

April 25, 2019

Claudia Smith
Environmental Scientist
US EPA Region 8 Air Program
1595 Wynkoop Street
Mail Code 8P-AR
Denver, CO 80202

Via email: smith.claudia@epa.gov

**Re: South Ignacio Central Delivery Point, #SMNSR-SU-000013-2016.003
Synthetic Minor New Source Review Permit Revision
Red Cedar Gathering Company**

Red Cedar Gathering Company requests revision of South Ignacio Central Delivery Point's federal minor NSR permit #SMNSR-SU-000031-2016.003. The changes requested herein are intended to better align compliance-related activities across Red Cedar's facilities and do not otherwise affect the physical or operational state of the facility.

Red Cedar requests removal of the facility-wide HAP and HCHO emission limits. A previous owner of the facility voluntarily requested these limits to avoid major HAP requirements and they are not necessary. This request will not change the facility's emissions as all engines will continue to operate with the same emission controls currently installed in order to comply with the major RICE MACT requirements triggered by this change.

Red Cedar requests removal of the benzene emission limit for the dehydration units. A previous owner of the facility voluntarily requested this limitation and it is not necessary. The attached GRI_GLYCalc 4.0 calculations demonstrate uncontrolled actual benzene emissions from the dehydration units are less than 0.9 megagrams per year. Therefore, per §63.764(e)(1)(ii), these units are inherently exempt from 40 CFR part 63, subpart HH, regardless of any federally enforceable emission limits.

Red Cedar requests removal of the CO and formaldehyde emission limits for each of the seven lean-burn engines and the formaldehyde emission limit for the rich-burn engine. A previous owner of the facility voluntarily requested these limits and they are no longer necessary. This request will not change the facility's emissions as all the engines will continue to operate with the same emission controls currently installed in order to comply with the major RICE MACT requirements triggered by this change.

The requested changes above would not cause any change to the facility equipment, operations, or emissions but would cause the facility to be considered a major PSD source. The attached facility construction history demonstrates that the requested permit changes do not constitute PSD avoidance. Red Cedar does not have any plans to change equipment at the facility but understands future modifications would be subject to a lower PSD permitting threshold.

Red Cedar also requests the following permit changes for the rich-burn engine to better align its current compliance requirements with those in 40 CFR part 63, subpart ZZZZ, for new >500 HP 4SRB RICE located at a major source of HAP, to which the engine will be subject. These requested changes will streamline compliance activities but will not affect equipment, operations, or emissions.

- Remove quarterly NOx and CO monitoring requirements and replace with semiannual NOx and CO performance test requirements. If the results of any two consecutive subsequent semiannual

performance tests demonstrate compliance with the emission limits the required frequency for NOx and CO testing may change from semiannually to annually.

- Change monitoring frequency of the pressure drop across the catalyst bed from once every 7 days to once every 30 days.

Certification of truth, accuracy, and completeness:

I certify under penalty of law, based on information and belief formed after reasonable inquiry, the statements and information contained in these documents are true, accurate, and complete.

Name (signed): Kourtney Hadrick

Name (typed): Kourtney Hadrick

Date: 4 / 25 / 2019

Should you have any questions or need any additional information, please do not hesitate to contact me at (970)764-6921.

Sincerely,
RED CEDAR GATHERING COMPANY



Kyle Hunderman
Environmental Compliance Specialist II – Air Quality

Cc: SUIT AQP, via email: airquality@southernute-nsn.gov

CONTINUOUS POWER RATINGS: L7044GSI VHP SERIES FOUR

Brake Horsepower (kWb Output)

Model	I.C. Water Inlet Temp. °F (°C) (T _{cra})	C.R.	800 rpm	900 rpm	1000 rpm	1100 rpm	1200 rpm
L7044GSI	130° (54°)	8:1	1120 (836)	1260 (940)	1400 (1044)	1540 (1149)	1680 (1253)

Rating Standard: All models: Ratings are based on ISO 3046/1-1995 with mechanical efficiency of 90% and auxiliary water temperature T_{cra} (clause 10.1) as specified above limited to ± 10° F (± 5° C). Ratings are also valid for SAE J1349, BS5514, DIN6271 and API17B-11C standard atmospheric conditions.

ISO Standard Power/Continuous Power Rating: The highest load and speed which can be applied 24 hours a day, seven days a week, 365 days per year except for normal maintenance. It is permissible to operate the engine at up to 10% overload, or maximum load indicated by the intermittent rating, whichever is lower, for two hours in each 24 hour period.

All natural gas engine ratings are based on a fuel of 900 Btu/ft³ (35.3 MJ/m³) SLHV value, with a 91 Waukesha Knock Index®.

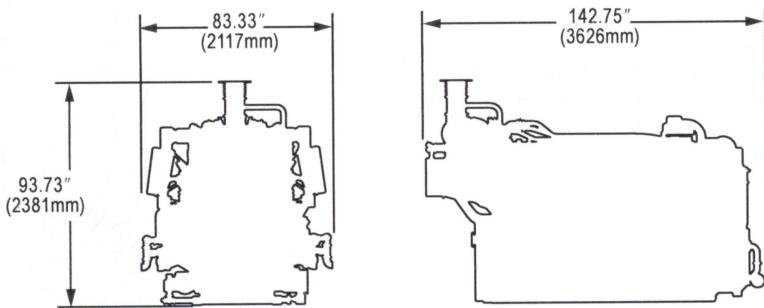
For conditions or fuels other than standard, consult the Waukesha Engine Sales Engineering Department.

PERFORMANCE: L7044GSI VHP SERIES FOUR

English 130° F I.C. Water Temperature		Metric 54° C I.C. Water Temperature	
Pre-Catalyst Settings	RPM	1200	1000
	Power (Bhp)	1680	1400
	BSFC (Btu/bhp-hr)	7780	7685
	NOx (grams/bhp-hr)	12.6	12.1
	CO (grams/bhp-hr)	13.8	12.2
Low Fuel Consumption Settings	NMHC (grams/bhp--hr)	0.36	0.36
	BSFC (Btu/bhp-hr)	7595	7535
	NOx (grams/bhp-hr)	21.3	20.7
	CO (grams/bhp-hr)	1.6	1.6
	NMHC (grams/bhp--hr)	0.30	0.30

NOTES:

- 1) Fuel consumption and exhaust emissions are based on ISO 3046/1-1995 standard reference conditions and commercial quality natural gas of 900 Btu/ft³ (35.38 MJ/m³ [25, V(0; 101.325)]) saturated lower heat value, Waukesha Knock Index® of 91 and 93% methane content by volume. ISO 3046/1-1995 standard reference conditions are 77°F (25°C) ambient temperature, 29.54 inches Hg (100 kPa) barometric pressure, 30% relative humidity (1kPa/0.3 inches Hg water vapor pressure).
- 2) S.I. exhaust emissions are corrected to 5% O₂ (0°C and 101.325 kPa).
- 3) Data will vary due to variations in site conditions. For conditions and/or fuels other than standard, consult the Waukesha Engine Sales Engineering Department.



Waukesha

WAUKESHA ENGINE
DRESSER, INC.
1000 West St. Paul Avenue
Waukesha, WI 53188-4999
Phone: (262) 547-3311 Fax: (262) 549-2795
waukeshaengine.dresser.com

Bulletin 7045 0102

WAUKESHA ENGINE
DRESSER INDUSTRIAL PRODUCTS, B.V.
Farmsumerweg 43, Postbus 330
9900 AH Appingedam, The Netherlands
Phone: (31) 596-652222 Fax: (31) 596-628111

Consult your local Waukesha Distributor for system application assistance. The manufacturer reserves the right to change or modify without notice, the design or equipment specifications as herein set forth without incurring any obligation either with respect to equipment previously sold or in the process of construction except where otherwise specifically guaranteed by the manufacturer.

