

Local Applications of Innovative Groundwater Cleanup Using Zero Valent Metals

January 31, 2008

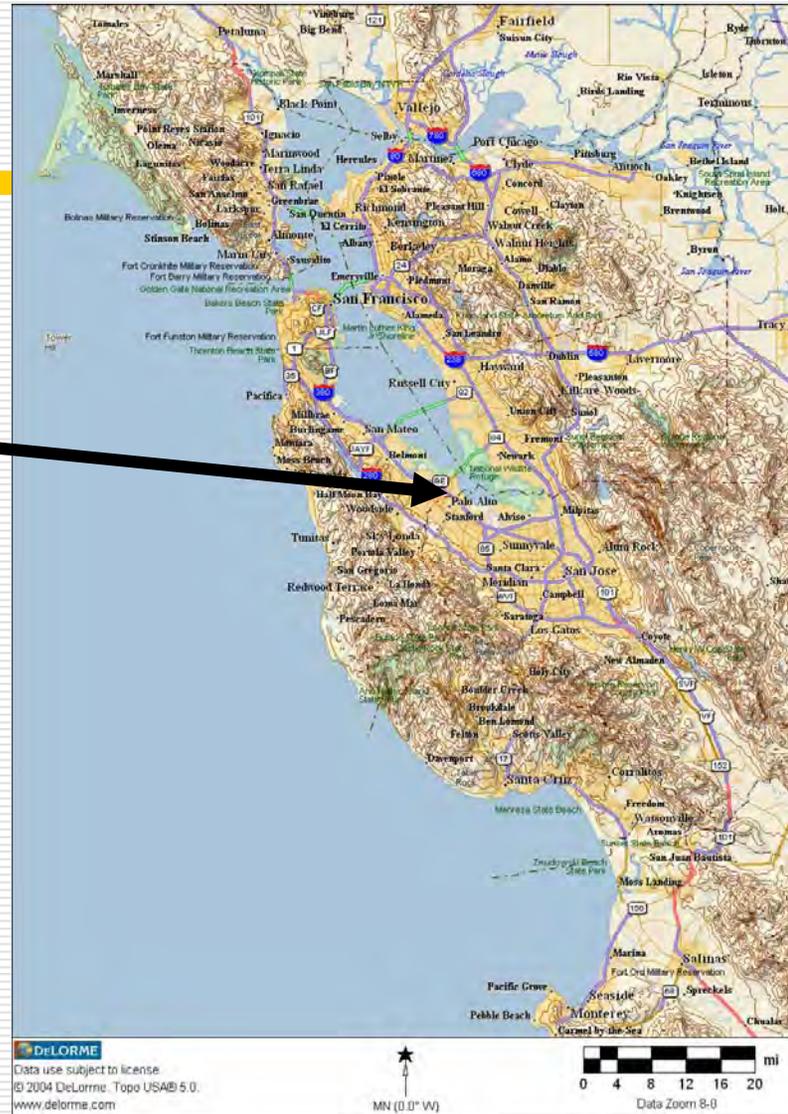
US EPA Region 9

**Lester Feldman, Peggy Peischl
and Peter Bennett**

OUTLINE

1. Site History and Conditions
2. Zero Valent Iron for GW Cleanup
3. Field Preparation and In Situ Testing of ZVI-Pd Nanoparticles in Palo Alto
4. Installation of a Multiple Funnel & Gate PRB in Palo Alto

SITE



PART I: Site History and Conditions

i.e. What drove us to do this?

Site History – 20th Century

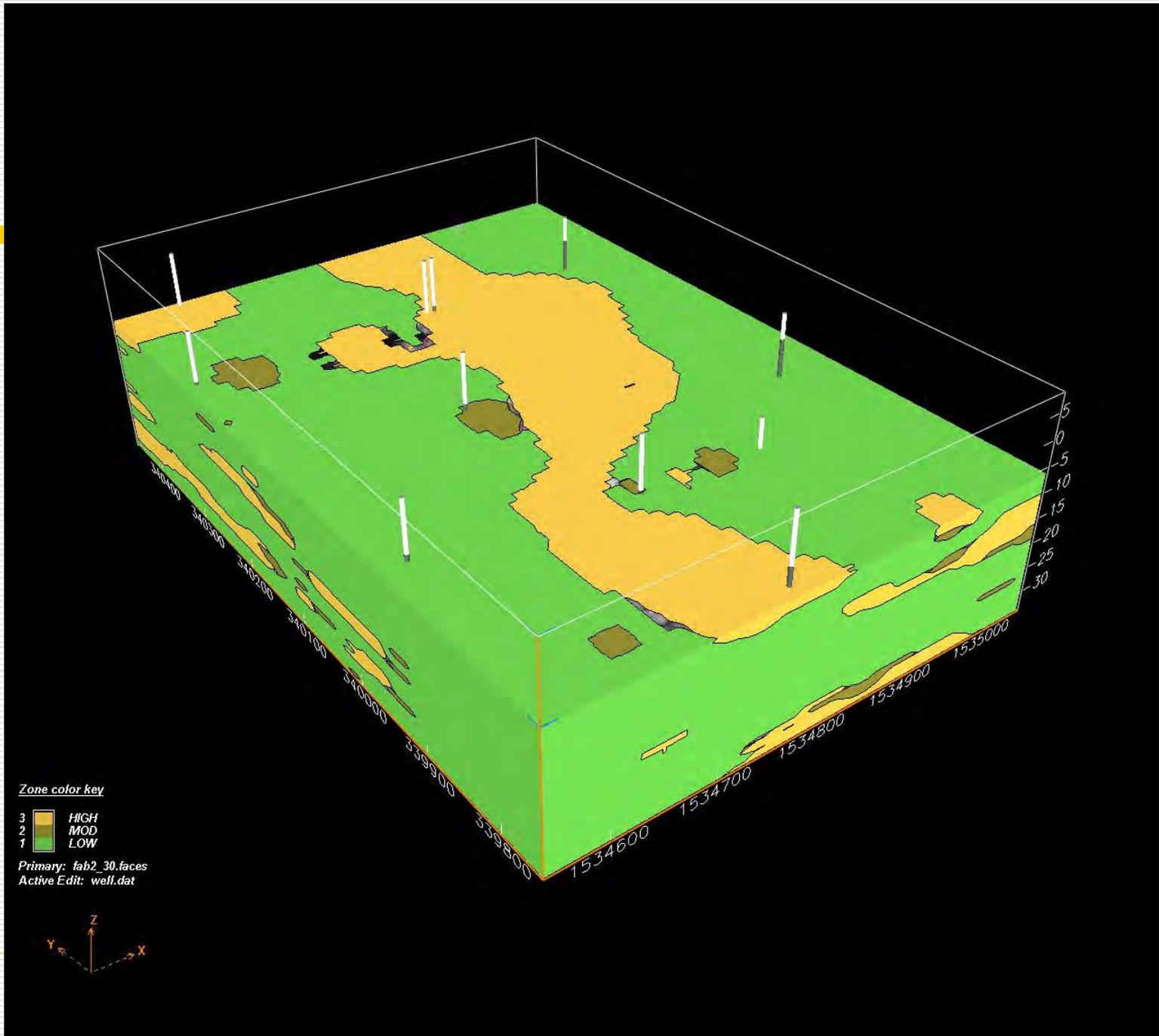
- Aerospace facility operated since the late 1950's
- Surface releases of PCE reportedly occurred along a fence line (weed control?)
- Characterization and GW Monitoring begins in the late 1980's (offsite plumes suspected)
- Soil remediation of source area in the mid-1990's (excavation of >5,000 cy with onsite thermal desorption)
- Dissolved plume contained by building dewatering sump, where discharge is treated and regulated under NPDES (as the IRM)
- Quarterly monitoring continues
- TCE plume arrives at upgradient monitoring well in the mid-90's

Site History – 21st Century

- **2001** – Site is partitioned for redevelopment
- **2004** – GMX conducts first high-resolution investigation (>60 CPT locations, >140 GW samples); offsite plumes mapped, residual onsite source identified
- **2005** – GMX conducts high resolution source area characterization (MIP)
- **2006** – GMX pilot tests remediation technologies (ISB, ZVI, nZVI); Final GW Cleanup Plan submitted; completes “Transect G”
- **2007** – GMX Implements Cleanup Plan (PRB + ISB in the source area)

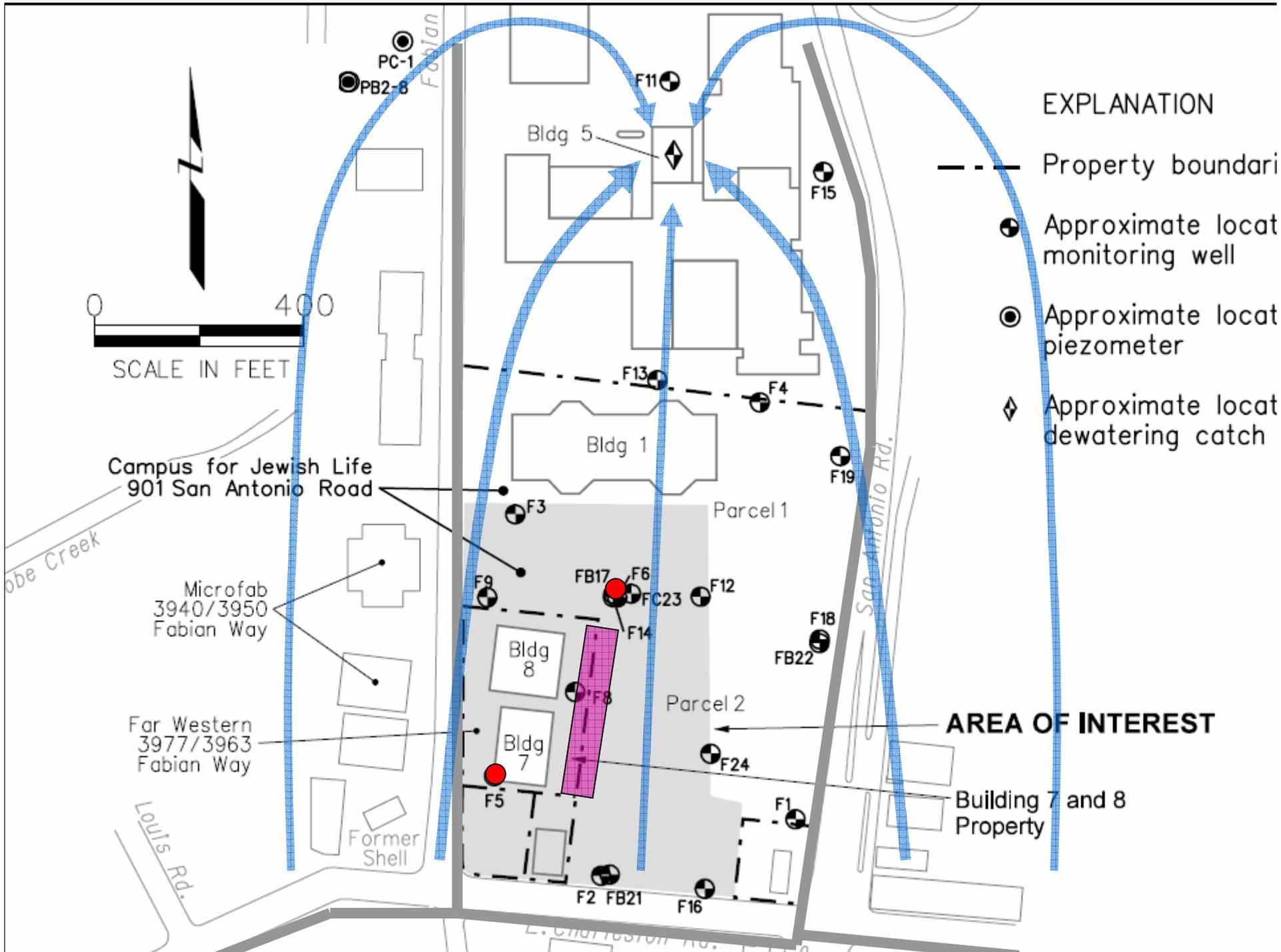
Site Hydrogeology

- Groundwater encountered at 8 to 10 feet below ground surface
- Water table at 6 feet below ground surface under confined conditions
- Complex alluvial environment
 - ▶ Multiple water-bearing units
 - ▶ sand and gravel zones separated by low-permeability clays
- Groundwater flow rates measured with tracer tests vary from 0.4 to 5.1 feet per day
- Groundwater flow direction and VOC migration controlled by ancient buried stream channels



Chemical Distribution

- PCE in source zone up to 26,000 µg/L
- PCE in dissolved plume along northern property line at 850 µg/L from 10 - 60 ft bgs
- Offsite sources impact site, with TCE > 70,000 µg/L, Freon 113 > 1,000 µg/L



EXPLANATION

- Property boundary
- ⊕ Approximate locat monitoring well
- ⊙ Approximate locat piezometer
- ◇ Approximate locat dewatering catch

AREA OF INTEREST

Building 7 and 8 Property

0 400
SCALE IN FEET

Campus for Jewish Life
901 San Antonio Road

Microfab
3940/3950
Fabian Way

Far Western
3977/3963
Fabian Way

Former Shell

Bldg 5

Bldg 1

Bldg 8

Bldg 7

Parcel 1

Parcel 2

Building 7 and 8
Property

L. Childress Rd.

Louis Rd.

Obie Creek

Fabian

San Antonio Rd.

PC-1
PB2-8

F11

F15

F13

F4

F19

F3

F9

FB17

F6

FC23

F12

F14

F18

FB22

F24

F1

F5

F2

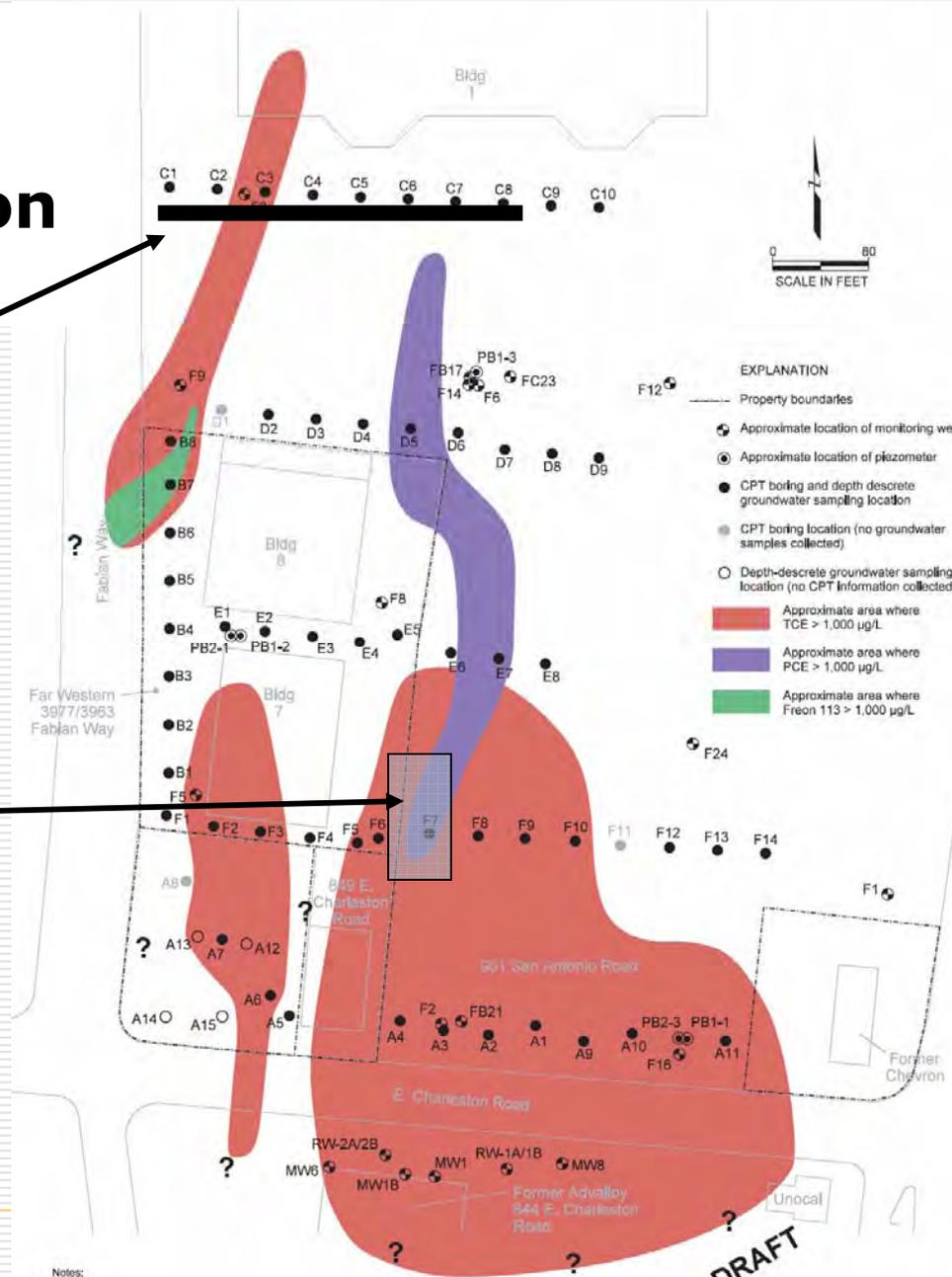
FB21

F16

Characterization Results Drive Remediation Strategy

PRB

in situ source zone remediation



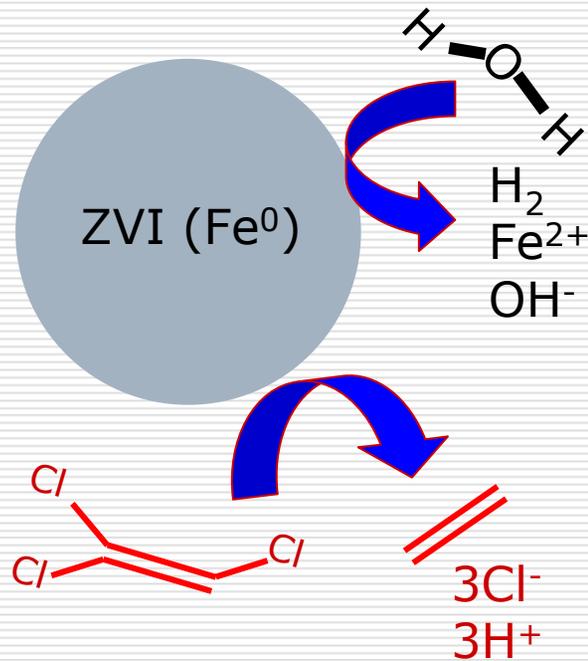
Notes:

DRAFT matrix

PART 2: Treatment of Chlorinated VOCs with ZVI

A passive, low profile, low energy approach for chlorinated solvent sites.

