newfield Green River Collector well. An additional 175 acre-feet will be withdrawn from the Newfield Green River Collector Well for the Rocky Point project, for a total of 917 acre-feet per year.

5

The following paragraphs further clarify the Recovery Program's role:

In determining if sufficient progress has been achieved under the Recovery Program, we consider--a) actions which result in a measurable population response, a measurable improvement in habitat for the fishes, legal protection of flows needed for recovery, or a reduction in the threat of immediate extinction; b) status of fish populations; c) adequacy of flows; and, d) magnitude of the Project impact. In addition, we consider support activities (funding, research, information, and education, etc.) of the Recovery Program if they help achieve a measurable population response, a measurable improvement in habitat for the fishes, legal protection of flows needed for recovery, or a reduction in the threat of immediate extinction. We evaluate progress separately for the Colorado River and Green River Subbasins; however, it gives due consideration to progress throughout the Upper Basin in evaluating progress toward recovery.

Water depletion impacts can be offset by: a) the water Project proponent's one-time contribution to the Recovery Program in the amount of \$19.21 per acre-foot of the Project's average annual depletion; b) appropriate legal protection of instream flows pursuant to State law; and, c) accomplishment of activities necessary to recover the endangered fishes as specified under the RIPRAP. We believe it is essential that protection of instream flows proceed expeditiously, before significant additional water depletions occur. As the project's peak annual new depletion of 917 acre-feet is below the current sufficient progress threshold of 4,500 acre-feet, Recovery Program activities will serve as the conservation measures to minimize adverse effects to the Colorado pikeminnow, razorback sucker, humpback chub, and bonytail and destruction or adverse modification of critical habitat caused by the project's new depletion.

With respect to (a) above (i.e., depletion charge), Newfield will make a one-time payment which has been calculated by multiplying the Project's peak annual depletion (917 acre-feet) by the depletion charge in effect at the time payment is made. For Fiscal Year 2012 (October 1, 2012, to September 30, 2012), the depletion charge is \$19.21 per acre-foot for the average annual depletion which equals a total payment of \$17,615.57 for this Project. A minimum of 10% of the total payment will be provided to the Service's designated agent, the <u>National Fish and Wildlife Foundation</u> (Foundation), at the time of issuance of the Federal approvals from the BIA, with the rest to be paid when construction commences. Fifty percent of the endangered fishes (unless otherwise recommended by the Implementation Committee); the balance will be used to support other recovery activities for the Colorado River endangered fishes. All payments should be made to the National Fish and Wildlife Foundation.

National Fish and Wildlife Foundation 1133 15th Street, NW Suite 1100 Washington, DC 20005 Each payment is to be accompanied by a cover letter that identifies the Project and biological opinion that requires the payment, the amount of payment enclosed, check number, and any special conditions identified in the biological opinion relative to disbursement or use of the funds (there are none in this instance). A copy of the cover letter and of the check is to be sent directly to our office. The cover letter shall identify the name and address of the payer, the name and address of the Federal Agency responsible for authorizing the Project, and the address of the Service office issuing the biological opinion. This information will be used by the Foundation to notify the payer, the lead Federal Agency, and the Service that payment has been received. The Foundation is to send notices of receipt to these entities within 5 working days of its receipt of payment.

#### **II. TERMS AND CONDITIONS**

In order to be exempt from the prohibitions of section 9 of the Act, BIA, Newfield, and Ute Energy must comply with the following terms and conditions, which implement the reasonable and prudent measures described above and outline required reporting/monitoring requirements. These terms and conditions are non-discretionary.

The following terms and conditions are assumed to include all previously listed applicant-committed environmental protection measures, but in some cases include more restrictive or more detailed measures. Conservation measures include implementing the Recovery Program (and relevant RIPRAP measures).

#### **III. REPORTING REQUIREMENTS**

In order to be exempt from the prohibitions of section 9 of the Act, the BIA must comply with all Recovery Program activities and the monitoring proposed below.

The implementing regulations for incidental take require that Federal agencies must report the progress of the action and its impact on the species (50 CFR 402.14(i)). To meet this mandate, the BIA will monitor and report the progress of their action as follows:

- 1. The BIA is required to submit to our office an annual report of water depletions associated with oil and gas development, including the following information:
  - Project name and/or applicant name
  - Permit number and/or special use authorization
  - General location and legal description
  - Depletion amount in acre-feet
  - Timing of depletion

7

- Identify if new or historic depletion<sup>1</sup>
- Sub-total water depletion (acre-feet) for each applicant
- Total depletion for the entire year in acre-feet
- Total number of APDs approved
- Total number of wells spudded

Reports shall be due to our office on a yearly basis by October 31. The address for the Utah Fish and Wildlife Service Field Office is:

2369 West Orton Circle, Suite 50 West Valley City, Utah 84119

#### **IV. REINITIATION - CLOSING STATEMENT**

This concludes formal consultation on the action outlined in your request. As provided in 50 CFR §402.16, reinitiation of formal consultation is required where discretionary Federal agency involvement or control over the action was retained (or is authorized by law) and if: (1) the average annual water withdrawals out of the Upper Colorado River Drainage System exceed the estimated 917 acre-feet by more than 10 percent; (2) new information reveals effects of the agency action that may affect listed species or critical habitat in a manner or to an extent not considered in this opinion; (3) the agency action is subsequently modified in a manner that causes an effect to the listed species or critical habitat not considered in this opinion; or (4) a new species is listed or critical habitat designated that may be affected by the action. In instances where the amount or extent of incidental take is exceeded, any operations causing such take must cease pending reinitiation.

We appreciate your commitment in the conservation of endangered species. If the project changes or it is later determined that the project affects listed species differently than identified above; it may become necessary to reinitiate section 7 consultation. If you require further assistance or have any questions, please contact Jessi Brunson, (435) 781-4448, or Drew Crane, (801) 975-3330, extension 124.



<sup>&</sup>lt;sup>1</sup> It is important to include information on whether each depletion is new or historic (occurring prior to January 1988), because we addresses new and historic depletions differently under the new section 7 agreement of March 11, 1993. Historic depletions, regardless of size, do not pay a depletion fee.