Waukesha L7042GL Emission Calculations
South Ignacio Central Delivery Point
Red Cedar Gathering Company

Waukesha L7042 GL - Internal Combustion Engine (4SLB)

Units E2 - E4

Manufacturer Unit Rating:	1,480	hp @ 1200rpm
Site Specific Unit Rating ^a :	1,337	hp @ 6,320 ft
BSFC:	7,284	btu/hp-hr
Maximum Heat Input:	9.7	MMBtu/hr
Operating Schedule:	8,760	hr/yr
Maximum Fuel Use ^b :	94.4	mmscf/yr

^a Based on manufacturer's site derate of 2% for every 1,000 ft above 1,500 ft elevation.

^b Based on LHV of:
900 btu/scf

Potential Criteria Pollutant Emissions

Pollutant	Uncontrolled Emissions			
	Emission Factors	Data Source	(lb/hr)	(ton/yr)
NO _x	1.5 g/bhp-hr	Engine Manufacturer	4.42	19.37
CO	2.70 g/bhp-hr	Engine Manufacturer	7.96	34.87
VOC	1.0 g/bhp-hr	Engine Manufacturer	2.95	12.91
PM ₁₀	9.91E-03 lb/MMBtu	AP-42; Table 3.2-2	0.10	0.42
SO ₂	5.88E-04 lb/MMBtu	AP-42; Table 3.2-2	0.01	0.02
CO ₂	110.00 lb/MMBtu	AP-42; Table 3.2-2	1,067.00	4,673.46
Methane	1.25 lb/MMBtu	AP-42; Table 3.2-2	12.13	53.11
CO ₂ e	--	--	--	5,444.15 MT/yr

Hazardous Air Pollutant (HAP) Emissions

Pollutant	Emission Factors ^c	Data Source	Uncontrolled Emissions	
			(lb/hr)	(ton/yr)
1,3-Butadiene	2.67E-04 lb/MMBtu	AP-42; Table 3.2-2	2.59E-03	1.13E-02
2,2,4-Trimethylpentane	2.50E-04 lb/MMBtu	AP-42; Table 3.2-2	2.43E-03	1.06E-02
Acetaldehyde	8.36E-03 lb/MMBtu	AP-42; Table 3.2-2	8.11E-02	0.36
Acrolein	5.14E-03 lb/MMBtu	AP-42; Table 3.2-2	4.99E-02	0.22
Benzene	4.40E-04 lb/MMBtu	AP-42; Table 3.2-2	4.27E-03	1.87E-02
Biphenyl	2.12E-04 lb/MMBtu	AP-42; Table 3.2-2	2.06E-03	9.01E-03
Formaldehyde	5.28E-02 lb/MMBtu	AP-42; Table 3.2-2	5.12E-01	2.24
Methanol	2.50E-03 lb/MMBtu	AP-42; Table 3.2-2	2.43E-02	0.11
n-Hexane	1.11E-03 lb/MMBtu	AP-42; Table 3.2-2	1.08E-02	4.72E-02
Toluene	4.08E-04 lb/MMBtu	AP-42; Table 3.2-2	3.96E-03	1.73E-02
Xylene	1.84E-04 lb/MMBtu	AP-42; Table 3.2-2	1.78E-03	7.82E-03
Total	--		< 0.70	< 3.05

^c Uncontrolled emission factors for 4-stroke, lean-burn (4SLB) engines from GRI-HAPCalc 3.01, based on the highest emission factor between EPA's AP-42, GRI field data and GRI literature data sets.

Waukesha L5794LT Emission Calculations
South Ignacio Central Delivery Point
Red Cedar Gathering Company

Waukesha L5794LT - Internal Combustion Engine (4SLB)

Units E5 - E8

Manufacturer Unit Rating:	1,447 hp @ 1200rpm
Site Specific Unit Rating ^a :	1,401 hp @ 6,320 ft
BSFC:	7,600 btu/hp-hr
Maximum Heat Input:	10.6 MMBtu/hr
Operating Schedule:	8,760 hr/yr
Maximum Fuel Use ^b :	103.6 mmscf/yr

^a Based on manufacturer's site derate of 2.4% for every 1,000 ft above 5,000 ft elevation.

^b Based on LHV of:
900 btu/scf

Potential Criteria Pollutant Emissions

Pollutant	Uncontrolled Emissions			
	Emission Factors	Data Source	(lb/hr)	(ton/yr)
NO _x	2.08 g/bhp-hr	Engine Manufacturer	6.43	28.14
CO	1.84 g/bhp-hr	Engine Manufacturer	5.68	24.90
VOC	0.17 g/bhp-hr	Engine Manufacturer	0.53	2.30
PM ₁₀	9.91E-03 lb/MMBtu	AP-42; Table 3.2-2	0.11	0.46
SO ₂	5.88E-04 lb/MMBtu	AP-42; Table 3.2-2	0.01	0.03
CO ₂	110.00 lb/MMBtu	AP-42; Table 3.2-2	1,171.37	5,130.60
Methane	1.25 lb/MMBtu	AP-42; Table 3.2-2	13.31	58.30
CO ₂ e	--	--	--	5,976.67 MT/yr

Hazardous Air Pollutant (HAP) Emissions

Pollutant	Emission Factors ^c	Data Source	Uncontrolled Emissions	
			(lb/hr)	(ton/yr)
1,3-Butadiene	2.67E-04 lb/MMBtu	AP-42; Table 3.2-2	2.84E-03	1.25E-02
2,2,4-Trimethylpentane	2.50E-04 lb/MMBtu	AP-42; Table 3.2-2	2.66E-03	1.17E-02
Acetaldehyde	8.36E-03 lb/MMBtu	AP-42; Table 3.2-2	8.90E-02	0.39
Acrolein	5.14E-03 lb/MMBtu	AP-42; Table 3.2-2	5.47E-02	0.24
Benzene	4.40E-04 lb/MMBtu	AP-42; Table 3.2-2	4.69E-03	2.05E-02
Biphenyl	2.12E-04 lb/MMBtu	AP-42; Table 3.2-2	2.26E-03	9.89E-03
Formaldehyde	5.28E-02 lb/MMBtu	AP-42; Table 3.2-2	5.62E-01	2.46
Methanol	2.50E-03 lb/MMBtu	AP-42; Table 3.2-2	2.66E-02	0.12
n-Hexane	1.11E-03 lb/MMBtu	AP-42; Table 3.2-2	1.18E-02	5.18E-02
Toluene	4.08E-04 lb/MMBtu	AP-42; Table 3.2-2	4.34E-03	1.90E-02
Xylene	1.84E-04 lb/MMBtu	AP-42; Table 3.2-2	1.96E-03	8.58E-03
Total	--		< 0.76	< 3.34

^c Uncontrolled emission factors for 4-stroke, lean-burn (4SLB) engines from GRI-HAPCalc 3.01, based on the highest emission factor between EPA's AP-42, GRI field data and GRI literature data sets.

Hunderman, Kyle

From: Aaron Countryman <aaron.countryman@wpi.com>
Sent: Friday, March 22, 2019 8:55 AM
To: Hunderman, Kyle
Subject: [EXTERNAL] RE: L5794LT Specs - A few more engines

Yes they do. I am very familiar with your entire engine fleet, and all of your 5794LT's are the same vintage 5794LT w/ESM.



Aaron Countryman
Regional Sales Representative
PH: 505.632.3602
Cell: 505.258.9536
WPI – A Pearce Industries Company
www.wpi.com

Join our new LinkedIn page [Oil & Gas Solutions](#) to receive updates on your mobile device.

From: Hunderman, Kyle [mailto:khunderman@redcedargathering.com]
Sent: Friday, March 22, 2019 6:53 AM
To: Aaron Countryman <aaron.countryman@wpi.com>
Subject: L5794LT Specs - A few more engines

Aaron,

Do the attached L5794LT specs you sent me also apply to the following serial numbers?