VOC Destruction on ZVI



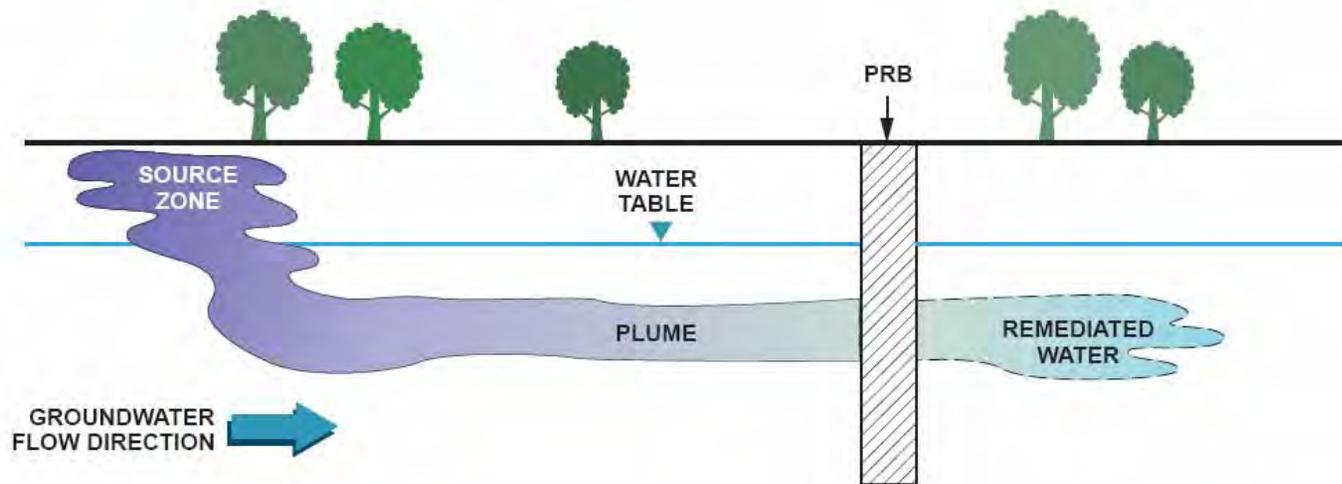
ZVI: TCE half-life = 1 hour

nZVI: TCE half-life < 20 min

**nZVI particles are coated with exotic metals such as palladium to catalyze destruction of contaminants such as TCE*

PRB composed of ZVI:

- Dissolved plume containment with a permeable reactive barrier (PRB)

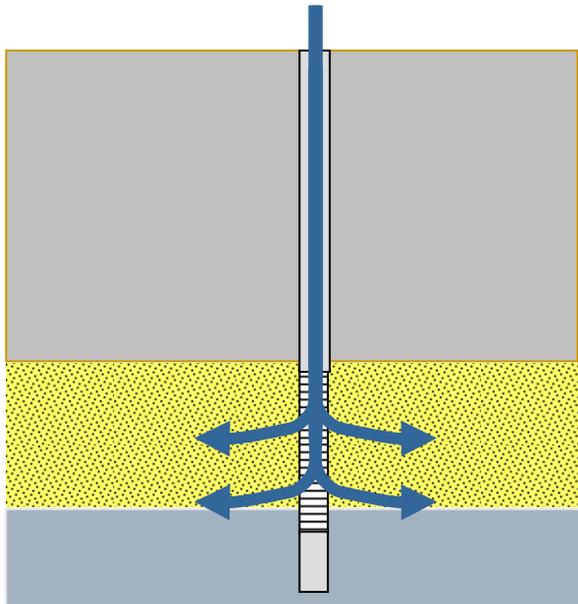


Metallic Nanoparticles for Groundwater Cleanup

- 1 to 100 nanometers in diameter
- Usually formed by precipitation from metallic ions
- Small = fast reaction rates (good catalysts)
- Small = effective delivery to natural systems

Source Treatment with nZVI:

- nZVI particles are injected into a well and transported through the source area by advection



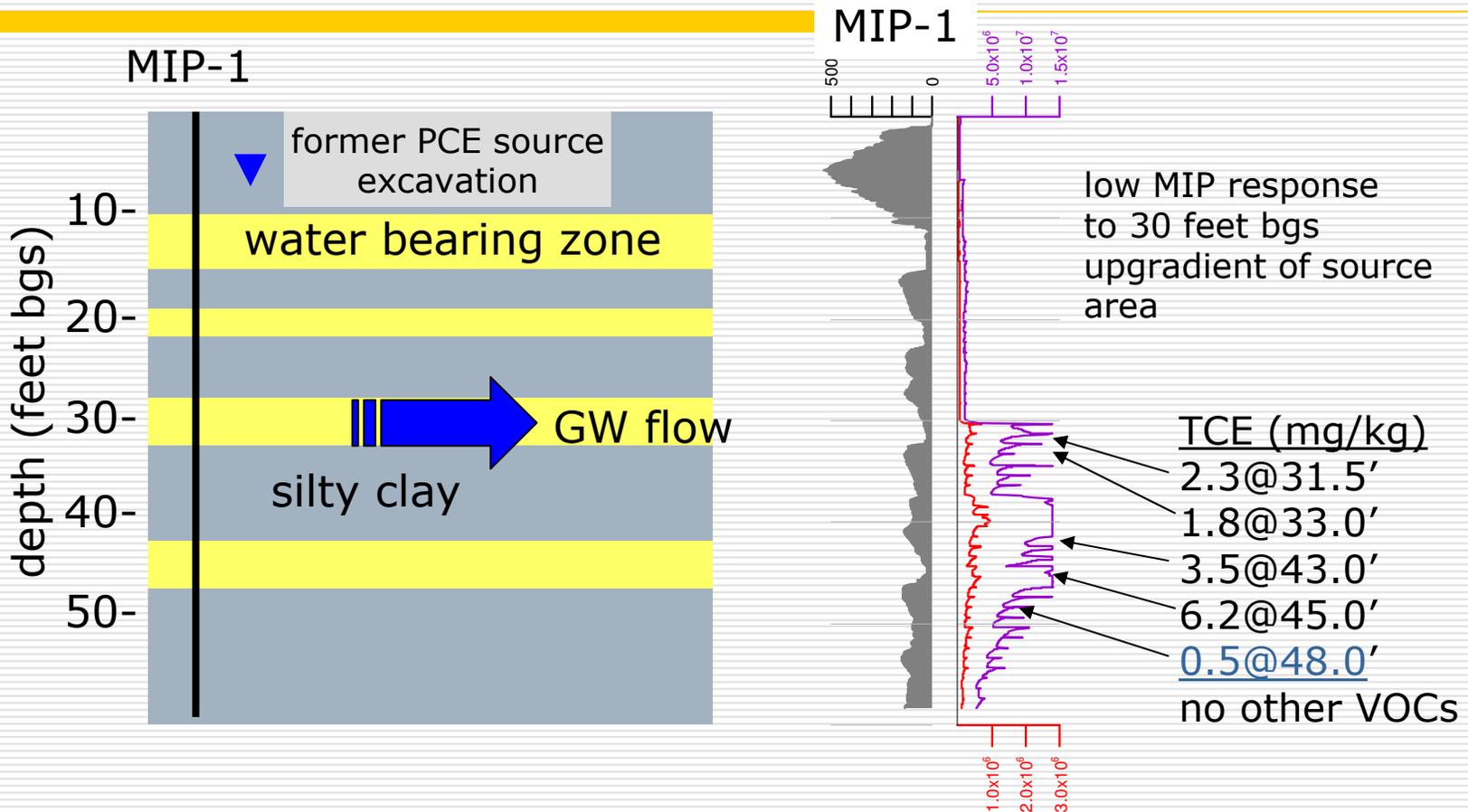
Big Picture Questions on metallic nanoparticles (nZVI)

1. Delivery?
 2. Reactive Lifetime?
 3. Dose (i.e. suspension concentration)?
 4. Cost of Cleanup?
- *Assuming \$50 per pound, 1 g Fe/L, cost for treating 1 cy = \$21 (materials costs only)*

PART 3: Onsite Preparation and Field Testing of Reactive Metal Nanoparticles

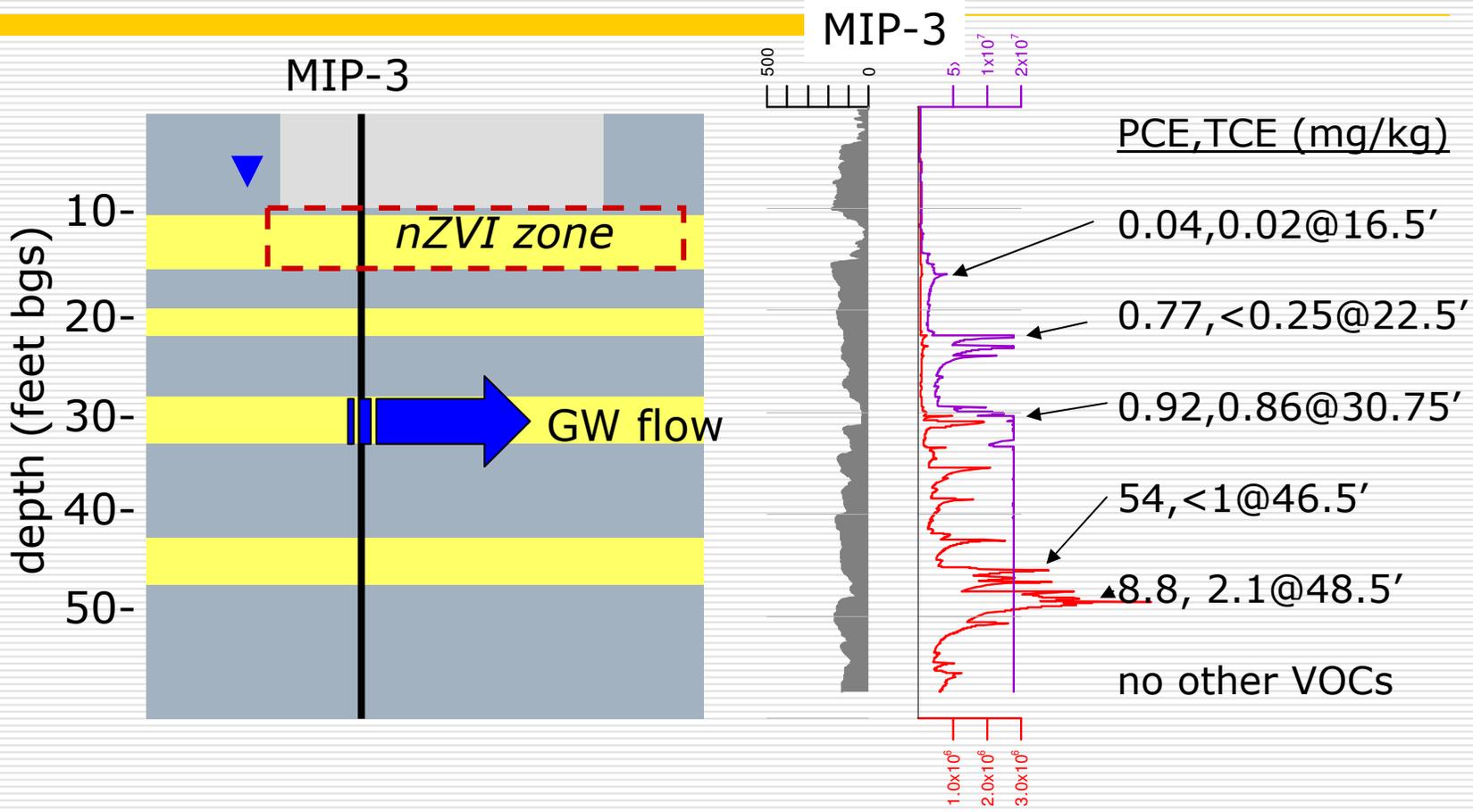
Fun with exotic chemicals...

Source Area: Upgradient Plume



This MIP profile indicated the location of an offsite TCE plume

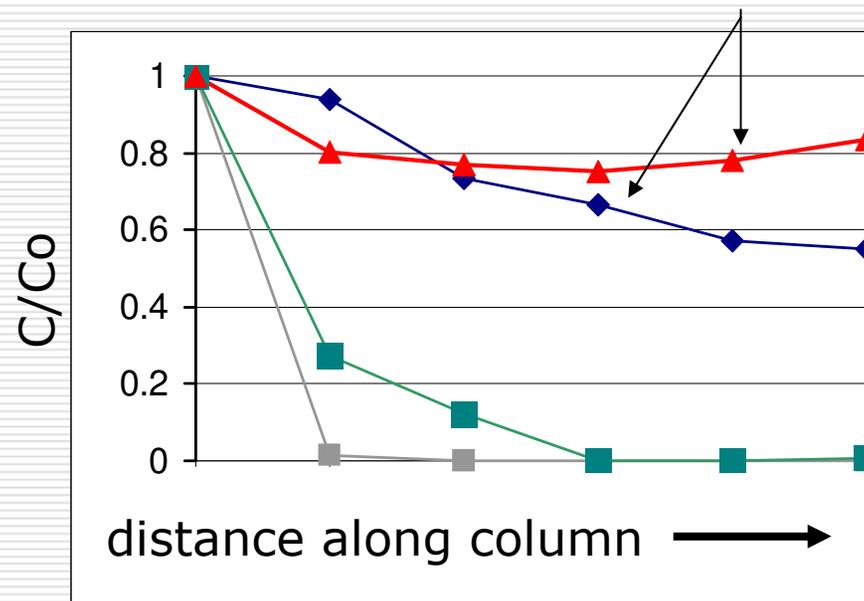
Source Area: Commingled Release



Nano-Scale Iron Column Tests

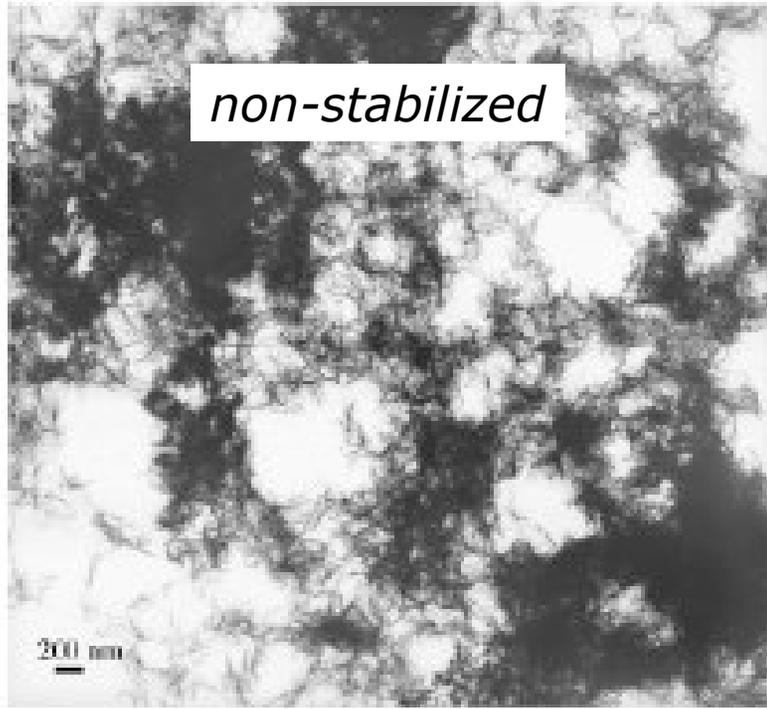


“starch-stabilized” nano iron

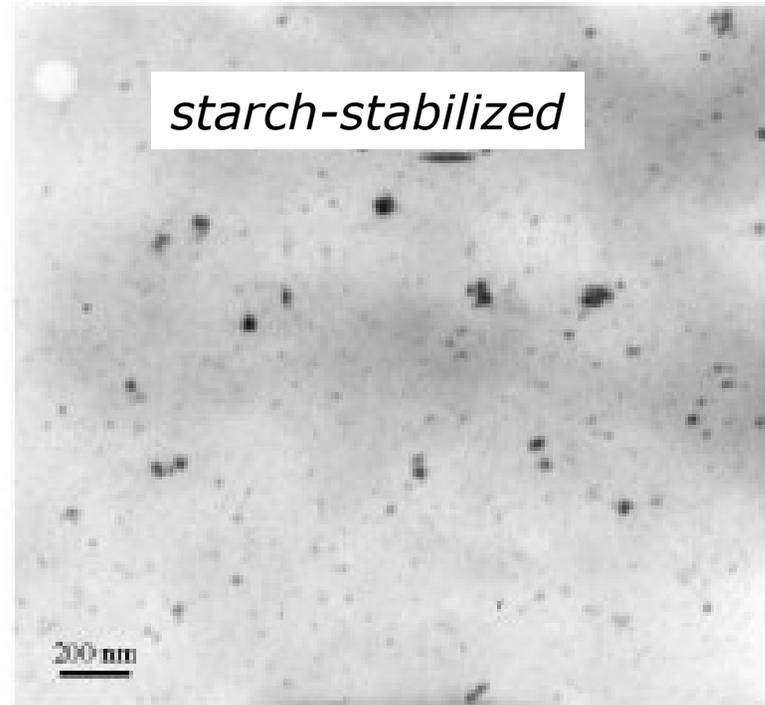


Starch-Stabilized nZVI Particles

(a)



(b)



Feng He and Dongye Zhao, 2005. Preparation and Characterization of a New Class of Starch-Stabilized Bimetallic Nanoparticles for Degradation of Chlorinated Hydrocarbons in Water, *Environ. Sci. Technol.*, 39, 3314-3320.

Our Specific Objectives

- Prepare “starch-stabilized” nZVI particles in suspensions of sufficient volume for field testing
- Assess *in situ* transport and reactivity of nZVI particles by a series of Push-Pull Tests

Synthesis of nZVI:

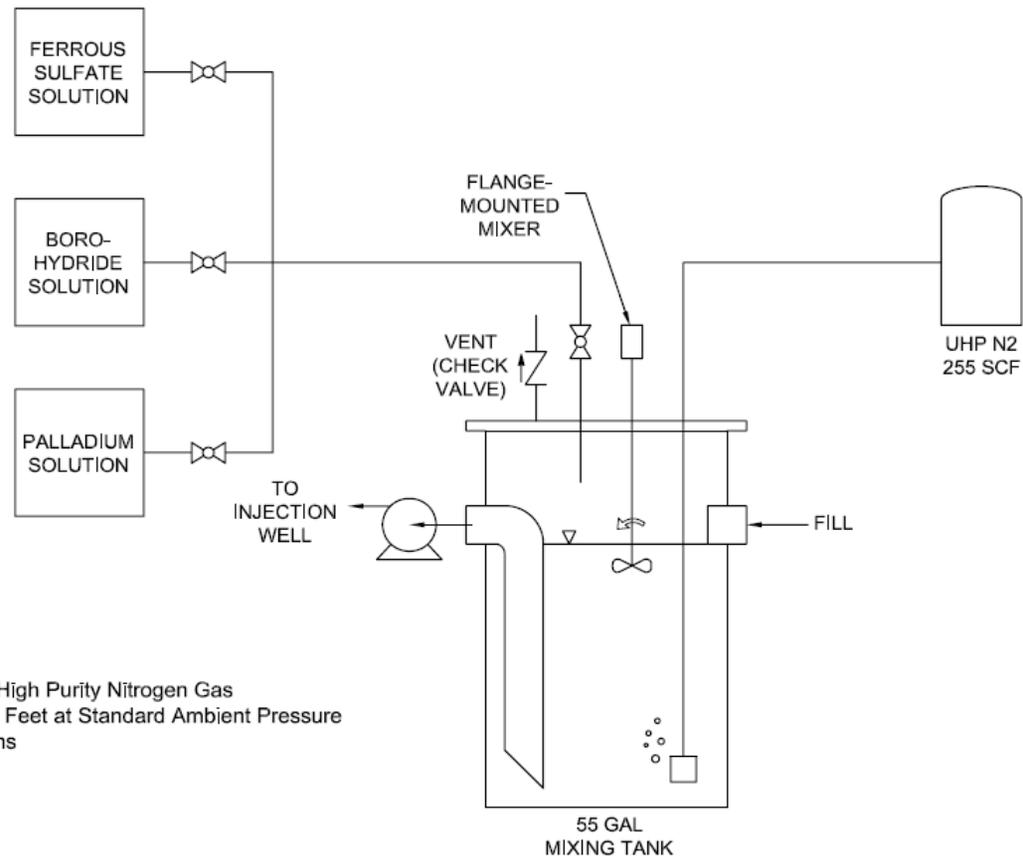
1. Prepare Starch (CMC 90K) and Ferrous Iron solution (remove O₂)
2. Reduce Ferrous Iron with Borohydride



3. Coat nZVI particles with Palladium Metal



3. Field Batch Reactor



NOTES:
UHP N2 = Ultra High Purity Nitrogen Gas
SCF = Cubic Feet at Standard Ambient Pressure
GAL = Gallons

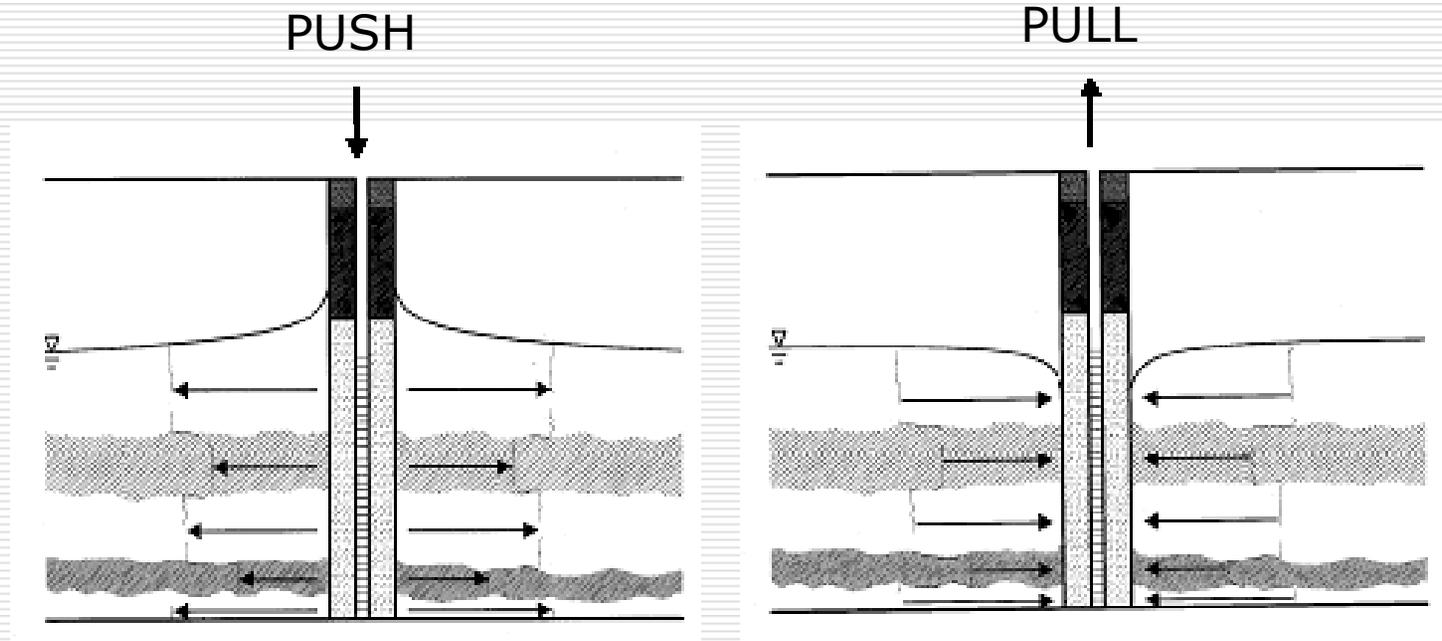




Summary of nZVI batches

Reagent	Units	Test Batches		
		PPT-2	PPT-3	PPT-4
Volume	L	117	113	329
Starch - NaCMC (90K)	Wt%	0.82	0.40	0.29
Iron	mg/L	962	207	345
Borohydride (as B)	mg/L	371	80	136
Palladium (as Pd)	mg/L	0	0	0.329
Sodium Bromide – as Br	mg/L	285	284	140

Push-Pull Tests



FIGURES FROM OREGON STATE UNIVERSITY WEBSITE.

Injection Wellhead



Push-Pull Tests

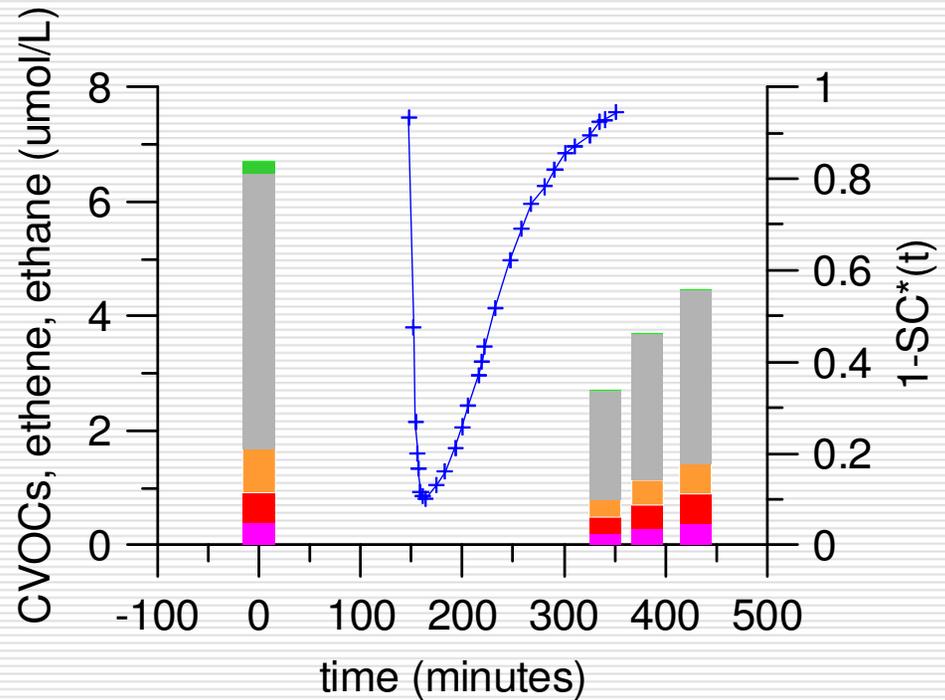
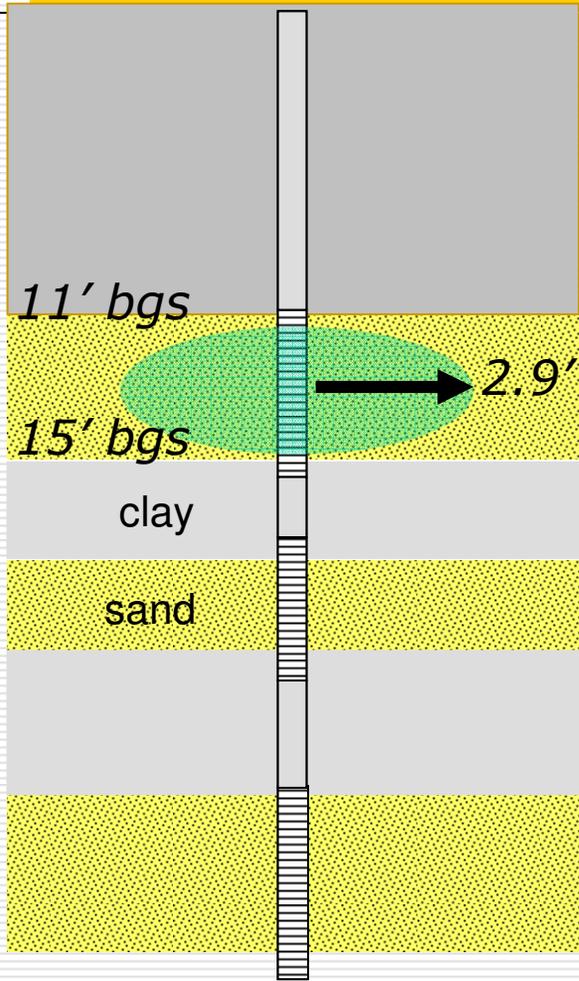


$$V_{inj} = 699 + 53 \text{ L}, V_{ext} = 1,440 \text{ L}, V_{ext}/V_{inj} = 1.9$$

Push-Pull Test #1

Tap Water Injection

$$SC^*(t) = \frac{SC_t - SC_{gw}}{SC_{inj} - SC_{gw}}$$

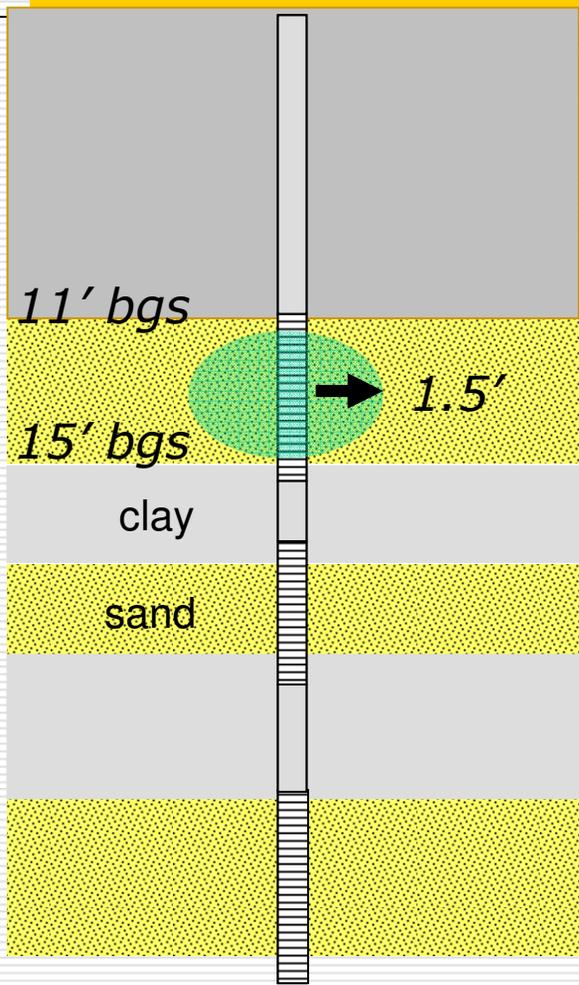


PCE TCE cDCE VC ETHENE 1-SC*(t)