C-15026/1
C-15809/1
C-15963/1
C-17235/1

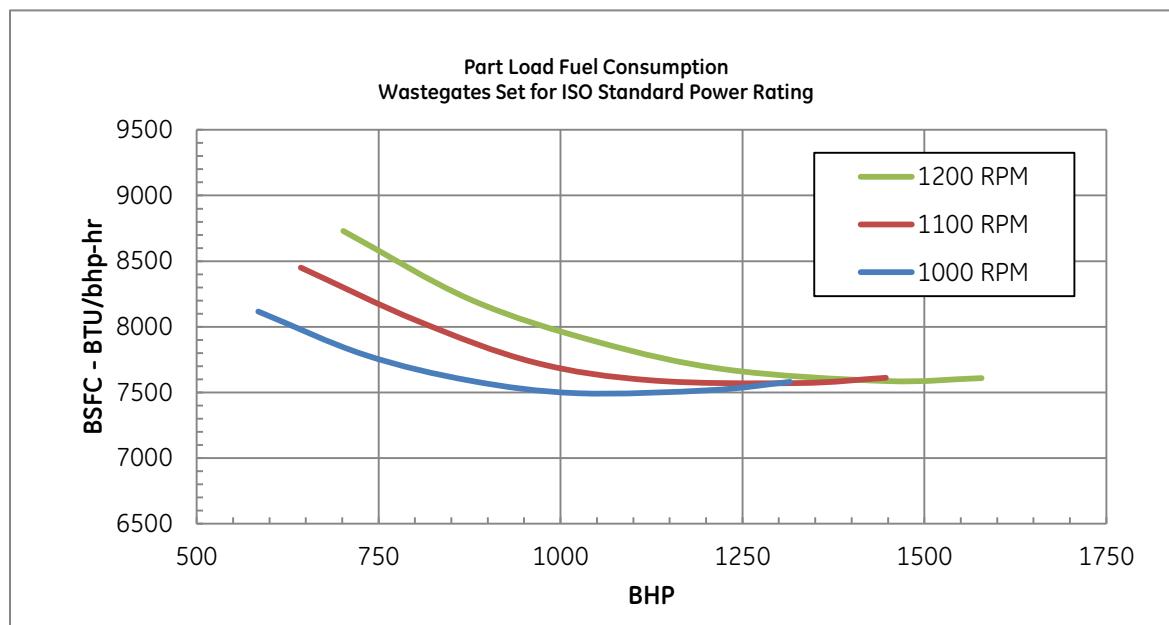
Thanks,

Kyle Hunderman



Environmental Compliance Specialist II – Air Quality
970•764•6921 | office
970•749•9468 | mobile

Engine Ratings and Fuel Consumption
ISO Standard (Continuous) Ratings for Model L5794LT with ESM*
130°F (54°C) Auxiliary Water Temperature



RPM	800	900	1000	1000*	1100	1200
CONTINUOUS BHP	614	954	1206	1272	1326	1447
OVERLOAD BHP	None	None	1315	None	1447	1579

OVERLOAD	Allowed 2 Hours per 24 Hours	
STANDARD CONDITIONS	Barometer 29.54 in. Hg. (100 kPa)	Ambient Temperature 77°F (25°C)
DEDUCTIONS	Altitude: 2.4% per 1000 ft. (305 m) above 5000 ft. (1524 m) Ambient Temperature: 2.4% per 10°F (5.5°C) above 100°F (38°C)	
FUEL	Dry Natural Gas – 900 Btu/ft³ (35.38 MJ/m³) SLHV; 91 WKI* Refer to S-7884-7 for Full Fuel Specification	
EQUIPMENT	Engine Equipped with Lube Oil and Cooling Water Pumps but without Radiator Fan	
ENGINE DATA	Turbocharged & Intercooled with 130°F (54°C) Intercooler Water 10.2:1 Compression Ratio	

NOTES:

1. ISO Standard (continuous) power ratings conform to ISO 3046/1, latest version, with a mechanical efficiency of 90% and auxiliary water temperature, T_{cra}, of 130°F (54°C) limited to ± 10°F (± 5.5°C).
2. Reference Heat Rejection and Operating Data Standard Sheet S-6124-79.
3. Engine set to an exhaust oxygen concentration of 7.8% at ESM ignition timing for 2.25 g/bhp-hr NO_x (0.91 g/nm³ @ 5% O₂).
4. Power generation continuous BHP at 1000 RPM is 1272 BHP @ 7.4% O₂ with no overload allowed.

*Trademark of General Electric Company. All other trademarks are the property of their respective owners.



Engine Ratings & Fuel Consumption Model L5794LT with ESM 130°F (54°C) Auxiliary Water Temperature 180°F (82°C) Jacket Water Temperature	EN: 155598 DATE: 5/13	Ref. C 977-5
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Analysis Certificate

Analysis Requested:

GPA 2286_14

Client:	Red Cedar Gathering	Project #:	95031-0055
Site Name:	South Ignacio	Compensations:	Air & Helium Free
Laboratory ID:	P903003-01	Date Reported:	03-21-19
Sampled by:	K Hunderman	Date Sampled:	02-26-19
Analyzed by:	Irene Yazzie	Date Received:	03-01-19
Sample Pressure:	395.7 psig	Date Analyzed:	03-15-19
Sample Temperature:	86.8 F	Analysis Time:	Std

GPA 2286_14 report

Components	Mol %	Wt %	L.V. %
Helium	BRL	BRL	BRL
Oxygen	BRL	BRL	BRL
Nitrogen	BRL	BRL	BRL
Carbon Dioxide	5.9368	14.7106	5.9590
Methane	93.6937	84.6267	93.4510
Ethane	0.3392	0.5743	0.5310
Propane	0.0215	0.0535	0.0590
Iso-Butane	0.0034	0.0113	BRL
N-Butane	0.0027	0.0090	BRL
Iso-Pentane	BRL	BRL	BRL
N-Pentane	BRL	BRL	BRL
iso-Hexanes	0.0013	0.0064	BRL
Benzene	0.0001	0.0005	BRL
n-Hexane	BRL	BRL	BRL
iso-Heptanes	0.0011	0.0064	BRL
Toluene	BRL	BRL	BRL
n-Heptane	BRL	BRL	BRL
iso-Octanes	0.0002	0.0013	BRL
n-Octane	BRL	BRL	BRL
n-Nonane	BRL	BRL	BRL
iso-Decanes	BRL	BRL	BRL
n-Decane	BRL	BRL	BRL
Totals	100.0000	100.0000	100.0000

BRL = Value below the method reportable limit = 0.0001%

N/R = Parameter not recorded

Analysis Certificate

Analysis Requested:
GPA 2286_14

Client:	Red Cedar Gathering	Project #:	95031-0055
Site Name:	South Ignacio	Compensations:	Air & Helium Free
Laboratory ID:	P903003-01	Date Reported:	03-21-19
Sampled by:	K Hunderman	Date Sampled:	02-26-19
Analyzed by:	Irene Yazzie	Date Received:	03-01-19
Sample Pressure:	395.7 psig	Date Analyzed:	03-15-19
Sample Temperature:	86.8 F	Analysis Time:	Std

GPA 2261_13 Report

Components	Mol %	Wt %	L.V. %
Carbon Dioxide	5.9368	14.7106	5.9590
Hydrogen Sulfide	BRL	BRL	BRL
Nitrogen	BRL	BRL	BRL
Methane	93.6937	84.6267	93.4510
Ethane	0.3392	0.5743	0.5310
Propane	0.0215	0.0535	0.0590
Iso-Butane	0.0034	0.0113	BRL
N-Butane	0.0027	0.0090	BRL
Iso-Pentane	BRL	BRL	BRL
N-Pentane	BRL	BRL	BRL
C6+	0.0027	0.0146	BRL
Helium	BRL	BRL	BRL
Oxygen	BRL	BRL	BRL
Totals	100.0000	100.0000	100.0000