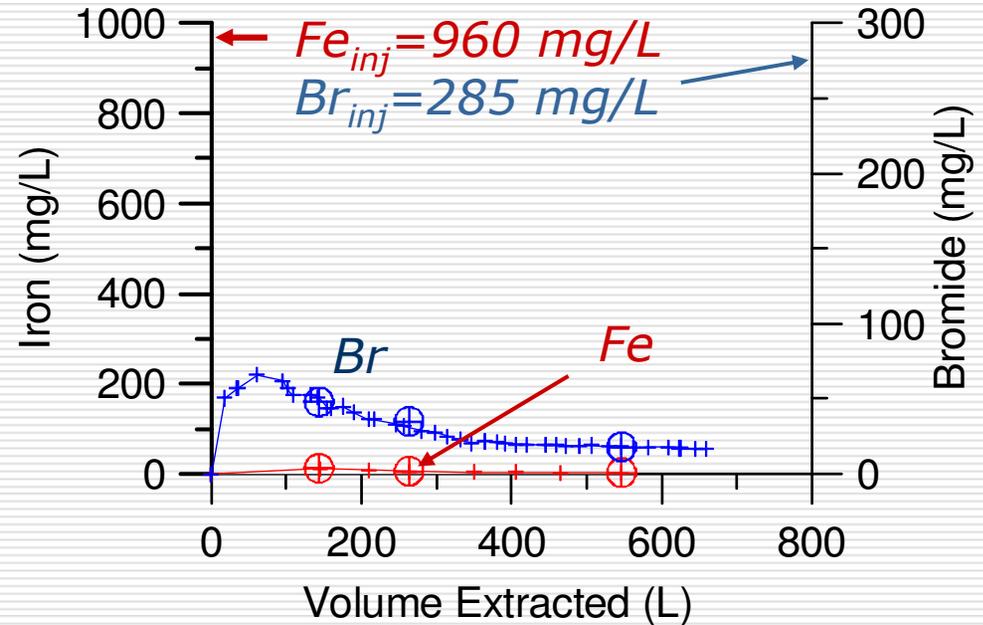
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Push-Pull Test #2

nZVI (960 mg/L), 13 hr between injection & extraction



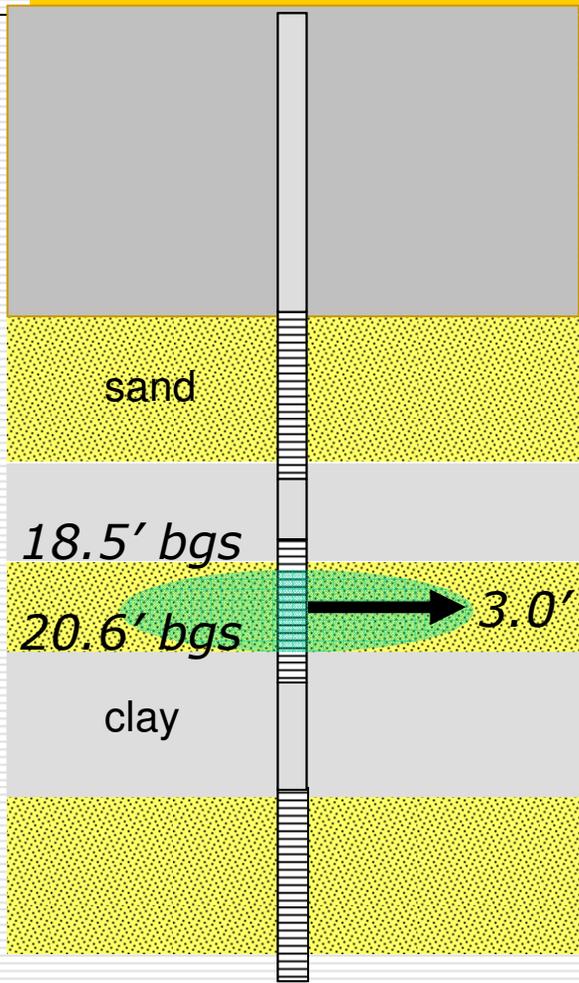
$$V_{inj} = 117 + 111 \text{ L}, V_{ext} = 659 \text{ L}, V_{ext}/V_{inj} = 2.9$$



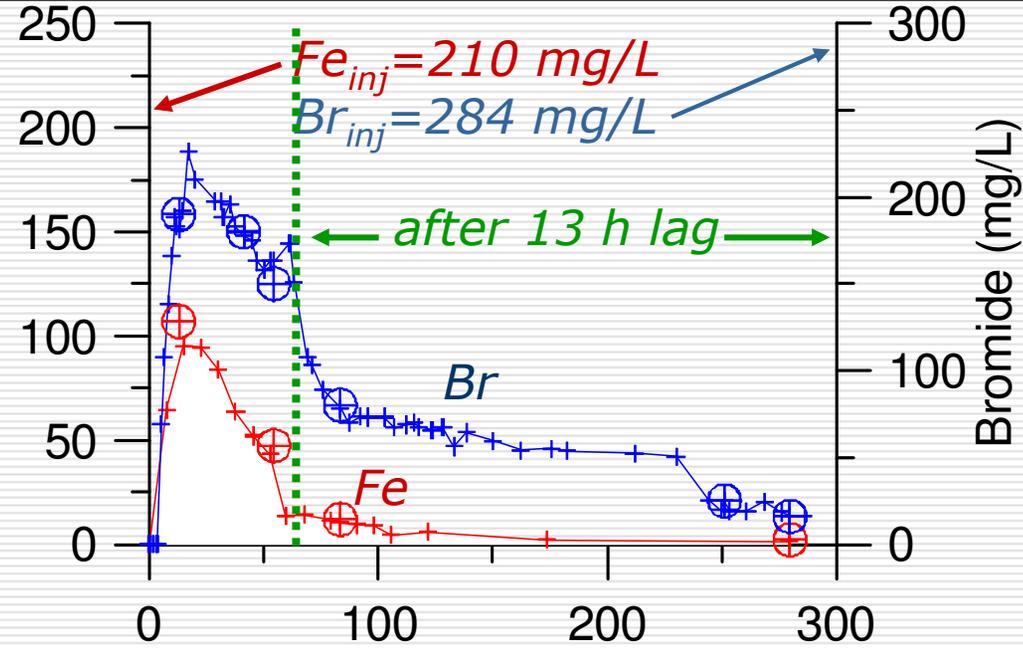
***recovered 61% of injected Br, but only 2.6% of injected Fe**

Push-Pull Test #3

nZVI (210 mg/L), 13 hr lag after extracting 60 L



$$V_{inj} = 113 + 19 L, V_{ext} = 286 L, V_{ext}/V_{inj} = 3.0$$

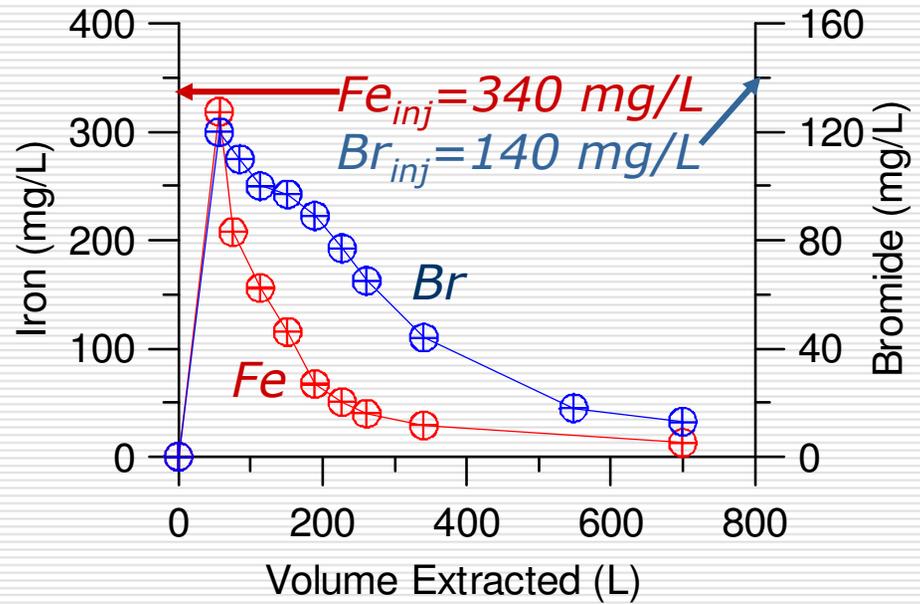
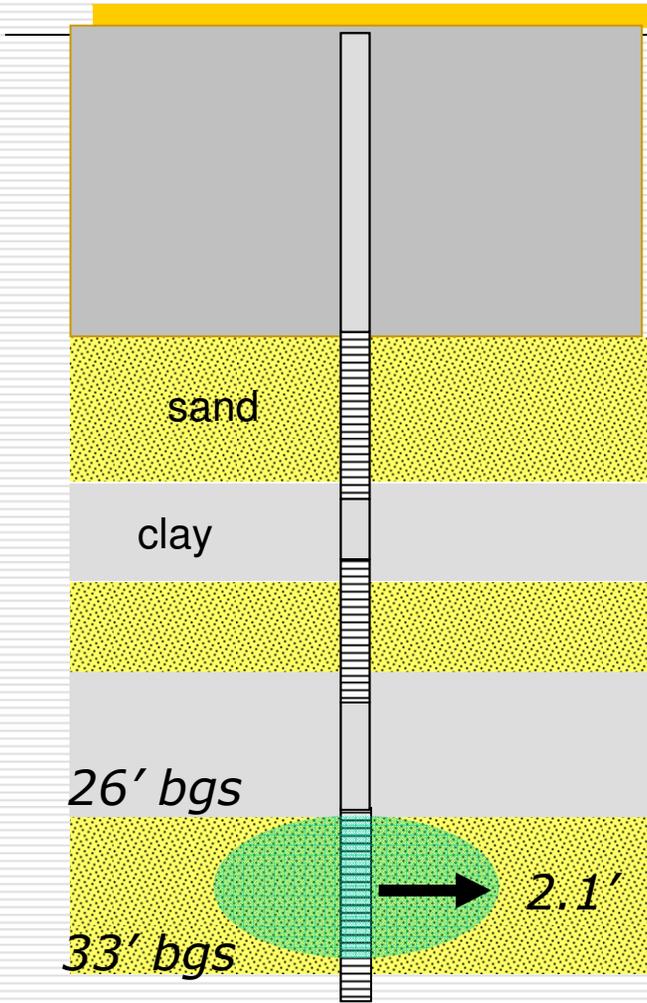


***recovered 73% of injected Br and 21% of injected Fe (all extracted pre-lag)**

Push-Pull Test #4

nZVI (340 mg/L), no lag time

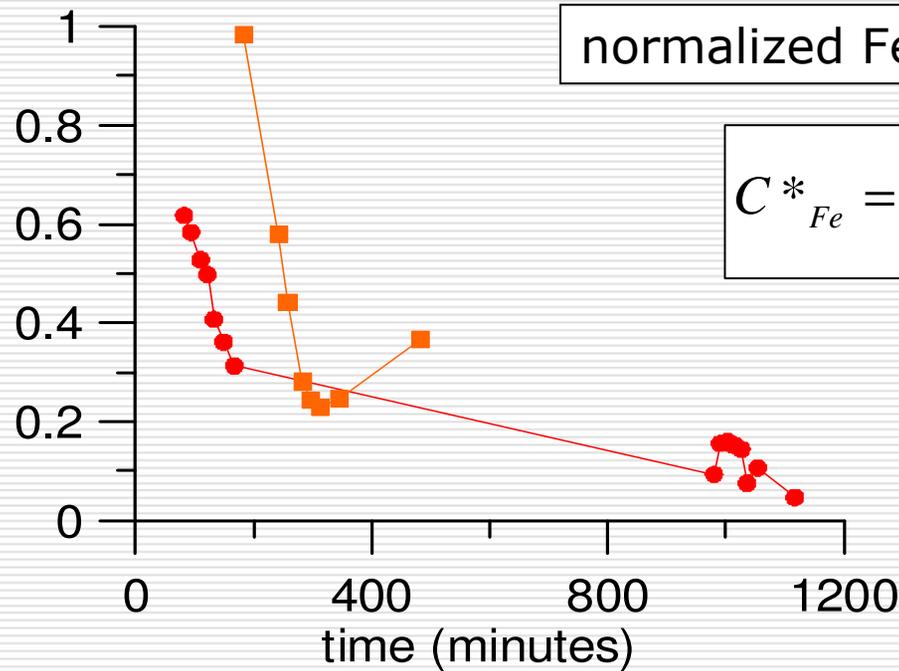
$$V_{inj} = 329 + 40 \text{ L}, V_{ext} = 756 \text{ L}, V_{ext}/V_{inj} = 2.0$$



***recovered 76% of injected Br and 31% of injected Fe (best recovery of 3 PP tests)**

Push-Pull Tests #3 & #4

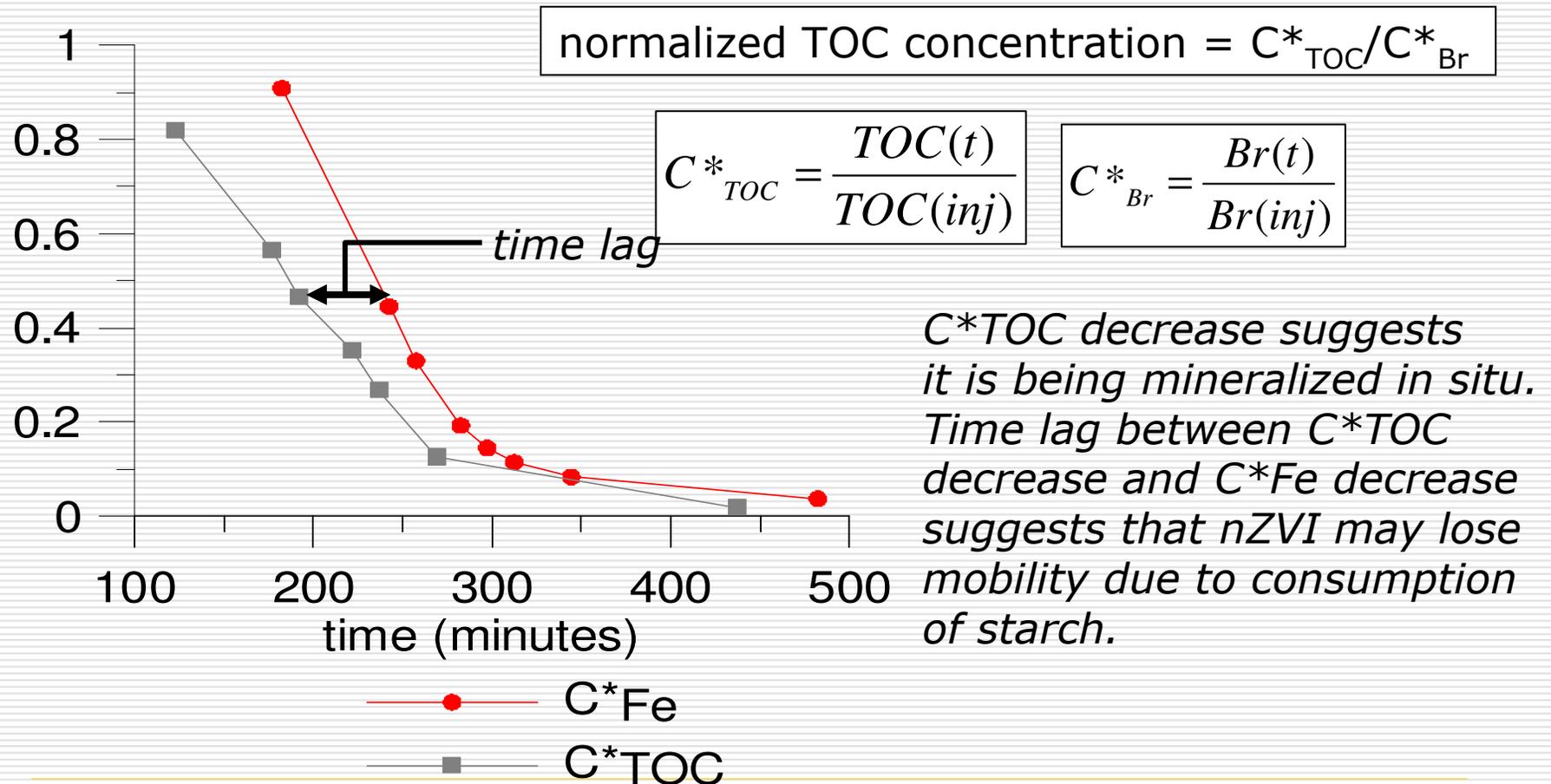
Decrease in iron mobility with time



—●— PPT-3
—■— PPT-4

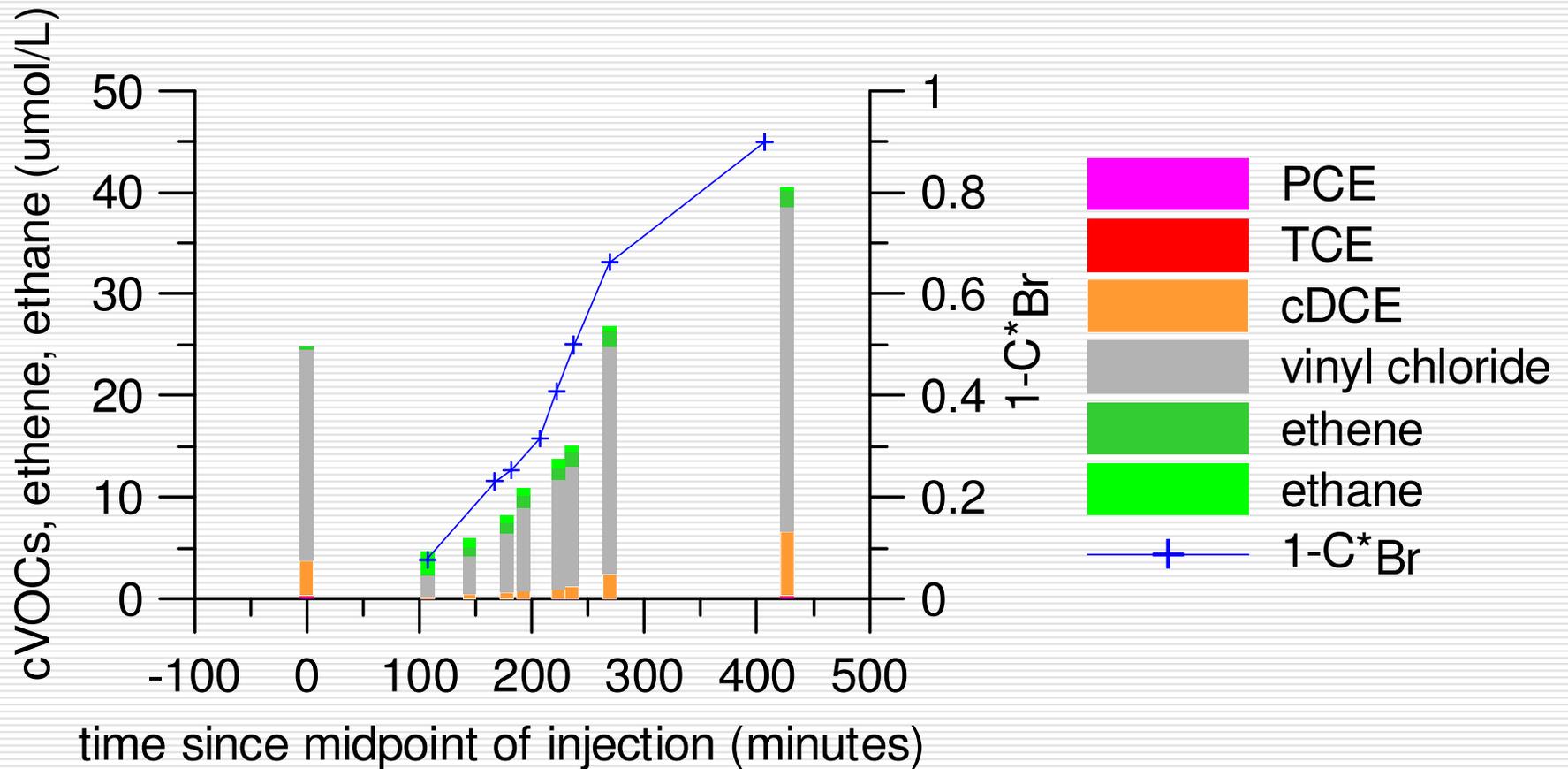
Push-Pull Test#4

Starch degradation as a potential explanation for loss of nZVI mobility



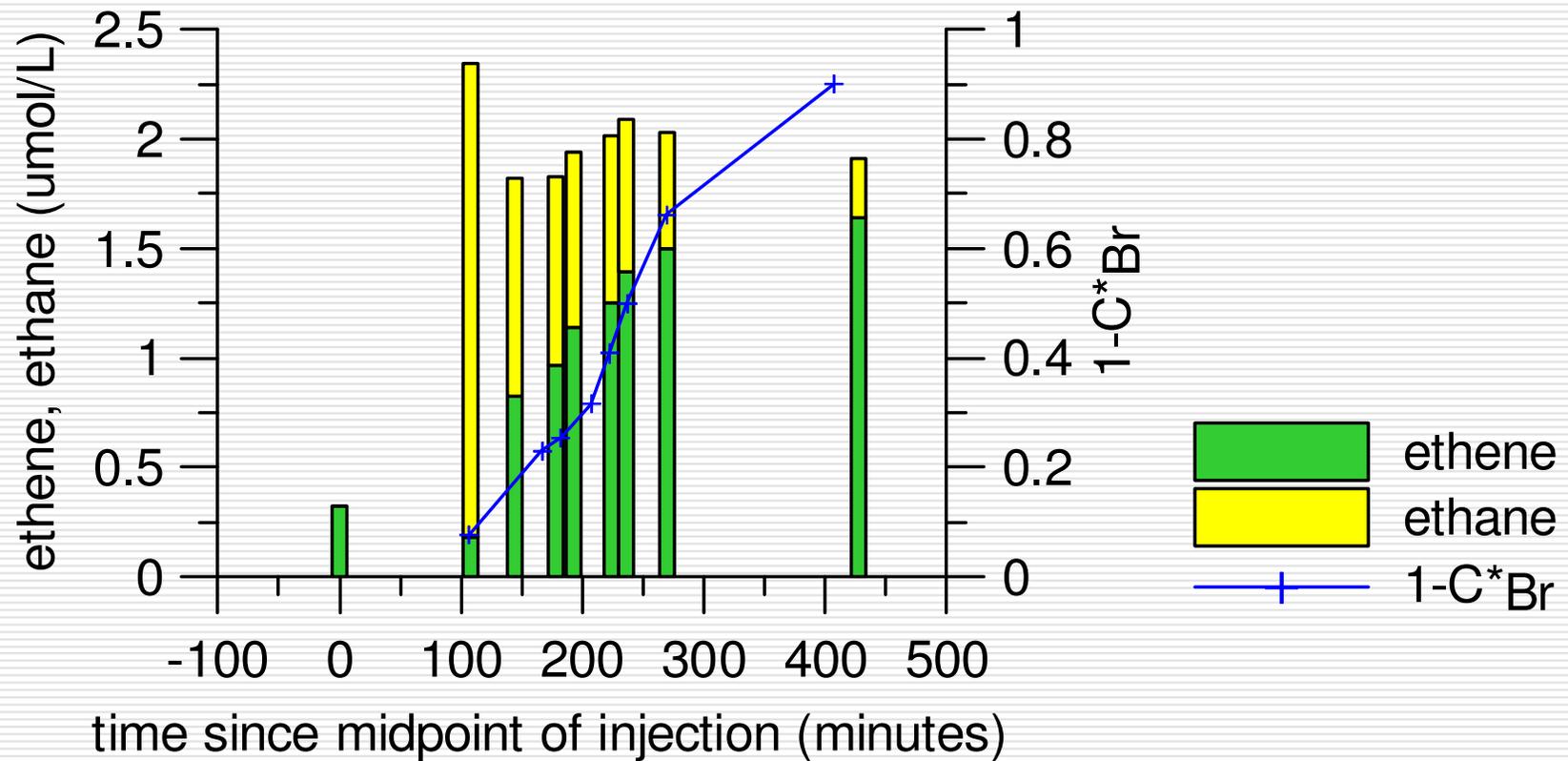
Push-Pull Test #4

Reactivity Assessment



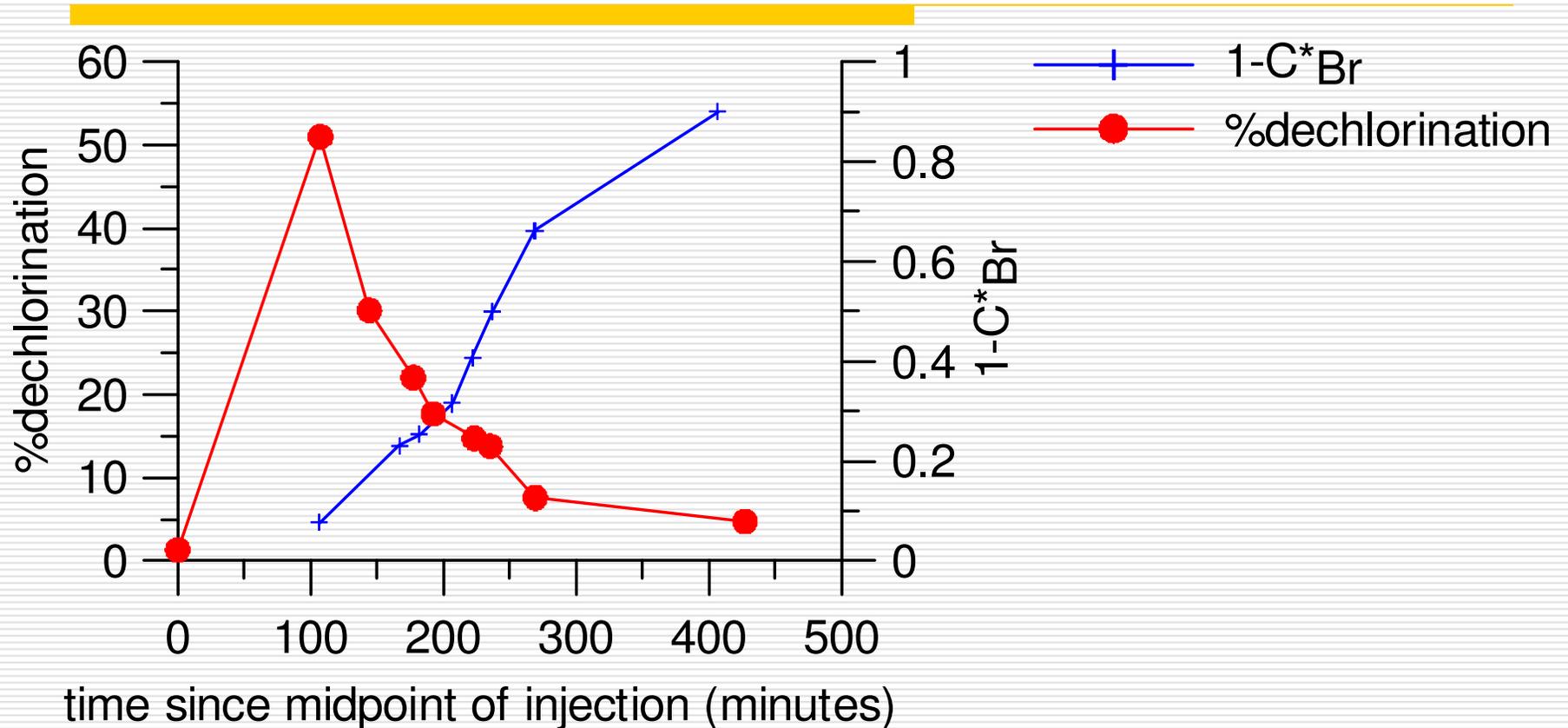
Push-Pull Test #4

Ethane and Ethene Production



Push-Pull Test #4

%Dechlorination of CVOCs in extracted water samples



$$\%dechlorination = \frac{[ethene] + [ethane]}{[PCE] + [TCE] + [cDCE] + [VC] + [ethene] + [ethane]} \times 100\%$$

Conclusions

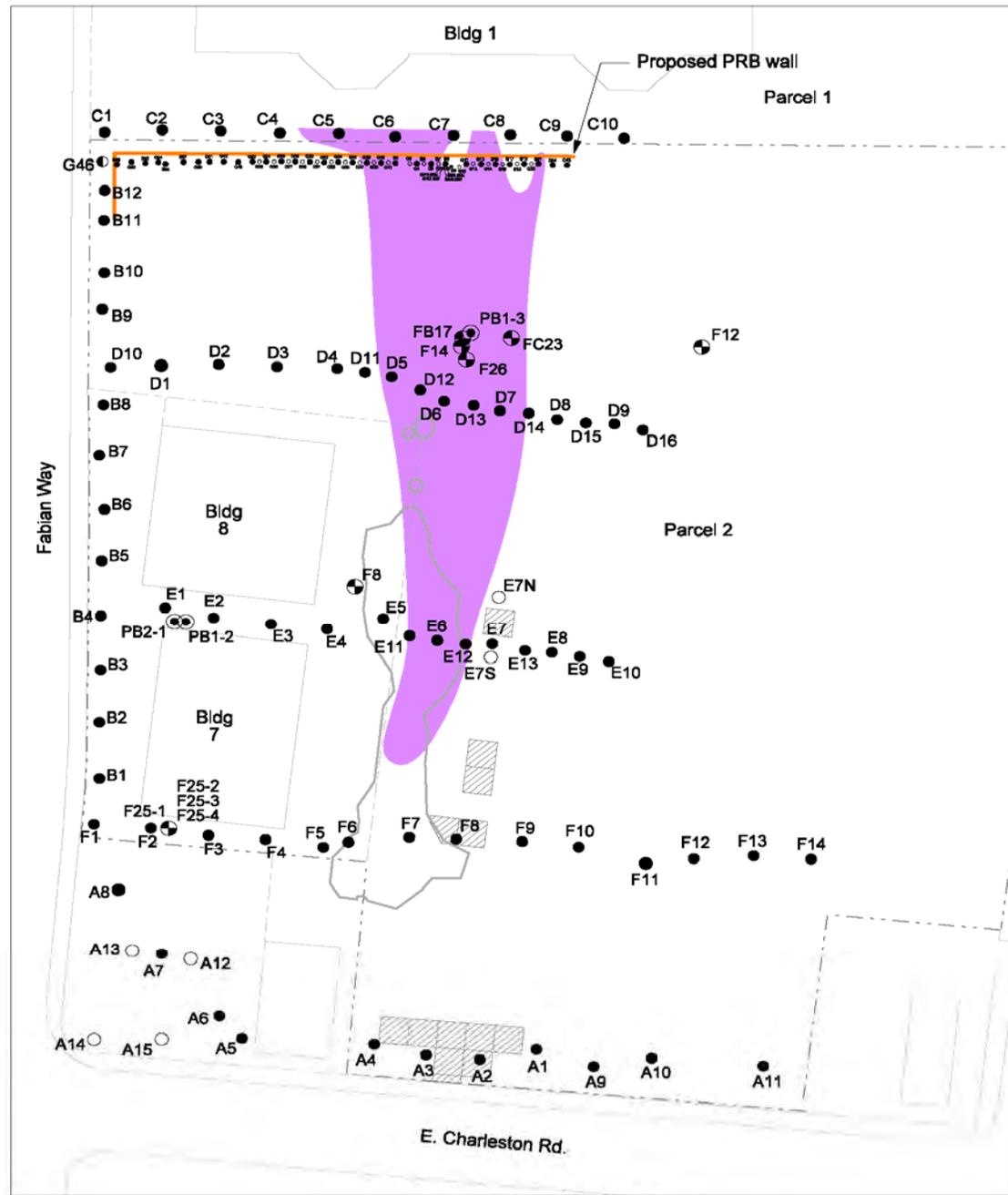
- Field preparation of nanoparticles is feasible
- Mobility is short-lived, perhaps because the stabilizer is consumed quickly in the subsurface
- Complete dechlorination of CVOCs occurred at a rapid rate
- More information is needed to scale-up nZVI applications to full scale

PART 4: Installation of a Multiple Funnel&Gate PRB

The design was based on a very high resolution transect of lithology and gw chemistry