BRL = Value below the method reportable limit = 0.0001%

N/R = Parameter not recorded

Group Reports

Components	Mol %	Wt %	L.V. %
Hexanes	0.0014	0.0069	BRL
Heptanes	0.0011	0.0064	BRL
Octanes	0.0002	0.0013	BRL
Nonanes	BRL	BRL	BRL
Heaviers	BRL	BRL	BRL
Totals	0.0027	0.0146	0.0000
C6+	0.0027	0.0146	BRL
C7+	0.0013	0.0077	BRL
C8+	0.0002	0.0013	BRL
C9+	BRL	BRL	BRL

BRL = Value below the method reportable limit = 0.0001%

N/R = Parameter not recorded

Analysis Certificate

Analysis Requested:
GPA 2286_14

Client:	Red Cedar Gathering	Project #:	95031-0055
Site Name:	South Ignacio	Compensations:	Air & Helium Free
Laboratory ID:	P903003-01	Date Reported:	03-21-19
Sampled by:	K Hunderman	Date Sampled:	02-26-19
Analyzed by:	Irene Yazzie	Date Received:	03-01-19
Sample Pressure:	395.7 psig	Date Analyzed:	03-15-19
Sample Temperature:	86.8 F	Analysis Time:	Std

Glycal Report

Components	Mol %	Wt %	L.V. %
Carbon Dioxide	5.9368	14.7106	5.9590
Hydrogen Sulfide	BRL	BRL	BRL
Nitrogen	BRL	BRL	BRL
Methane	93.6937	84.6267	93.4510
Ethane	0.3392	0.5743	0.5310
Propane	0.0215	0.0535	0.0590
Iso-Butane	0.0034	0.0113	BRL
N-Butane	0.0027	0.0090	BRL
Iso-Pentane	BRL	BRL	BRL
N-Pentane	BRL	BRL	BRL
Cyclopentane	BRL	BRL	BRL
n-Hexane	BRL	BRL	BRL
Cyclohexane	BRL	BRL	BRL
Other Hexanes	0.0013	0.0064	BRL
n-Heptane	BRL	BRL	BRL
Methylcyclohexane	0.0001	0.0006	BRL
2,2,4 Trimethylpentane	BRL	BRL	BRL
Benzene	0.0001	0.0005	BRL
Toluene	BRL	BRL	BRL
EthylBenzene	BRL	BRL	BRL
Xylenes	BRL	BRL	BRL
Heaviers	BRL	BRL	BRL

BRL = Value below the method reportable limit = 0.0001%

N/R = Parameter not recorded

Analysis Certificate

Analysis Requested:
GPA 2286_14

Client:	Red Cedar Gathering	Project #:	95031-0055
Site Name:	South Ignacio	Compensations:	Air & Helium Free
Laboratory ID:	P903003-01	Date Reported:	03-21-19
Sampled by:	K Hunderman	Date Sampled:	02-26-19
Analyzed by:	Irene Yazzie	Date Received:	03-01-19
Sample Pressure:	395.7 psig	Date Analyzed:	03-15-19
Sample Temperature:	86.8 F	Analysis Time:	Std

GPA 2172_09 Report Calculations @ 14.696 psia and 60 degrees F

Compressibility Factor Dry Gas	0.9978	Compressibility Factor Sat Gas	0.9975
GPM C2+	0.099	GPM C3+	0.009
GPM C4+	0.003	GPM C5+	0.001
Ideal Dry Gas Relative Density:	0.613	Ideal Sat Gas Relative Density:	0.603
Real Dry Gas Relative Density:	0.614	Real Sat Gas Relative Density:	0.604
Dry Molecular Weight:	17.761	Sat Molecular Weight:	17.451
Gross HV per Ideal Dry ft3:	953.19	Gross HV per Ideal Sat ft3:	936.56
Gross HV per Real Dry ft3:	955.29	Gross HV per Real Sat ft3:	938.91

C6+ Calculations

Ideal C6+ Dry Relative Density	3.288	C6+ Dry Molecular Weight	95.218
C6+ Compressibility Factor	0.883	C6+ Gross HV per Ideal Dry ft3	5215.5

BRL = Value below the method reportable limit = 0.0001%
N/R = Parameter not recorded


3/21/2019

Analyst

Date

Irene Yazzie

Printed

Comments: 03-21-19 revised per Khunderman.
Note: The above analyses are performed in compliance with GPA 2286_14 quality assurance procedures.
References: GPA 2286_14, TP-17, GPA Standard 2145-09 and GPA Standard 2172-09

GRI-GLYCalc VERSION 4.0 - AGGREGATE CALCULATIONS REPORT

Case Name: South Ignacio - D1 PTE - Feb '19
 File Name: \\durnetapp101\Shared\Durango Shared\EHS\Air Permits\GLYCalc files\South Ignacio\SOU D1 2019 02 PTE (uncontrolled).ddf
 Date: March 27, 2019

DESCRIPTION:

Description: 30 MMscfd dehy unit; Feb '19 gas analysis, max design gas flow, temp, and pressure; max glycol rate (1 Kimray 50015)

Annual Hours of Operation: 8760.0 hours/yr

EMISSIONS REPORTS:

UNCONTROLLED REGENERATOR EMISSIONS

Component	lbs/hr	lbs/day	tons/yr
Methane	0.5159	12.382	2.2596
Ethane	0.0390	0.935	0.1707
Propane	0.0116	0.279	0.0509
Isobutane	0.0046	0.110	0.0200
n-Butane	0.0055	0.132	0.0241
Other Hexanes	0.0089	0.213	0.0388
Methylcyclohexane	0.0066	0.159	0.0289
Benzene	0.0348	0.835	0.1523
Total Emissions	0.6268	15.044	2.7455
Total Hydrocarbon Emissions	0.6268	15.044	2.7455
Total VOC Emissions	0.0719	1.727	0.3151
Total HAP Emissions	0.0348	0.835	0.1523
Total BTEX Emissions	0.0348	0.835	0.1523

FLASH GAS EMISSIONS

Component	lbs/hr	lbs/day	tons/yr
Methane	0.5157	12.377	2.2589
Ethane	0.0100	0.241	0.0440
Propane	0.0013	0.030	0.0055
Isobutane	0.0003	0.007	0.0013
n-Butane	0.0003	0.006	0.0012
Other Hexanes	0.0002	0.005	0.0008
Methylcyclohexane	<0.0001	<0.001	0.0001
Benzene	<0.0001	<0.001	0.0001
Total Emissions	0.5278	12.668	2.3119
Total Hydrocarbon Emissions	0.5278	12.668	2.3119
Total VOC Emissions	0.0021	0.049	0.0090
Total HAP Emissions	<0.0001	<0.001	0.0001
Total BTEX Emissions	<0.0001	<0.001	0.0001

FLASH TANK OFF GAS

Component	lbs/hr	lbs/day	tons/yr
Methane	10.3146	247.549	45.1778
Ethane	0.2010	4.823	0.8802
Propane	0.0251	0.603	0.1100
Isobutane	0.0060	0.145	0.0265
n-Butane	0.0054	0.129	0.0235
Other Hexanes	0.0038	0.092	0.0169
Methylcyclohexane	0.0004	0.009	0.0017
Benzene	0.0003	0.008	0.0014
Total Emissions	10.5566	253.359	46.2379
Total Hydrocarbon Emissions	10.5566	253.359	46.2379
Total VOC Emissions	0.0411	0.986	0.1800
Total HAP Emissions	0.0003	0.008	0.0014
Total BTEX Emissions	0.0003	0.008	0.0014