PCE > 100 ppb

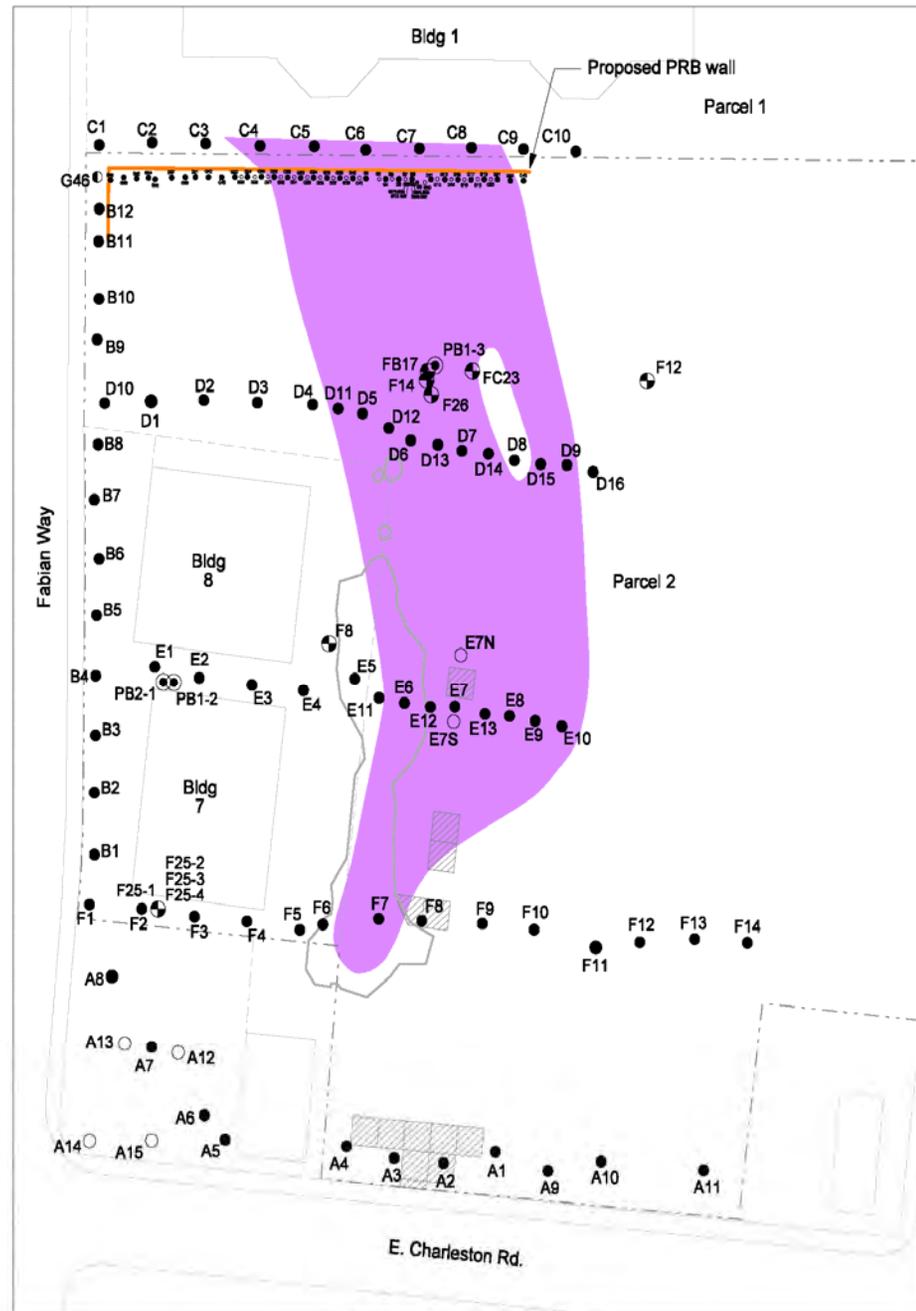
8 to 15 feet bgs



8-15 Feet Below Ground Surface

PCE > 100 ppb

15 to 40 feet bgs

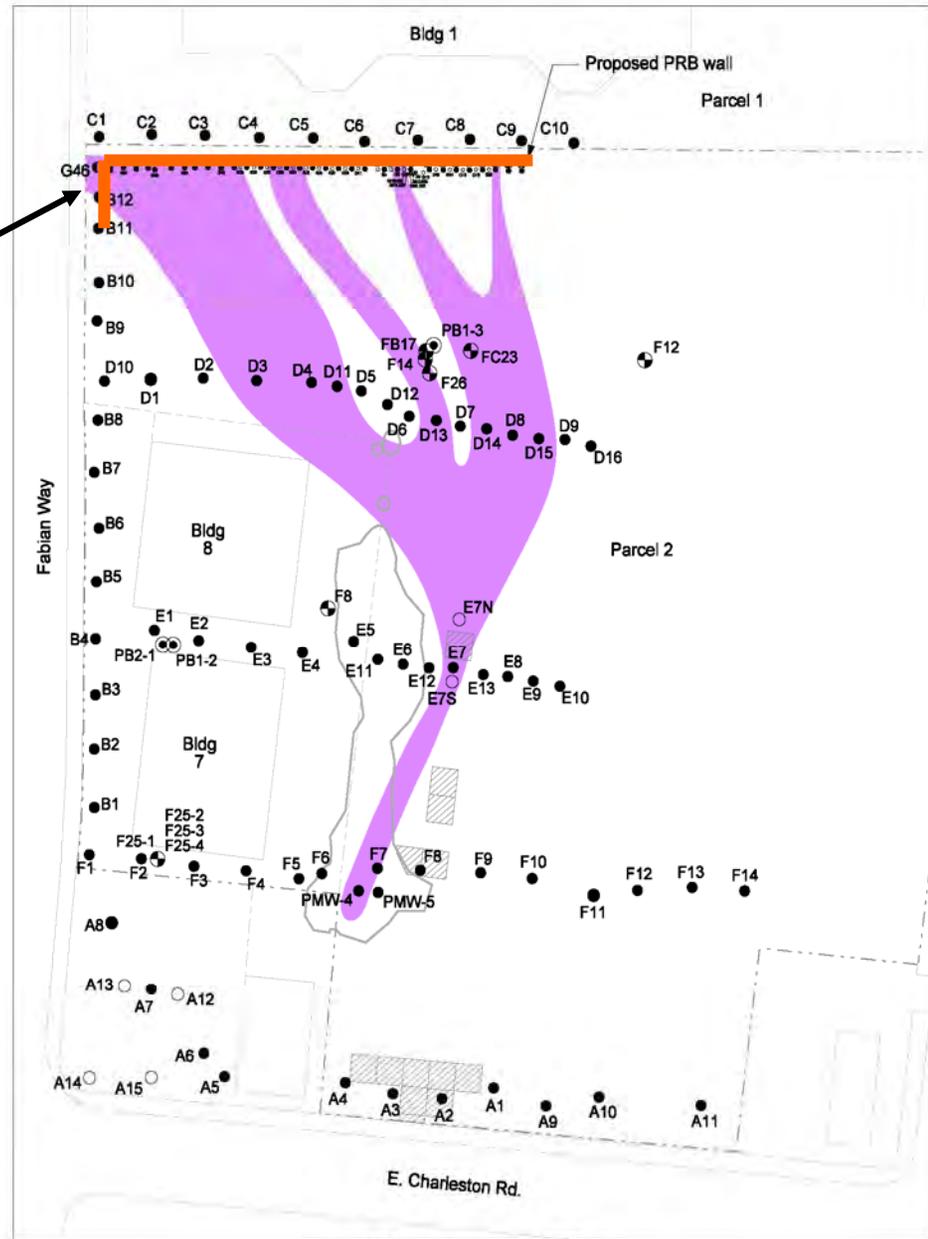


15-40 Feet Below Ground Surface

PRB

PCE > 100 ppb

40 to 55 feet bgs



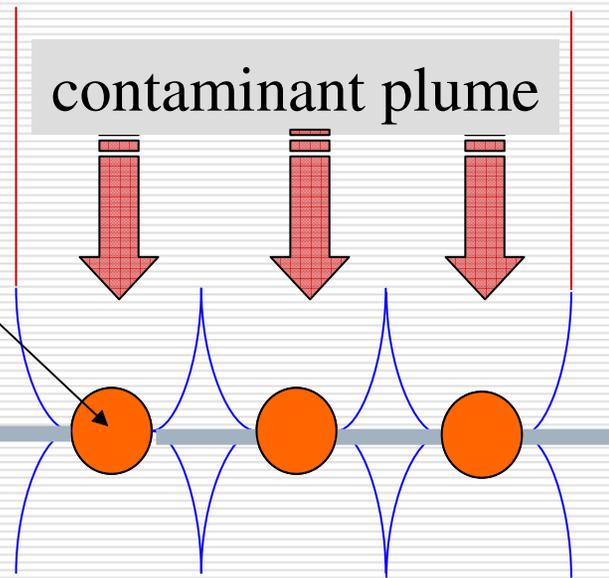
40-55 Feet Below Ground Surface

Design Challenges

- 4 to 5 separate water-bearing zones
- Maintain hydraulic vertical separation of different water-bearing zones
- Treatment area up to 60 feet deep
- 370 feet in length

Multiple Funnel-and-Gate Design Concept

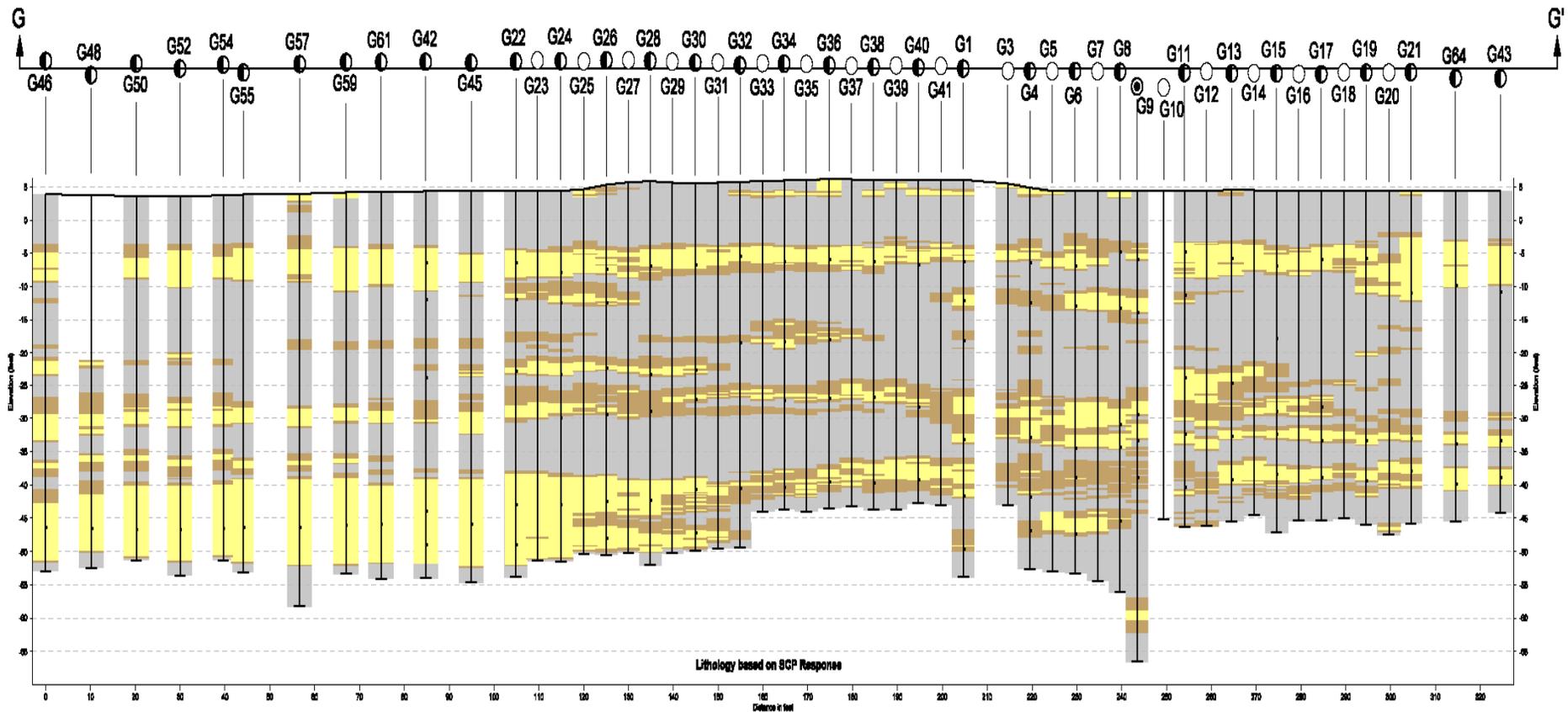
ZVI gates
3 ft diameter
multi-layered
caissons



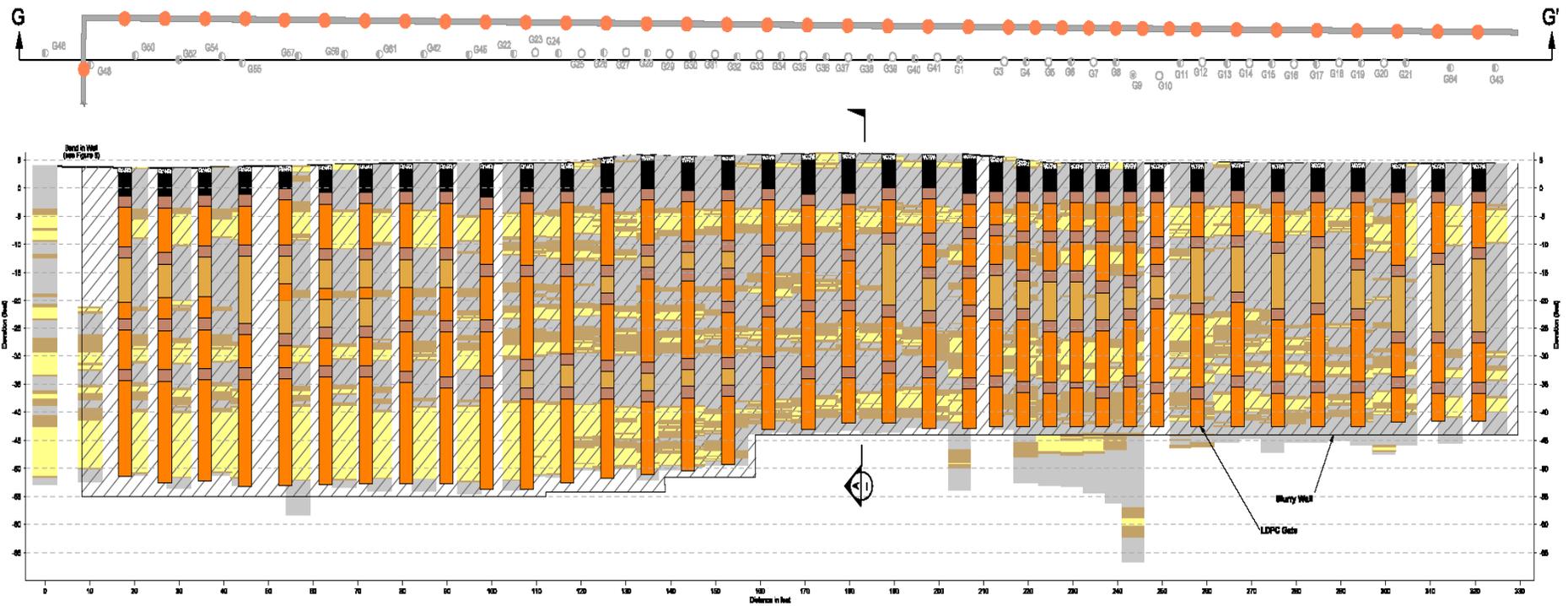
Caisson gates can be installed with multiple vertically-separated treatment zones Possible up to 100' deep.

Slurry wall funnels
370 ft long continuous
slurry wall

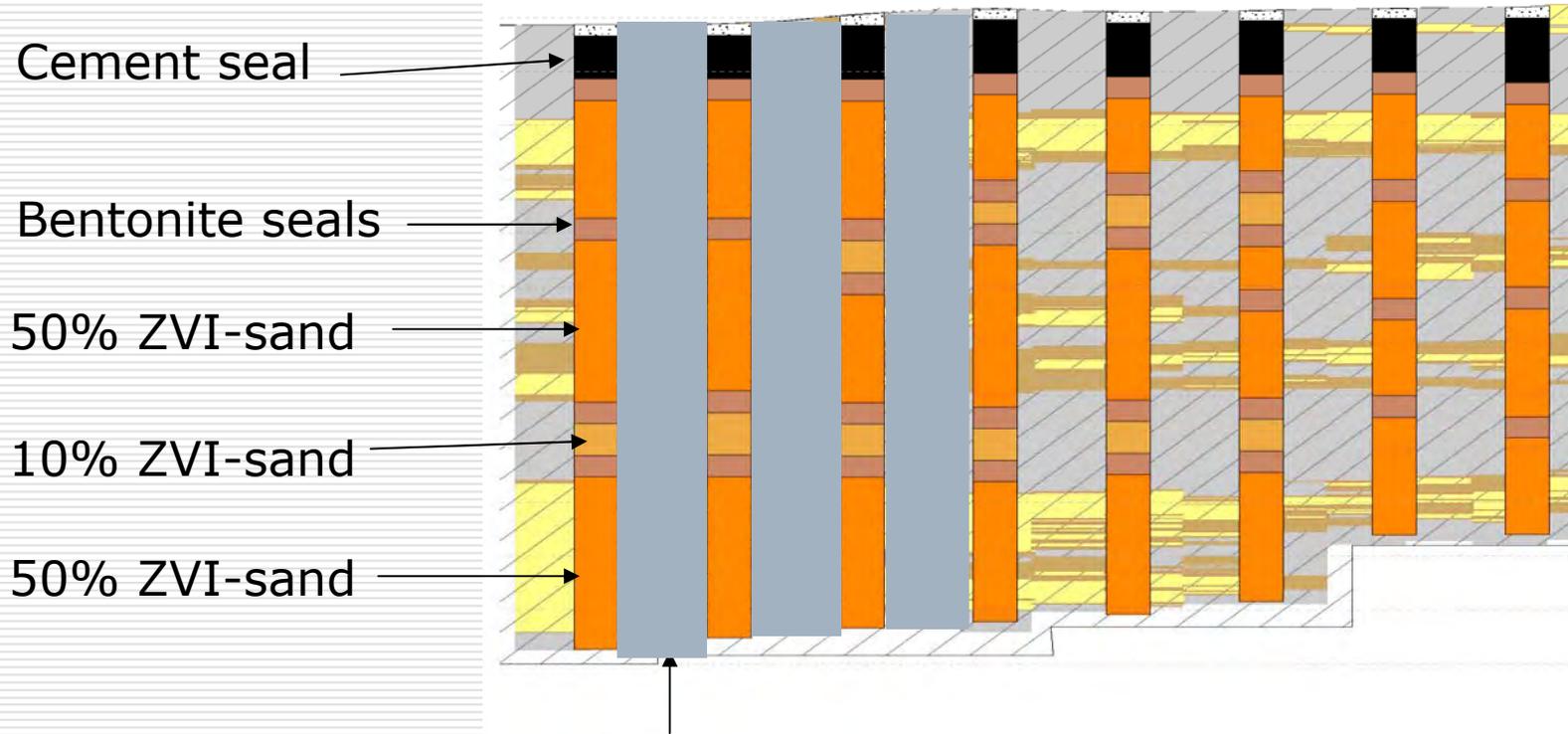
Cross-section Along PRB



PRB Design

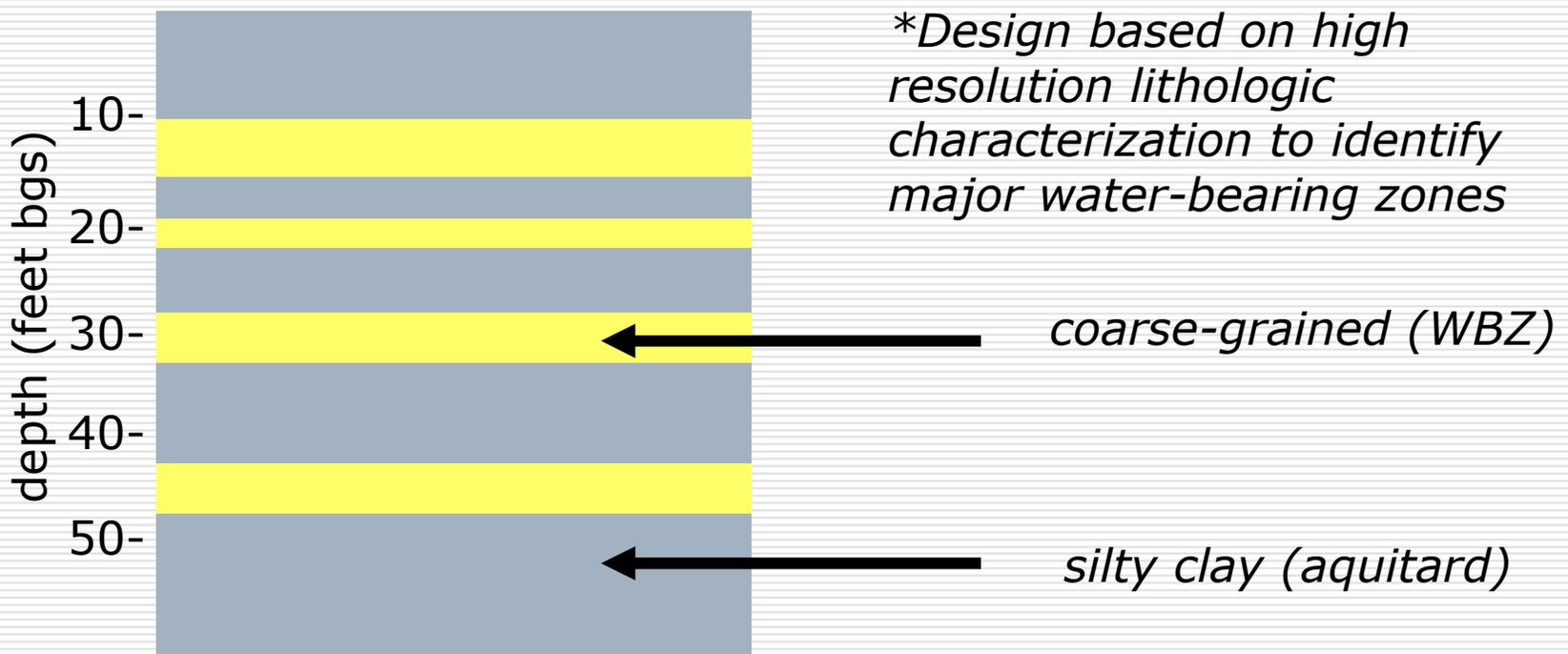


PRB Design

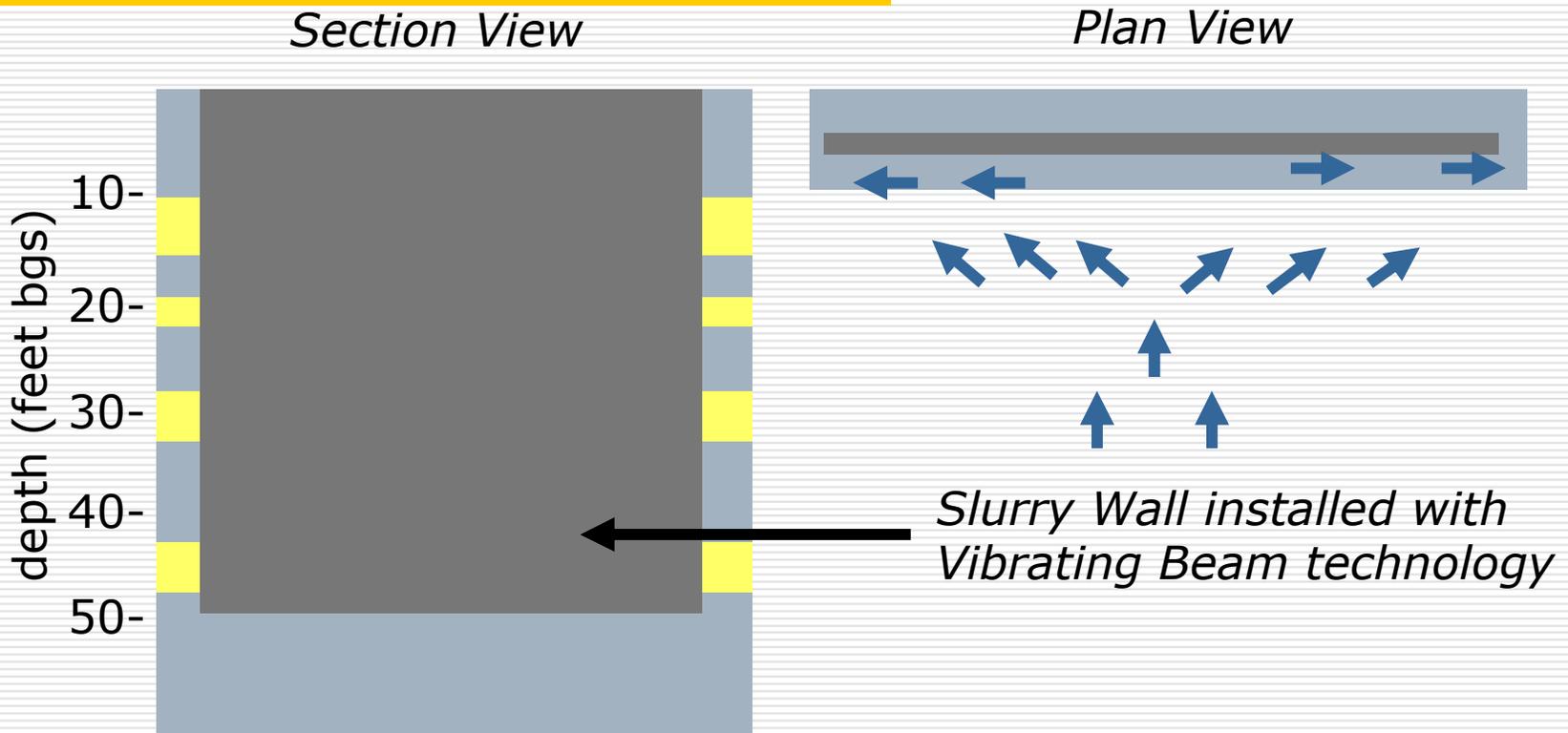


Slurry wall panels between borings

Construction Methods – Step I

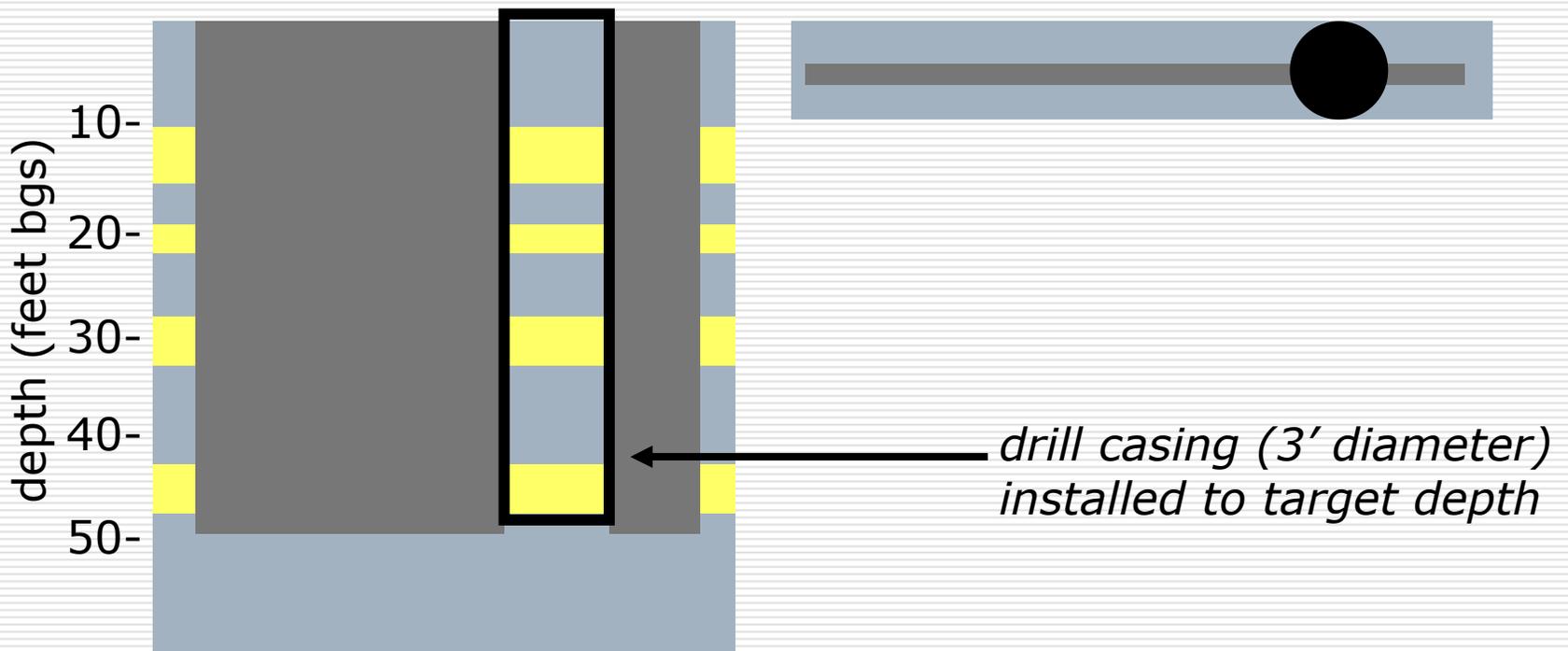


Construction Methods – Step 2



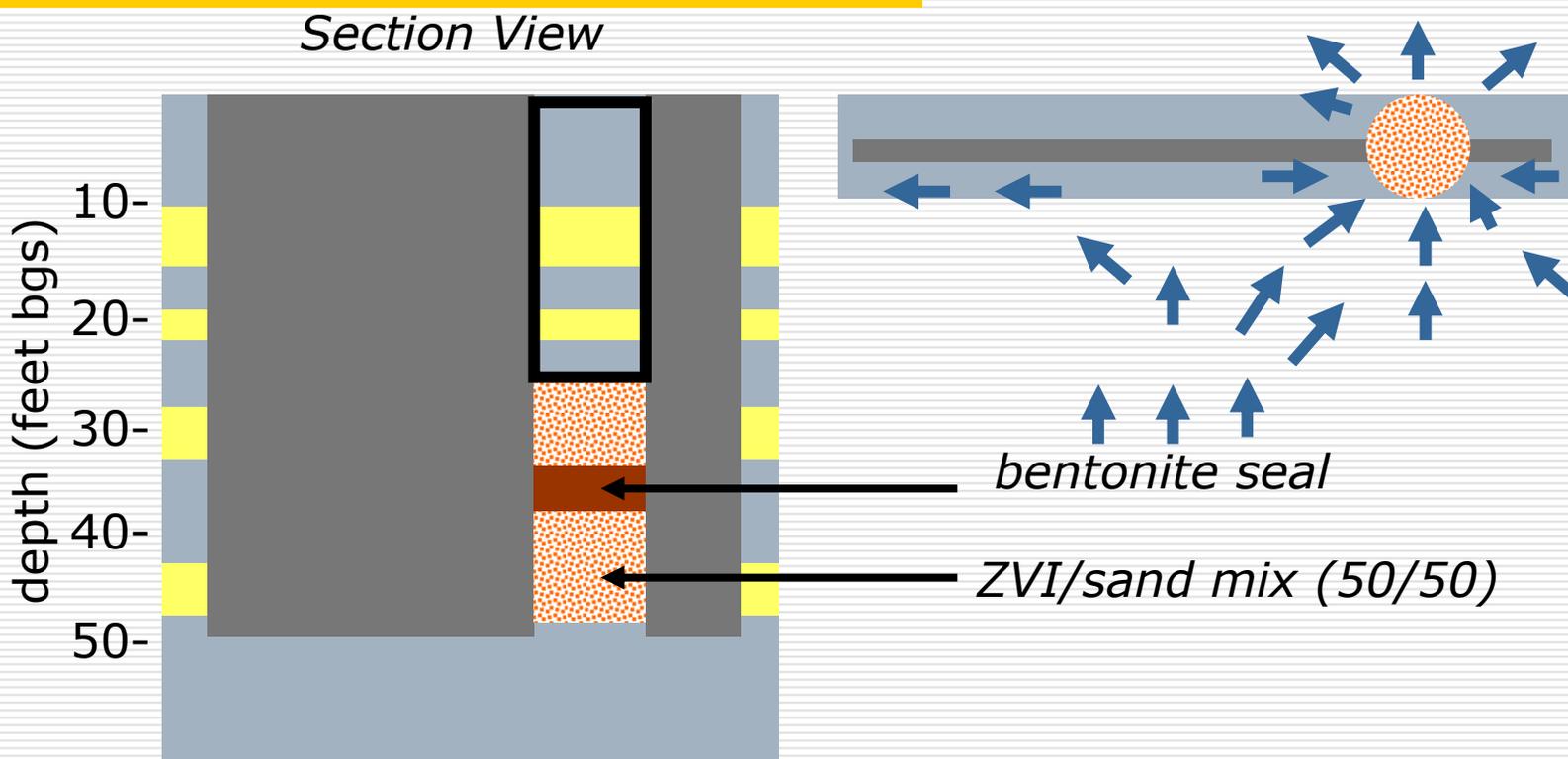
A thin slurry wall is installed across the PRB alignment to divert gw flow

Construction Methods – Step 3



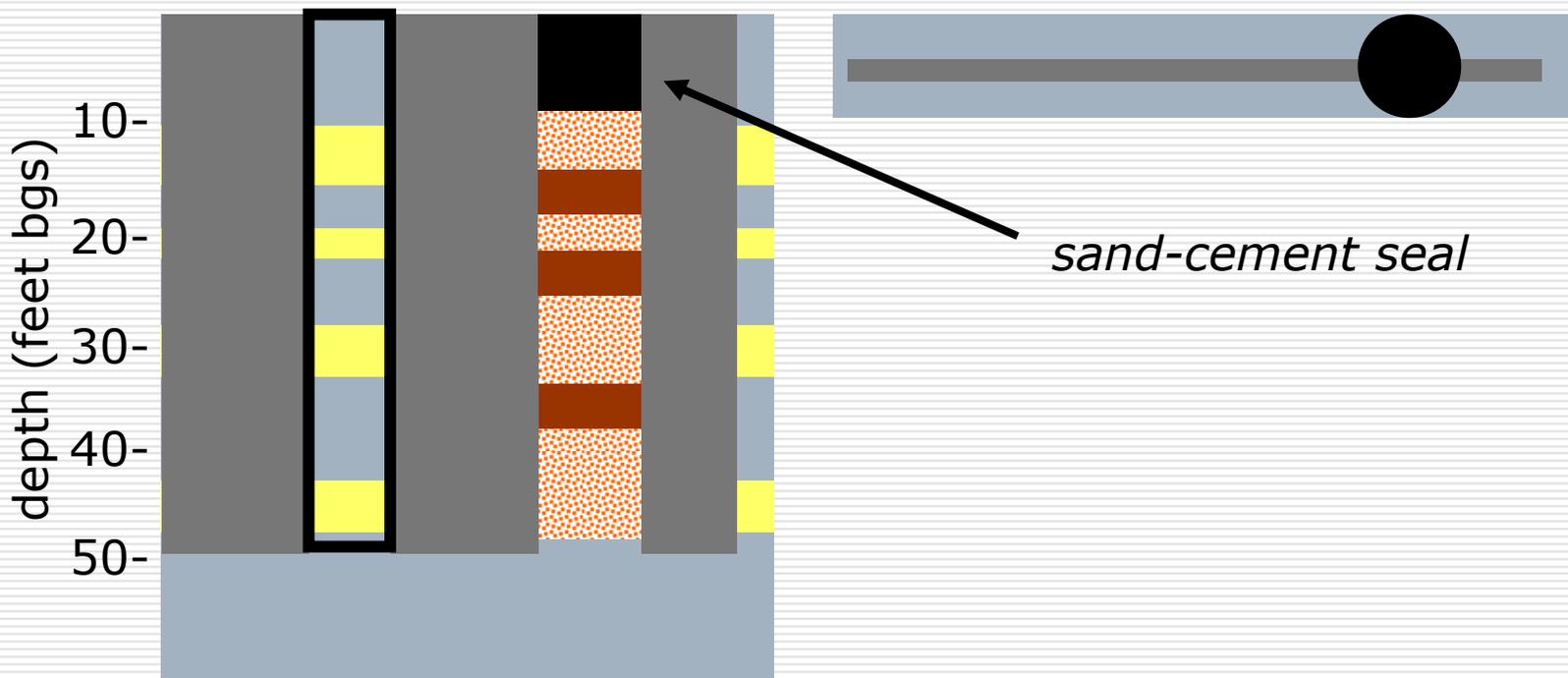
*A section of slurry wall is drilled out to allow for
emplacement of ZVI and bentonite layers*