COMBINED REGENERATOR VENT/FLASH GAS EMISSIONS

Component	lbs/hr	lbs/day	tons/yr
Methane	1.0316	24.759	4.5185
Ethane	0.0490	1.177	0.2147
Propane	0.0129	0.309	0.0564
Isobutane	0.0049	0.117	0.0213
n-Butane	0.0058	0.139	0.0253
Other Hexanes	0.0091	0.217	0.0397
Methylcyclohexane	0.0066	0.159	0.0290
Benzene	0.0348	0.835	0.1524
Total Emissions	1.1546	27.712	5.0574
Total Hydrocarbon Emissions	1.1546	27.712	5.0574
Total VOC Emissions	0.0740	1.776	0.3241
Total HAP Emissions	0.0348	0.835	0.1524
Total BTEX Emissions	0.0348	0.835	0.1524

COMBINED REGENERATOR VENT/FLASH GAS EMISSION CONTROL REPORT:

Component	Uncontrolled tons/yr	Controlled tons/yr	% Reduction
Methane	47.4374	4.5185	90.47
Ethane	1.0509	0.2147	79.57
Propane	0.1609	0.0564	64.93
Isobutane	0.0465	0.0213	54.12
n-Butane	0.0476	0.0253	46.94
Other Hexanes	0.0557	0.0397	28.76
Methylcyclohexane	0.0306	0.0290	5.27
Benzene	0.1538	0.1524	0.89
Total Emissions	48.9834	5.0574	89.68
Total Hydrocarbon Emissions	48.9834	5.0574	89.68
Total VOC Emissions	0.4951	0.3241	34.54
Total HAP Emissions	0.1538	0.1524	0.89
Total BTEX Emissions	0.1538	0.1524	0.89

EQUIPMENT REPORTS:

ABSORBER

NOTE: Because the Calculated Absorber Stages was below the minimum allowed, GRI-GLYCalc has set the number of Absorber Stages to 1.25 and has calculated a revised Dry Gas Dew Point.

Calculated Absorber Stages: 1.25
 Calculated Dry Gas Dew Point: 6.52 lbs. H₂O/MMSCF
 Temperature: 120.0 deg. F
 Pressure: 720.0 psig
 Dry Gas Flow Rate: 30.0000 MMSCF/day
 Glycol Losses with Dry Gas: 0.6375 lb/hr
 Wet Gas Water Content: Saturated
 Calculated Wet Gas Water Content: 131.06 lbs. H₂O/MMSCF
 Calculated Lean Glycol Recirc. Ratio: 3.20 gal/lb H₂O

Component	Remaining in Dry Gas	Absorbed in Glycol
Water	4.96%	95.04%
Carbon Dioxide	99.74%	0.26%
Methane	99.98%	0.02%
Ethane	99.93%	0.07%
Propane	99.88%	0.12%
Isobutane	99.84%	0.16%
n-Butane	99.79%	0.21%
Other Hexanes	99.66%	0.34%
Methylcyclohexane	97.84%	2.16%
Benzene	86.36%	13.64%

FLASH TANK

Flash Control: Combustion device
 Flash Control Efficiency: 95.00 %
 Flash Temperature: 100.0 deg. F
 Flash Pressure: 30.0 psig

Component	Left in Glycol	Removed in Flash Gas
Water	99.98%	0.02%
Carbon Dioxide	42.67%	57.33%
Methane	4.76%	95.24%
Ethane	16.25%	83.75%
Propane	31.66%	68.34%
Isobutane	43.04%	56.96%
n-Butane	50.59%	49.41%
Other Hexanes	70.02%	29.98%
Methylcyclohexane	94.68%	5.32%
Benzene	99.11%	0.89%

REGENERATOR

No Stripping Gas used in regenerator.

Component	Remaining in Glycol	Distilled Overhead
Water	13.03%	86.97%
Carbon Dioxide	0.00%	100.00%
Methane	0.00%	100.00%
Ethane	0.00%	100.00%
Propane	0.00%	100.00%
Isobutane	0.00%	100.00%
n-Butane	0.00%	100.00%
Other Hexanes	1.43%	98.57%
Methylcyclohexane	4.22%	95.78%
Benzene	5.04%	94.96%

STREAM REPORTS:

WET GAS STREAM

Temperature: 120.00 deg. F
 Pressure: 734.70 psia
 Flow Rate: 1.25e+006 scfh

Component	Conc. (vol%)	Loading (lb/hr)
Water	2.76e-001	1.64e+002
Carbon Dioxide	5.92e+000	8.61e+003
Methane	9.34e+001	4.95e+004
Ethane	3.38e-001	3.36e+002
Propane	2.14e-002	3.12e+001
Isobutane	3.39e-003	6.51e+000
n-Butane	2.69e-003	5.17e+000
Other Hexanes	1.30e-003	3.69e+000
Methylcyclohexane	9.97e-005	3.24e-001
Benzene	9.97e-005	2.57e-001
Total Components	100.00	5.87e+004

DRY GAS STREAM

Temperature: 120.00 deg. F
 Pressure: 734.70 psia
 Flow Rate: 1.25e+006 scfh

Component	Conc. (vol%)	Loading (lb/hr)
Water	1.37e-002	8.15e+000
Carbon Dioxide	5.92e+000	8.59e+003
Methane	9.37e+001	4.95e+004
Ethane	3.39e-001	3.36e+002
Propane	2.15e-002	3.12e+001
Isobutane	3.40e-003	6.50e+000
n-Butane	2.69e-003	5.16e+000
Other Hexanes	1.30e-003	3.68e+000
Methylcyclohexane	9.79e-005	3.17e-001
Benzene	8.64e-005	2.22e-001

Methane	6.79e+001	1.03e+001
Ethane	7.06e-001	2.01e-001
Propane	6.02e-002	2.51e-002

Isobutane	1.10e-002	6.04e-003
n-Butane	9.77e-003	5.38e-003
Other Hexanes	4.72e-003	3.85e-003
Methylcyclohexane	4.17e-004	3.88e-004
Benzene	4.46e-004	3.29e-004

Total Components	100.00	2.35e+001
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FLASH TANK GLYCOL STREAM

Temperature: 100.00 deg. F
 Flow Rate: 8.62e+000 gpm

Component	Conc.	Loading
	(wt%)	(lb/hr)
TEG	9.61e+001	4.65e+003
Water	3.71e+000	1.80e+002
Carbon Dioxide	1.99e-001	9.63e+000
Methane	1.07e-002	5.16e-001
Ethane	8.05e-004	3.90e-002
Propane	2.40e-004	1.16e-002
Isobutane	9.43e-005	4.56e-003
n-Butane	1.14e-004	5.50e-003
Other Hexanes	1.86e-004	8.99e-003
Methylcyclohexane	1.42e-004	6.90e-003
Benzene	7.56e-004	3.66e-002
Total Components	100.00	4.84e+003

FLASH GAS EMISSIONS

Flow Rate: 8.34e+002 scfh
 Control Method: Combustion Device
 Control Efficiency: 95.00

Component	Conc.	Loading
	(vol%)	(lb/hr)
Water	5.67e+001	2.24e+001
Carbon Dioxide	4.19e+001	4.05e+001
Methane	1.46e+000	5.16e-001
Ethane	1.52e-002	1.00e-002
Propane	1.29e-003	1.26e-003
Isobutane	2.36e-004	3.02e-004
n-Butane	2.10e-004	2.69e-004
Other Hexanes	1.02e-004	1.92e-004
Methylcyclohexane	8.97e-006	1.94e-005
Benzene	9.59e-006	1.65e-005
Total Components	100.00	6.35e+001

REGENERATOR OVERHEADS STREAM

Temperature: 212.00 deg. F
 Pressure: 14.70 psia
 Flow Rate: 3.39e+003 scfh

Component	Conc. (vol%)	Loading (lb/hr)
Water	9.72e+001	1.56e+002
Carbon Dioxide	2.45e+000	9.63e+000
Methane	3.60e-001	5.16e-001
Ethane	1.45e-002	3.90e-002
Propane	2.96e-003	1.16e-002
Isobutane	8.80e-004	4.56e-003
n-Butane	1.06e-003	5.50e-003
Other Hexanes	1.15e-003	8.87e-003
Methylcyclohexane	7.54e-004	6.60e-003
Benzene	4.99e-003	3.48e-002
Total Components	100.00	1.66e+002

GRI-GLYCalc VERSION 4.0 - SUMMARY OF INPUT VALUES

Case Name: South Ignacio - D1 PTE - Feb '19
 File Name: \\durnetapp101\Shared\Durango Shared\EHS\Air Permits\GLYCalc files\South Ignacio\SOU D1 2019 02 PTE (uncontrolled).ddf
 Date: March 27, 2019

DESCRIPTION:

Description: 30 MMscfd dehy unit; Feb '19 gas analysis,
 max design gas flow, temp, and pressure; max
 glycol rate (1 Kimray 50015)

Annual Hours of Operation: 8760.0 hours/yr

WET GAS:

Temperature: 120.00 deg. F
 Pressure: 720.00 psig
 Wet Gas Water Content: Saturated

Component	Conc. (vol %)
Carbon Dioxide	5.9368
Methane	93.6937
Ethane	0.3392
Propane	0.0215
Isobutane	0.0034
n-Butane	0.0027
Other Hexanes	0.0013
Methylcyclohexane	0.0001
Benzene	0.0001

DRY GAS:

Flow Rate: 30.0 MMSCF/day
 Water Content: 7.0 lbs. H₂O/MMSCF

LEAN GLYCOL:

Glycol Type: TEG
 Water Content: 0.5 wt% H₂O
 Flow Rate: 8.3 gpm

PUMP:

Glycol Pump Type: Electric/Pneumatic

FLASH TANK:

Flash Control: Combustion device
 Flash Control Efficiency: 95.00 %
 Temperature: 100.0 deg. F
 Pressure: 30.0 psig

APPLICATIONS:

- Circulating pump for gas glycol dehydrators, gas amine units and other pumping applications.

FEATURES:

- No Gas Emissions
- No Packing
- Hydraulically Balanced Diaphragms
- Double-ended Shaft
- Stud Extenders for easy Head Installation
- Pulse-Free flow
- Direct or Belt Driven

SPECIFICATIONS:

• Capacity @ max. pressure:	rpm	gpm	l/min
1500 psi (103 bar)	1200	8.3	31.4
• RPM:	1200 max.- 200 min.		
• Inlet			
	250 psi max		
• Connections:			
	Inlet: 1" NPT		
	Outlet: 3/4" NPT		
• Temperature:			
	Max: 250° F (121.1° C)		
	Min: 40° F (4.4° C)		
	[contact factory for temperatures below 40° F (4.4° C)]		
• Fluid End Material, Manifold :	SA395 / SA479		
• Elastomers:	Highly Saturated Nitrile		
• Oil Capacity:	2.75 quarts KIMRAY Part No. 7266		
	2.60 Liters		
• Weight (dry):	100 lbs (45.7 kg)		
• Bi Directional Shaft Rotation			

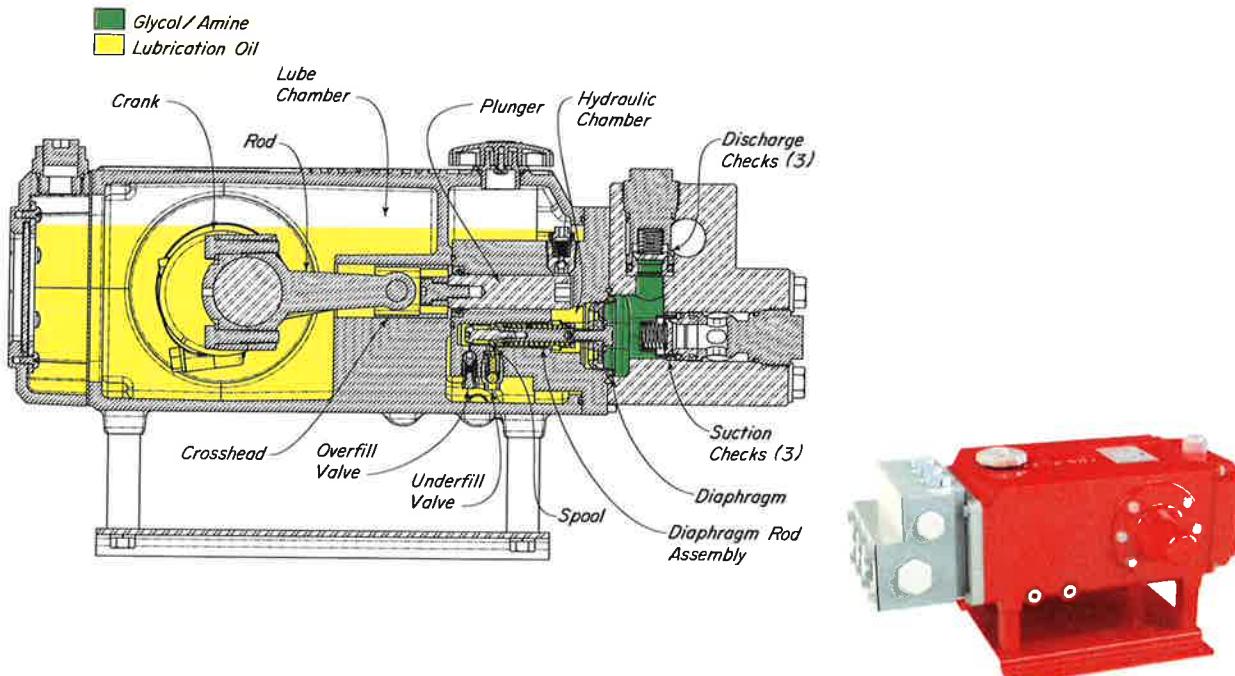
OPERATION:

The KIMRAY ELECTRIC GLYCOL PUMP is a uniquely designed hydraulically balanced diaphragm/plunger positive displacement pump. Power to the pump is provided by a properly sized and specified electric motor either directly connected or belt driven. PLUNGERS are utilized to energize DIAPHRAGMS which in turn pressurize glycol/amine solutions used in gas processing. The Plungers operate and are lubricated in clean oil isolated from the process fluids by DIAPHRAGMS. The DIAPHRAGMS are in contact with the hydraulic oil on one side and the glycol/amine solution and on the other side. KIMZOIL EGP1 is a hydraulic/lubrication oil designed for high end pump performance designed for this application. This design allows for the protection of the reciprocating pumping internals from the process fluids.

As shown in the diagram, the PLUNGER(S) are connected to the CROSSHEAD(s) and displace the oil (YELLOW) in the HYDRAULIC CHAMBER as they reciprocate. As the Plunger moves to the right on the pressure stroke, oil is displaced in the Hydraulic Chamber and forces the DIAPHRAGM(s) to move to the right. The Diaphragm movement displaces the glycol/amine solution (GREEN) on the opposing side of the Diaphragm and forces it through the DISCHARGE CHECK VALVE(s). During the pressure stroke, a small amount of oil (YELLOW) leaks past the clearance between the Plunger and cylinder.

As the Plunger moves back on the suction stroke, the pressure drops in the Hydraulic Chamber and a small amount of oil is drawn in through the UNDER-FILL VALVE to replace the oil lost during the pressure stroke. The position of the Spool Valve regulates how much oil is drawn in. The SPOOL VALVE is positioned by the DIAPHRAGM ROD ASSEMBLY which is connected to the Diaphragm. The cycle then repeats.