Construction Methods – Step 4



Emplacement of ZVI and bentonite layers, flow through boring occurs

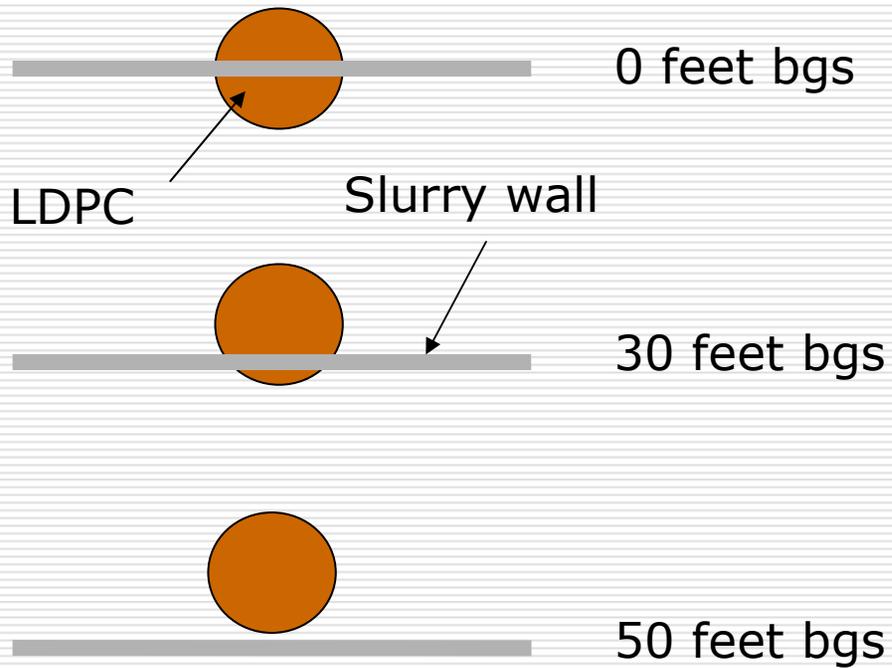
Construction Methods – Step 5



Drilling of adjacent boring

Possible Deviation Issues

Plan View



Section

































Construction Summary

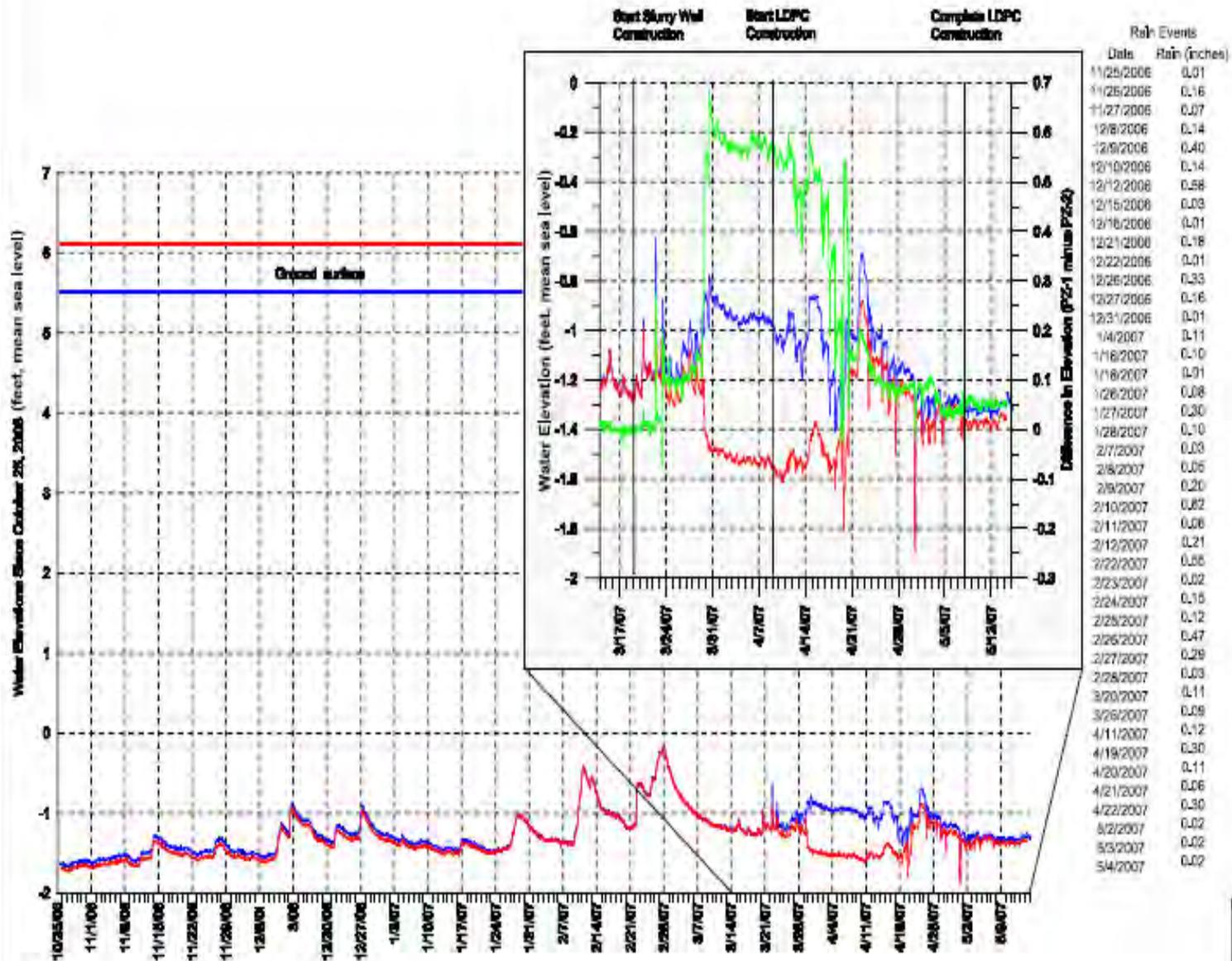
GENERAL	
Construction period	56 days
VIBRATING BEAM BARRIER WALL	
Total length	371 feet
Maximum depth	60 feet
Minimum depth	48.5 feet
Total square feet of wall	20,480 square feet
Slurry produced	13,699 cubic feet
Excess slurry disposed off-site	6,460 cubic feet
Average thickness of slurry wall ³	5.8 inches

Construction Summary

LARGE DIAMETER PERMEABLE COLUMNS	
Diameter of LDPCs	36 inches
Number of LDPCs	39
Number of Treatment Gates	172
Total volume of ZVI/sand Used	385 cubic yards
Total Volume of Bentonite Used	100 cubic yards

Performance Summary

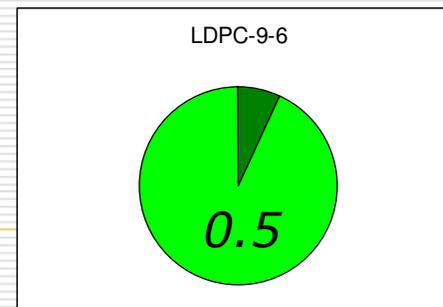
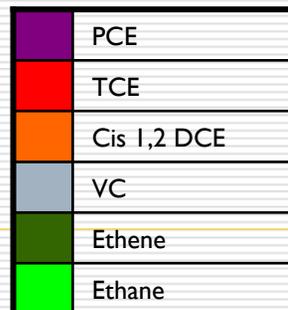
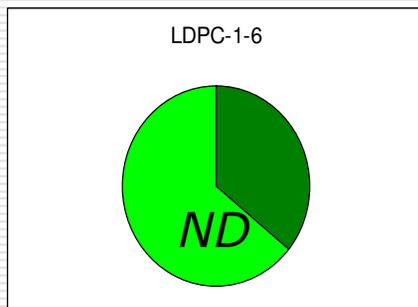
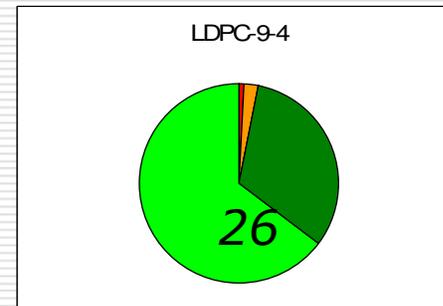
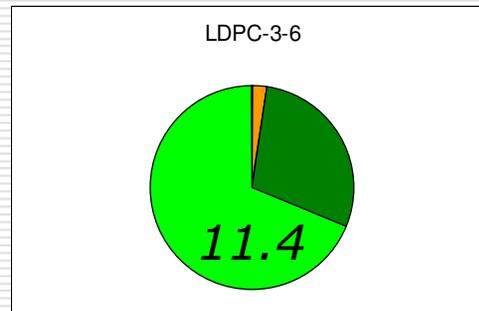
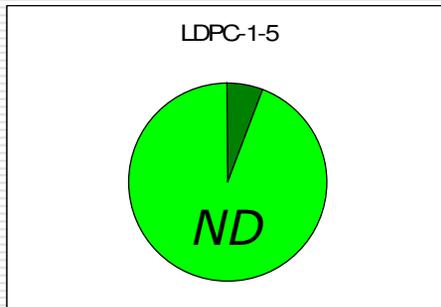
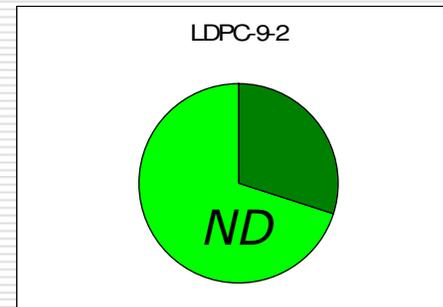
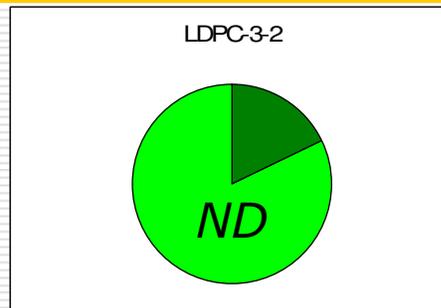
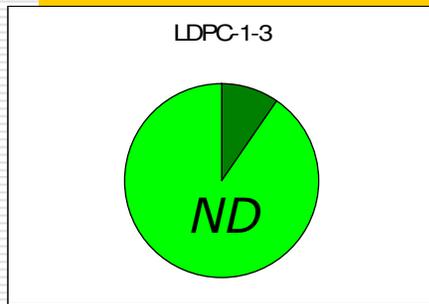
- Piezometers installed prior to construction upgradient and downgradient of PRB
- Water level response
 - ▶ After slurry wall
 - ▶ After LDPC installation
- Groundwater chemistry



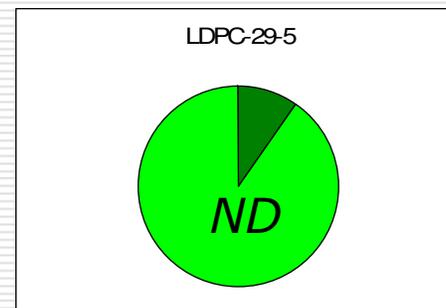
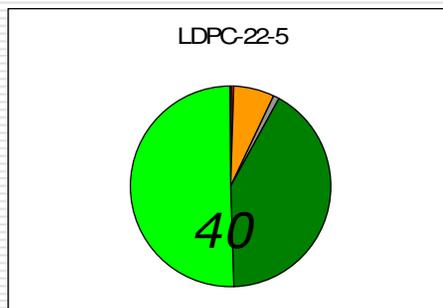
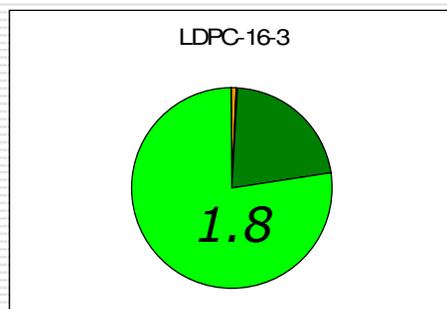
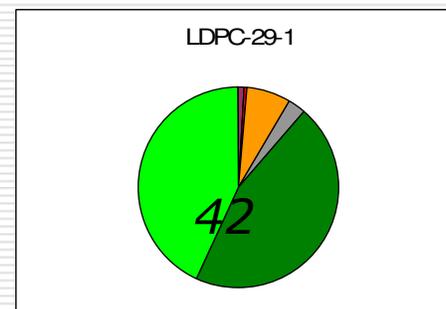
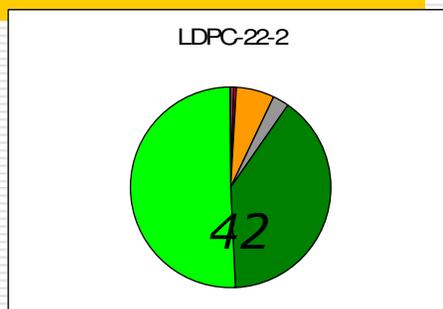
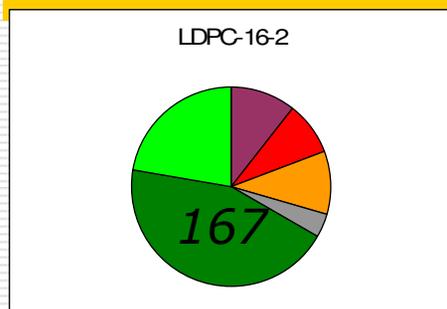
- Explanation**
- PZ-1 water level (upgradient of the slurry wall)
 - PZ-2 water level (downgradient of the slurry wall)
 - Difference in water level elevations (inset only)

Note:
Groundwater elevation data for PZ-2 was adjusted to account for disturbance of the well casing during construction activities.

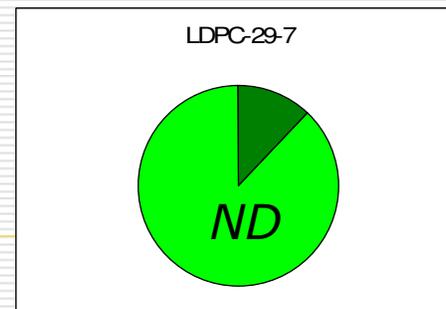
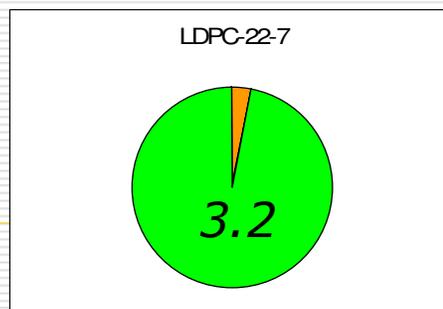
First Round Monitoring Results (numerical values are total CVOCs)



First Round Monitoring Results



	PCE
	TCE
	Cis 1,2 DCE
	VC
	Ethene
	Ethane



Summary of VOC Removal

- Chlorinated VOCs low to non-detect in samples within PRB
- Calculated % Destruction is 99 to 100% in all but two sampling locations (80% and 89%)
- Data needs: Install upgradient and downgradient monitoring points

Acknowledgements

- R&D funding provided by client and Geomatrix
- Dr. Dongye Zhao and Feng He (Auburn University)
- OTHER GMX TEAM MEMBERS

Matthew Goerz, Michael Calhoun, Frank Szerdy, Andy Cox, Deepa Gandhi, Spencer Archer, Murray Einarson, Brian Aiken, Dave Pearson