When the Diaphragm moves too far forward, the Under-Fill port closes and the Over-Fill port opens. The Under-Fill Valve is a check valve that lets oil in during the suction stroke, but will not allow oil to leave. The OVER-FILL VALVE is a check valve that lets oil out during the pressure stroke, but prevents oil from coming in. The spool valve position opens the port to one of the two valves depending on the need for more or less oil.



Kimray is an ISO 9001-certified manufacturer.

GRI-GLYCalc VERSION 4.0 - AGGREGATE CALCULATIONS REPORT

Case Name: South Ignacio - D2 PTE - Feb '19
 File Name: \\durnetapp101\Shared\Durango Shared\EHS\Air Permits\GLYCalc files\South Ignacio\D2\SOU D2 2019 02.ddf
 Date: March 27, 2019

DESCRIPTION:

Description: 40 MMscfd dehy unit; Feb '19 gas analysis;
 max design gas flow, temp, and pressure; max glycol rate (3-Kimray 20015)

Annual Hours of Operation: 8760.0 hours/yr

EMISSIONS REPORTS:

UNCONTROLLED REGENERATOR EMISSIONS

Component	lbs/hr	lbs/day	tons/yr
Methane	0.8086	19.405	3.5415
Ethane	0.0278	0.668	0.1219
Propane	0.0070	0.167	0.0304
Isobutane	0.0027	0.066	0.0120
n-Butane	0.0033	0.080	0.0146
Other Hexanes	0.0067	0.162	0.0295
Methylcyclohexane	0.0087	0.208	0.0379
Benzene	0.0565	1.355	0.2473
Total Emissions	0.9213	22.111	4.0352
Total Hydrocarbon Emissions	0.9213	22.111	4.0352
Total VOC Emissions	0.0849	2.037	0.3718
Total HAP Emissions	0.0565	1.355	0.2473
Total BTEX Emissions	0.0565	1.355	0.2473

FLASH GAS EMISSIONS

Component	lbs/hr	lbs/day	tons/yr
Methane	5.3786	129.086	23.5582
Ethane	0.0465	1.116	0.2036
Propane	0.0051	0.122	0.0222
Isobutane	0.0012	0.029	0.0053
n-Butane	0.0011	0.026	0.0048
Other Hexanes	0.0010	0.023	0.0043
Methylcyclohexane	0.0002	0.004	0.0007
Benzene	0.0002	0.004	0.0008
Total Emissions	5.4338	130.410	23.7999
Total Hydrocarbon Emissions	5.4338	130.410	23.7999
Total VOC Emissions	0.0087	0.209	0.0381
Total HAP Emissions	0.0002	0.004	0.0008
Total BTEX Emissions	0.0002	0.004	0.0008

FLASH TANK OFF GAS

Component	lbs/hr	lbs/day	tons/yr
Methane	107.5715	2581.716	471.1631
Ethane	0.9297	22.313	4.0721
Propane	0.1015	2.437	0.4447
Isobutane	0.0244	0.585	0.1067
n-Butane	0.0219	0.525	0.0958
Other Hexanes	0.0195	0.469	0.0856
Methylcyclohexane	0.0033	0.078	0.0143
Benzene	0.0036	0.085	0.0156
Total Emissions	108.6753	2608.207	475.9977
Total Hydrocarbon Emissions	108.6753	2608.207	475.9977
Total VOC Emissions	0.1741	4.178	0.7626
Total HAP Emissions	0.0036	0.085	0.0156
Total BTEX Emissions	0.0036	0.085	0.0156

COMBINED REGENERATOR VENT/FLASH GAS EMISSIONS

Component	lbs/hr	lbs/day	tons/yr
Methane	6.1871	148.491	27.0996
Ethane	0.0743	1.784	0.3255
Propane	0.0120	0.289	0.0527
Isobutane	0.0040	0.095	0.0174
n-Butane	0.0044	0.106	0.0194
Other Hexanes	0.0077	0.185	0.0338
Methylcyclohexane	0.0088	0.212	0.0386
Benzene	0.0566	1.359	0.2481
Total Emissions	6.3550	152.521	27.8351
Total Hydrocarbon Emissions	6.3550	152.521	27.8351
Total VOC Emissions	0.0936	2.246	0.4099
Total HAP Emissions	0.0566	1.359	0.2481
Total BTEX Emissions	0.0566	1.359	0.2481

COMBINED REGENERATOR VENT/FLASH GAS EMISSION CONTROL REPORT:

Component	Uncontrolled tons/yr	Controlled tons/yr	% Reduction
Methane	474.7045	27.0996	94.29
Ethane	4.1940	0.3255	92.24
Propane	0.4751	0.0527	88.91
Isobutane	0.1187	0.0174	85.38
n-Butane	0.1104	0.0194	82.42
Other Hexanes	0.1151	0.0338	70.64
Methylcyclohexane	0.0522	0.0386	26.00
Benzene	0.2629	0.2481	5.63
Total Emissions	480.0329	27.8351	94.20
Total Hydrocarbon Emissions	480.0329	27.8351	94.20
Total VOC Emissions	1.1344	0.4099	63.86
Total HAP Emissions	0.2629	0.2481	5.63
Total BTEX Emissions	0.2629	0.2481	5.63

EQUIPMENT REPORTS:

ABSORBER

NOTE: Because the Calculated Absorber Stages was below the minimum allowed, GRI-GLYCalc has set the number of Absorber Stages to 1.25 and has calculated a revised Dry Gas Dew Point.

Calculated Absorber Stages: 1.25
 Calculated Dry Gas Dew Point: 2.49 lbs. H₂O/MMSCF

Temperature: 100.0 deg. F
 Pressure: 720.0 psig
 Dry Gas Flow Rate: 42.0000 MMSCF/day
 Glycol Losses with Dry Gas: 0.3733 lb/hr
 Wet Gas Water Content: Saturated
 Calculated Wet Gas Water Content: 74.99 lbs. H₂O/MMSCF
 Calculated Lean Glycol Recirc. Ratio: 4.72 gal/lb H₂O

Component	Remaining in Dry Gas	Absorbed in Glycol
Water	3.31%	96.69%
Carbon Dioxide	99.74%	0.26%
Methane	99.98%	0.02%
Ethane	99.93%	0.07%
Propane	99.89%	0.11%
Isobutane	99.84%	0.16%
n-Butane	99.79%	0.21%
Other Hexanes	99.63%	0.37%
Methylcyclohexane	97.51%	2.49%
Benzene	83.48%	16.52%

FLASH TANK

Flash Control: Combustion device
 Flash Control Efficiency: 95.00 %
 Flash Temperature: 100.0 deg. F
 Flash Pressure: 30.0 psig

Component	Left in Glycol	Removed in Flash Gas
Water	99.88%	0.12%
Carbon Dioxide	10.00%	90.00%
Methane	0.75%	99.25%
Ethane	2.91%	97.09%
Propane	6.41%	93.59%
Isobutane	10.13%	89.87%
n-Butane	13.24%	86.76%
Other Hexanes	26.19%	73.81%
Methylcyclohexane	73.67%	26.33%
Benzene	94.37%	5.63%

REGENERATOR

No Stripping Gas used in regenerator.

Component	Remaining in Glycol	Distilled Overhead
Water	18.13%	81.87%
Carbon Dioxide	0.00%	100.00%
Methane	0.00%	100.00%
Ethane	0.00%	100.00%
Propane	0.00%	100.00%
Isobutane	0.00%	100.00%
n-Butane	0.00%	100.00%
Other Hexanes	2.80%	97.20%
Methylcyclohexane	5.16%	94.84%
Benzene	5.25%	94.75%

STREAM REPORTS:

WET GAS STREAM

Temperature: 100.00 deg. F
 Pressure: 734.70 psia
 Flow Rate: 1.75e+006 scfh

Component	Conc. (vol%)	Loading (lb/hr)
Water	1.58e-001	1.31e+002
Carbon Dioxide	5.93e+000	1.21e+004
Methane	9.35e+001	6.93e+004
Ethane	3.39e-001	4.71e+002
Propane	2.15e-002	4.37e+001
Isobutane	3.39e-003	9.12e+000
n-Butane	2.70e-003	7.24e+000
Other Hexanes	1.30e-003	5.17e+000
Methylcyclohexane	9.98e-005	4.53e-001
Benzene	9.98e-005	3.60e-001
Total Components	100.00	8.21e+004

DRY GAS STREAM

Temperature: 100.00 deg. F
 Pressure: 734.70 psia
 Flow Rate: 1.75e+006 scfh

Component	Conc. (vol%)	Loading (lb/hr)
Water	5.24e-003	4.36e+000
Carbon Dioxide	5.92e+000	1.20e+004
Methane	9.37e+001	6.93e+004
Ethane	3.39e-001	4.70e+002
Propane	2.15e-002	4.37e+001
Isobutane	3.40e-003	9.10e+000
n-Butane	2.70e-003	7.22e+000
Other Hexanes	1.30e-003	5.15e+000
Methylcyclohexane	9.75e-005	4.42e-001
Benzene	8.35e-005	3.01e-001

Total Components 100.00 8.19e+004

LEAN GLYCOL STREAM

Temperature: 100.00 deg. F
 Flow Rate: 9.99e+000 gpm

Component	Conc. (wt%)	Loading (lb/hr)
TEG	9.95e+001	5.60e+003
Water	5.00e-001	2.82e+001
Carbon Dioxide	5.62e-011	3.16e-009
Methane	7.95e-018	4.48e-016
Ethane	2.62e-009	1.47e-007
Propane	3.50e-011	1.97e-009
Isobutane	7.78e-012	4.38e-010
n-Butane	6.73e-012	3.79e-010
Other Hexanes	3.44e-006	1.94e-004
Methylcyclohexane	8.35e-006	4.70e-004
Benzene	5.56e-005	3.13e-003
Total Components	100.00	5.63e+003

RICH GLYCOL AND PUMP GAS STREAM

Temperature: 100.00 deg. F
 Pressure: 734.70 psia
 Flow Rate: 1.06e+001 gpm
 NOTE: Stream has more than one phase.

Component	Conc. (wt%)	Loading (lb/hr)
TEG	9.47e+001	5.60e+003
Water	2.63e+000	1.55e+002
Carbon Dioxide	8.15e-001	4.82e+001
Methane	1.83e+000	1.08e+002
Ethane	1.62e-002	9.58e-001
Propane	1.83e-003	1.08e-001
Isobutane	4.58e-004	2.71e-002
n-Butane	4.26e-004	2.52e-002
Other Hexanes	4.48e-004	2.65e-002
Methylcyclohexane	2.09e-004	1.24e-002
Benzene	1.07e-003	6.31e-002
Total Components	100.00	5.91e+003

FLASH TANK OFF GAS STREAM

Temperature: 100.00 deg. F
 Pressure: 44.70 psia
 Flow Rate: 2.94e+003 scfh

Component	Conc. (vol%)	Loading (lb/hr)
Water	1.29e-001	1.79e-001
Carbon Dioxide	1.27e+001	4.34e+001

Methane	8.67e+001	1.08e+002
Ethane	4.00e-001	9.30e-001
Propane	2.98e-002	1.02e-001

Isobutane	5.42e-003	2.44e-002
n-Butane	4.86e-003	2.19e-002
Other Hexanes	2.93e-003	1.95e-002
Methylcyclohexane	4.29e-004	3.26e-003
Benzene	5.88e-004	3.55e-003

Total Components	100.00	1.52e+002
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FLASH TANK GLYCOL STREAM

Temperature: 100.00 deg. F
 Flow Rate: 1.03e+001 gpm

Component	Conc.	Loading
	(wt%)	(lb/hr)
TEG	9.72e+001	5.60e+003
Water	2.69e+000	1.55e+002
Carbon Dioxide	8.36e-002	4.82e+000
Methane	1.40e-002	8.09e-001
Ethane	4.83e-004	2.78e-002
Propane	1.21e-004	6.95e-003
Isobutane	4.76e-005	2.74e-003
n-Butane	5.79e-005	3.34e-003
Other Hexanes	1.20e-004	6.93e-003
Methylcyclohexane	1.58e-004	9.12e-003
Benzene	1.03e-003	5.96e-002
Total Components	100.00	5.76e+003

FLASH GAS EMISSIONS

Flow Rate: 7.82e+003 scfh
 Control Method: Combustion Device
 Control Efficiency: 95.00

Component	Conc.	Loading
	(vol%)	(lb/hr)
Water	6.23e+001	2.32e+002
Carbon Dioxide	3.60e+001	3.27e+002
Methane	1.63e+000	5.38e+000
Ethane	7.50e-003	4.65e-002
Propane	5.58e-004	5.08e-003
Isobutane	1.02e-004	1.22e-003
n-Butane	9.12e-005	1.09e-003
Other Hexanes	5.50e-005	9.77e-004
Methylcyclohexane	8.05e-006	1.63e-004
Benzene	1.10e-005	1.78e-004
Total Components	100.00	5.64e+002

REGENERATOR OVERHEADS STREAM

Temperature: 212.00 deg. F
 Pressure: 14.70 psia
 Flow Rate: 2.74e+003 scfh

Component	Conc. (vol%)	Loading (lb/hr)
Water	9.78e+001	1.27e+002
Carbon Dioxide	1.52e+000	4.82e+000
Methane	6.98e-001	8.09e-001
Ethane	1.28e-002	2.78e-002
Propane	2.18e-003	6.95e-003
Isobutane	6.54e-004	2.74e-003
n-Butane	7.95e-004	3.34e-003
Other Hexanes	1.08e-003	6.74e-003
Methylcyclohexane	1.22e-003	8.65e-003
Benzene	1.00e-002	5.65e-002
Total Components	100.00	1.33e+002

GRI-GLYCalc VERSION 4.0 - SUMMARY OF INPUT VALUES

Case Name: South Ignacio - D2 PTE - Feb '19
 File Name: \\durnetapp101\Shared\Durango Shared\EHS\Air Permits\GLYCalc files\South Ignacio\D2\SOU D2 2019 02.ddf
 Date: March 27, 2019

DESCRIPTION:

Description: 40 MMscfd dehy unit; Feb '19 gas analysis;
 max design gas flow, temp, and pressure; max glycol rate (3-Kimray 20015)

Annual Hours of Operation: 8760.0 hours/yr

WET GAS:

Temperature: 100.00 deg. F
 Pressure: 720.00 psig
 Wet Gas Water Content: Saturated

Component	Conc. (vol %)
Carbon Dioxide	5.9368
Methane	93.6937
Ethane	0.3392
Propane	0.0215
Isobutane	0.0034
n-Butane	0.0027
Other Hexanes	0.0013
Methylcyclohexane	0.0001
Benzene	0.0001

DRY GAS:

Flow Rate: 42.0 MMSCF/day
 Water Content: 7.0 lbs. H₂O/MMSCF

LEAN GLYCOL:

Glycol Type: TEG
 Water Content: 0.5 wt% H₂O
 Flow Rate: 10.0 gpm

PUMP:

Glycol Pump Type: Gas Injection
 Gas Injection Pump Volume Ratio: 0.080 acfm gas/gpm glycol

FLASH TANK:

Flash Control: Combustion device
 Flash Control Efficiency: 95.00 %
 Temperature: 100.0 deg. F

Pressure: 30.0 psig

